# CO<sub>2</sub> SPARGING PROOF OF CONCEPT TEST REPORT

Revision 1

LCP CHEMICAL SITE, BRUNSWICK, GA

Prepared for Honeywell

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April 1, 2013

#### **EXECUTIVE SUMMARY**

The Proof of Concept test was designed to evaluate the feasibility of CO<sub>2</sub> sparging to remediate a sub-surface caustic brine pool (CBP) formed by historical production of industrial chemicals at the LCP Chemicals Site (Brunswick, GA). The test was conducted in accordance with the "Final Work Plan for CO<sub>2</sub> Sparging Proof of Concept Test, LCP Chemical Site, Brunswick, GA" (Mutch Associates, 2012) dated September 11, 2012, and approved by EPA on September 10, 2012. This CBP has been defined as groundwater with a pH above 10.5. In the area around the Proof of Concept test, the CBP is situated at the 30 to 50 ft interval below land surface (bls) and is underlain by a variably cemented sandstone aquitard.

The specific objectives of the Proof of Concept test as set forth in the EPA-approved work plan included:

- Determine the radius of influence (ROI) of a representative CO<sub>2</sub> sparging well as defined by pH reduction to target levels
- Determine the kinetics of the pH neutralization reaction
- Determine the efficiency of the CO<sub>2</sub> sparging as defined by the amount of pH reduction achieved per mass of CO<sub>2</sub> injected
- Assess whether significant reductions in aquifer hydraulic conductivity occurred within the ROI as a result of the CO<sub>2</sub> sparging
- Assess whether there is significant reduction in the specific capacity of the sparge well, which served as the aquifer testing groundwater extraction well before and after the CO<sub>2</sub> sparging test
- Determine the impact of the CO<sub>2</sub> sparging on the geochemistry of the aquifer within the ROI and in particular on the concentrations of mercury and other metals
- Determine the vertical magnitude, radial extent, rate of propagation, and life-cycle of any groundwater mounding caused by the CO<sub>2</sub> sparging and the extent of groundwater level collapse following cessation of sparging
- Determine practical CO<sub>2</sub> injection rates and ways in which sparging efficiency can be enhanced
- Monitor over time potential rebound in pH, metals, or other geochemical parameters

All of these objectives were met except for completion of the long-term post-sparge rebound monitoring which is scheduled for February and May of 2013. The most important result of this test was that CO<sub>2</sub> sparging was effective in lowering the pH of the CBP at significant distances away from the sparge well. The lower pH results in significantly reduced mobility for the metals, particularly mercury.

#### **Well Network and Test Protocol**

Prior to the test, one sparge well (SW-1), and seven new monitoring wells were installed at various radial distances and depths. The screened interval of SW-1 was located at 40 to 45 ft bls. New monitoring wells were installed and screened at three intervals denoted shallow, intermediate, and deep.

A total of 14 monitoring wells were used during the test. These wells were located within 100 ft of the sparge well (Figure 1). To avoid artesian flow from the monitoring wells during sparging, all wells within the monitoring network were fitted with a PVC compression fitting and extended approximately 6

ft with 2 in diameter PVC pipe, such that all wells extended roughly 8-10 ft above ground surface. The wells were also sealed from the atmosphere to prevent  $CO_2$  gas channels from intercepting the well screen and preferentially flowing up through the well. The target flow rate for the test was 20 standard cubic feet per minute (scfm). An upper limit on pressure was set at 25 psig to avoid pneumatic fracturing of the formation.

Pre- and post-sparging aquifer tests were conducted using SW-1 as the pumping well to discern if sparging caused any changes in aquifer properties. Data collection included monitoring of groundwater levels, barometric pressure, the stage of the waterway adjacent to causeway near the junction of Purvis Creek and the Unnamed Ditch, pre-sparge aquifer test pumping, and post-sparge aquifer test pumping.

A round of groundwater samples was taken from the monitoring well network before and after the test. Analysis of pH, specific conductivity (SC), dissolved oxygen (DO), temperature, and oxidation-reduction potential (ORP) was performed in the field as part of normal well purge protocols. In addition, specific gravity was measured using a field hydrometer. Test America (Savannah, GA) was used for analysis of lab pH, dissolved inorganic carbon, alkalinity, total organic carbon, total dissolved solids, dissolved silica, ferrous iron, dissolved sulfide, chloride, mercury, and TAL metals (which includes chromium, arsenic, calcium, magnesium, sodium, etc.). SF<sub>6</sub> in groundwater collected post-sparging was analyzed by CH2M Hill's Applied Sciences Laboratory.

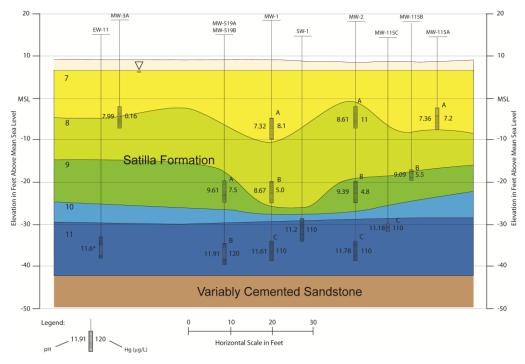
#### **Sparging Activity**

Sparging began on Monday October 29, 2012. Flow rates of 20 to 60 scfm were easily achievable at pressures ranging from 22.0 and 25.0 psig. During the first week, sparging into SW-1 took place on five consecutive days for approximately 8.0 hrs/day. The weekend (November 3<sup>rd</sup> and 4<sup>th</sup>) was used as a rest period to observe potential pH rebound. In week 2, sparging into SW-1 took place on five consecutive days at approximately 8.7 hrs/day. Sparging occurred at slightly higher flow rates to assess effect on pH reductions in the deep Satilla wells. Once again, the weekend (November 10<sup>th</sup> and 11<sup>th</sup>) was used as a rest period to observe potential pH rebound.

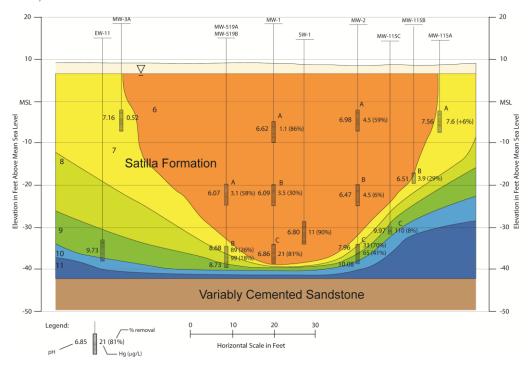
Prior to the 11th day of sparging, a decision was made (in consultation with and verbal approval by EPA) to change the sparging point from SW-1 to MW-1C. MW-1C is screened 5 feet deeper than SW-1 and is at the same interval as MW-2C and MW-519B. The reason for this change was to try to lower the pH to between 7 and 8 in the deep Satilla monitoring wells to evaluate the effect of pH and the overall geochemistry of the aquifer. With this change, flow rates of 50 to 60 scfm were achievable at pressures up to 25 psig. Sparging took place on six consecutive days into MW-1C for approximately 9 hrs/day.

#### Changes in pH

Values from the baseline continuous pH monitoring are shown in profile in Figure 1. Deep Satilla wells had pH values ranging from 11.2 to 11.9. These values are consistent with historical pH values of deep Satilla wells at the site. Shallow and intermediate Satilla well pH values were alkaline (pH > 7), but did not have as high pH as the deep Satilla wells.



**Figure 1:** Cross section of pre-sparge pH and mercury concentrations in the area near the Proof of Concept Test. Contours represent pH values. Values shown for pH were recorded in the field, just prior to the start of sparging (October 29, 2012 at 8:45 AM). Mercury values are laboratory measurements from samples collected from October 2 to October 3, 2012.



**Figure 2:** Cross section of post-sparge pH and mercury concentrations in the area near the Proof of Concept Test. Contours represent pH values. Values shown for pH were recorded in the field, one week after the conclusion of sparging (November 28, 2012). Mercury values are laboratory measurements from samples collected from November 27 to November 28, 2012. Note: MW-2C Hg value is the average of field sample and field duplicate.

The day-to-day pH responses of individual wells during the sparging period showed large variations and are discussed in detail in this report. The overall change in pH after 2 weeks of sparging into SW-1 is of note. The lowest pH values recorded were in SW-1 itself (6.60). However, with the exception of SW-1, pH levels in the deep Satilla wells did not decrease to a large extent from pre-sparge levels. The monitoring well that showed the largest decrease in pH after two weeks was MW-2C, which showed a decrease from 11.78 to 9.19 at the top of screen. The pH at the top of the MW-2C well screen was more than 1 pH unit lower than at the bottom of the screen.

The influence on the deep Satilla wells was much more pronounced after sparging was switched from SW-1 to MW-1C (Figure 2). MW-1C, MW-519B and MW-2C all experienced pH decreases of greater than 3 units from pre-sparge levels. MW-519B and MW-2C had post-sparge pH values of 7.96 and 8.68 in water pumped from the top of the well screen. These wells are 15.1 and 19.9 ft from MW-1C, respectively. Decreases in pH in MW-115C and EW-11 were more modest, with post-sparge pH values between 9 and 10. These wells were 24.6 ft and 44.1 ft away from MW-1C. Based upon this information, the effective radius of influence for sparging within the deep Satilla was conservatively estimated at 20 ft.

The sparging efficiency was calculated by dividing the theoretical CO<sub>2</sub> demand of CBP water by the total amount of CO<sub>2</sub> used for sparging. A numerical titration was performed to calculate the theoretical CO<sub>2</sub> demand of CBP. The efficiency considering the total amount of CO<sub>2</sub> injected into both SW-1 and MW-1C was 4.1%. Since the majority of the demand is present in the deep Satilla, an alternative way of calculating the sparging efficiency is to consider only the amount of CO<sub>2</sub> injected into MW-1C. The sparging efficiency in this case is calculated to be 9.7%. This alternative calculation assumes that the demand of the intermediate and shallow portions of the aquifer would have already been met prior to the 54.5 hr sparging duration into MW-1C. This is a reasonable assumption given the rapid decreases in pH observed in the intermediate and shallow monitoring wells after the start of sparging. Note that the calculated efficiency of 9.7% is very similar to the 10% efficiency assumed as part of the CO<sub>2</sub> demand calculations in the EPA-approved Proof of Concept work plan.

# Mercury and other Geochemical Changes

Pre-sparge soluble mercury concentrations in the deep Satilla in the area near SW-1 were consistently between 110 and 120  $\mu$ g/L (Figure 1). After the three week sparging program, there was a considerable decrease in mercury concentrations in the deep Satilla wells that had post-sparge pH values near 7.0 (Figure 2). For example, SW-1 (11  $\mu$ g/L) and MW-1C (20  $\mu$ g/L) showed a reduction of 81% and 90% percent respectively. The next largest reduction among the deep Satilla wells was MW-2C, which showed a 70% reduction in mercury concentrations in water sampled from the top of the well screen. Wells in the intermediate Satilla showed more modest percent reductions.

Changes in TDS, specific gravity, dissolved arsenic (As), chromium (Cr), silicon (Si) and vanadium (V) were quantified by the pre- and post-sparge monitoring data. TDS did not change appreciably from pre-to post-sparging, which is consistent with the expectation for TDS. Dissolved concentrations of As, Cr, Si and V all decreased significantly and to varying extents in deep Satilla wells after sparging.

# **Aquifer Test Results**

The principal objective of the pre-sparging and post-sparging aquifer testing was to determine the extent to which the  $CO_2$  sparging and the associated lowering of pH may have reduced aquifer transmissivity through solids precipitation, particularly precipitation of silica gel. Aquifer testing was used to assess this possible occurrence since aquifer testing measures the transmissivity and hydraulic conductivity of the entire zone of influence of the  $CO_2$  sparging test and, ultimately as the test continues, around the periphery of the test zone. The pre-sparging aquifer testing demonstrated that the basal portion of the aquifer, specifically the lower 20 feet of the aquifer (which roughly corresponds with the high pH, high density CBP waters), had a pre-sparging transmissivity of 1,325 gpd/ft and a mean early-time storativity of  $1.4 \times 10^{-3}$ . After the  $CO_2$  sparging, the transmissivity of the basal portion of the aquifer declined by 66% to 450 gpd/ft. This corresponds to a reduction in hydraulic conductivity from 8.9 ft/day to 2.4 ft/day.

The decline in transmissivity and hydraulic conductivity is believed to be principally the result of residual saturation of CO<sub>2</sub> in aquifer and not the result of silica solid precipitation. The residual saturation was estimated to range from 0.1 to 0.5 (10% to 50% of the pore space). The presence of a substantial residual saturation of CO<sub>2</sub> gas in the aquifer also increased the storativity of the aquifer due to the drawdown-induced expansion of the CO<sub>2</sub> gas.

During sparging, significant mounding of the potentiometric surface was measured, particularly in the deep wells. Less mounding was observed in the intermediate zone and even less in the shallow zone. Nonetheless, during the course of the sparging test, the groundwater table did rise to within a foot of the surface within a 20-foot radius of the sparge wells (SW-1 and MW-1C). Also, the piezometric surface in the deep zone rose as much as 6.5 feet at MW-517B, which is over 100 ft from the sparge well. Mounding and the anticipated superposition of mounding from adjacent sparge wells will be an important factor in design of full-scale implementation. Seasonal or other fluctuations in the level of the groundwater table will also be factors in full-scale implementation.

#### **Conclusions**

The results of this test show at the proof of concept level that pH levels can be reduced significantly in the deep Satilla by sparging with CO<sub>2</sub>. Furthermore, all of the specific objectives stated in the Proof of Concept test workplan were met, with the exception of long-term, post-sparging rebound monitoring which will occur in February and May of 2013. The following conclusions can be drawn from the test:

- 1. CO<sub>2</sub> sparging into the Satilla Formation is feasible without the need for fracturing.
- 2. Significant pH reductions from pH 11-12 in the deep Satilla were achievable in 5 to 7 days sparging at circa 50 scfm.
- 3. Hg levels in the high pH CBP fully-impacted by the sparging declined from 110-120  $\mu$ g/L to 11-33  $\mu$ g/L (70 to 90% reductions)
- 4. Limited evidence of silica precipitation was observed in wells within the zone of influence of the sparge test.
- 5. The pH of deep Satilla wells was not lowered to below 6.5 at any point during sparging, which indicates that potential dissolution of the sandstone aquitard is not a risk that would bar use of the CO<sub>2</sub> approach.

- 6. A radius of influence of at least 20 feet was achieved at the top of the CBP and greater than 60 feet at the water table surface.
- 7. Some CO<sub>2</sub> gas channels extended out more than 100 feet from the sparge wells.
- 8. The CO<sub>2</sub> sparging resulted in a significant residual saturation of CO<sub>2</sub> gas in the zone of influence
- 9. During sparging, significant mounding of the potentiometric surface was measured, particularly in the deep wells.

The Proof of Concept test indicated that CO<sub>2</sub> sparging would be an effective, innovative technology, suitable for full-scale implementation at the site. Observations made during testing further indicate that full-scale implementation of CO<sub>2</sub> sparging be conducted over a multiple-year, sequential effort. The principal drivers for this sequential implementation are:

- Management of groundwater mounding caused by superposition of multiple, closely-spaced sparge wells; and
- Maximization of sparging efficiency to reduce emissions of CO<sub>2</sub>.

Groundwater mounding during full scale implementation is particularly critical as mounding during the Proof of Concept test was substantial. The groundwater table rose to within 1 foot of the ground surface during the testing. This mounding will be exacerbated by superposition of mounding from multiple nearby sparging wells and by seasonal rises of the groundwater table. Moreover, in some areas of the CBP, the water table is even closer to the surface than in the test site. Conducting the implementation over multiple years will allow active sparge wells to be further apart, thereby reducing the superposition of groundwater mounding. The optimal time for sparging is when the groundwater table is at its lowest during the drier summer and early fall months.

The Proof of Concept test results suggest that CO<sub>2</sub> sparge efficiency can be enhanced by a sparge regimen that emphasizes short bursts of sparging (anywhere from ½ to 4 hrs.) followed by relatively lengthy rest periods. The rest periods would allow CO<sub>2</sub> gas residual saturation remaining in the formation to both dissolve and diffuse into the surrounding CBP waters. It is proposed that in the first year of sparging, different sparge regimens be tested in an effort to optimize sparge efficiency. In subsequent years, the optimized sparge regimen would be adopted.

Taking these factors into consideration, it is believed that full scale implementation could be accomplished over approximately three years, with four to five months of sparging during the late summer and early fall followed by a seven- to eight-month period of relaxation of sparging. During the relaxation period, data collected from the site would be analyzed using a three-dimensional visualization program. These analyses would permit planning of the next year of the sparge program.

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#### LIST OF ACRONYMS

Alk Alkalinity

bls Below land surface
btoc Below top of casing
CBP Caustic brine pool
CO<sub>2</sub> Carbon dioxide

CO<sub>2</sub>(aq) Aqueous carbon dioxide CO<sub>2</sub>(g) Gaseous carbon dioxide

CO<sub>3</sub><sup>2</sup>- Carbonate ion

DIC Dissolved inorganic carbon

DO Dissolved oxygen

DOC Dissolved organic carbon
DOM Dissolved organic matter

En Redox potential relative to the Standard Hydrogen Electrode
ESTCP Environmental Security Technology Certification Program

GEPD Georgia Environmental Protection Division

H<sub>2</sub>CO<sub>3</sub>(aq) Carbonic acid

H<sub>2</sub>CO<sub>3</sub>\* Sum of carbonic acid and aqueous carbon dioxide

HCO<sub>3</sub>- Bicarbonate ion H<sub>2</sub>SO<sub>4</sub> Sulfuric acid Hg Mercury

K Equilibrium constant
Kh Hydraulic conductivity
K<sub>sp</sub> Solubility product constant
LCP Linden Chemicals and Plastics
NTU Nepholometric Turbidity Unit
ORP Oxidation Reduction Potential

psi Pounds per square inch

psig Pounds per square inch – gauge

PVC Poly vinyl chloride

RAO Remedial Action Operation
RI Remedial Investigation
ROI Radius of influence

scfm Standard cubic feet per minute

SC Specific conductivity
SF6 Sulfur hexafluoride
TDS Total dissolved solids
TSS Total suspended solids

# 1. INTRODUCTION

Mutch Associates, LLC, in collaboration with Parsons Corporation (Parsons), have prepared this report of the CO<sub>2</sub> sparging Proof of Concept test conducted at the LCP Chemical Site in Brunswick, Georgia. The Proof of Concept test was conducted in accordance with the "Final Work Plan for CO<sub>2</sub> Sparging Proof of Concept Test, LCP Chemical Site, Brunswick, GA" (Mutch Associates, 2012) dated September 11, 2012. Formal approval of the workplan was granted in a letter from EPA on September 10, 2012. The Proof of Concept test was designed to evaluate the feasibility of CO<sub>2</sub> sparging to remediate a sub-surface caustic brine pool (CBP) formed by historical production of industrial chemicals on the site.

The CBP is being addressed under an Administrative Settlement Agreement and Order of Consent (AOC) issued by the U.S. Environmental Protection Agency (EPA) Region 4 on April 18, 2007. The remedial action objectives (RAO) were defined in the AOC and included reducing the pH of the CBP to between 10 and 10.5 and reducing the density of the CBP. The Proof of Concept test work plan was also designed to evaluate the ability of CO<sub>2</sub> sparging to reduce trace metals, particularly mercury, within the CBP. It also incorporated pre- and post-sparging aquifer testing to detect any change in aquifer properties due to precipitation of silica or other factors.

This report is organized in the following manner:

- Section 2 Describes the technical objectives of the Proof of Concept test;
- Section 3 Describes the specific protocols employed in the proof of concept test;
- Section 4 Presents the results of the Proof of Concept test; and,
- Section 5 Conclusions.

# 1.1. Site Description

The LCP Chemicals site is located at 4125 Ross Road, in the City of Brunswick, in Glynn County, Georgia. The site is bordered by the Turtle River marshes to the west and south and the urban populations of Brunswick to the north and east. The site encompasses approximately 813 acres, of which 684 acres are tidally influenced salt marsh.

Industrial operations were conducted by multiple parties from 1919 until 1994. The site was originally owned and operated by the Atlantic Refining Company (ARCO) who operated a petroleum refinery from 1919 until 1930 and a petroleum storage facility until approximately 1955. Portions of the site were also owned by Georgia Power Company and the Dixie O'Brien Paint Company. In 1955, the property was purchased by Allied Chemical, Inc. From 1956 to 1979, chlorine, hydrochloric acid, and sodium hydroxide were produced by Allied Chemical by the electrolysis of sodium chloride using mercury cells (the chlor-alkali chemical manufacturing process). In 1979, LCP Chemicals purchased the property and continued to operate the chlor-alkali process.

During chemical production activities at the site, a portion of the shallow aquifer was contaminated by residuals of chlor-alkali-manufacturing operations. A subsurface pool of caustic brine formed, characterized by elevated pH and total dissolved solids and elevated concentrations of dissolved metals. This CBP has been defined as groundwater with a pH above 10.5.

# 2. TECHNICAL OBJECTIVES

Specific objectives of the Proof of Concept test were listed in the EPA-approved workplan (Mutch Associates, 2012). These objectives included:

- Determine the radius of influence (ROI) of a representative CO<sub>2</sub> sparging well as defined by pH reduction to target levels
- Determine the kinetics of the pH neutralization reaction
- Determine the efficiency of the CO<sub>2</sub> sparging as defined by the amount of pH reduction achieved per mass of CO<sub>2</sub> injected
- Assess whether significant reductions in aquifer hydraulic conductivity occurred within the ROI as a result of the CO<sub>2</sub> sparging
- Assess whether there is significant reduction in the specific capacity of the sparge well, which served as the aquifer testing groundwater extraction well before and after the CO<sub>2</sub> sparging test
- Determine the impact of the CO<sub>2</sub> sparging on the geochemistry of the aquifer within the ROI and in particular on the concentrations of mercury and other metals
- Determine the vertical magnitude, radial extent, rate of propagation, and life-cycle of any groundwater mounding caused by the CO<sub>2</sub> sparging and the extent of groundwater level collapse following cessation of sparging
- Determine practical CO<sub>2</sub> injection rates and ways in which sparging efficiency can be enhanced
- Monitor over time potential rebound in pH, metals, or other geochemical parameters

All of these objectives were met, with the exception of the long-term, post-sparging rebound monitoring which will occur in February and May of 2013. The objectives and the findings from Proof of Concept test will be discussed in more detail in Section 4 of this report.

# 3. PROOF OF CONCEPT TESTING PROTOCOL

# 3.1. Sparge and Monitoring Well Network

The sparge and monitoring well network used to implement the Proof of Concept testing consisted of a combination of existing and newly installed wells, as shown on Table 3-1. The location of the sparge and monitoring wells relative to the test area is shown on Figure 3-1. Cross section A-A' of the well network is shown on Figure 3-2.

**Table 3-1: Monitoring Well Network** 

		Distance from	Distance from	Screened Interval	Newly Installed
	Monitoring Well	SW-1 (ft)	MW-1C (ft)	(ft)	(Y/N)
	MW-1A	7.3	9.8	12 - 17	Y
Shallow	MW-2A	13.1	21.3	12 - 17	Y
Sha	MW-3A	42.6	36.2	12 - 17	Y
01	MW-115A	30.7	36.6	12 - 17	N
ate	MW-1B	7.9	4.8	30 - 35	Y
edia	MW-2B	13.5	21.4	30 - 35	Y
Intermediate	MW-115B	25.7	33.1	27 - 30	N
I	MW-519A	20.8	15.4	30 - 35	N
	MW-115C	18.7	24.6	40 – 42	N
	MW-1C	8.4	0.0	45 - 50	Y
də	MW-2C	13.1	19.9	45 - 50	Y
Deep	MW-519B	20.6	15.1	42 - 48	N
	MW-517B	104.9	97.2	46 – 51	N
	EW-11	50.6	44.1	43 – 48	N

The new wells were installed during the week of September 17, 2012; boring logs / well construction diagrams are provided in Appendix A. Sonic core samples were collected to depth from wells SW-1, MW-1A, MW-1B, and MW-2C, and from the screened interval for the other wells. Based on the lithology, the total depth of sparge well SW-1 was determined to be 45 ft below land surface (bls), as the zone from 40-45 ft (screened interval) appeared to be more permeable than that from 45-50 ft.

Based on observations made prior to proof of concept testing, the following adaptations were made to the well network with approval from EPA:

- EW-11 was initially proposed in the workplan as a monitoring well, but based on the
  inability to access the screened interval with a Hach pH electrode, was replaced with
  MW-517.
- SW-1 was used as the sparge well for the first two weeks of testing. However, as further described in Section 4, and after consultation with EPA on November 12, 2012, MW-1C was used as the sparge well for the last week of testing in order to inject CO<sub>2</sub> lower into the formation.

# 3.2. Aquifer Testing

Pre- and post-sparging aquifer tests were conducted using SW-1 as the pumping well. This section describes the implementation of those aquifer tests from the initial test pumps through data collection. The data collection included antecedent monitoring of groundwater levels, barometric pressure, the stage of the waterway adjacent to causeway near the junction of Purvis Creek and the Unnamed Ditch, pre-sparge aquifer test pumping, and post-sparge aquifer test pumping.

# 3.2.1. Antecedent Monitoring of Groundwater Levels, Barometric Pressure and Tidal Efficiency for the Pre-Sparge Test

Prior to the aquifer test, antecedent groundwater level monitoring was conducted throughout the monitoring well network. Solinst Levelloggers were used in conjunction with periodic manual water levels. The level loggers were set to record at a frequency of 15s. Level loggers and manual water levels were deployed in the following wells: 1A, 1B, 1C, 2A, 2B, 2C, 115A, 115B, 115C, 519A, 519B, 3A, 517B, SW-1, Tidal Gage. A Solinst Barologger was set to record barometric pressure at a frequency of 15s and hung outside the well casing of well 1B.

Data collection began on October 3<sup>rd</sup>, 2012. The test ran October 6<sup>th</sup> -7<sup>th</sup> 2012 with a 24 hour recovery period lasting into October 8<sup>th</sup> 2012. The antecedent data showed negligible tidal and barometric efficiencies as demonstrated in the annotated hydrographs in Appendix B. The hydrographs also show a downward trend in water levels. The aquifer test drawdown data was adjusted to correct for the trend.

# 3.2.2. Pre-Sparge Pumping of Aquifer Test Well

The sparge well, SW-1, was equipped with a four inch-diameter 0.5HP Grundfos submersible pump. The pump was yield tested and set to a flow rate of 7.72 gallons per minute (gpm) on October 5<sup>th</sup> 2012. An inline GPI TM050 flow meter was used to dial in and maintain instantaneous flow rate of 7.72 gpm. The 24-hour aquifer test was initiated at 07:45 on October 6<sup>th</sup> 2012 at a constant in-line flow rate 7.72 gpm. The pump was shut down between 18:35-18:43 to safely refuel the generator powering the pump. The test was completed at 07:50 on October 7<sup>th</sup> 2012. The discharge water was pumped to a 17,500 gallon discharge tank approximately 400ft away. The discharge tank was cylindrical and had a spyglass to measure water level. The average flow rate for the aquifer test was calculated by tracking the change in water level in discharge tank as a function of time. The average flow for the pre-sparging aquifer test was 7.2 gpm.

# 3.2.3. Antecedent Monitoring of Groundwater Levels, Barometric Pressure and Tidal Efficiency for the Post-Sparging Test

Prior to the aquifer test, antecedent groundwater level monitoring was conducted throughout the monitoring well network. Solinst Levelloggers were used in conjunction with periodic manual water levels. The level loggers were set to record at a frequency of 15 seconds. Level loggers and manual water levels were deployed in the following wells: 1A, 1B, 1C, 2A, 2B, 2C, 115A, 115B, 115C, 519A, 519B, 3A, 517B. A Solinst Barologger was set to record barometric pressure at a frequency of 15 seconds and hung outside the well casing of MW-1B. There was no tidal gage deployed in the post-sparging test since the pre-sparging test established the absence of tide-induced groundwater level fluctuations.

Data collection began on November 28<sup>th</sup>, 2012. The test ran November 30<sup>th</sup> –December 1<sup>st</sup>, 2012 with a 24 hour recovery period lasting into December 2<sup>nd</sup>, 2012. The antecedent data showed negligible

barometric efficiency as demonstrated in the annotated hydrographs in Appendix B. The hydrographs also show a downward trend in water levels. The aquifer test drawdown data was adjusted to correct for the trend.

# 3.2.4. Post-Sparging Pumping of Aquifer Test Well

The sparge well, SW-1, was equipped with a four inch-diameter 0.5 HP Grundfos submersible pump. SW-1 was yield tested and the pump set to a flow rate of 7.72 gpm on November 29, 2012. An inline GPI TM050 flow meter was used to dial in and maintain instantaneous flow rate of 7.72 gpm. The 24-hour aquifer test was initiated at 07:32 on November 30, 2012 at a constant in-line flow rate 7.72 gpm. The pump was shut down between 18:05-18:11 to safely refuel the generator powering the pump. The test was completed at 07:38 on December 1, 2012. The discharge water was pumped to a 17,500 gallon discharge tank approximately 400 feet away. The discharge tank was cylindrical and had a spyglass to measure water level. The average flow rate for the aquifer test was determined by tracking the change in water level in discharge tank as a function of time. The average flow for the pre-sparging aquifer test was 7.2 gpm.

# 3.3. Groundwater Monitoring

Prior to the commencement of CO<sub>2</sub> sparging, on October 1, 2 and 3, 2012, twelve monitoring wells and one extraction well (MW-1A, 1B, 1C; MW-2A, 2B, 2C; MW-3A, MW-115A, 115B, 115C; MW-519A, 519B; and EW-11) were sampled to provide a pre-sparge groundwater quality baseline. The wells were purged and sampled using the low flow "Tubing-in-Screened-Interval" method, pursuant to US EPA Region IV Environmental Investigations Standard Operating Procedure (SOP) — October 2011. The guidance document *Groundwater Sampling Guidelines for Superfund and RCRA Project Managers* was also referenced for additional technical support.

Per the method, the tubing intake was lowered to the middle of the screened interval of the well, and a peristaltic pump was used to purge the groundwater at a very low flow rate. Throughout the purge process, depth to water measurements were collected to assess and maintain stable drawdown. A minimum one equipment volume was purged prior to stabilization parameters (pH, specific conductivity, dissolved oxygen, and turbidity) being collected. Although not considered stabilization parameters, temperature and oxidation reduction potential were also recorded. Once the required parameters were stable for three consecutive readings, groundwater samples were collected for laboratory analysis as described in Table 3-2.

The groundwater samples were preserved on ice and submitted to TestAmerica Laboratories in Savannah, GA for analysis. Once the groundwater samples had been collected, approximately 900 mL of groundwater were pumped into a graduated cylinder and the specific gravity was determined using a hydrometer.

**Table 3-2: Water Quality Analytes and Associated Laboratory Methods** 

Analyte	Method	Description
pН	EPA SW-846 9040B	Ion selective electrode
Alkalinity	SM 2320B	Potentiometric titration
Total mercury	EPA SW-846 7470A	Cold-vapor atomic absorption
		spectrophotometry
Total dissolved solids	SM 2540C	Gravimetric
Chloride and sulfate	EPA SW-846 9056	Ion chromatography
Sulfide	SM 4500 S2 F	Iodometric titration
Total metals & silica <sup>(a)</sup>	EPA SW-846 6010B	Inductively Coupled Plasma –
		Atomic Emission Spectroscopy
Dissolved and total organic	SM 5310B	Combustion / Infrared
carbon		Spectrophotometry
Ferrous iron	SM 3500-Fe-D	Spectrophotometry
_		

<sup>&</sup>lt;sup>(a)</sup> Total metals included aluminum, barium, beryllium, calcium, cobalt, chromium, iron, potassium, magnesium, manganese, sodium, nickel, selenium, vanadium, zinc.

Upon completion of CO<sub>2</sub> sparging, on November 26, 27, and 28, groundwater samples were collected from 12 monitoring wells and the sparge well (MW-1A, 1B, 1C; MW-2A, 2B, 2C; MW-3A, MW-115A, 115B, 115C; MW-519A, 519B; and SW-1) via the same method as the pre- sparge test sampling. SW-1 was sampled in place of EW-11. Additionally, during CO<sub>2</sub> sparging, it was observed that pH at the top of the screen was lower than that at the middle of the screen. To assess for pH-related differences in constituent concentrations, once the middle of the screen samples had been collected from MW-2C and MW-519B, the tubing intake was raised to the top of screen, the well was re-stabilized, and another round of samples was collected from the top of the screen from those wells

The post-sparge samples were collected November 26, 27, and 28, 2012 and submitted for the laboratory analyses described in Table 3-2. Post-sparge groundwater samples were also collected for SF<sub>6</sub> analyses. The analyses for SF<sub>6</sub> was performed by the CH2M Hill Applied Sciences Laboratory in Corvallis, OR. Samples were analyzed via gas chromatography with electron capture detection on a Lagus AUTOTRAC analyzer. Assuming no matrix interference, this technique has an approximate detection limit of  $0.0002~\mu g/L$ .

Purge logs, a summary of stabilization parameters, a summary of collected specific gravity measurements, and analytical data are provided in Appendix C.

#### 3.4. CO<sub>2</sub> Injection and Monitoring

#### 3.4.1. CO<sub>2</sub> Sparge Equipment

A process flow diagram for the CO<sub>2</sub> sparge system is shown on Figure 3-3. The trailer-mounted mobile system consisted of a bulk storage tank with a heated vaporizer and a gas panel to regulate discharge gas flow and pressure. Instrumentation on the gas panel included flow, temperature and pressure monitors. The gas panel also contained flow and pressure regulating valves to optimize flow and pressure during the pilot tests. A separate cylinder with a tracer gas (sodium hexafluoride) was connected to the CO<sub>2</sub> line downstream of the gas panel. The tracer gas line had a dedicated pressure regulator and flow regulating

valve to bleed in tracer gas at required rate and pressure. All operation on the sparge system was manual. Pictures of the trailer and control panel are provided as Figure 3-4.

The sparge well (SW-1) was equipped with a well head that included a pressure indicator, flow indicator, pressure regulating valve and a flow regulating valve to optimize pressure and flow at the well head. The well head that was connected to the gas panel using braided steel hose. A picture of the set-up is provided as Figure 3-5.

A diesel generator was used to power the heater vaporizer on the trailer. The generator was operated only during periods of sparge operation.

# 3.4.2. CO<sub>2</sub> Injection Design Flow Rate and Pressure

The target flow rate for the test was 20 standard cubic feet per minute (scfm) (Mutch Associates, 2012). This flow rate was selected based upon guidance from ESTCP (Leeson et al., 2002), USEPA (2004) and the Army Corps of Engineers Design Manual (2008). The work plan called for (14) 8 hour sparging cycles. This calculation was based on the design flow rate of 20 scfm, an assumed 15 ft radius and 45 ft saturated thickness. The CO<sub>2</sub> demand of CBP water was based upon sulfuric acid titrations of EW-10 water to a pH of 7.5. EW-10 was selected for these calculations because of its similar water quality to EW-11, which is approximately 50 ft from SW-1 (Mutch Associates, 2012).

The flow rate of CO<sub>2</sub> (in ACFM) to the sparge well was read from the rotameter just upstream of the well head (Figure 3-5). This flow rate was converted to SCFM of CO<sub>2</sub> using the following:

$$Q(SCFM) = Q(ACFM) \left(\frac{T_{std}}{T_{act}}\right) \left(\frac{P_{act}}{P_{std}}\right) \sqrt{\frac{1}{SG}}$$
(3-1)

where  $P_{act}$  is the actual pressure (in psia),  $P_{std}$  is the standard pressure (14.7 psia),  $T_{act}$  is the actual temperature (in  ${}^{\circ}R$ ),  $T_{std}$  is the standard temperature (520  ${}^{\circ}R$ ) and SG is the specific gravity of CO<sub>2</sub> gas at 520  ${}^{\circ}R$  (1.5189). Throughout this report, CO<sub>2</sub> flow rates are reported in SCFM of CO<sub>2</sub>.

Fractures can be generated in geologic formations if air or any other gas is injected at a pressure that exceeds the sum of the natural strength of the formation and the in-situ stresses present (Suthersan, 1997). The pressure required to fracture a consolidated geologic formation is a function of the cohesive or tensile strength of the formation and the pressure exerted by the weight of soil and water. Ignoring the cohesion of the soil, and considering only the weight of the water and soil, the minimum pneumatic fracture initiation pressure,  $P_i$  is:

$$P_{i} > d_{w}(\gamma_{w}\eta + \gamma_{soil}(1-\eta)) + (d_{tot} - d_{w})\gamma_{soil}(1-\eta)$$
 (3-2)

where  $d_w$  is the depth of water (saturated thickness),  $d_{tot}$  is the total depth of soil,  $\eta$  is the soil porosity,  $\gamma_w$  is the specific weight of water (62.4 lb/ft³) and  $\gamma_{soil}$  is the specific weight of soil. The minimum pneumatic fracture initiation pressure for SW-1 was calculated to be 30 psig assuming a saturated thickness of 35 ft, 40 ft of soil, porosity of 0.30, and a specific gravity of soil equal to 2.65. As such, the upper limit of injection pressures was set as 25 psig so that fracturing of the Satilla would not occur.

# 3.4.3. Well Preparation

Prior to CO<sub>2</sub> injection, an air sparge test was performed to assess the capacity of sparge well SW-1 to accept gas. The test was performed using an air compressor with the discharge connected to the well head. Pressure and flow of air was regulated using the flow control valve and pressure regulator on the well head. The test was performed by gradually increasing flow and pressure of the air being injected into the well. The air sparge test confirmed the capacity of the sparge well to accept flow at 20 scfm at a pressure below 25 psi.

Water levels were monitored during the air sparge test and a rise in the water elevation was observed within approximately 10 minutes from the start of the air sparge test. Subsequently, 5-foot extensions were installed on all the monitoring wells to contain the rise of water. Fittings and ports were provided at the top of the extensions to allow for instrumentation cables (i.e., for pH probes) and so that manual pressure measurements could be obtained. The well extensions and fittings were sealed to prevent CO<sub>2</sub> gas from preferentially flowing up though the wells. A picture of the extensions and fittings is provided as Figure 3-6; a picture of the well set-up as a whole (for MW-519A and MW-519B) is provided as Figure 3-7.

# 3.4.4. System Start-up and Operation

Prior to beginning of CO<sub>2</sub> injection, the system was started-up and tuned to obtain the required carbon dioxide flow and pressure. Based on observations made during start-up, a daily start-up method was developed wherein the injection system was initially set to a low pressure and flow which was slowly increased to desired flow and pressure. This method was employed to mitigate groundwater elevation rises and immediate development of gas channels.

The system was operated for 16 days during the period October 29 through November 17, 2012. System operation data, including injection pressure, flow, and temperature, is provided in Appendix D.

#### 3.4.5. Groundwater pH Monitoring

Groundwater pH was continuously monitored during the Proof of Concept test in each of the 13 monitoring wells using field pH electrodes (Hach model PHC101 Rugged) with varying cable lengths (10, 15 and 30 m). The electrodes were connected to portable field pH meters (Hach Model HQ40d and HQ11d) (Figure 3-7). The meters were strapped to the well casing. The electrodes were lowered to a depth of 1 foot below the top of screen in each well. These meters were pre-programmed to collect data at 15 minute intervals. The data was recorded and stored within the internal memory of the meters and downloaded daily.

All pH electrodes were calibrated prior to first use. Calibration of pH electrodes involved immersing the electrode in a fresh pH standard and storing the resulting mV reading in the internal memory of the pH meter. This process continued until all standards were read. Typically, a three or four point standard curve was employed using pH 4.01, 7.00, 10.01 and 12.45 standards. Once all of the standards were entered, a valid pH calibration curve was obtained only when the slope was within 5% of the theoretical value of -59 mV/pH.

A calibration check was performed for pH electrodes in deep zone wells MW-1C, MW-2C, MW-115C, and MW-519B on a daily basis. MW-517B was calibrated on a weekly basis because it was outside the expected radius of influence. A calibration check was performed for all other monitoring wells on a weekly basis. A calibration check consisted of uncapping the well, retrieving the electrode, and bringing it

to the surface. The electrode was rinsed using deionized water and blotted with a lint-free laboratory wipe. Then, the electrode was submersed in a pH 7.00 standard and the pH was measured. If the pH was outside of the range 6.85 < pH < 7.15, the electrode was recalibrated. Upon re-calibration, if the electrode failed the slope and intercept calibration criteria, it was taken out of service for reconditioning or replacement.

All pH electrodes were reconditioned once per week. The electrode was rinsed with deionized water and blotted dry with a lint-free cloth. The glass bulb of the electrode was soaked for 12 to 16 hours in an electrode cleaning solution (Hach Product #2965249). The electrode was then soaked for 1 minute in deionized water.

Continuous pH monitoring occurred on site for the duration of the sparging Proof of Concept test, October  $29 - \text{November } 17^{\circ} 2012$ , and for 7 days following the sparging test, November 17 - 21 and November 25 - 28. November 22 - 24 were not monitored due to the Thanksgiving holiday.

Groundwater pH was periodically measured in EW-11 by low flow sampling. In addition, wells MW-1C, MW-2C, MW-115C, MW-517A, MW-517B, MW-519B and SW-1 were periodically measured for pH by low flow sampling. A Global Water pump was used to low flow sample the wells. The wells were pumped for approximately 2.5 gallons of CBP water then a sample was taken and pH was measured by a Hach PHC101 electrode. The data from these sampling events were also stored on a Hach field pH meter and downloaded daily. The collected pH data is presented and discussed in Section 4.

# 3.4.6. Air Monitoring

Ambient air monitoring during the sparge test included continuous direct monitoring of oxygen, carbon dioxide, and hydrogen sulfide using a MultiRae continuous monitoring device. Grab sample monitoring for mercury in the breathing zone was also conducted. The concentrations of constituents monitored generally remained steady and near normal ambient concentrations during the period of the testing. The MultiRae meter occasionally displayed a high ambient oxygen concentration, which was considered to be a fault alarm. Most ambient air within the work zone had CO<sub>2</sub> readings between 410 and 490 ppmv. No exceedances in the ambient carbon dioxide, hydrogen sulfide, and mercury concentration were observed as shown in Table 3-3.

Table 3-3: Ambient Air Monitoring Measurements						
Air Constituent	Units	Action Level	Minimum Observed Level	Maximum Observed Level		
CO <sub>2</sub>	ppmv	2500	320	920 (at rear of trailer)		
O <sub>2</sub> (%)	% by volume	< 19.5% and > 22.0%	20.0	30.0 <sup>(a)</sup>		
Hg	mg/m <sup>3</sup>	0.05	0.000	0.000		
H <sub>2</sub> S	ppmv	10	0	1		

<sup>(</sup>a) This reading was probably the result of a sensor error. Oxygen levels returned to ambient conditions upon resetting the meter.

# 4. PROOF OF CONCEPT RESULTS

#### 4.1. Overview of Test Results

Section 4 describes the results from the various elements of the Proof of Concept Test. The Proof of Concept workplan called for 14 days of sparging into SW-1 at 8 hrs/day. Weekends were reserved for an extended rest period to observe rebound potential. After sparging into SW-1 for 10 days, the pH of the deep Satilla monitoring wells were not appreciably changed. Prior to the 11<sup>th</sup> day of sparging, a decision was made to change from SW-1 to MW-1C. MW-1C is screened 5 feet deeper than SW-1 and is at the same interval as MW-2C and MW-519B. The basis for this change was the importance of lowering the pH to between 7 and 8 in the deep Satilla to evaluate the effect of pH on mercury concentrations and the overall geochemistry of the aquifer. This decision was made in consultation with Honeywell. Verbal approval was granted by EPA on the morning of November 12, 2012.

# 4.2. Sparge Well Flow Rates

Sparging began on Monday October 29<sup>h</sup>, 2012. In the first week, sparging into SW-1 took place on five consecutive days for approximately 8.0 hrs/day (Figure 4-1). The weekend (November 3<sup>rd</sup> and 4<sup>th</sup>) was used as a rest period to observe potential pH rebound. In week 2, sparging into SW-1 took place on five consecutive days at approximately 8.7 hrs/day. Sparging occurred at slightly higher flow rates to assess effect on pH reductions in the deep Satilla wells. Once again, the weekend (November 10<sup>th</sup> and 11<sup>th</sup>) was used as a rest period to observe potential pH rebound. On November 12<sup>th</sup>, the sparge well was switched from SW-1 to MW-1C. Sparging took place on six consecutive days into MW-1C for approximately 9.1 hrs/day. A summary of all sparging activities is provided in Table 4-1. The record of sparging flow rates is included in Appendix D.

**Table 4-1: Summary of Proof of Concept Sparging Activity** 

	SW-1 (Week 1 & 2)	MW-1C (Week 3)	Total
Days of Sparging:	10	6	16
Duration of Sparging, t <sub>sparge</sub> :	83.3 hr	54.5 hr	137.8 hr
	(8.3 hr/d)	(9.1 hr/d)	(8.6  hr/d)
Q, Time-weighted average	50.5 SCFM	57.6 SCFM	53.3 SCFM
Flow Rate <sup>1</sup> :			
Total Mass of CO <sub>2</sub> injected <sup>2</sup> :	13,290 kg	9,900 kg	23,190 kg
Į ,	(29,300 lb /14.7 tons)	(21,800 lb / 10.9 tons)	(51,100 lb /25.6 tons)

A typical CO<sub>2</sub> sparging daily program is shown in Figure 4-2 for SW-1 on November 2, 2012. Setup occurred each morning at approximately 7:30 am. Sparging typically began between 8:30 and 11:00 am. Start-up involved slowly increasing the pressure at the injection well over a 15 to 30 minute period. It was observed that after the static well head and capillary pressures are exceeded, the flow rate increases dramatically with small increases in pressure. This threshold pressure was approximately 22 psig. On most

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<sup>&</sup>lt;sup>1</sup> Time-weighted average flow rate was calculated by numerically integrating the instantaneous flow rate as a function of time and dividing by the sparging duration.

<sup>&</sup>lt;sup>2</sup> Mass of CO<sub>2</sub> injected was calculated according to:  $\overline{Q}\rho_{gas}t_{sparge}$  where  $\rho_{gas}$  is the density of CO<sub>2</sub> at 14.7 psia and 520 °R (1.857 g/L or 0.1157 lb/ft<sup>3</sup>)

days, the pressure was increased and maintained between 24 and 25 psig. These pressures were shown to be capable of sustaining sparging flow rates between 30 and 75 scfm of CO<sub>2</sub> in both SW-1 and MW-1C.

# 4.3. Changes in pH

The pH of the treatment area was measured as part of the baseline pre-sparge well sampling and as part of continuous pH monitoring. Values from the baseline continuous pH monitoring are shown in profile in Figure 4-3. These values were recorded a few hours prior to the start of sparging (November 29, 2012 at 8:45 AM). The deep Satilla wells had pH values ranging from 11.18 to 11.91. These values are consistent with historical pH values of the deep Satilla wells. The shallow and intermediate Satilla well pH values were alkaline (pH > 7), but did not have as high pH as the deep Satilla wells.

The pH response of each of the monitoring wells is shown in Figures 4-4 through 4-10. The deep Satilla wells are shown in Figures 4-4, 4-5, and 4-6. The intermediate Satilla wells are shown in Figures 4-7 and 4-8. The shallow Satilla wells are shown in Figures 4-9 and 4-10. Each data point (black circles) represents a pH value recorded at a 15 minute interval. Note that for the deep Satilla wells, additional pH data was recorded by pumping the wells with a peristaltic pump. These data points are either yellow or blue depending upon whether water was collected at the top or bottom of the well screen.

The day-to-day pH responses of individual wells showed large variations and it is not practical to describe the various daily changes in pH of the entire monitoring well network. However, the following observations are of note:

- In general, all wells with the exception of MW-115A (30.7 feet away from SW-1), and MW-517B (over 100 ft away SW-1) showed a decrease in pH.
- Some wells showed a significant pH decrease only after multiple days of sparging. Examples of this include MW-1C (Figure 4-4), MW-2A (Figure 4-8) and MW-115B (Figure 4-7).
- Responses in monitoring wells after sparging were fairly rapid. Once sparging started, monitoring wells started showing a change in pH after approximately 1 hour.
- Significant pH rebound during the early phases of CO<sub>2</sub> injection typically occurred within an hour of stopping the flow of CO<sub>2</sub> gas to the sparge well. This can be seen very clearly for MW-2C (Figure 4-4) on Day 1 (October 29<sup>th</sup>). The pH started at 11.5, dropped to 6.8 during sparging and then increased to 10.5 before the beginning of the next day of sparging.
- Not all monitoring wells showed the same responses each day. For example, MW-1C (Figure 4-4) showed virtually no change in pH after the first day of sparging. However, on Day 2 (October 30<sup>th</sup>), the pH dropped from 11.7 to 10.3 and then rebounded significantly back to 11.3. This indicates that CO<sub>2</sub> channels are not in the same physical location each day, and that adequate coverage around the sparge well can only be achieved by sparging on multiple days.
- Many shallow wells, for example MW-1A and MW-3A, showed modest increases in pH during sparging for the first few days. This is probably the result of a modest movement of lower Satilla water upward into the well screen as pore spaces fill with CO<sub>2</sub>. This was followed by a sudden, dramatic decrease to pH 6 or 7 during sparging without significant

subsequent rebound. This is an indication that CO<sub>2</sub> channels have come into close contact with water in the area near these monitoring wells.

Values of pH after 2 weeks of sparging into SW-1 (November 11, 2012) are shown in profile on Figure 4-11. SW-1 had the lowest pH (6.60) of all the deep Satilla wells. However, other than SW-1, pH levels in the deep Satilla wells did not decrease to a large extent from pre-sparge levels. In the deep Satilla monitoring wells, the pH at the bottom of screen was consistently higher than that at the top of the screen indicating a large change in water quality across a relatively small (5 ft) vertical distance. The most notable difference in pH across the well screen was at MW-2C with a difference of greater than 1 pH unit. The well which showed the largest pH decrease was MW-2C which showed a decrease from 11.78 to 9.19 at the top of screen. The intermediate Satilla wells located laterally within 20 feet of SW-1 showed large decreases in pH. Specifically, wells MW-1B, MW-519A, and MW-2B had post-sparge pH values of 5.97, 5.86 and 6.23 respectively. These wells had pH values of approximately 9.0 pre-sparge (Figure 4-3), and therefore this represents a decrease in pH of approximately 3 units.

As described earlier, the sparge well was switched from SW-1 to MW-1C. MW-1C was sparged for 6 continuous days. At the conclusion of the week sparging program, there was a 1 week of pH rebound continuous monitoring. Values of pH at the end of this monitoring period (November 28, 2012) are shown in profile in Figure 4-12 and summarized in Table 4-2. The following discussion of the results of sparging on pH levels is broken up into three sections according to the screened interval of the various monitoring wells in the Satilla (i.e. deep, intermediate and shallow).

Table 4-2: Changes in pH at Conclusion of Proof of Concept Test<sup>3</sup>

	Monitoring Well	Pre-sparge pH	Post-sparge pH	ΔpΗ
	MW-1A	7.32	6.62	-0.70
Shallow	MW-2A	8.61	6.98	-1.63
Sha	MW-3A	7.99	7.16	-0.83
	MW-115A	7.36	7.56	+0.20
ıte	MW-1B	8.67	6.09	-2.58
edis	MW-2B	9.39	6.47	-2.92
Intermediate	MW-115B	9.09	6.51	-2.58
In	MW-519A	9.61	6.07	-3.54
	MW-115C	11.18	9.97	-1.21
	MW-1C	11.61	6.86	-4.75
Deep	MW-2C	11.78	7.96 / 10.08	-3.82 / -1.70
De	MW-519B	11.91	8.68 / 8.73	-3.23 / -3.18
	EW-11	11.60	9.73	-1.87
	MW-517B	11.42	10.95	-0.47
No	te: When two values are listed, first ent	ry is value at top of	screen, second entry	is at mid screen

<sup>3</sup>Pre-sparge values recorded in the field prior to the start of sampling using continuous pH monitoring (October 29, 2012 at 8:45 AM) with the exception of EW-11 which was sampled shortly after the start of sparging on October 31, 2012. Post-sparge pH values recorded in field using low-flow sampling at end of post-sparge monitoring period on November 28, 2012. Measurement of pH was also performed in the field during the pre and post-sparge sampling events. The final pH values for the deep Satilla wells were: MW-115C (10.4); MW-1C (6.74); MW-2C (6.88 / 7.74); MW-519B (8.80 / 9.22). The values are similar to those listed in Table 4-2 except for MW-2C which are somewhat lower in pH.

The influence on the deep Satilla wells was much more pronounced after sparging was switched from SW-1 to MW-1C. MW-1C, MW-519B and MW-2C all experienced pH decreases of greater than 3 units. MW-519B and MW-2C are 15.1 and 19.9 ft from MW-1C, respectively. Decreases in pH in MW-15C and EW-11 were more modest, with post-sparge pH values between 9 and 10. These wells are 24.6 ft and 44.1 ft away from MW-1C. Based upon this information, the effective radius of influence of sparging within the deep Satilla was at least 20 ft. Essentially all wells at the intermediate depth were lowered to pH values between 6 and 7. Most notable was MW-115B which dropped to pH 6.51 after the switch from SW-1 to MW-1C. MW-115C is 33.1 ft from MW-1C. Also notable, was the visible bubbling and low pH (6.43) of MW-517A observed while sparging into, MW-1C. MW-517A is screened at the intermediate depth and is 97.2 ft from MW-1C. Based upon this information, the effective radius of influence within the intermediate Satilla is at least 33 ft and could extend as far as 100 ft in some areas.

The shallow Satilla initial pH values were only slightly alkaline, with values ranging from 7.32 to 8.61. All of the shallow wells were directly influenced by sparging into SW-1 and MW-1C with the exception of MW-115A. MW-115A is in the shallow Satilla and is 30.7 and 36.6 ft away from SW-1 and MW-1C, respectively.

# 4.3.1. Efficiency of CO<sub>2</sub> Sparging

One of the objectives of the Proof of Concept test was to assess the efficiency of  $CO_2$  sparging. Since  $CO_2$  is a weak acid, the amount of  $CO_2$  required to reach a specific pH is dependent upon the initial pH, the final pH, and the alkalinity of the water. A numerical titration was performed to calculate the  $CO_2$  demand of CBP water. The first step in this titration was determination of the total carbonate,  $C_T$  of representative water from the deep, intermediate and shallow Satilla. To start, all of the alkalinity (Alk) of the water was assumed to be present as carbonates, silicates and hydroxide ion:

$$Alk = [HCO_3^-] + 2[CO_3^{2-}] + [Si(OH)_3^-] + 2[Si(OH)_2^{2-}] + [OH^-] - [H^+]$$
(4-1)

The concentrations of all 6 components of Equation (4-1) are a function of pH, and are related by laws of mass action:

$$H_2CO_3^* \rightleftharpoons HCO_3^- + H^+$$
 ${}^{c}K_{a1} = \frac{[HCO_3^-][H^+]}{[H_2CO_3^*]}$ 
(4-2)

$$HCO_3^- \rightleftharpoons CO_3^{2-} + H^+$$
  ${}^{c}K_{a2} = \frac{[CO_3^{2-}][H^+]}{[HCO_2^-]}$  (4-3)

$$Si(OH)_4(aq) \rightleftharpoons Si(OH)_3^- + H^+$$

$${}^{c}K_{a1,Si} = \frac{[Si(OH)_3^-][H^+]}{[Si(OH)_4(aq)]}$$
(4-4)

$$Si(OH)_{3}^{-} \rightleftharpoons Si(OH)_{2}^{2-} + H^{+}$$

$${}^{c}K_{a2,Si} = \frac{[Si(OH)_{2}^{2-}][H^{+}]}{[Si(OH)_{3}^{-}]}$$
(4-5)

where  ${}^{c}K_{a1}$ ,  ${}^{c}K_{a2}$ ,  ${}^{c}K_{a1,Si}$  and  ${}^{c}K_{a2,Si}$  are concentration-based acidity constants<sup>4</sup>. The concentrations of the species in Equation (4-1) were calculated by combining the appropriate mole balance equations with the mass action laws shown above. For the carbonate system:

$$C_{T} = [H_{2}CO_{3}^{*}] + [HCO_{3}^{-}] + [CO_{3}^{2-}]$$
(4-6)

$$[HCO_3^-] = C_T \frac{{}^{c}K_{a1}[H^+]}{[H^+]^2 + {}^{c}K_{a1}[H^+] + {}^{c}K_{a1}{}^{c}K_{a2}}$$
(4-7)

$$[CO_3^{2-}] = C_T \frac{{}^{c}K_{a1}{}^{c}K_{a2}}{[H^{+}]^2 + {}^{c}K_{a1}[H^{+}] + {}^{c}K_{a1}{}^{c}K_{a2}}$$
(4-8)

For the silica system:

$$Si_{T} = [Si(OH)_{4}(aq)] + [Si(OH)_{3}^{-}] + [Si(OH)_{2}^{2-}]$$
 (4-9)

$$[Si(OH)_{3}^{-}] = Si_{T} \frac{{}^{c}K_{a1,Si}[H^{+}]}{[H^{+}]^{2} + {}^{c}K_{a1,Si}[H^{+}] + {}^{c}K_{a1,Si}{}^{c}K_{a2,Si}}$$
(4-10)

$$[Si(OH)_{2}^{2-}] = C_{T} \frac{{}^{c}K_{al,Si} {}^{c}K_{a2,Si}}{[H^{+}]^{2} + {}^{c}K_{al,Si} [H^{+}] + {}^{c}K_{al,Si} {}^{c}K_{a2,Si}}$$
(4-11)

For hydroxide ion:

$$[OH^{-}] = \frac{{}^{c}K_{w}}{[H^{+}]}$$

$$(4-12)$$

Equations (4-7), (4-8), (4-10), and (4-11) were combined with (4-1) to obtain an equation which relates the alkalinity, total carbonate, total silica and  $[H^+]$ :

$$Alk = C_{T} \left( \frac{{}^{c}K_{a1}[H^{+}] + 2{}^{c}K_{a1}{}^{c}K_{a2}}{[H^{+}]^{2} + {}^{c}K_{a1}[H^{+}] + {}^{c}K_{a1}{}^{c}K_{a2}} \right) + Si_{T} \left( \frac{{}^{c}K_{a1,Si}[H^{+}] + 2{}^{c}K_{a1,Si}{}^{c}K_{a2,Si}}{[H^{+}]^{2} + {}^{c}K_{a1,Si}[H^{+}] + {}^{c}K_{a1,Si}{}^{c}K_{a2,Si}} \right) + \frac{{}^{c}K_{w}}{[H^{+}]} - [H^{+}]$$
(4-13)

Water quality data was available for deep, intermediate and shallow Satilla wells for Alk,  $Si_T$  and pH. From these values, Equation (4-13) was used to calculate  $C_T$  from Alk,  $Si_T$  and pH.

The numerical titration was performed by incrementally increasing the  $C_T$  of the system until the target pH was achieved (pH 7.5). This process assumes Alk and  $Si_T$  are constant. The difference in  $C_T$  from the start of the titration to the end represents the total amount of  $CO_2$  that is needed to satisfy the demand. The results of the numerical titrations for a selection of shallow, intermediate and deep Satilla wells are shown in Figure 4-13. The results for all the wells are tabulated in Table 4-3. MW-3A had

 $K_{a2} = 10^{-10.329}, \, K_{a1,Si} = 10^{-9.84}, \, K_{a2,Si} = 10^{-13.2}, \, K_w = 10^{-13.997}.$ 

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<sup>&</sup>lt;sup>4</sup> In low TDS (low ionic strength) water, concentration-based equilibrium constants are often assumed to be equal to equal to the true activity-based (thermodynamic constants). Since the Satilla has high TDS, ionic strength corrections were performed. The ionic strength was estimated using the Langelier (1936) relationship  $I = \text{TDS}(2.65 \times 10^{-5})$ , where I is the ionic strength (in mol/L) and TDS is the total dissolved solids in mg/L. The Davies equation (1962) was then used to calculate activity coefficients, which were then applied to the activity-based constants to calculate the concentration based constants. The values of the activity-based constants used for the calculation were:  $K_{a1} = 10^{-6.532}$ ,

alkalinity and TDS values that were approximately 5-times larger than nearby shallow Satilla wells, but had a similar pH. The cause of this variability across the shallow Satilla monitoring wells is not known.

Table 4-3: Theoretical CO<sub>2</sub> Demand for Shallow, Intermediate and Deep Satilla Wells

**Pre-sparge Water Quality** 

		Tie-sparge water			T	
		Alkalinity	pH (lab)	Silica	TDS	CO <sub>2</sub> Demand
		(mg/L as CaCO <sub>3</sub> )		(mg/L as	(mg/L)	(mol/L)
	Well			SiO <sub>2</sub> )		
	MW-1A	810	8.42	44	5,000	0.0011
Shallow	MW-2A	920	8.68	80	5,200	0.0018
Sha	MW-3A	4,900	8.14	13	30,000	0.0045
	MW-115A	600	7.66	19	3,700	0.00018
					Average:	0.0019
ate	MW-1B	800	8.93	57	8,500	0.0024
Intermediate	MW-2B	770	9.16	30	4,300	0.0028
ern	MW-115B	640	9.11	18	3,400	0.0021
Int	MW-519A	920	9.71	30	5,800	0.0064
					Average:	0.0034
	MW-115C	5,800	11.77	2,870	33,000	0.068
	MW-1C	5,700	11.20	2,000	48,000	0.078
Deep	MW-2C	5,300	11.30	1,900	38,000	0.074
-	MW-519B	7,410	11.76	3,200	44,000	0.11
	EW-11 <sup>(a)</sup>	5,000	11.71	2,270	26,600	0.077
					Average:	0.081
(a) <b>L</b>	Data from May 20	010				

The total CO<sub>2</sub> demand for the Proof of Concept Test was estimated by considering the Satilla to consist of three discrete layers, each with a constant CO<sub>2</sub> demand. The layering used for the calculation was consistent with the shallow/intermediate/deep designation shown in Table 3-1 and used throughout the report. The calculation is shown schematically in Figure 4-14. The volume of the deep Satilla layer was calculated assuming a 20 ft radius of influence, and a 15 ft thickness. Assumptions related to ROI and thickness within the intermediate and deep Satilla layers are shown in Table 4-4. Note that this CO<sub>2</sub> demand is a conservative estimate because there was evidence of pH reductions (i.e. consumption of CO<sub>2</sub> demand) at radial distances larger than 20 ft in the deep Satilla.

**Table 4-4: CO<sub>2</sub> Demand Estimate** 

		Sat.					
	ROI	Thickness	Volume of water	(a)	CO <sub>2</sub> Demand	-	
Layer:	(ft)	(ft)	(ft <sup>3</sup> )	(gal)	(mol/L)	(kg)	(lb)
Shallow	60	19	75,210	562,606	0.0019	178	391
Intermediate	40	15	26,389	197,406	0.0034	112	246
Deep	20	15	6,597	49,351	0.0814	668	1,470
(a)					TOTALS:	958	2,107

<sup>(</sup>a) Calculation assumes porosity of 0.35

Based on the mass of  $CO_2$  injected (Table 4-1) and the estimate of  $CO_2$  demand (Table 4-4), the sparging efficiency,  $\eta$ , can be calculated from the following:

$$\eta = \frac{\text{CO}_2 \text{ demand (kg)}}{\text{mass of CO}_2 \text{ injected (kg)}} \times 100\%$$
 (4-14)

The sparging efficiency considering the total amount of CO<sub>2</sub> injected into both SW-1 and MW-1C is 4.1%. Since the majority of the demand is present in the deep Satilla, an alternative way of calculating the sparging efficiency is to consider only the amount of CO<sub>2</sub> injected into MW-1C. The sparging efficiency in this case is 9.7%. This alternative calculation assumes that the demand of the intermediate and shallow portions of the aquifer would have already been met prior to the 54.5 hr sparging duration into MW-1C. This is a reasonable assumption given the rapid decreases in pH observed in the intermediate and shallow monitoring wells after the start of sparging (see Figures 4-4 through 4-10). Note that this is not far off from the 10% efficiency assumed as part of the CO<sub>2</sub> demand calculations in Proof of Concept work plan. However, it is important to note that the Proof of Concept test was not designed to optimize CO<sub>2</sub> efficiency. As discussed in Section 2, this test was intended to show at the proof of concept level that pH levels could be reduced in the deep Satilla by sparging with CO<sub>2</sub>.

The efficiency calculated above describes the amount of CO<sub>2</sub> required to meet the CO<sub>2</sub> demand within a prescribed treatment ROI. The efficiency calculation does not represent a mass balance on CO<sub>2</sub> or the amount of CO<sub>2</sub> lost to the atmosphere. This is because the demand estimate is based upon the assumption that no demand was met outside of the ROI used in the calculation. In reality, pH monitoring data indicate that some CO<sub>2</sub> demand was consumed outside of the 20 ft ROI used to compute the demand in the deep Satilla. For example, the pH of EW-11 was reduced by almost 2 full pH units. In addition, the post-sparge aquifer test results (described in section 4.6.6) indicate that a large amount of residual saturation of CO<sub>2</sub> remained in the aquifer after the test was complete.

The CO<sub>2</sub> sparging efficiency is dependent upon many factors including the CO<sub>2</sub> flow rate, extent of radial travel of CO<sub>2</sub> gas channels, time for gas channels to reach the surface, and rate of mass transfer of CO<sub>2</sub> from the gas phase to the water. Increasing the flow rate of CO<sub>2</sub> pushes gas channels out further (increases the treatment ROI), but also leads to less efficient use of CO<sub>2</sub> once channels reach the surface. Increasing the sparging efficiency may be possible by sparging for shorter periods of time, thereby limiting the amount of CO<sub>2</sub> escape to the atmosphere. Furthermore, a longer rest period in-between sparging event may allow the trapped CO<sub>2</sub> gas to dissolve into the water before the start of the next sparging event.

#### 4.4. Changes in Aquifer Geochemistry

# 4.4.1. Pre and Post Differences Observed During Field Sampling

The majority of the monitoring wells sampled over the two events displayed very similar characteristics in regards to water table drawdown, percent dissolved oxygen content, and specific conductivity as the majority of the readings were within the same order of magnitude (Appendix C). The A wells, which are screened approximately 15-20 feet bls, exhibited the least variation in the water quality characteristics. The pH of the groundwater decreased for all of the wells sampled. Turbidity decreased significantly in many of the monitoring wells to levels so low that the field instrument was unable to

measure it. During the pre-test sampling event, it was noted that the majority of the generated purge water had a strong indistinguishable odor, while the post-test purge water did not smell as strongly.

Specific gravity increased slightly from pre- to post- sparging in many of the deep Satilla wells. During the post-sparge specific gravity measurements, there was noticeable gas evolution from wells screened in the deep interval. This likely increased the buoyancy of the field hydrometer resulting in biased specific gravity readings. Note that a similar increase was not observed in TDS (Section 4.4.3). This is further evidence for positive bias in the post-sparge readings since specific gravity and TDS are linearly related.

Two monitoring wells (MW-2C and MW-115B) displayed very notable differences between the pre- and post- sparge testing. During the first event, MW-2C had slight drawdown, but the water table stabilized quickly; while drawdown was quite significant during the post-test sampling. The MW-2C purge process commenced on November 26, 2012, at a very low flow rate, and the water level dropped from 8.91 feet below top of casing (btoc) to 14.5 feet btoc, at which time the purge was stopped. MW-2C was purged and sampled on the following day, and the water table had not recovered completely as it was recorded to be 9.22 feet btoc at the beginning of the purge. The water level had dropped to 13.06 feet by the end of the purge.

During the pre-test groundwater sampling, MW-115B had a recorded pH of 9.49 SU, which was stable throughout the purge. However, the post-test pH for MW-115B did not stabilize as it fluctuated from 6.40 to 11.43 SU. The pH started off low and gradually decreased and then began to increase to subsequently decrease and increase again. It is theorized that the pH fluctuation was due in part to the well's upgradient location, and to the well location on the perimeter of radius of the CO<sub>2</sub> sparge influence.

# **4.4.2.** Mercury

Pre-sparge mercury dissolved phase concentrations are shown in cross section on Figure 4-15. Mercury concentrations in the deep Satilla in the area near SW-1 were consistently between 110 and 120  $\mu$ g/L. Concentrations in the intermediate and shallow Satilla were considerably lower with concentrations ranging from 0.16 to 11  $\mu$ g/L. Note that pH values are also shown on Figure 4-15 for reference. Wells with elevated Hg levels (Table 4-5) were always accompanied by pH values greater than 11.0. The intermediate Satilla wells also had a narrow range in mercury concentrations and were approximately 20-times less than the deep Satilla, with an average concentration of 5.8  $\mu$ g/L. The shallow Satilla wells were of comparable magnitude to the intermediate Satilla wells but had a larger range. A complete summary of the laboratory analytical data is provided in Appendix E.

Figure 4-16 shows a cross section of post-sparge mercury and pH concentrations. The contours shown on this figure are for pH. Among the deep Satilla wells, the two wells that exhibited the largest decreases in Hg concentrations were the two sparge wells: SW-1 and MW-1C. Both SW-1 and MW-1C had post-sparge pH values near 7.0. The next largest reduction (in terms of  $\Delta$ Hg) was MW-2C which showed a change of -77  $\mu$ g/L (70% reduction) in water sampled from the top of the well screen. This water had a pH of 7.96.

The relationship between pH and mercury concentrations was examined further by plotting preand post-sparge Hg versus pH for the deep Satilla wells (Figure 4-17a). Data points represent water samples taken during the pre- and post-sparging sampling events. As discussed earlier, the pre-sparge deep Satilla wells possessed a consistent dissolved mercury concentration (orange circles). The post-sparge deep Satilla wells show a clear trend of decreasing Hg concentrations with decreasing pH. Once the pH drops below 8.5, mercury concentrations begin to decrease dramatically.

Table 4-5: Percent Reduction of Dissolved Phase Mercury at Conclusion of Proof of Concept Test

		Pre-Sparge	Post-Sparge		
	Well	Hg (µg/L)	Hg (µg/L)	ΔHg (μg/L)	% Reduction
	MW-1A	8.1	1.1	-7.0	86%
low	MW-2A	11	4.5	-6.5	59%
Shallow	MW-3A	0.16 J	0.52	0.36	
<i>S</i> <sub>2</sub>	MW-115A	7.2	7.6	0.4	-6%
ate	MW-1B	5.0	3.5	-1.5	30%
Intermediate	MW-2B	4.8	4.5	-0.3	6%
	MW-115B	5.5	3.9	-1.6	29%
Inte	MW-519A	7.9	3.1	-4.8	61%
	MW-115C	120	110	-10	8%
_	MW-1C	110	21	-89	81%
Deep	MW-2C	110	64.5 / 33	-45.5 / -77	41% / 70%
D	MW-519B	120	99 / 89	-21 / -31	18% / 26%
	SW-1	110	11	-99	90%
No	te: When two v	alues are listed,	first entry is value	at top of screen, seco	ond entry is at mid screen

There is also a relationship between pH and Hg in the intermediate Satilla; it is different, however, than the deep Satilla (Figure 4-17b). Pre-sparge concentrations of the intermediate Satilla wells fall below the curve shown earlier for the deep Satilla (Figure 4-17a). All of the intermediate Satilla wells experienced a significant change in pH with final post-sparge values all showing little variability between 6.0 and 6.5 (Table 4-2). This resulted in very constant post-sparge Hg values in the intermediate Satilla of approximately  $3.8~\mu g/L$ .

The relationships between Hg and pH (Figure 4-17) indicate that local Hg concentrations behave predictably as a function of pH over the portion of the site used for the Proof of Concept test. As one might expect, this relationship is specific to the geochemical conditions of the aquifer. Since the geochemical conditions of the CBP are vertically stratified, the attenuation of dissolved Hg as a function of pH is different for the three intervals employed in the Proof of Concept test.

The CBP is a sulfide-rich, reducing environment. In sulfide-rich environments, mercury speciation is known to be dominated by (Skyllberg, 2008):

- Hg(II) complexes with sulfide such as HgHS<sup>-</sup>, HgS<sub>2</sub><sup>2-</sup>
- Hg(II) complexes with polysulfides such as  $Hg(S_x)_2^{2-}$ ,  $HgS_xOH^-$ ,
- Hg(II) complexes with thiol groups present on dissolved organic matter (DOM)
- HgS(s) precipitated as metacinnabar or cinnabar

Speciation models have been developed by many investigators for Hg complexes with reduced sulfur. In general, these models show that dissolved mercury concentrations decrease with decreasing pH in systems containing sulfides and polysulfides. For example, Jay et al. (2000) used a speciation model to describe total dissolved mercury concentrations as a function of pH in systems containing synthetic cinnabar and dissolved sulfide. The extent of the decrease in mercury concentrations with pH was dependent upon the total dissolved sulfide in the system and whether or not zero valent sulfur is present.

The geochemical conceptual model for mercury within the CBP is discussed in the RI (GeoSyntec, 1997). E<sub>h</sub>-pH diagrams were prepared for a representative "background water" and CBP water. The E<sub>h</sub>-pH diagrams indicate that there is a transition from soluble mercury sulfide complexes to insoluble HgS(s) that occurs under moderately reducing conditions between pH 8.5 and 10.5. The data collected as part of the Proof of Concept test is consistent with this conceptual model. All of the deep Satilla wells contain significant dissolved sulfide concentrations that are well in excess of the dissolved mercury concentrations (Appendix E). The decrease in dissolved Hg concentrations as the pH decreased is most likely due to a shift in equilibrium toward mercury sulfide (HgS(s)) precipitation.

# 4.4.3. Additional Geochemical Changes

Changes in TDS, As, Cr, Si and V are shown in Table 4-6. TDS did not change appreciably from pre- to post-sparging. Dissolved concentrations of arsenic, chromium, silicon and vanadium all decreased significantly in deep Satilla wells after sparging (Table 4-6).

The decrease in dissolved silica concentrations in the deep Satilla wells is due to precipitation of silica solids. Laboratory testing of CBP water with similar characteristics to the water near EW-11 showed precipitation of small to moderate amounts of silica solids gel upon sparging of CBP with carbon dioxide to pH 6.5 (Mutch Associates, 2012). Silica is known to be less soluble at lower pH and so some precipitation is to be expected. There was also visual evidence of some solids precipitation covering pH electrodes in the deep and intermediate Satilla wells a few days after sparging.

One concern over  $CO_2$  sparging into the Satilla was the potential dissolution of the variably cemented sandstone. The  $CO_2$  Work Plan (Mutch Associates, 2012) discusses various kinetic and thermodynamic calculations which suggested that conditions which promote dolomite dissolution would not be present as a result of sparging. Specifically, laboratory sparging results showed that pH < 6.5 would not be attained in the deep Satilla where CBP water is in contact with the variably cemented sandstone. This result was confirmed in the Proof of Concept test, as the pH of deep Satilla wells was not lowered to below 6.5 during sparging. Values of pH as low as 5.9 were obtained temporarily, but this was in the intermediate Satilla wells which are not in contact with the variably cemented sandstone.

Table 4-6: Chan	ges in Tl	DS, As, C	Cr, Si and	l V in Dee	p S	Satilla W	'ells <sup>5</sup>		
					-				
	TDS					Silicon			
Well	Pre (mg/L)	Post (mg/L)	ΔTDS (mg/L)	% Change		Pre (mg/L)	Post (mg/L)	ΔSi (mg/L)	% Change
MW-115C	33000	34000	1000	3.0%		2000	470	-1530	-76.5%
MW-1C	48000	48000	0	0.0%		2000	86	-1914	-95.7%
MW-2C (mid)	38000	35000	-3000	-7.9%		1900	180	-1720	-90.5%
MW-2C (top)	-	32000	_	-		-	110	-	-
MW-519B (mid)	43000	46000	3000	7.0%		2000	210	-1790	-89.5%
MW-519B (top)	-	45000	-	-		-	180	-	-
			Avg:	0.5%				Avg:	-88%
	Arsenic					Chromium			
Well	Pre (mg/L)	Post	$\Delta As$	% Change		Pre (mg/L)	Post (mg/L)	ΔCr	% Change
MW-115C	(mg/L) 280	(mg/L) 98	(mg/L)	Change -65%		(mg/L) 340	(mg/L) 340	(mg/L)	Change 0%
MW-1C	320	120	-200	-63%		500	320	-180	-36%
MW-2C (mid)	260	44	-216	-83%		370	320	-50	-14%
MW-2C (top)	-	26	-	-		-	300	-	-
MW-519B (mid)	390	170	-220	-56%		610	380	-230	-38%
MW-519B (top)	-	130	-	-		-	390	-	-
_			Avg:	-67%				Avg:	-22%
	Vanadium Pre Post ΔV %								
				%					
Well	(mg/L)	(mg/L)	(mg/L)	Change					
MW-115C	1500	1400	-100	-6.7%					
MW-1C	2200	370	-1830	-83.2%					
MW-2C (mid)	1700	760	-940	-55.3%					
MW-2C (top)		620	-	-					
MW-519B (mid)	2300	1100	-1200	-52.2%					
MW-519B (top)		1100	-	-					
			Avg:	-49%					

<sup>&</sup>lt;sup>5</sup> Pre-sparge water samples were collected only from mid-screen of monitoring wells. Top-of-screen water samples were collected post-sparge because of the significant pH gradient observed across the well screen while sparging and during the post-sparge monitoring period of the Proof of Concept test

#### 4.5. SF<sub>6</sub> Tracer Distribution

As described earlier,  $SF_6$  was added to the  $CO_2$  gas throughout most of the duration of the Proof of Concept test. Concentrations of dissolved  $SF_6$  (in  $\mu g/L$ ) are listed Table 4-7.  $SF_6$  concentrations were detected in all wells. In addition, two sets of "direct sparge" samples were prepared by bubbling the  $CO_2/SF_6$  mixture into VOA vials. These samples had 44.1 and 39.8  $\mu g/L$  of  $SF_6$  respectively.

Table 4-7: SF<sub>6</sub> Tracer Concentrations at Conclusion of Test

	Well $SF_6 (\mu g/L)$		Maximum Pressure During	Maximum Pressure During		
			Sparging into SW-1 (psi)	Sparging into MW-1C (psi)		
	MW-1A	8.8	9	8		
Shallow	MW-2A	26.2	2	-		
Shal	MW-3A	3.8	8	6		
	MW-115A	0.49	-	-		
ate	MW-1B	0.62	16	16		
Intermediate	MW-2B	104	16	-		
erm	MW-115B	12.7	-	-		
Int	MW-519A	0.70	16	16		
	MW-115C	61.6	-	-		
	MW-1C	10.0	-	N/A		
eb	MW-2C	104	-	-		
Deep	MW-519B	133	-	-		
	MW-517B	3.4	-	-		
	SW-1	0.77	N/A	N/A <sup>6</sup>		

The purpose of adding  $SF_6$  throughout the test was to determine where the injected gas travelled throughout the test.  $SF_6$  is commonly used as a tracer for sparging studies because it does not occur naturally and background concentrations are extremely low. For example surface waters in equilibrium with current atmospheric  $SF_6$  levels (6.9 pptv) have approximately 0.24 ng/L of dissolved  $SF_6$ . Also  $SF_6$  can be detected at extremely low concentrations in water and is not biodegradable, so it acts as a conservative tracer to show where the injected gas was delivered.

The concentrations of SF<sub>6</sub> present in a monitoring water during sparging are a function of the CO<sub>2</sub>/SF<sub>6</sub> ratio in the gas mixture, the effectiveness of mass transfer to the water as gas channels travel thorough the aquifer, and additional advective or dispersive mass transfer through groundwater that does

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<sup>&</sup>lt;sup>6</sup> Prior to sparging into MW-1C, SW-1 was converted to a monitoring well by installing a well extension as described in Section 3.3.2. However, the well casing became unsealed during installation. As a result there was visible gas escaping from the well pack once sparging started. A packer was placed inside the well to prevent CO<sub>2</sub> gas from escaping. This prevented a measurement of pressure in the well during sparging into MW-1C.

not directly contact gas channels. Slight changes in the  $CO_2/SF_6$  ratio can result in uneven delivery of  $SF_6$  to the aquifer. As such, it is best to interpret  $SF_6$  tracer concentrations based on whether they have the same order of magnitude. The direct sparge of the  $CO_2/SF_6$  gas yielded concentrations of approximately  $40~\mu g/L$ . Thus, concentrations greater than  $4~\mu g/L$  are a good indication that the injected gas has either directly travelled through the area, or close enough such that advective and dispersive transport would impart very high concentrations of  $SF_6$ .

Within the deep Satilla, all wells with the exception of SW-1 and MW-517B showed concentrations greater than 4  $\mu$ g/L. This indicates that the injected gas reached all of the deep Satilla monitoring wells that are within 35 ft of the two sparge wells. Even MW-115C, which only saw a slight lowering of pH at the end of the test, showed high SF<sub>6</sub> concentrations. This indicates that the injected gas (CO<sub>2</sub> and SF<sub>6</sub>) was in fact reaching MW-115C. However, the mass flow of CO<sub>2</sub> to this area was not sufficient to satisfy the acid demand.

Water from MW-517B contained 3.4  $\mu$ g/L of SF<sub>6</sub> and is approximately 100 ft away from SW-1 and MW-1C. Recall that MW-517A directly intercepted CO<sub>2</sub> gas channels during sparging into MW-1C. MW-517A is in the same location as MW-517B, but is screened approximately 15 ft higher. There was no evidence (pressure buildup or rapid pH decreased) that MW-517B directly intercepted gas channels during sparging. The appearance of SF<sub>6</sub> at MW-517B is likely the result of advective or diffusive transport of aqueous SF<sub>6</sub> from nearby areas that were in direct contact with the injected gas.

It is surprising that the sparge well, SW-1, had lower concentrations of  $SF_6$  than the other deep Satilla wells. Also, many intermediate and shallow wells which showed large pH decreases had lower than expected  $SF_6$  concentrations. For example, MW-1B showed a large decrease in pH from 8.67 to 6.09 after sparging. This indicates that this well was clearly influenced by the  $CO_2$  sparging program. Large  $SF_6$  concentrations would be expected in this well, but the concentration was only  $0.62~\mu g/L$ .

There appears to be a relationship between the occurrences of pressure in monitoring wells and lower than expected SF<sub>6</sub> concentrations. Table 4-7 shows pressure measurements that were recorded during sparging. Wells such as SW-1 and MW-1B were pressurized throughout the entire Proof of Concept test. Escape of SF<sub>6</sub> via off-gassing or volatilization prior to sample collection may have caused some loss of SF<sub>6</sub>.

#### 4.6. Pre- and Post-Sparging Aquifer Test Results

The principal objective of the pre-sparging and post-sparging aquifer testing was to determine the extent to which the CO<sub>2</sub> sparging and the associated lowering of pH may have reduced aquifer transmissivity through solids precipitation, particularly precipitation of silica gel. Aquifer testing was considered the best way to assess this possible occurrence since aquifer testing measures the transmissivity and hydraulic conductivity of the entire zone of influence of the CO<sub>2</sub> sparging test and, ultimately as the test continues, around the periphery of the test zone. In contrast, slug testing of individual wells only measures the hydraulic conductivity in the immediate vicinity of the well screens.

#### 4.6.1. Technical Approach to Aquifer Test Analysis

The following observations related to the hydrogeology of the site and the aquifer test serve as an important context for the technical approach to the aquifer test analyses described subsequently:

- 1. The Satilla formation in this area consists of fine- to medium-grained sand. The aquifer generally grades downward toward coarser-grained and more permeable deposits at its base, except for a discontinuous layer of clay and interbedded sand and clay that lies at the base of the formation.
- 2. The aquifer is underlain by the variably cemented sandstone, which in conjunction with the discontinuous clay, acts as a low permeability aquitard, defining the base of the aquifer.
- 3. The aquifer behaves as an unconfined aquifer. As is typically the case in unconfined aquifers, the aquifer test exhibits three phases—an early-time phase when the basal portion of the aquifer behaves much like a confined or semi-confined aquifer with rapid drawdown and low storativity, a second phase dominated by delayed gravity drainage from the upper portion of the aquifer during which further drawdown diminishes or ceases altogether, and then a third phase when drawdown begins anew as the aquifer begins to dewater. The first two phases are well-represented in this test, while the third phase is just beginning at the conclusion of the test.

The Satilla formation is both unconfined and the extraction well, SW-1, is partially-penetrating; that is, it penetrates only the basal portion of the saturated thickness of the aquifer. This dictates that care must be taken in selection of wells for aquifer test analysis and in the methodology used to analyze the data from those wells. First, observation wells must be selected that are in the specific stratigraphic interval being pumped by the extraction well. Wells overlying or underlying the pumped stratigraphic interval will exhibit less drawdown and when subject to conventional aquifer test methodologies, such as the Theis (1935) or Neuman (1972) methods, will yield unreliable results. Neuman, who developed a complete analytical solution for unconfined aquifers (1972), recommends that if the primary objective of the aquifer test of an unconfined aquifer is determination of the transmissivity of the pumped interval of the aquifer (as is the case here), three things should be done:

- 1. Drawdown should be measured in wells sufficiently close to the extraction well such that significant drawdown is observed before the onset of delayed gravity drainage,
- 2. Only early-time data, before significant delayed gravity drainage begins, should be analyzed, and
- 3. This early-time data should be analyzed by means of the Theis Method or the straight line Cooper-Jacob Method.

Therefore, we have selected four wells that are in the principal stratigraphic zone being pumped, are sufficiently close to the extraction well, and exhibit significant drawdown before the onset of delayed gravity drainage. These wells include MW-2C, MW-115C, MW-519B, and MW-517B.

The presence of a residual saturation of CO<sub>2</sub> gas in the aquifer following the CO<sub>2</sub> sparging complicates analysis of the post-sparging aquifer test. The CO<sub>2</sub> residual saturation has the effect of lowering the aquifer transmissivity and raising the aquifer storativity. This complication is addressed by a comparative analysis of calculated transmissivity using the DeGlee distance-drawdown method (DeGlee, 1930; DeGlee, 1951) using drawdown data from the conclusion of the aquifer test when the impacts of storativity are reduced. It is also addressed by deriving a new storativity term that incorporates the effects of CO<sub>2</sub> gas expansion on aquifer storativity. This allows us to "fit" calculated drawdown values to the observed data using the transmissivity value calculated by the DeGlee method and to calculate CO<sub>2</sub> residual saturations.

# 4.6.2. Aquifer Test Interpretation

In this section of the report, we describe the interpretation of the aquifer test data. This interpretation includes calculation of any barometric or tidal efficiencies of observation wells and calculation of pre-aquifer test water level trends. These calculated parameters were then used to adjust the observed aquifer test drawdown data, as necessary, to account for tidal fluctuations and variations in barometric pressure during the aquifer test or for any pre-aquifer test trends in water levels.

# 4.6.3. Pre-Processing of Aquifer Test Data

Hydrographs for all of the observation wells are found in Appendix C. These hydrographs show the water level in each observation well during the antecedent, aquifer test, and recovery periods. The hydrographs are annotated to show the start of the yield test, the start and conclusion of the aquifer test pumping period, and the temporary pump shut down for refueling of the generator. The graphs also show a calculation of the generally downward trend in aquifer water levels occurring between the start of the aquifer test and the conclusion of the recovery period. This trend was used to correct drawdown values to what they would have been had there been no trend in aquifer water levels during the test. Barometric pressure was virtually constant during the aquifer test and, therefore, no corrections to drawdown values were necessary to compensate for barometric pressure changes. The wells did not exhibit significant tidal-induced water level fluctuations, so no adjustments to the data were necessary to account for tidal fluctuations in Purvis Creek or the Turtle River.

# 4.6.4. Pre-Sparging Aquifer Test Analysis

Four wells were initially selected for early-time, Cooper-Jacob analysis. These wells were MW-2C, MW-115B, MW-519B, and MW-517B. These four wells are all in the stratigraphic interval being pumped by SW-1 and are at sufficiently close distances to SW-1 to minimize the effects of delayed gravity drainage on the early-time data. The results of the early-time Cooper-Jacob analyses are presented in Table 4-8. The Cooper-Jacob straight-line fits and calculations are illustrated in Figures 4-18 through 4-21. The transmissivity calculated from these four observation wells varied from 1,200 to 1,900 gallons per day per foot (gpd/ft). As shown in Table 4-8, the mean value of transmissivity calculated from the four Cooper-Jacob analyses of early-time data is 1,325 gpd/ft (177 ft²/day). The mean storativity is  $1.4 \times 10^{-3}$ .

Table 4-8: Summary of Time Drawdown Aquifer Test Analyses

Well	Transmissivity (gpd/ft)	Storativity (dimensionless)
MW-2C	1,150	$2.8 \times 10^{-3}$
MW-115C	1,150	$1.6 \times 10^{-3}$
MW-519B	1,150	9.6×10 <sup>-4</sup>
MW-517B	1,825	1.9×10 <sup>-4</sup>
Mean	1,325 gpd/ft	1.4×10 <sup>-3</sup>

In calculating the unit properties of the aquifer; that is, the hydraulic conductivity and the specific storage, it is important to understand the vertical thickness of the hydrostratigraphic zone being pumped. In this case, because the vertical thickness of the principal stratigraphic zone expands during the course of the aquifer test, it is important to understand the thickness of the hydrostratigraphic zone during the early-time

interval (i.e. the first 10 minutes or so) that has been analyzed by the Cooper-Jacob Method. Figure 4-22 shows a generally ENW to ESE cross section through the test zone showing drawdown contours after ten minutes of pumping. It can be seen that after 10 minutes of pumping, the principal hydrostratigraphic zone being influenced is approximately 20 feet in thickness. Therefore, for the purposes of calculating hydraulic conductivity and specific storage, an early-time, 20-foot vertical thickness of the aquifer is employed. Using this early-time vertical thickness, the mean hydraulic conductivity derived from the early-time, Cooper-Jacob analysis is 66 gpd/ft<sup>2</sup> (8.9 feet per day). Dividing the mean storativity of  $1.4 \times 10^{-3}$  by this same early-time vertical thickness of 20 feet yields a specific storage of  $7.0 \times 10^{-5}$  ft<sup>-1</sup>. This value of specific storage is consistent with values commonly found in medium dense sands (Batu, 1998).

## 4.6.5. Post-Sparging Aquifer Test Analysis

The most striking observation made relative to the post-sparging aquifer test data is the markedly smaller amounts of drawdown observed in the CO<sub>2</sub> sparging test zone after 10 minutes of pumping as compared to the pre-sparging test. Even though the two tests were run at the same pumping rate, after 10 minutes of pumping, there is very nearly 1/10th as much drawdown in the post-sparging test as there was in the earlier, pre-sparging aquifer test. This observation is illustrated in Figure 4-23, which shows contours of drawdown at 10 minutes for both the pre-sparging aquifer test (in red) and the post-sparging aquifer test (in blue). Where at the same time in the pre-sparging test there was nearly 2.0 feet of drawdown, there is now 0.2 feet. Where there was 1.0 feet of drawdown, there is now approximately 0.1 feet. This can only be attributable to a large *increase* in the storativity of the aquifer in this region of the aquifer. The cause of this is the residual saturation of CO<sub>2</sub> within the proof of concept test zone of influence. The disparity between pre- and post-sparging drawdown diminishes, but is never completely eliminated over the course of the 24-hour aquifer test. Figures 4-24 and 4-25 depict pre- and post-sparging contours of drawdown at times of 100 and 1000 minutes, respectively. As the post-sparging aquifer test approaches steady-state conditions, storativity becomes less of a dominant factor and the tests come into closer alignment with each other.

CO<sub>2</sub> gas within the aquifer test cone of influence increases the aquifer's storativity because it expands in response to declines in hydraulic head (i.e. drawdown) produced by the aquifer test. As it expands, it increases its partial saturation of the pore spaces at the expense of water. It does so because CO<sub>2</sub>, being a gas, expands far more in response to changes in pressure than water, which is very nearly incompressible. The result is an increase in the percent saturation of CO<sub>2</sub> gas and a release of water from storage in the aquifer.

The CO<sub>2</sub> gas also *decreases* the transmissivity of the aquifer as the gas occupies pore spaces that would otherwise be occupied by groundwater and be available for groundwater flow. Moreover, capillary behavior dictates that the non-wetting fluid, in this case, CO<sub>2</sub>, will tend to preferentially migrate through and occupy as a residual saturation the larger pore spaces within the porous media. Those are the same pore spaces that groundwater can more easily flow through. Consequently, reductions in transmissivity resulting from increasing saturation of a non-wetting fluid are not proportional to the decrease in fractional water saturation. A typical relative permeability graph for two immiscible fluids in a porous medium is illustrated in Figure 4-26.

The top and bottom axes of the graph are saturation of the non-wetting fluid  $(S_{nw})$  and saturation of the wetting fluid  $(S_w)$ , respectively. The left axis is relative permeability  $(k_r)$  of either the wetting fluid (water) marked  $(k_{rw})$  or the non-wetting fluid (in this case,  $CO_2$  gas) marked  $(k_{rnw})$ . The figure has been

further annotated in red to illustrate that at a water saturation ( $S_w$ ) of 0.75 (a 25% reduction in water saturation), the permeability of the formation for water flow has been disproportionately reduced by more than 50%. This is typical and reflects the fact that saturation of non-wetting fluids (like  $CO_2$  in a groundwater system) tends to begin in and expand outward from the larger-diameter, more permeable, pore spaces. As the  $CO_2$  gas dissolves into the groundwater over time, the residual saturation of  $CO_2$  will decline to zero and those vacated pore spaces will be re-occupied by groundwater.

The CO<sub>2</sub> gas-related increase in storativity makes interpretation by time-drawdown techniques, like the early-time, Cooper-Jacob analysis of the pre-sparging aquifer test difficult for the following reasons:

- The amount of gas expansion is not linearly related to the amount of drawdown, but is a function
  of both the total hydraulic head, including barometric pressure, and the drawdown in hydraulic
  head.
- 2. The gas is not omnipresent or uniformly distributed in the aquifer, consequently the storativity associated with gas expansion is not a uniform property of the aquifer.

The non-linearity of the CO<sub>2</sub>-induced storativity makes direct curve fitting to the early-time drawdown of the post-sparging aquifer test inappropriate. Fitting a straight line to any of the semi-logarithmic plots of early-time drawdown, as was done without issue in the pre-sparging test, produces a calculated transmissivity *greater* than in the pre-sparge aquifer test—a result that is clearly in error. Recognizing this problem, a distance-drawdown technique is used to estimate the post-sparging decline in transmissivity.

In a confined aquifer, distance-drawdown analyses can be performed using the distance-drawdown, Cooper-Jacob methodology (Cooper and Jacob, 1946). In this methodology, drawdown is plotted on a semi-logarithmic graph, with drawdown on the Cartesian scale and distance from the pumping well plotted on a logarithmic scale. Plotted in this manner, drawdown data (except for early-time data) generally plot as a straight line and transmissivity can be calculated based upon the slope of that line. However, in an unconfined aquifer, such as this one, steady-state (or near steady-state) drawdowns similarly plotted semi-logarithmically, do not form a straight line. Instead, drawdown in the outlying portions of the cone of influence is reduced due to delayed gravity drainage from the upper portion of the aquifer.

DeGlee developed a distance-drawdown methodology for analyzing drawdowns in semi-confined aquifers (DeGlee, 1930; DeGlee, 1951; Anonymous, 1964). The methodology involves a log-log plotting of drawdown and associated distances from the pumping well and matching those drawdowns to a type curve (referred to herein as the DeGlee type curve). This methodology can be used to obtain an approximate transmissivity of an unconfined aquifer during delayed gravity drainage since delayed gravity drainage is similar to the leakage through an overlying aquitard. A DeGlee Method analysis of the drawdowns at the conclusion of the pre- and post-sparging aquifer test is presented as Figure 4-27. Only wells MW-2C, MW-115C. and MW-519B are used in this analysis as only these wells pass the DeGlee method criterion that "u" be less than 0.01. In Figure 4-27, each data point is annotated to indicate the particular observation well represented by that data point. As can be seen in Figure 4-27, the slope of the post-sparging data points is considerably steeper than the pre-sparging data points indicating that the transmissivity is lower in the post-sparging test. The DeGlee method, although an approximate method under these circumstances, yields a pre-sparge transmissivity of 1,800 gpd/ft, which comports fairly well with the mean transmissivity of 1,325 gpd/ft calculated from the time-drawdown, Cooper-Jacob method.

In contrast to the pre-sparging data, the DeGlee method analysis of the post-sparging aquifer test data yields a transmissivity of 450 gpd/ft. This indicates that the aquifer transmissivity has been reduced by about 66%. It is believed that this diminution of transmissivity is principally the result of CO<sub>2</sub> residual saturation in the aquifer. As was discussed earlier in this report, the amount of silica in the groundwater is not believed to be sufficient to cause much clogging of the aquifer. Also, the degree of residual saturation of CO<sub>2</sub> gas in the proof of concept test zone of influence is quite substantial and could easily account for the measured decline in transmissivity. We'll look at this more closely in the following section.

## 4.6.6. Estimating the Residual Saturation of CO<sub>2</sub> in the Sparge Test Zone of influence

As described above, the presence of a residual saturation of CO<sub>2</sub> gas in the Satilla formation increases the overall storativity of the aquifer. The impact of the gas-related storativity is particularly evident in the early-time drawdown in the unconfined aquifer before actual pore space dewatering (i.e. specific yield) begins to occur later in the aquifer test. This is because during early-time behavior, storativity is normally limited to the effects of aquifer compression and water expansion, both of which are small in magnitude compared to specific yield. However, with a partial gas saturation in the formation, a third storativity term comes into play—gas expansion. As drawdown begins in the aquifer from the aquifer test pumping, pressure heads are accordingly reduced. This reduction in pressure head produces a concomitant reduction in gas pressure. This reduction in gas pressure, in turn, causes the gas to expand, releasing water from storage in the aquifer. In other words, as the gas expands, it increases its degree of saturation of the pore spaces and correspondingly reduces the degree of water saturation. Let's look at this phenomenon more quantitatively.

The Ideal Gas Law (Mortimer, 1967) states the following:

$$PV = nRT (4-15)$$

Where: P

P = pressure V = volume

n = number of moles of gas

R = constantT = temperature

Solving for the volume, V, we see that if all other terms remain equal, the volume of gas is inversely proportional to the pressure.

$$V = \frac{nRT}{P} \tag{4-16}$$

Consider for example, the post-sparging aquifer test that produced after 10 minutes of pumping approximately 0.2 feet of drawdown in the area within about 20 feet of the sparge well as shown in Figure 4-23. A 0.2 feet drop in total head (pressure head and atmospheric pressure) from a starting total head of 78 feet represents a 0.26 % drop in pressure (0.2/78 = 0.0026 = 0.26%). This would produce a corresponding expansion in the gas of 0.26% if we assume the gas temperature remains constant. If we assume for the moment that all the water released from storage during the first 10 minutes of the post-sparge aquifer test came from this one mechanism of gas expansion (we will see later that this is a reasonable assumption),

then it is possible to estimate how much gas is present in that area within 20 feet laterally of the sparge well.

The amount of water pumped (and thereby removed from storage) during the first ten minutes of the post-sparge aquifer test was 72 gallons (7.2 gpm times 10 minutes) or 9.63 cubic feet. The area of aquifer affected during the first 10 minutes of the test was an approximate cylinder of radius, 20 feet, and a height of 20 feet (See Figure 4-23). The volume of affected aquifer can simply be calculated using the equation of a cylinder:

$$V_{aa} = \pi r^2 d \tag{4-17}$$

Where:  $V_{aq} = Volume of aquifer$ 

r = radius of cylinder d = height of cylinder

The volume of affected aquifer is calculated to be:

$$V_{aa} = \pi (20 \text{ ft})^2 (20 \text{ ft}) = 25,132 \text{ ft}^3$$
 (4-18)

The volume of groundwater within that region can be calculated by multiplying the total volume of the aquifer by the approximate porosity of 0.35:

$$V_{gw} = 25,132 \text{ ft}^3(0.35) = 8,796 \text{ ft}^3$$
 (4-19)

If we assume that all of the water released from storage in the aquifer came from gas expansion, then gas expansion would equal the amount of water pumped from the aquifer during the first 10 minutes of the test or 72 gallons (9.63 cubic feet). The initial volume of gas in the affected area can then be calculated by dividing the volume of gas expansion by the fractional expansion as follows:

Initial Volume of gas = 
$$\frac{\text{Expansion Volume}}{\text{Fractional Expansion}} = \frac{9.63 \text{ feet}^3}{0.0026} = 3,700 \text{ ft}^3$$
 (4-20)

Comparing the calculated initial volume of gas to the total volume of all pore spaces in the affected region, we can calculate that the residual saturation of CO<sub>2</sub> gas in the affected region is approximately 0.42 (3,700 ft<sup>3</sup> of gas/8,796 ft<sup>3</sup> of total pore spaces). This value comports well with the findings of Lundegard and LaBrecque (1995) for air sparging in fine-grained dune sand. They measured 30 to 40% air saturation in the pore spaces 41 hours after cessation of sparging. It is also interesting that if you look at the typical relative permeability graph presented in Figure 4-26, a non-wetting fluid saturation of 0.42 (0.58 water saturation), corresponds to a roughly 75% decline in aqueous phase permeability, which is the decline measured by the DeGlee distance-drawdown method. Even though the graph in Figure 4-26 was not developed using sand from the Satilla formation, it is nonetheless generally representative of the behavior of sands.

The validity of the assumption that nearly all the water removed from storage during the first 10 minutes of the post-sparging aquifer test was attributable to  $CO_2$  gas expansion can be demonstrated by calculating the amount of water released from storage by the two conventional mechanisms of early-time unconfined aquifer test storativity—aquifer compression and water expansion. The combined storativity produced by these two mechanisms was calculated in the pre-sparging aquifer test to be  $1.4 \times 10^{-3}$ . Dividing

this early-time storativity by the early-time thickness of the aquifer affected by the pumping, 20 feet, yields a specific storage of  $7.0 \times 10^{-5}$  ft<sup>-1</sup>. We can then multiply the total affected area of the aquifer at 10 minutes by this storativity and the approximate average drawdown of 0.2 feet to get the volume of water released from storage by the conventional storativity mechanisms (V<sub>s</sub>), as follows:

$$V_S = Aquifer Volume \times Specific Storage \times Drawdown$$
 (4-21)

$$V_S = 25,132 \text{ ft}^3 \times 7.0 \text{x} 10^{-5} \text{ ft}^{-1} \times 0.2 \text{ feet}$$
 (4-22)

$$V_S = 0.35 \text{ ft}^3$$
 (4-23)

This volume of water represents only 3.6% of the total volume of water released from storage during the first 10 minutes of the post-sparging aquifer test indicating that our original assumption that nearly all the storativity was associated with CO<sub>2</sub> gas expansion was reasonable.

Another means to estimate the residual saturation of CO<sub>2</sub> gas in the proof of concept test zone of influence is by attempting to reproduce the early-time drawdown data measured in the post-sparging aquifer test. This can be done using the Theis equation, the above-calculated post-sparging transmissivity, and a storativity term that incorporates the additional storativity created by the presence of the CO<sub>2</sub> gas residual saturation. The storativity of a confined, semi-confined, or an unconfined aquifer during early-time behavior (before the onset of delayed gravity drainage) is attributable to two mechanisms—aquifer compression and water expansion. The equation for conventional storativity attributable to these two mechanisms is given by Walton (1970):

$$S = \overbrace{\eta \gamma m \beta}^{\text{water expansion}} + \alpha \gamma m \tag{4-24}$$

Where: S = Storativity

 $\eta = porosity$ 

 $\gamma$  = unit weight of water

m = aquifer thickness

 $\beta$  = water compressibility

 $\alpha$  = aguifer compressibility

We can derive an expanded storativity equation to take into account the impact of CO<sub>2</sub> gas expansion on aquifer storativity. The derivation is based upon the Ideal Gas Law and is provided in Appendix G. The expanded storativity equation is given below:

$$S = \overbrace{(1 - s_{CO_2})n\gamma m\beta}^{\text{water expansion}} + \alpha\gamma m + \overbrace{s_{CO_2} \text{ nms}}^{CO_2 \text{ expansion term}} + \overbrace{h_{p, \text{total}}}^{\text{CO_2}}$$
 (4-25)

Where:  $s_{CO2}$  = residual saturation of  $CO_2$ 

s = drawdown

 $h_{p,total}$  = total pressure head including atmospheric pressure

In the above equation, the water expansion term has been modified by changing the total porosity (n) to the water-filled saturation  $(1 - s_{CO2})$ n to properly reflect the fact that  $CO_2$  occupies a portion of the total porosity. However, because the water expansion term is de minimis compared to the  $CO_2$  expansion term, the equation can be simplified by using the total porosity in this term without sacrificing any significant accuracy, as shown below:

$$S = n\gamma m\beta + \alpha\gamma m + \frac{s_{CO_2}nms}{h_{p_{Total}}}$$
 (4-26)

The above equation can be substituted for the conventional storativity (S) in the Theis equation to calculate drawdown in the proof of concept zone of influence under the influence of  $CO_2$  gas residual saturation. However, because drawdown (s) is both the dependent variable and an independent variable, the Theis equation must be solved iteratively. A spreadsheet solution to the Theis equation, with the expanded storativity term, was developed in Excel using the solver function in Excel. A copy of this spreadsheet is available upon request.

The quality of the match is very much dependent upon the CO<sub>2</sub> gas residual saturation. Using the value of post-sparging transmissivity of 450 gpd/ft, calculated by the DeGlee Method, we can estimate the CO<sub>2</sub> residual saturation by fitting the calculated drawdown to the observed drawdown. Figures 4-28 through 4-31 show the drawdown matching and the calculated CO<sub>2</sub> residual saturation. In each case, the calculated CO<sub>2</sub> residual saturation declines with increasing time. This reflects the physical reality that CO<sub>2</sub> saturation decreases with increasing radial distance from the sparge well, especially beyond a radial distance of 20 feet, where most of the pH reduction occurred. Therefore, as the post-sparging aquifer test cone of influence expands, it increasingly encompasses portions of the aquifer, beyond the 20-foot radius of the principal zone of influence of the CO<sub>2</sub> sparging test, that contain progressively less CO<sub>2</sub> residual saturation. The calculated CO<sub>2</sub> residual saturations suggest that in close proximity to the sparge well residual saturations may be as high as 0.3 to 0.5, but rapidly decrease at radial distances beyond the approximately 20-foot radius within which pH declined to circumneutral values.

The findings of the SW-1 pre- and post-sparging aquifer tests are presented in Table 4-9 and can be summarized as follows:

- 1. The Satilla Aquifer behaves as an unconfined aquifer. As with most unconfined aquifers, during pumping it transitions from early-time, confined aquifer behavior, though an intermediate period of near steady-state conditions due to delayed gravity drainage from the upper portion of the aquifer, and finally to a late-time, unconfined aquifer behavior. The transition to unconfined behavior begins after about 1,000 minutes of pumping.
- 2. The basal portion of the aquifer, specifically the lower 20 feet of the aquifer (which roughly corresponds with the high pH, high density CBP waters), had a pre-sparging transmissivity of 1,325 gpd/ft and a mean early-time storativity of 1.4×10<sup>-3</sup>. After the CO<sub>2</sub> sparging, the transmissivity of the basal portion of the aquifer declined by 66% to 450 gpd/ft. This corresponds to a reduction in hydraulic conductivity from 8.9 to 2.4 ft/day.
- 3. The decline in transmissivity and hydraulic conductivity is believed to be principally the result of a residual saturation of  $CO_2$  in aquifer that was estimated to range from 0.1 to 0.5 (10% to 50% of the pore space).

- 4. The presence of a substantial residual saturation of CO<sub>2</sub> gas in the aquifer also increased the storativity of the aquifer due to the drawdown-induced expansion of the CO<sub>2</sub> gas.
- 5. The pre-sparging specific storage of the basal portion of the aquifer is  $7.0 \times 10^{-5}$  ft<sup>-1</sup>, which is consistent with typical values of specific storage of medium-dense sands.

Table 4-9: Summary of the Pre- and Post-Sparging Aquifer Testing Analyses		
Parameter	Analytical Methodology	Results
Pre-Sparging Transmissivity		
of the Basal Satilla Aquifer	Mean of Cooper-Jacob method analysis of	
(Lower 20 feet)	early-time drawdown data	1,325 gpd/ft
Pre-Sparge Transmissivity of		
the basal Satilla Aquifer	DeGlee Method	1,800 gpd/ft
Post-Sparge Transmissivity of		
the basal Satilla Aquifer	DeGlee Method	450 gpd/ft
Early-time storativity of basal	Mean of Cooper-Jacob method analysis of	
Satilla Aquifer	early-time drawdown data	$1.4 \times 10^{-3}$
	Mean transmissivity of basal Satilla	
Mean hydraulic conductivity	aquifer divided by the early-time aquifer	
of basal Satilla Aquifer	thickness of 20 feet	8.9 ft/day
Specific Storage of basal	Early-time storativity divided by the	
Satilla Aquifer	early-time aquifer thickness of 20 feet	$7.0 \times 10^{-5} \text{ft}^{-1}$
CO2 residual saturation in the	Matching early-time drawdown with	
basal portion of the sparge test	Theis Method and modified storativity	
zone of influence	term to account for expansion of CO2 gas	0.1 to 0.5

#### 4.7. Groundwater Mounding

Potentiometric levels in all of the observation wells were monitored by Solinst data loggers during the course of the entire CO<sub>2</sub> sparging Proof of Concept test. As with the pre- and post-sparging aquifer tests, MW-517B was substituted for EW-11. The transducers were generally programmed for 15-minute frequency readings during the Proof of Concept test. For a few days in the middle of the test, the frequency was increased to one minute intervals. As described earlier, a number of monitoring well screens were intercepted by CO<sub>2</sub> gas channels in the subsurface leading to CO<sub>2</sub> escape through the monitoring well. This phenomenon was observed on day one of the test in MW-1B. The escape of CO<sub>2</sub> in MW-1B was accompanied by significant foaming. Thereafter, all observation wells were fitted with special caps that would prevent escape of gas or foam during active sparging, but would also allow withdrawal and replacement of the Hach pH electrodes, as necessary, to check their calibration and to clean them. With these caps in place, once gas channels had intercepted a well screen, pressure readings in that well no longer represented groundwater levels, but rather a combination of groundwater head and pressure head in the well casing. Therefore, in interpreting water level mounding and recession data, we have carefully avoided using those portions of the data impacted by gas pressure build up in the monitoring well casings.

The daily CO<sub>2</sub> sparging during the Proof of Concept test created significant mounding, particularly in the deep, more permeable, stratigraphic zone at the base of the Satilla Formation. Wells screened in the intermediate vertical position within the aquifer experienced less mounding. Wells screened in the shallow

interval, nearer the groundwater table, experienced considerably less mounding during the course of the test. This pattern was observed in all the well clusters and is illustrated in Figure 4-31, which shows the hydrographs of Wells MW-2A, MW-2B, and MW-2C during the first three days of sparging. This time period was chosen because it precedes the time at which a gas channel reached MW-2B and pressurized the well. This figure is generally illustrative of the relative degree of mounding exhibited by the deep Satilla wells, the intermediate Satilla wells, and the upper Satilla wells, although higher levels are reached later in the test. Several aspects of this figure are worth noting:

- 1. In well MW-2C, representing the basal zone of the Satilla formation, piezometric levels rise almost immediately following initiation of sparging and reach a peak about 2 to 2 ½ hours later. This is believed to represent the time during which CO<sub>2</sub> channels are expanding outward through the zone of saturation, displacing water, before ultimately reaching the vadose zone and coming into a quasi-equilibrium state. Thereafter, the mound in piezometric levels created by intrusion of the CO<sub>2</sub> channels begins to slowly decline. Once the sparging is suspended at the end of each day, piezometric levels decline precipitously to levels well below the original static piezometric level. This collapse of the piezometric surface is a common phenomenon in air sparging and occurs as the air (or in this CO<sub>2</sub>) channels collapse and groundwater flows back in to reoccupy those previously air-filled pore spaces (Lundegard and LaBrecque, 1995).
- 2. The intermediate and shallow wells exhibit progressively less mounding much like the vertical extent of drawdown measured in the aquifer testing. The shallow well, MW-2A, nominally representing the groundwater table, shows about one foot of mounding. However, as the test progressed, mounding of the shallow wells increased to two or three feet and routinely brought the water table up to within one foot of the ground surface during active sparging.

The water level data for all of the observation wells is included in Appendix C.

Figure 4-32 shows the maximum level of the piezometric surface during the first day of sparging on November 29, 2012. The piezometric surface in the basal Satilla near the sparge well rose from a static elevation of about 4 to 5 feet above sea level to a level of 11.1 feet above sea level. As depicted in that figure, piezometric level mounding declined with increasing radial distance from the sparge well, but extended out to (and beyond) well MW-517B, which experienced a 3.5 feet rise in the piezometric surface at a distance of over 100 feet from the sparge well. Upon secession of sparging, the piezometric surface declined rapidly to levels well below the original static piezometric surface, as described above. This depression in the piezometric surface at its maximum extent is depicted in Figure 4-33. Near the sparge well, the piezometric surface fell to more than two feet *below* mean sea level and then began a recovery to near static levels before the next day's sparging. This cyclic pattern of mounding, followed by collapsing of the piezometric surface, and then slow recovery, was repeated each day during the Proof of Concept test.

The cyclic mounding had a minimal effect of the migration of the CBP around the periphery of the test site. As shown in Figure 4-34, the hydraulic head difference between MW-519B and MW-517B during the sparge period was 1.8 feet. The distance between the two wells is 90 feet. Therefore, the outward radial hydraulic gradient during the sparge period is about 0.02 (1.8 feet/90 feet). Using the hydraulic conductivity of the basal Satilla measured in the aquifer test of 8.9 feet per day and an effective porosity of 0.25, the average linear groundwater velocity can be calculated as follows:

$$\overline{v} = \frac{Ki}{n_e} \tag{4-27}$$

Where:  $\overline{\mathbf{v}}$  = average linear groundwater velocity

K = hydraulic conductivity

i = hydraulic gradient

 $n_e$  = effective porosity

$$\overline{v} = \frac{8.9 \text{ ft/day } (0.02)}{0.25} = 0.71 \text{ ft/day}$$
 (4-28)

Assuming that this gradient persisted throughout the entire 9 hour and 15 minute sparge period of Day 1 (0.39 days), the outward distance traveled would have been:

Distance traveled = 
$$0.71 \text{ feet/day} \times 0.39 \text{ days} = 0.28 \text{ feet}$$
 (4-29)

As depicted in Figure 4-33, once the sparging ceases, the piezometric mounding collapses into a deep depression. The hydraulic gradient is reversed and groundwater in the basal zone of the Satilla Aquifer flows backward toward the sparge well. The net impact on CBP migration is negligible.

The groundwater table also cyclically rose and fell during cyclic sparging. However, the magnitude of these fluctuations is less than in the intermediate or basal Satilla. The maximum elevation reached by the groundwater table (as defined by the shallow wells) on any date during the sparging test is depicted on Figure 4-34. Water table mounding reaches a peak of greater than nine feet above mean sea level near the sparge well. This means that the groundwater table rose to within one foot of the ground surface near the sparge well.

The monitoring of groundwater levels and the above analysis indicates that the impact of sparging on lateral groundwater migration is quite small. However, the mounding extends laterally more than 50 feet and near the sparge well is sufficient to bring the groundwater table up close to ground surface. This observed behavior has implications for full-scale implementation. It may not be feasible to simultaneously sparge into multiple wells or even two adjacent wells in a single area as the mounds from each well will superimpose upon each other increasing the likelihood of bringing the groundwater table to the surface. This issue would have to be carefully addressed in design of a full-scale CO<sub>2</sub> sparging system.

#### 5. CONCLUSIONS

This Proof of Concept test demonstrated that CO<sub>2</sub> sparging can reduce pH levels in the CBP to circumneutral and concomitantly lower concentrations of mercury and other trace metals such as chromium, arsenic, and vanadium. Furthermore, all of the specific test objectives stated in the Proof of Concept workplan (Section 2) were met, except for completion of long-term, post-sparge rebound monitoring. These monitoring events will occur in February and May of 2013 in accordance with the workplan. The following conclusions can be drawn from the test:

- 1. CO<sub>2</sub> sparging into the Satilla Formation is feasible without the need for fracturing.
- 2. Significant pH reductions from pH 11-12 in the deep Satilla were achievable in 5 to 7 days sparging at circa 50 scfm.
- 3. Hg levels in the high pH CBP fully-impacted by the sparging declined from 110-120  $\mu$ g/L to 11-33  $\mu$ g/L (70 to 90% reductions)
- 4. Limited evidence of silica precipitation was observed in wells within the zone of influence of the sparge test.
- 5. The pH of deep Satilla wells was not lowered to below 6.5 at any point during sparging, which indicates that potential dissolution of the sandstone aquitard is not a risk that would bar use of the CO<sub>2</sub> approach.
- 6. A radius of influence of at least 20 feet was achieved at the top of the CBP and greater than 60 feet at the water table surface.
- 7. Some CO<sub>2</sub> gas channels extended out more than 100 feet from the sparge wells.
- 8. The CO<sub>2</sub> sparging resulted in a significant residual saturation of CO<sub>2</sub> gas in the zone of influence. This CO<sub>2</sub> residual saturation did have the effect of lowering the transmissivity of the Satilla by 66% and substantially increasing the storativity of the aquifer. These impacts are expected to diminish over time as the entrapped CO<sub>2</sub> gas residual saturation dissolves into the surrounding groundwater. The observed residual saturation also provides an opportunity for improvement in process efficiency.
- 9. During sparging, significant mounding of the potentiometric surface was measured, particularly in the deep wells. Less mounding was observed in the intermediate zone and even less in the shallow zone. Nonetheless, during the course of the sparging test the groundwater table did rise to within a foot of the surface within a 20-foot radius of the sparge wells (SW-1 and MW-1C). Also the piezometric surface in the deep zone rose as much as 6.5 feet at MW-517B, which is over 100 feet from the sparge well. Control over mounding and the anticipated superposition of mounding from adjacent sparge wells will be an important factor in design of any full-scale implementation. Seasonal or other fluctuations in the level of the groundwater table will also be a factor in a full-scale implementation.

The Proof of Concept test indicated that CO<sub>2</sub> sparging would be an effective, innovative technology, suitable for full-scale implementation at the site. Observations made during testing further indicate that full-scale implementation of CO<sub>2</sub> sparging be conducted over a multiple-year, sequential effort. The principal drivers for this sequential implementation are:

- Management of groundwater mounding caused by superposition of multiple, closely-spaced sparge wells; and
- Maximization of sparging efficiency to reduce emissions of CO<sub>2</sub>.

Groundwater mounding during full scale implementation is particularly critical as mounding during the Proof of Concept test was substantial. The groundwater table rose to within 1 foot of the ground surface during the testing. This mounding will be exacerbated by superposition of mounding from multiple nearby sparging wells and by seasonal rises of the groundwater table. Moreover, in some areas of the CBP, the water table is even closer to the surface than in the test site. Conducting the implementation over multiple years will allow active sparge wells to be further apart, thereby reducing the superposition of groundwater mounding. The optimal time for sparging is when the groundwater table is at its lowest during the drier summer and early fall months.

The Proof of Concept test results suggest that CO<sub>2</sub> sparge efficiency can be enhanced by a sparge regimen that emphasizes short bursts of sparging (anywhere from ½ to 4 hrs.) followed by relatively lengthy rest periods. The rest periods would allow CO<sub>2</sub> gas residual saturation remaining in the formation to both dissolve and diffuse into the surrounding CBP waters. It is proposed that in the first year of sparging, different sparge regimens be tested in an effort to optimize sparge efficiency. In subsequent years, the optimized sparge regimen would be adopted.

Taking these factors into consideration, it is believed that full scale implementation could be accomplished over approximately three years, with four to five months of sparging during the late summer and early fall followed by a seven- to eight-month period of relaxation of sparging. During the relaxation period, data collected from the site would be analyzed using a three-dimensional visualization program. These analyses would permit planning of the next year of the sparge program.

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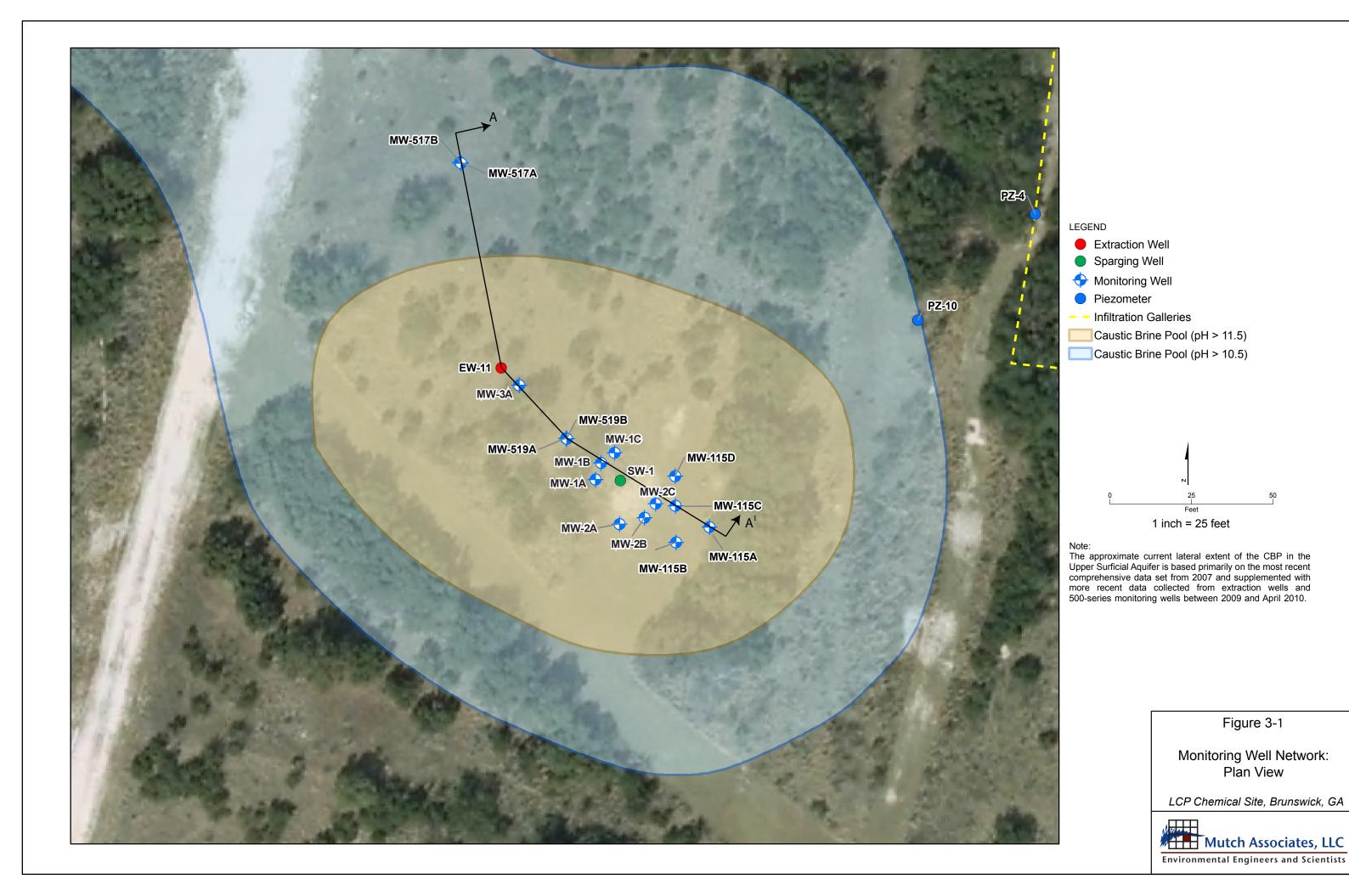
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# **FIGURES**



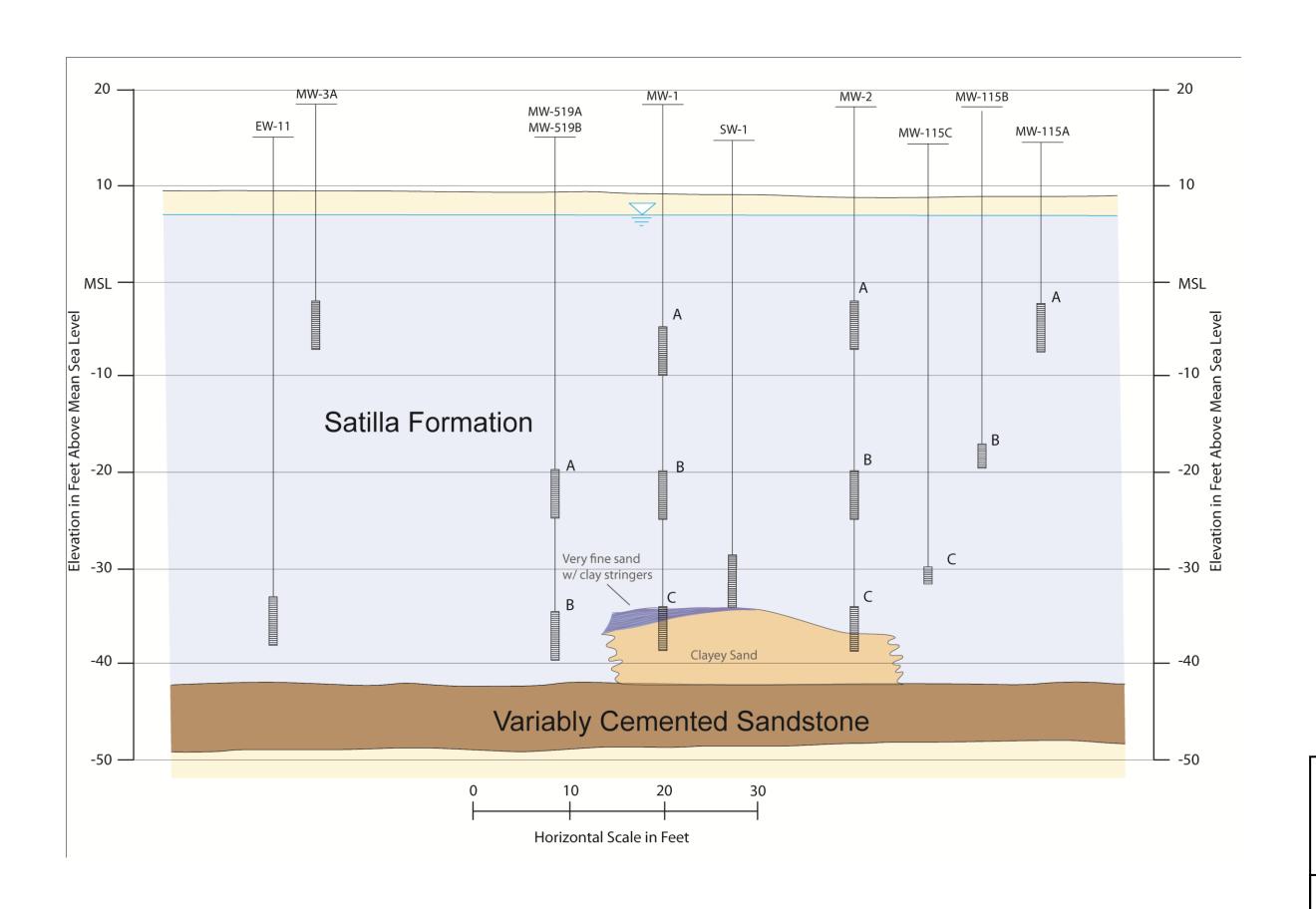
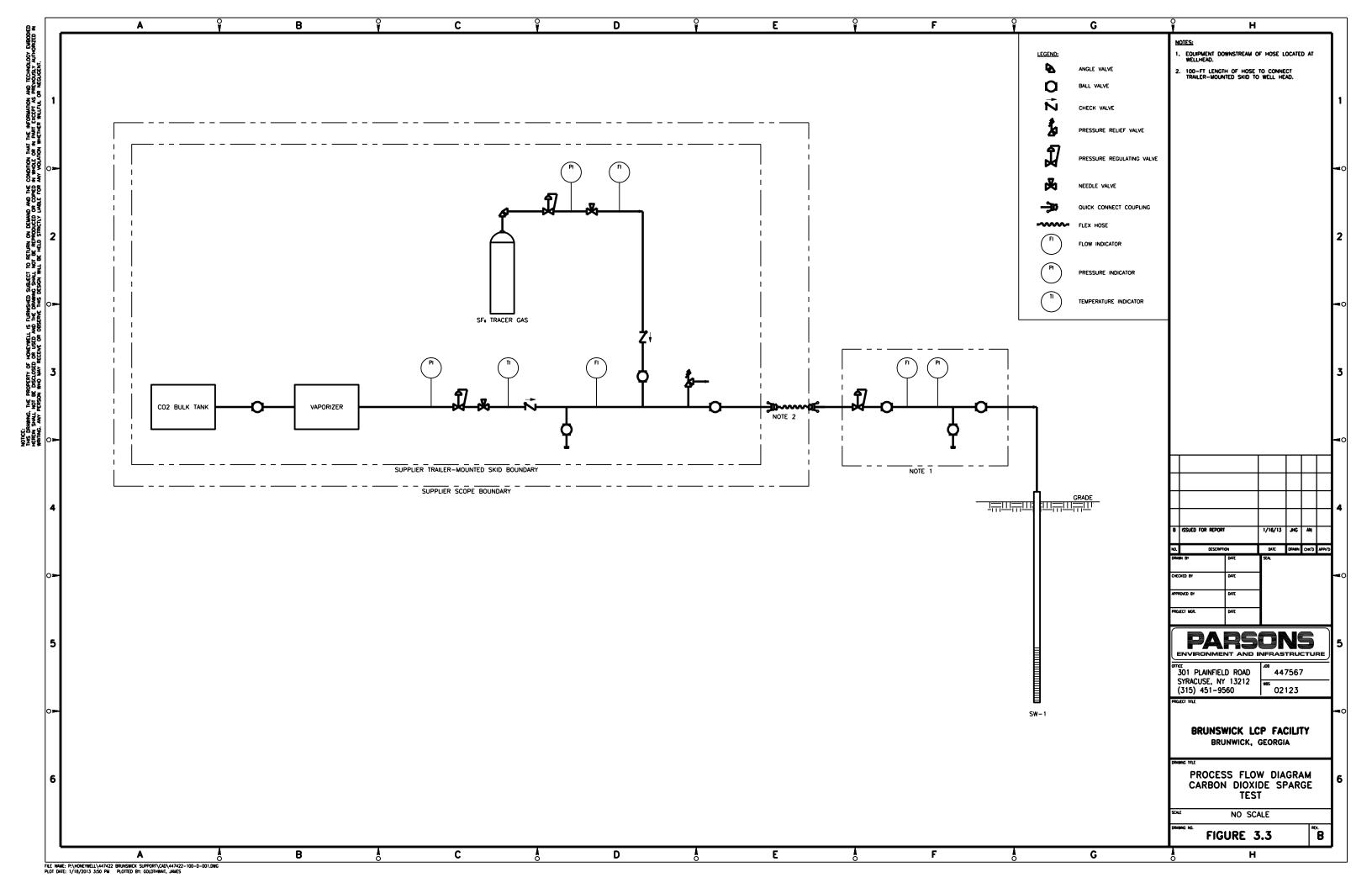


Figure 3-2

Monitoring Well Network: Cross Section A-A'







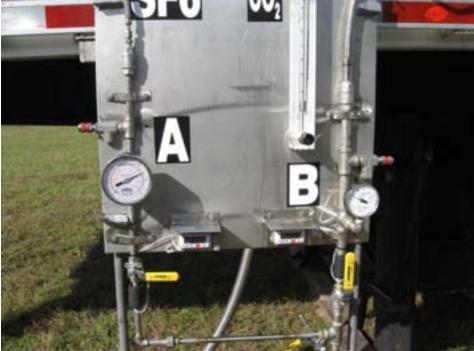


Figure 3-4

CO<sub>2</sub> Trailer and Control Panel





Figure 3-5
Sparge Well Setup (SW-1)





Figure 3-6

Monitoring Well Network With Well Extensions



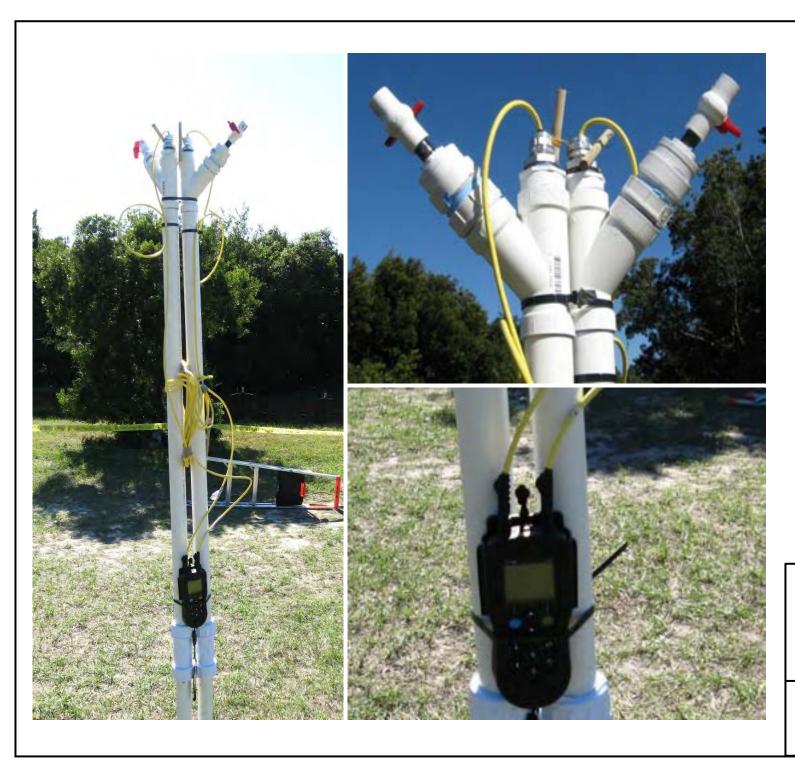
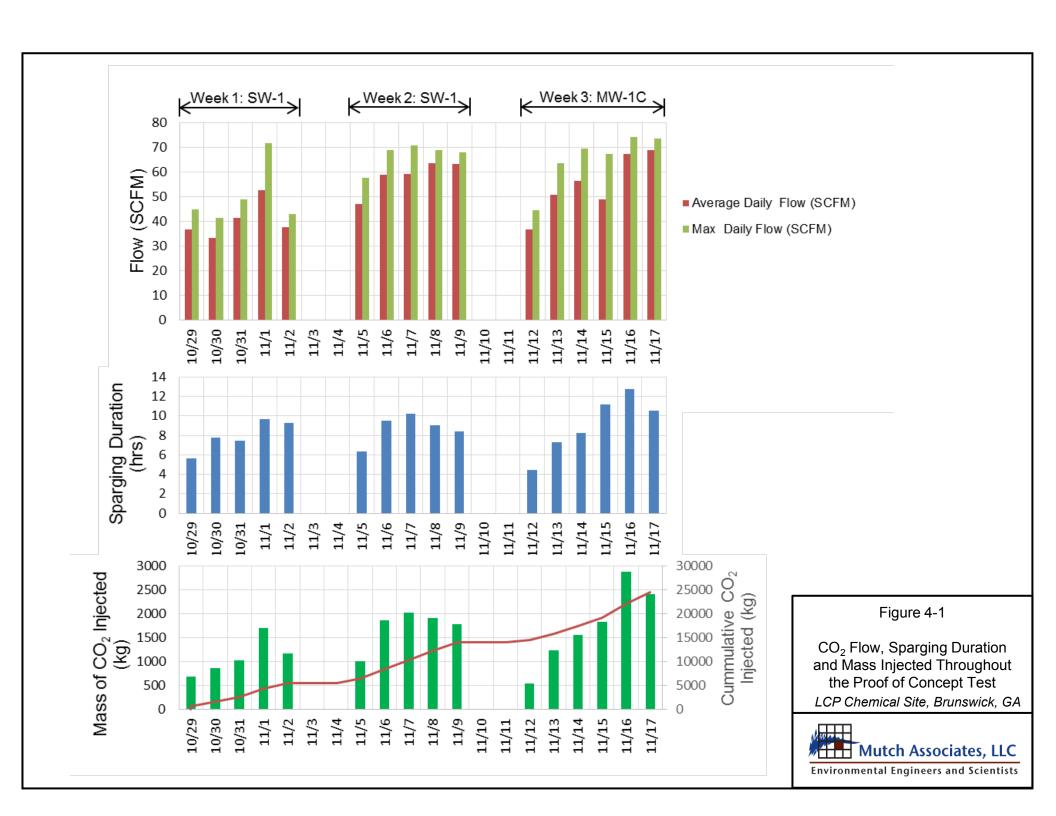
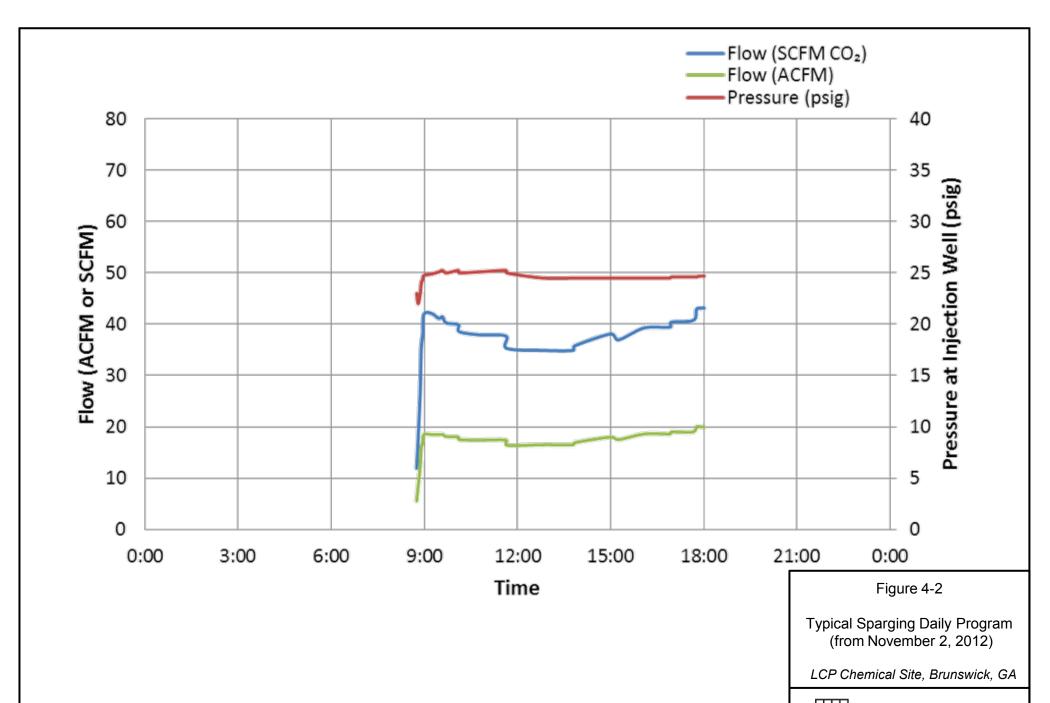


Figure 3-7

Monitoring Well Components Of MW-519A and MW-519B







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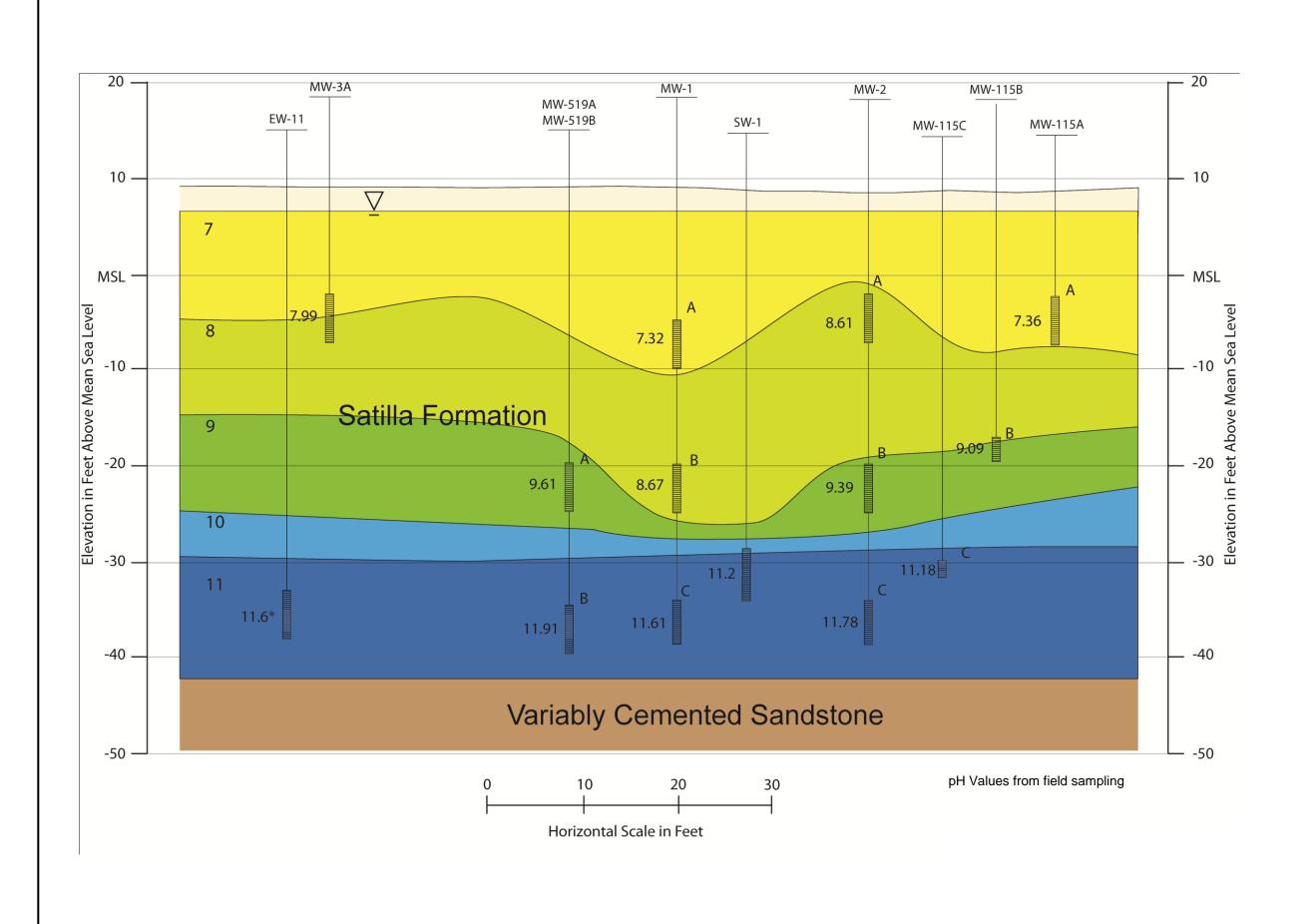
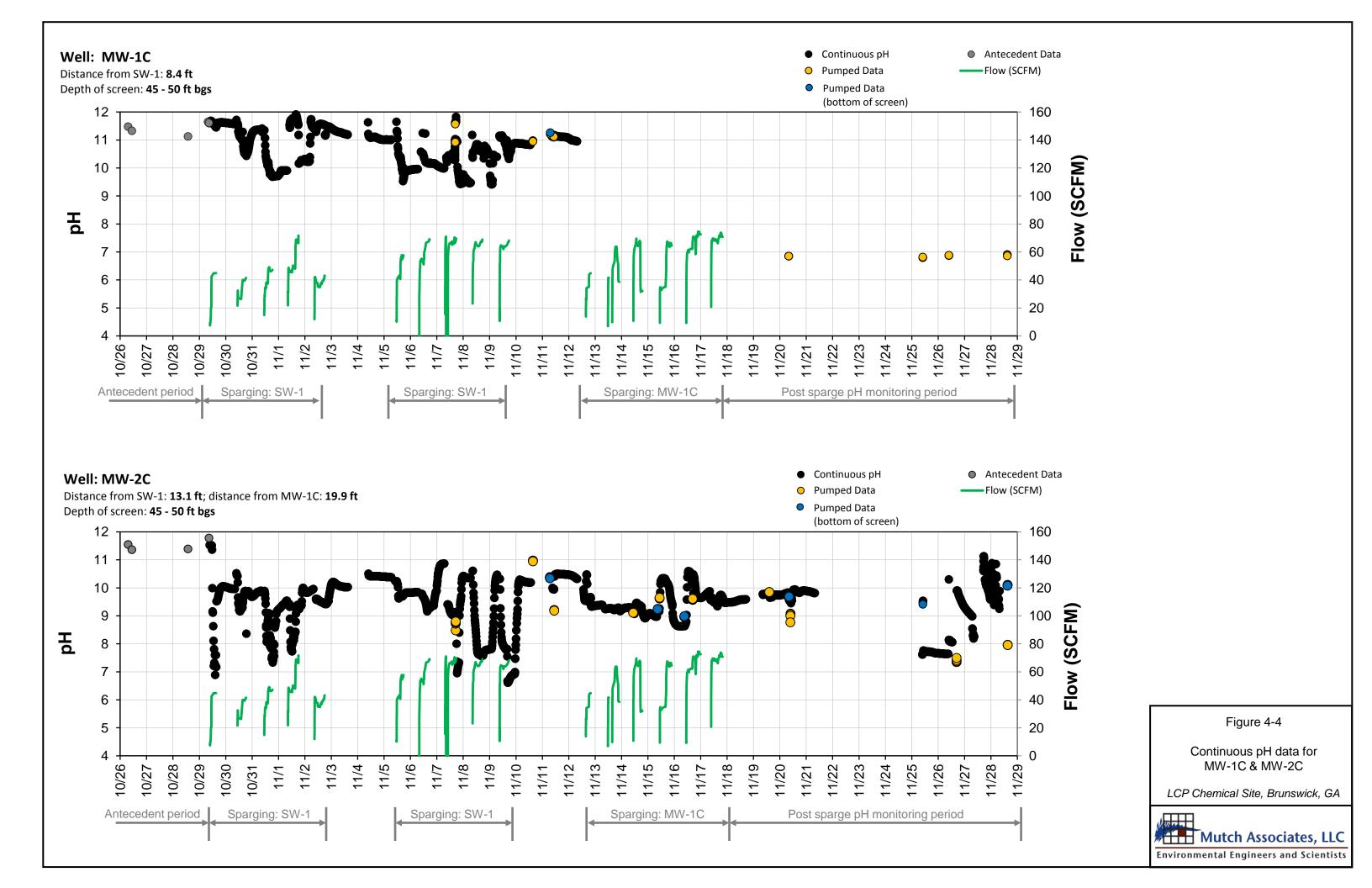
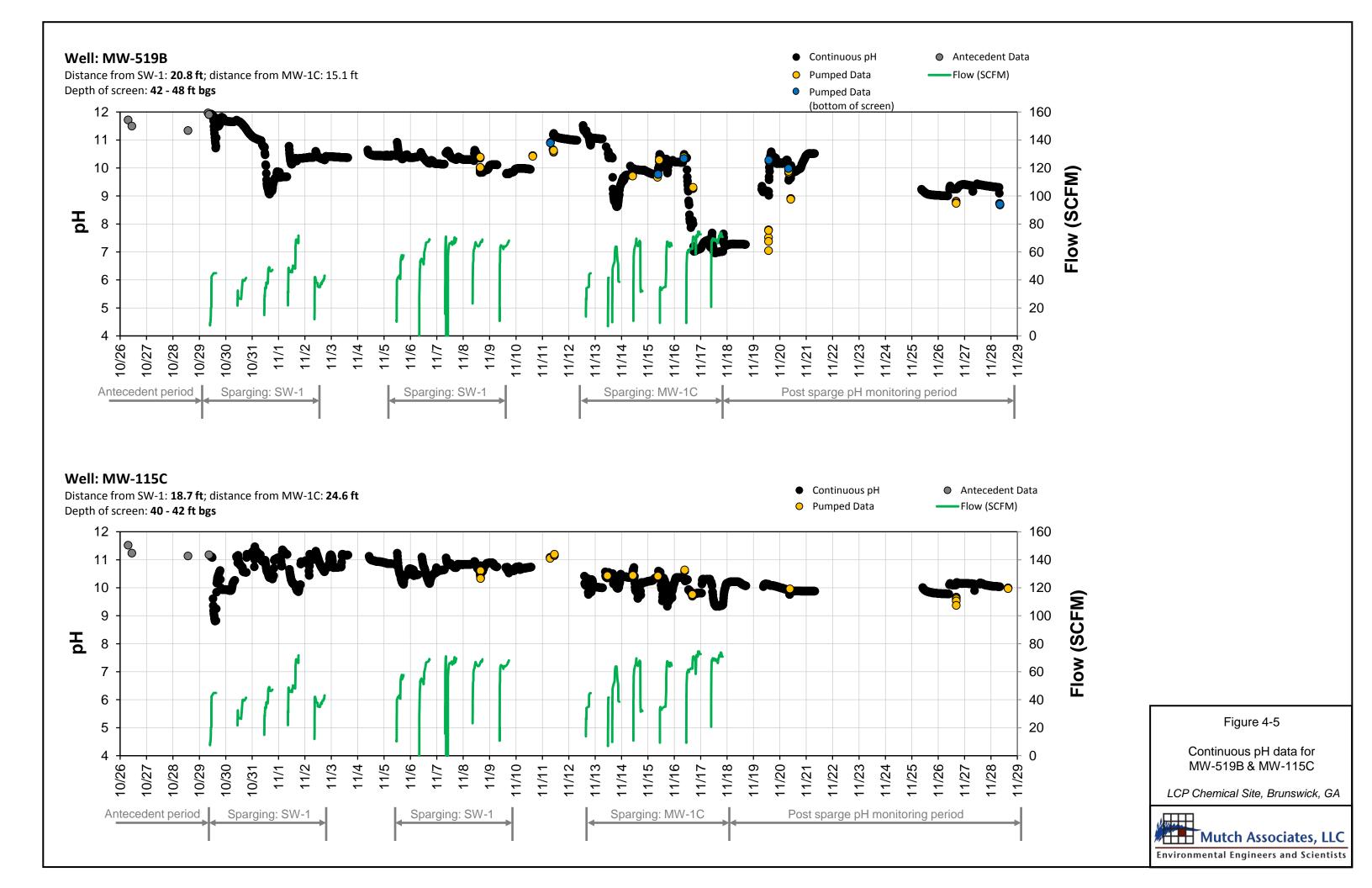


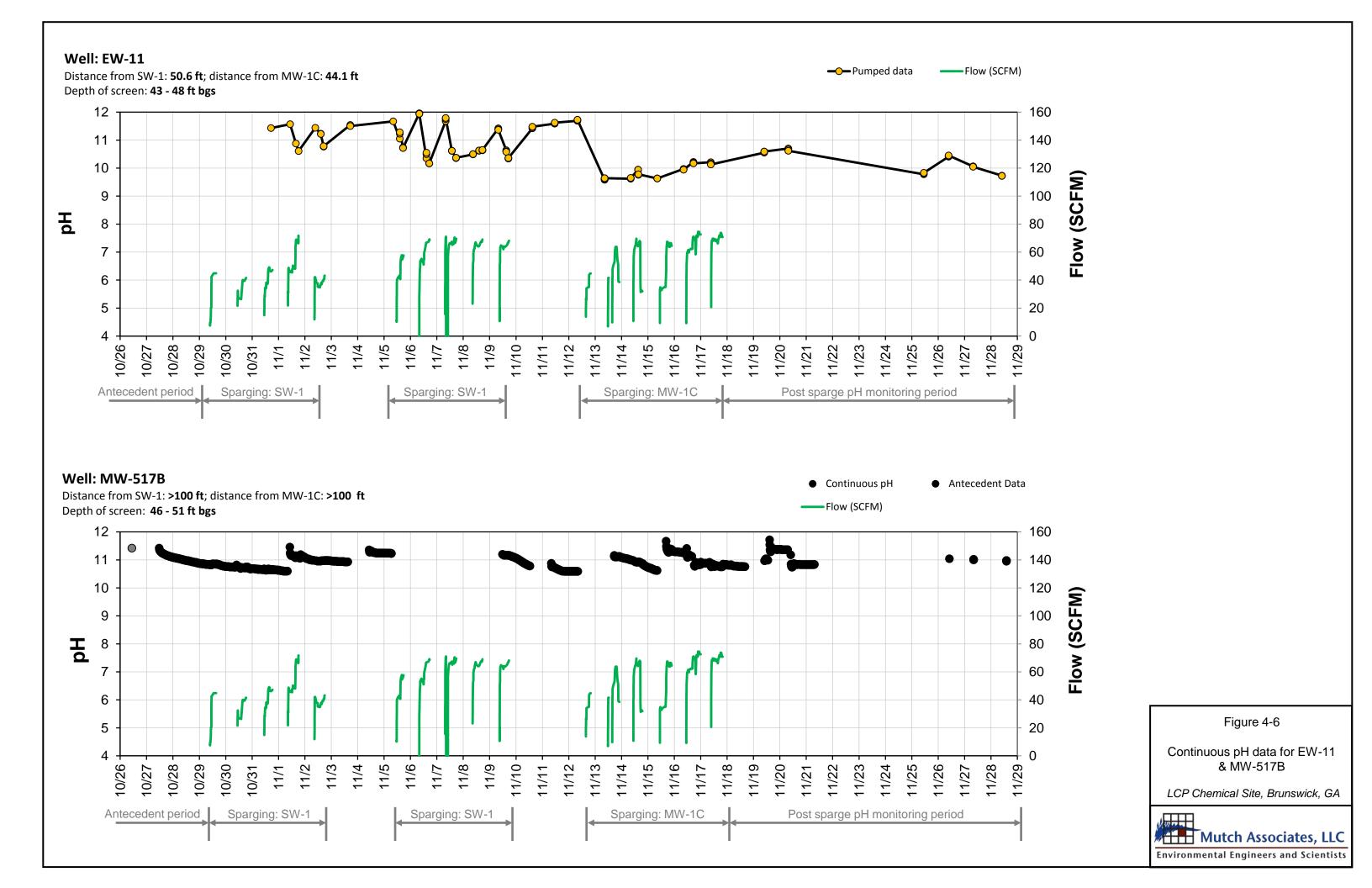
Figure 4-3

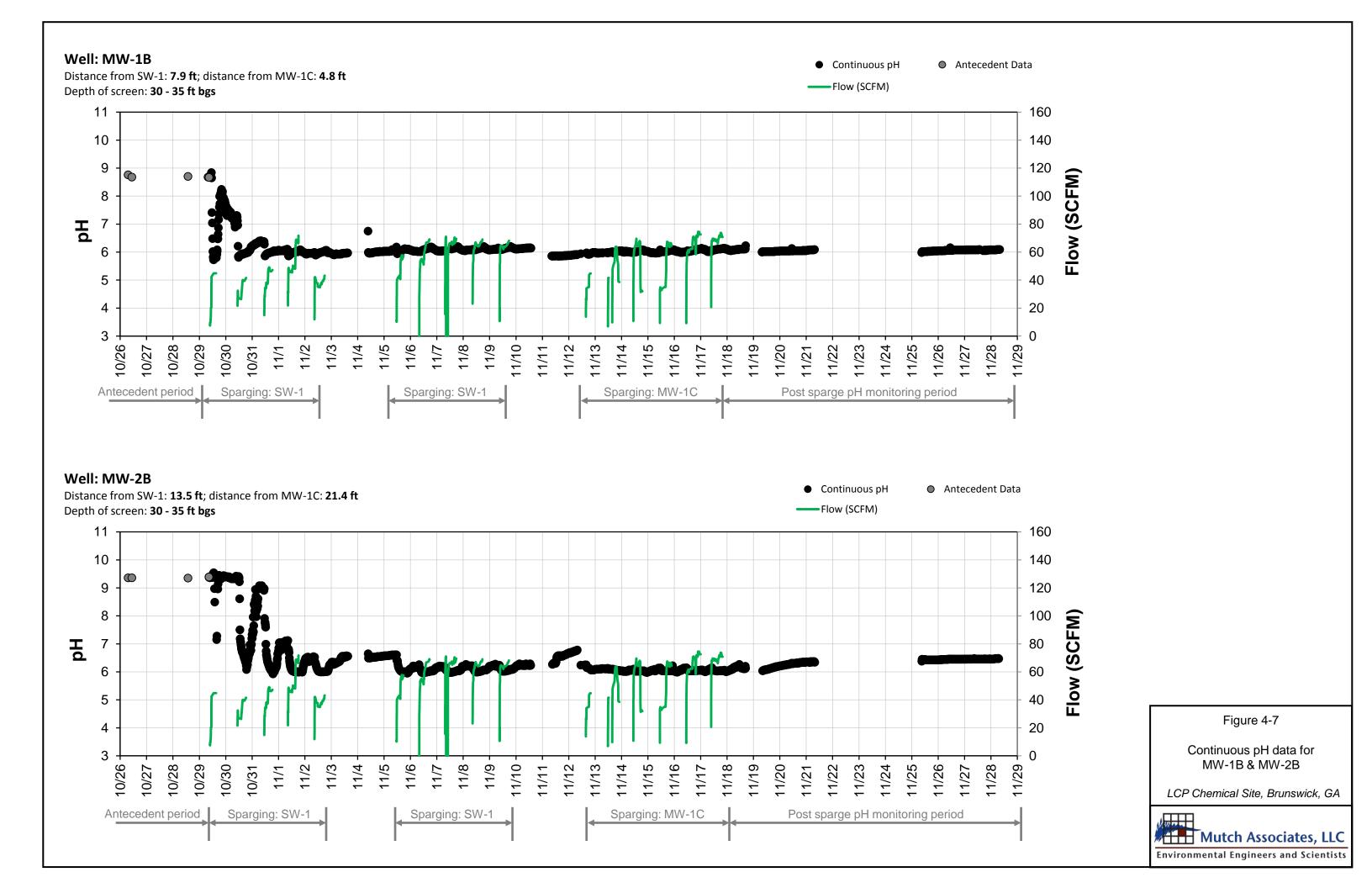
Pre-Sparge pH Levels (10/29/12 8:45 AM)

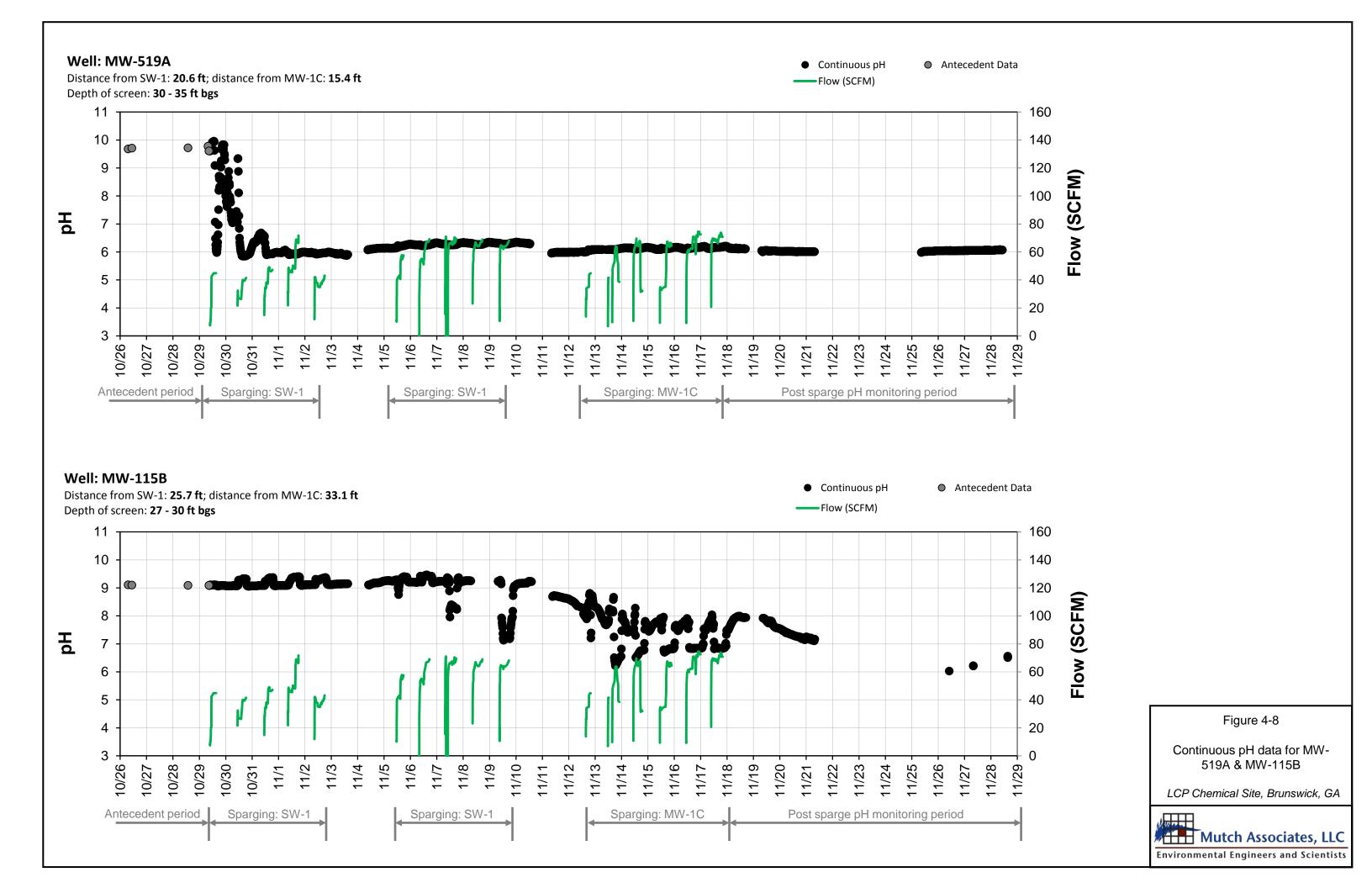


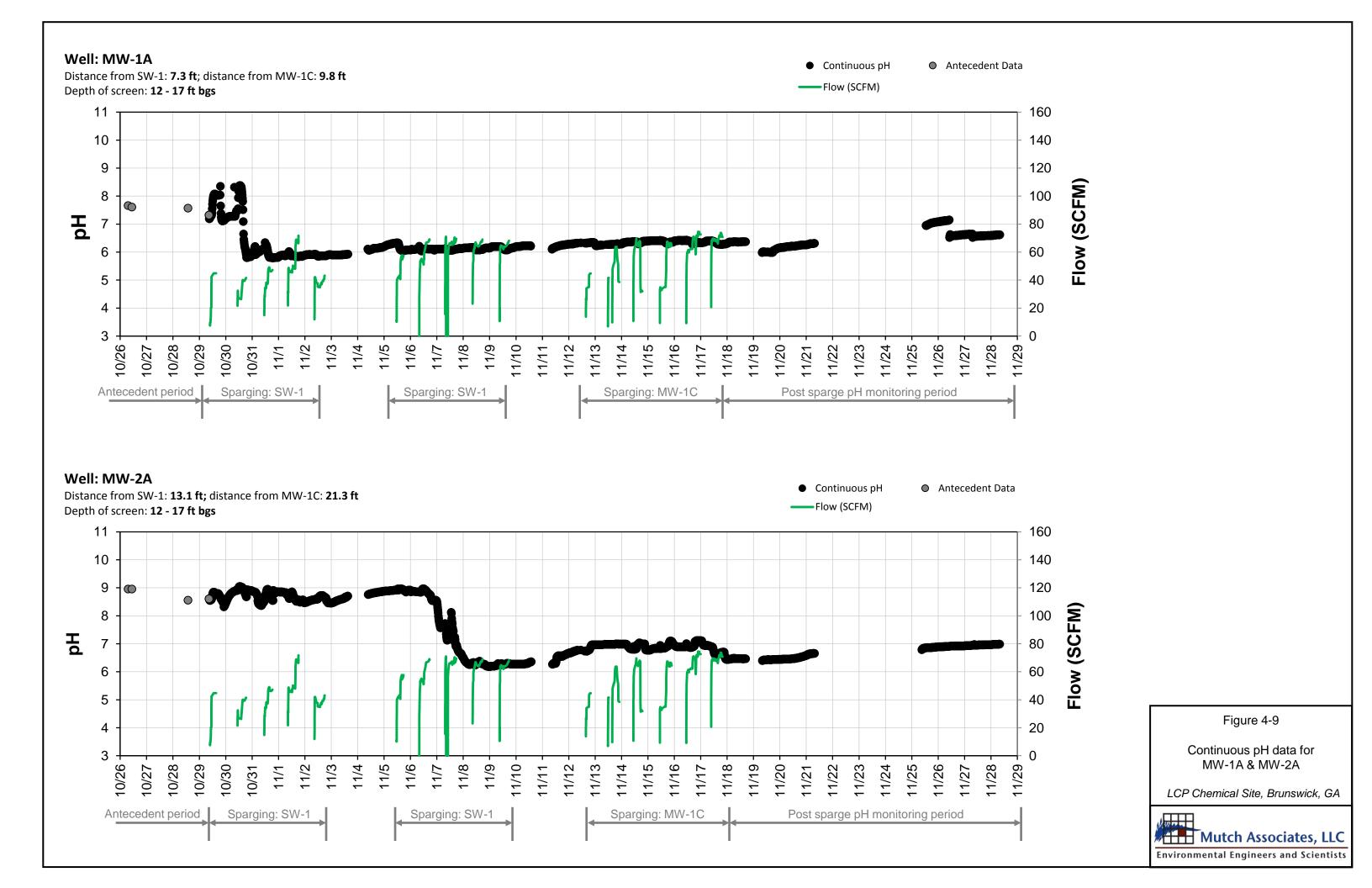


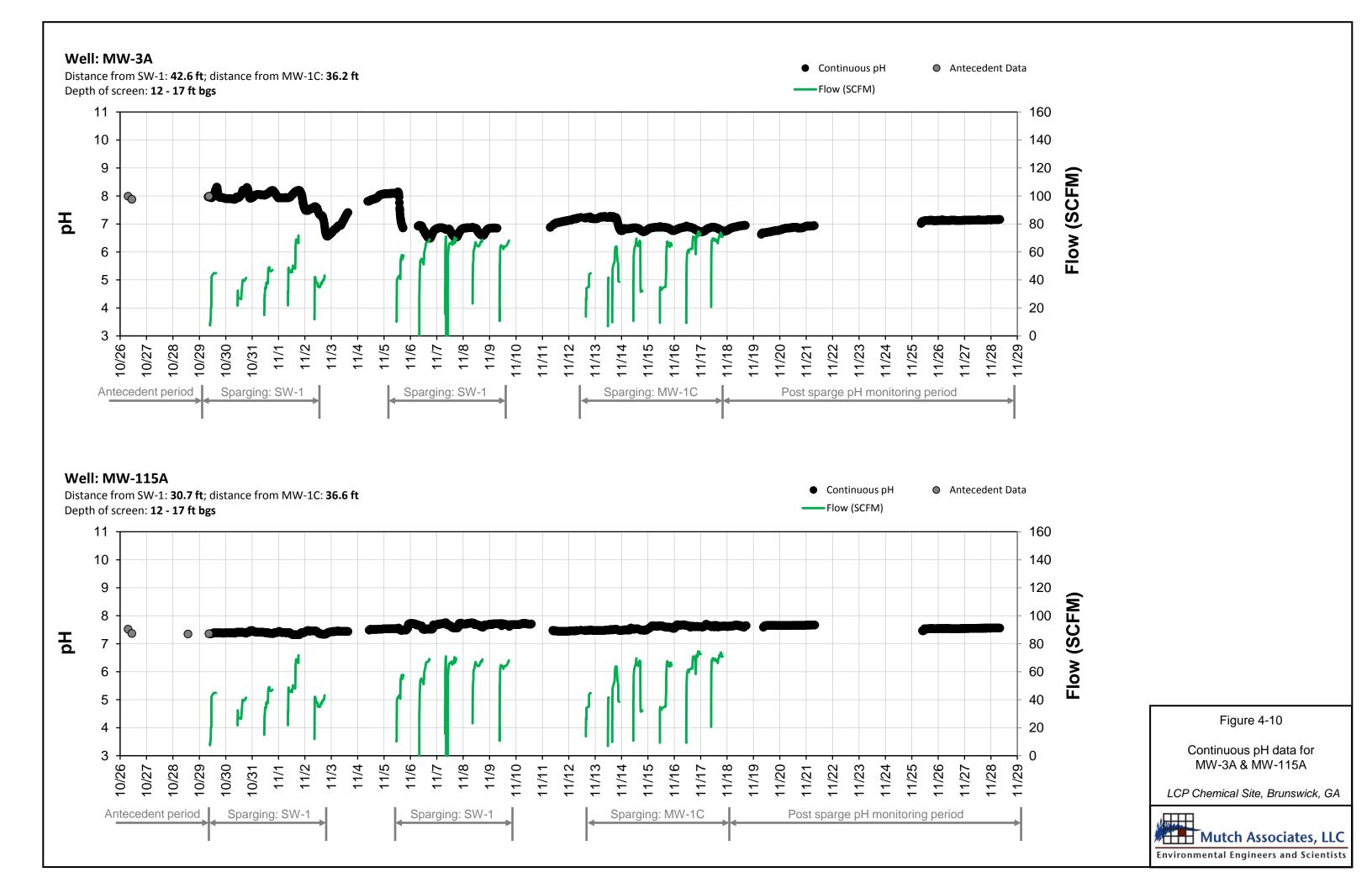












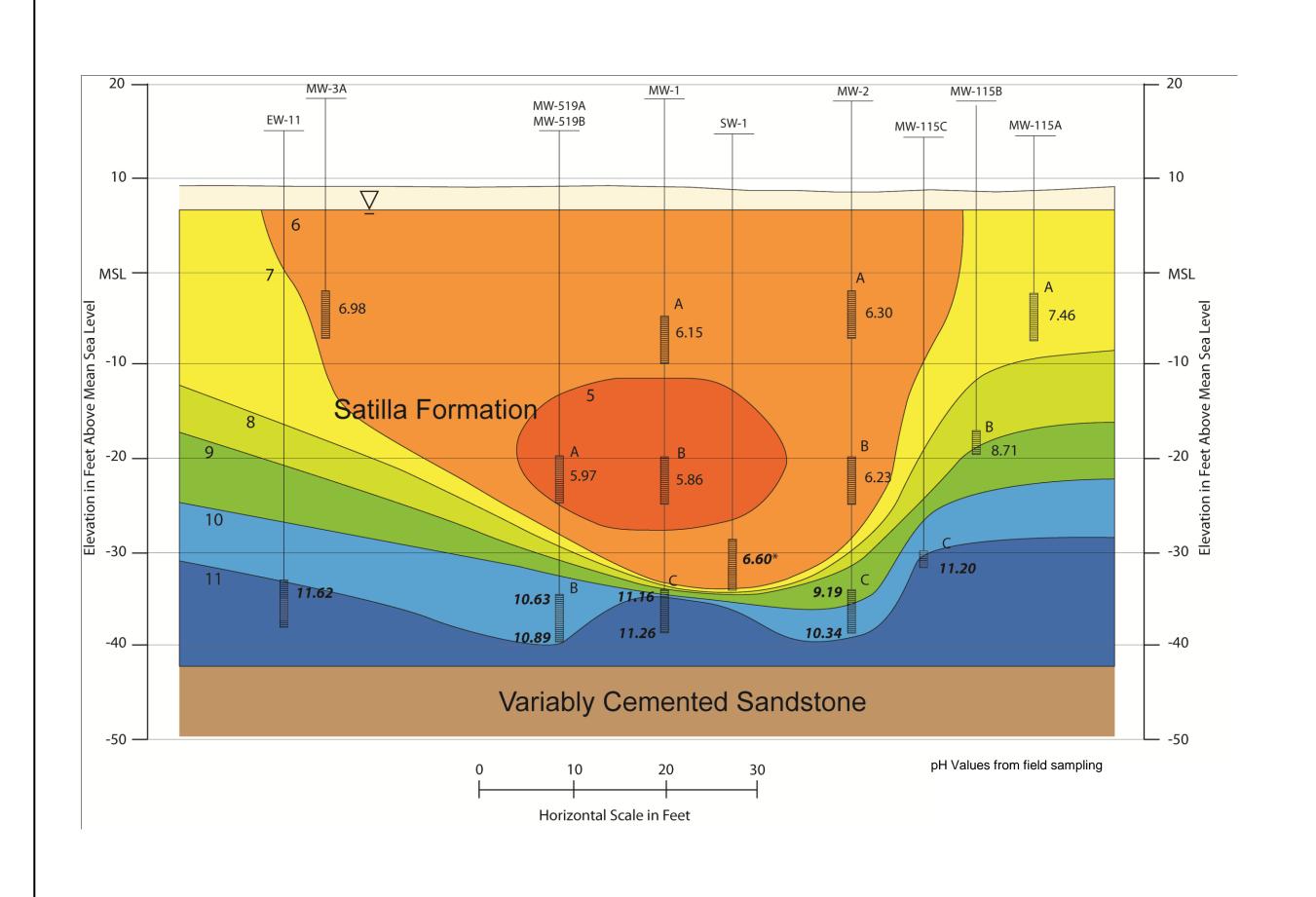


Figure 4-11 pH Levels After 2 Weeks of Sparging into SW-1 (11/11/12 10:00 AM)



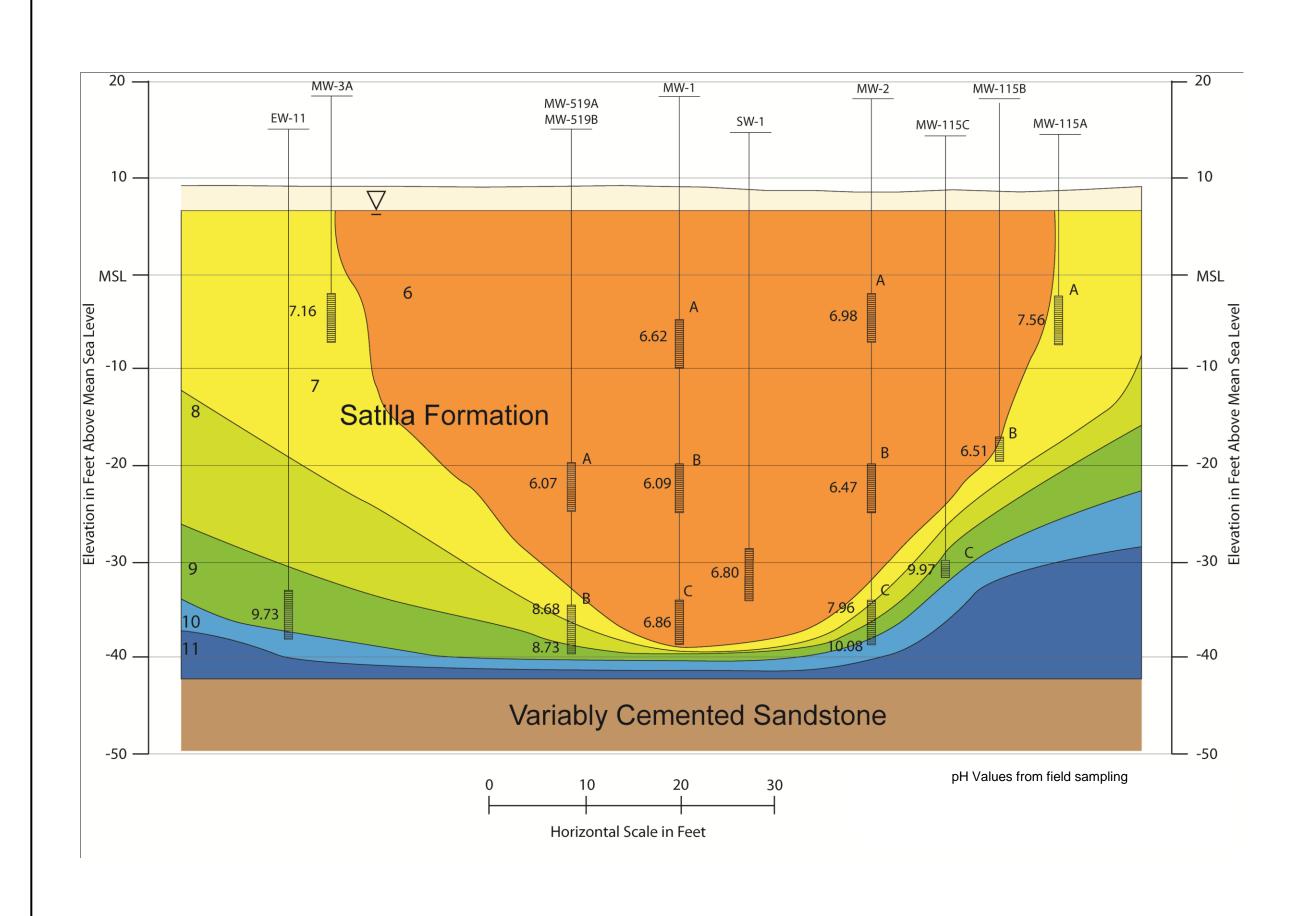
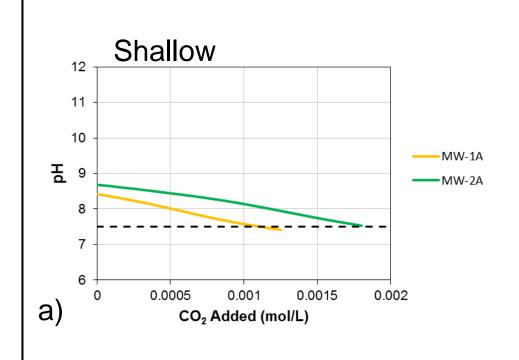
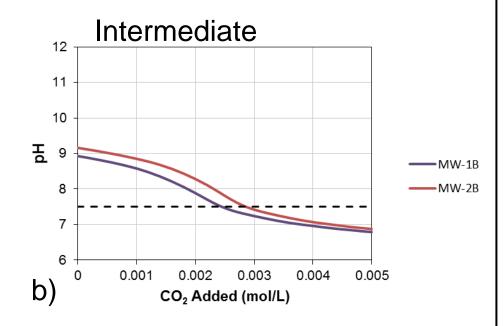
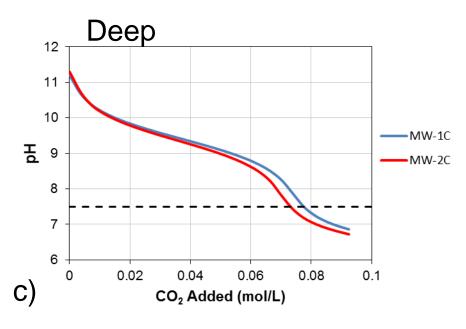


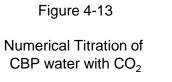
Figure 4-12 pH Levels at End of Post-Sparge Monitoring Period (11/28/12)













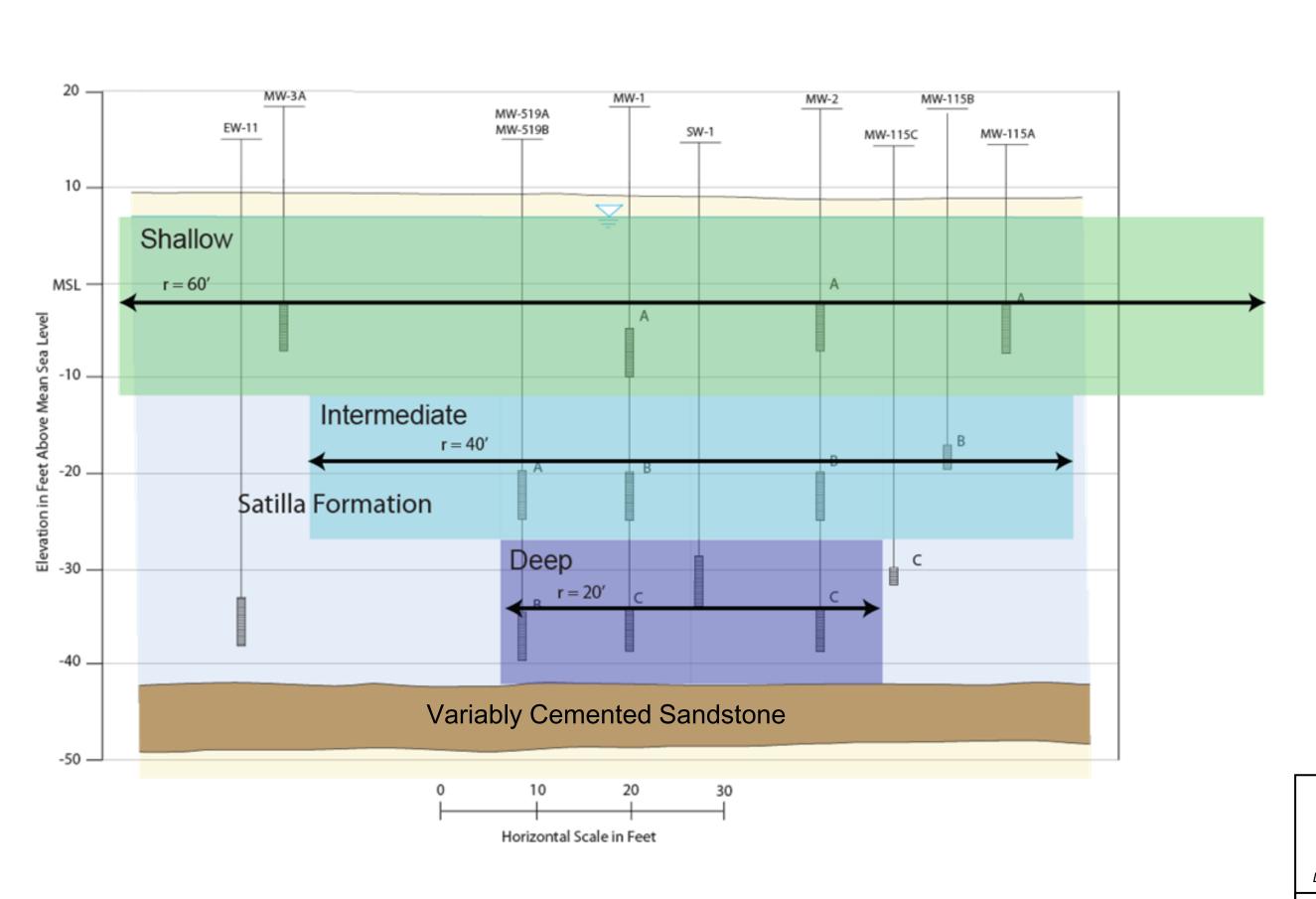


Figure 4-14
Shallow, Intermediate and
Deep Satilla Zones Used for
CO<sub>2</sub> Demand Calculations



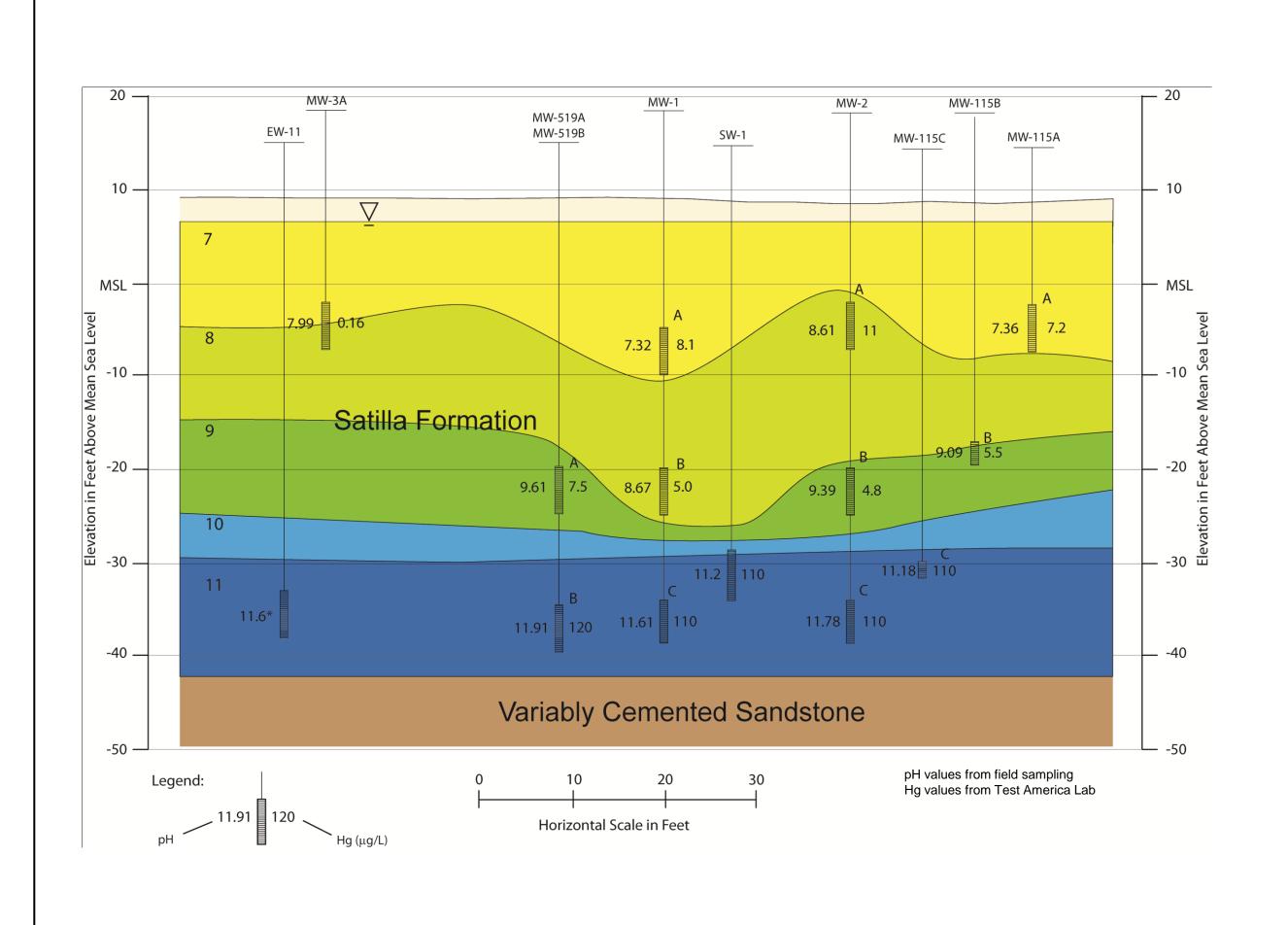


Figure 4-15

Pre-sparge pH and Mercury Concentrations



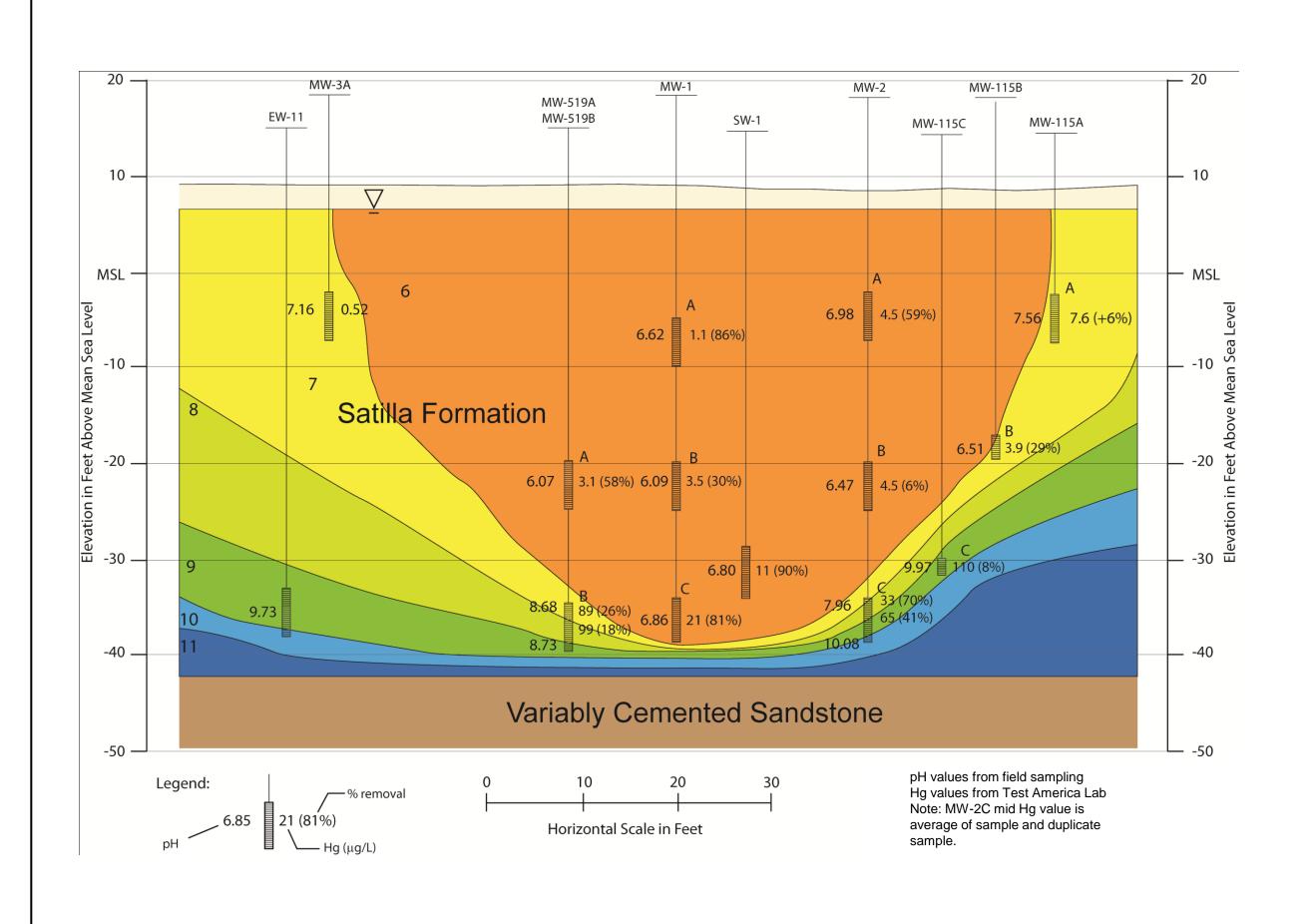
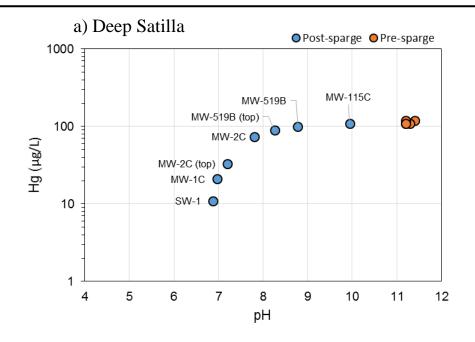


Figure 4-16
Post-Sparge pH and
Mercury Concentrations
(pH 11/28/12, Hg 11/26/12)





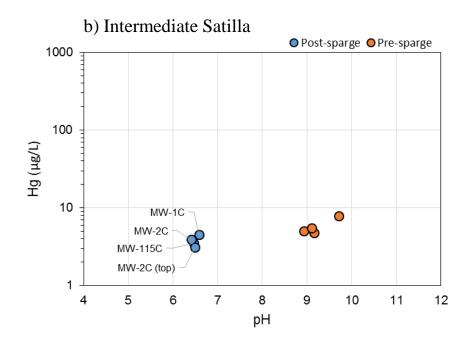
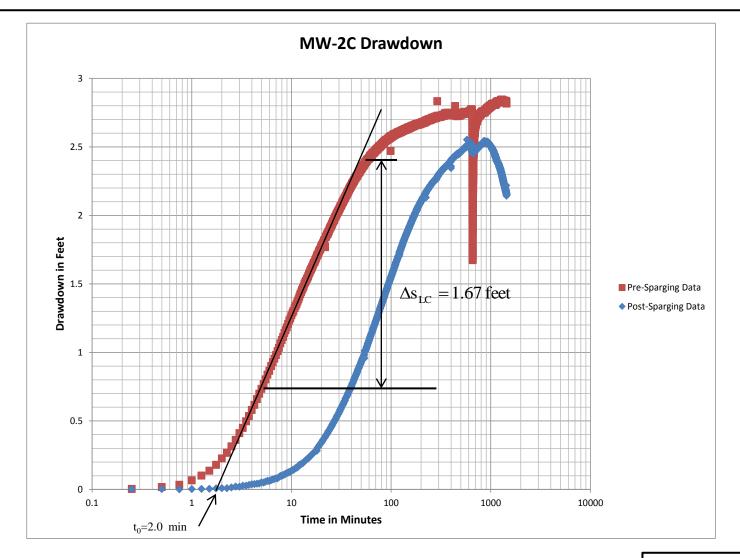


Figure 4-17
Mercury Concentration
Versus pH in a) Deep and b)
Intermediate Satilla Wells







$$T = \frac{264Q}{\Delta s_{LC}} = \frac{264(7.2)}{1.67}$$
$$T = 1,150 \text{ gpd/ft}$$

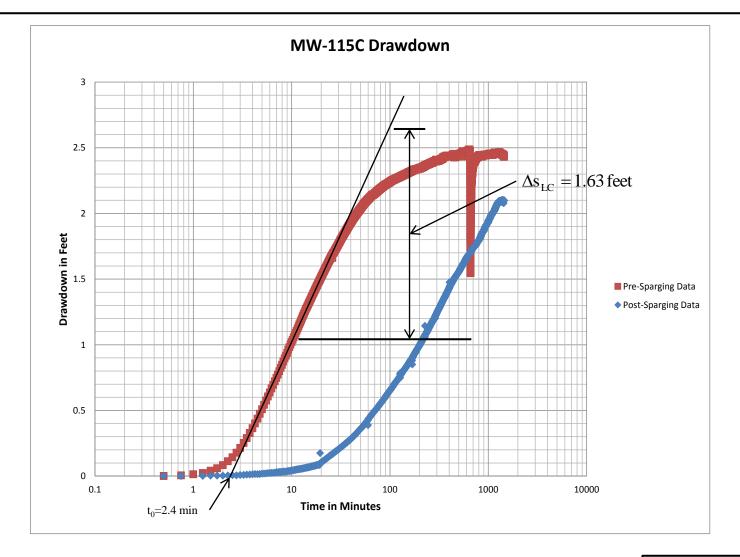
$$S = \frac{\text{Tt}_0}{4800\text{r}^2} = \frac{1,150 \text{ gpd/ft}(2.0 \text{ min})}{4800(13.1 \text{ ft})^2}$$
$$S = 2.8x10^{-3}$$

Figure 4-18

Cooper-Jacob Time-Drawdown Analysis of Early-Time Data from Well MW-2C LCP Chemical Site, Brunswick, GA







$$T = \frac{264Q}{\Delta s_{LC}} = \frac{264(7.2)}{1.63}$$
$$T = 1,150 \text{ gpd/ft}$$

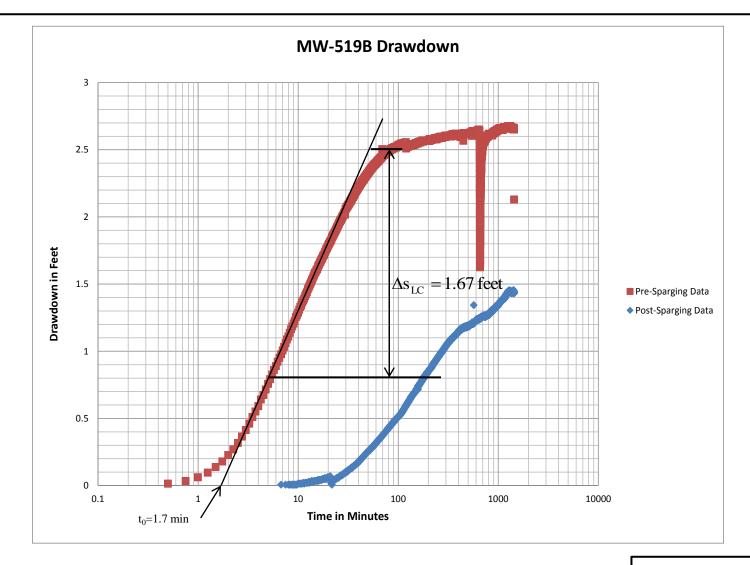
$$S = \frac{\text{Tt}_0}{4800\text{r}^2} = \frac{1,150 \text{ gpd/ft}(2.4 \text{ min})}{4800(18.7 \text{ ft})^2}$$
$$S = 1.6x10^{-3}$$

Figure 4-19

Cooper-Jacob Time-Drawdown Analysis of Early-Time Data from Well MW-115C







$$T = \frac{264Q}{\Delta s_{LC}} = \frac{264(7.2)}{1.67}$$
$$T = 1,150 \text{ gpd/ft}$$

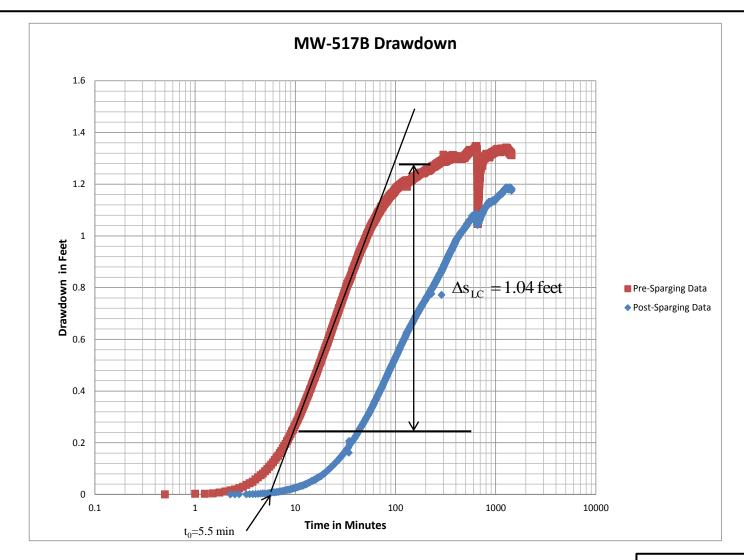
$$S = \frac{\text{Tt}_0}{4800\text{r}^2} = \frac{1,150 \text{ gpd/ft}(1.7 \text{ min})}{4800(20.6 \text{ ft})^2}$$
$$S = 9.6x10^{-4}$$

Figure 4-20

Cooper-Jacob Time-Drawdown Analysis of Early-Time Data from Well MW-519B LCP Chemical Site, Brunswick, GA







$$T = \frac{264Q}{\Delta s_{LC}} = \frac{264(7.2)}{1.04}$$

$$T = 1.825 \text{ and/ft}$$

$$T = 1,825 \text{ gpd/ft}$$

$$S = \frac{\text{Tt}_0}{4800\text{r}^2} = \frac{1,825 \text{ gpd/ft}(5.5 \text{ min})}{4800(104.9 \text{ ft})^2}$$
$$S = 1.9x10^{-4}$$

Figure 4-21

Cooper-Jacob Time-Drawdown Analysis of Early-Time Data from Well MW-517B



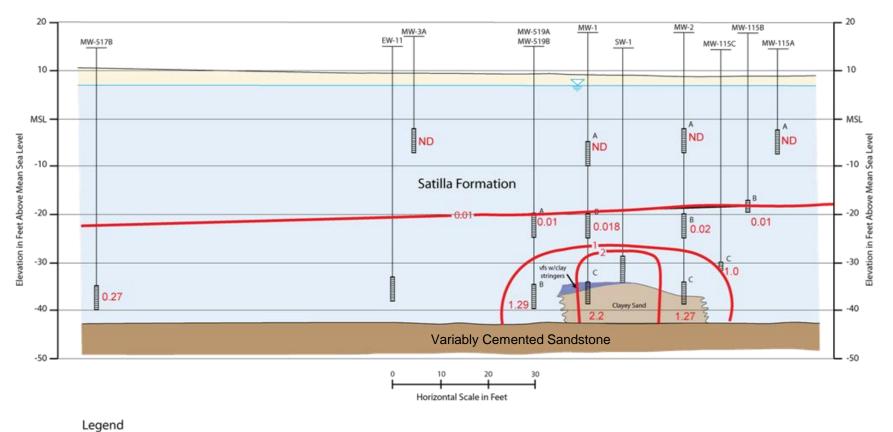




Figure 4-22

Pre-Sparge Drawdown @10 minutes



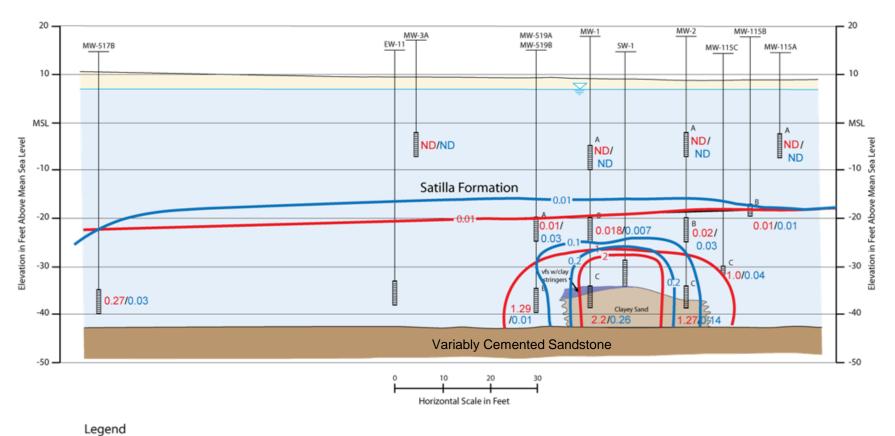




Figure 4-23

Pre- and Post-Sparge Drawdown @10 minutes



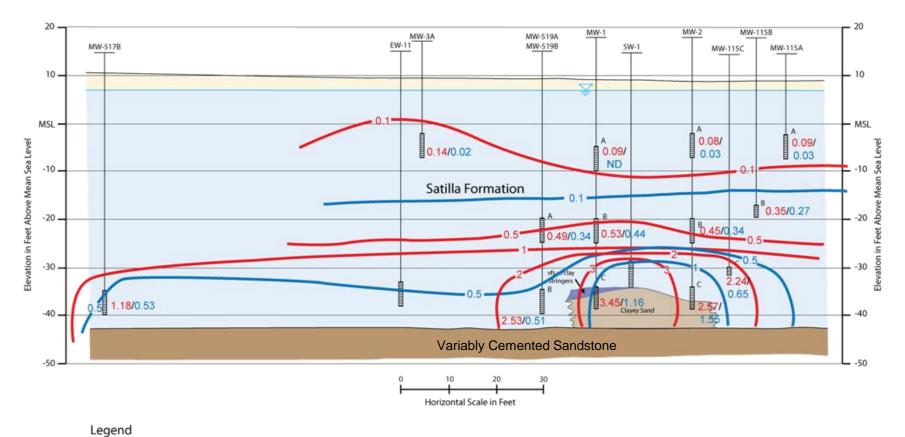




Figure 4-24

Pre- and Post-Sparge Drawdown @100 minutes



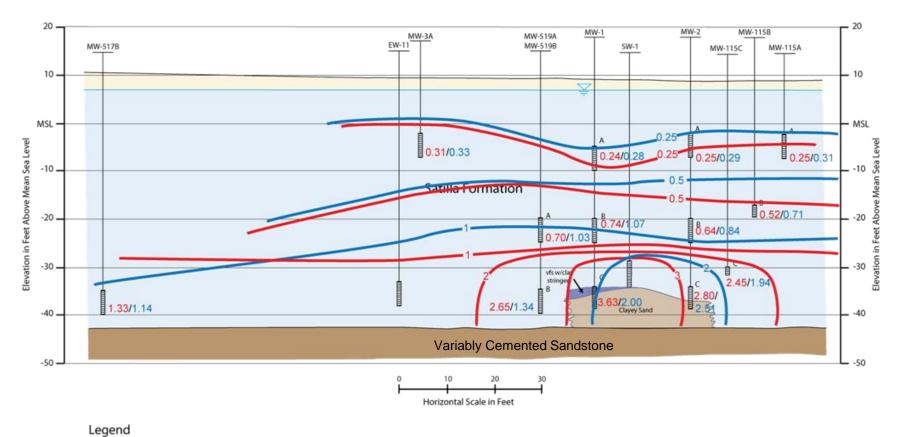
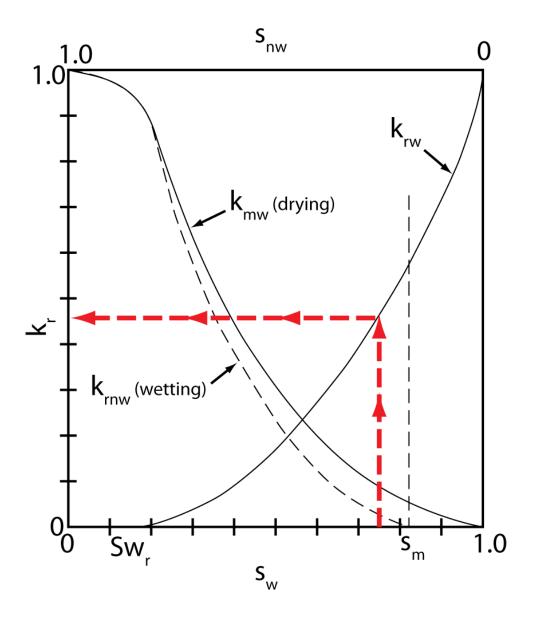




Figure 4-25

Pre- and Post-Sparge Drawdown @1000 minutes



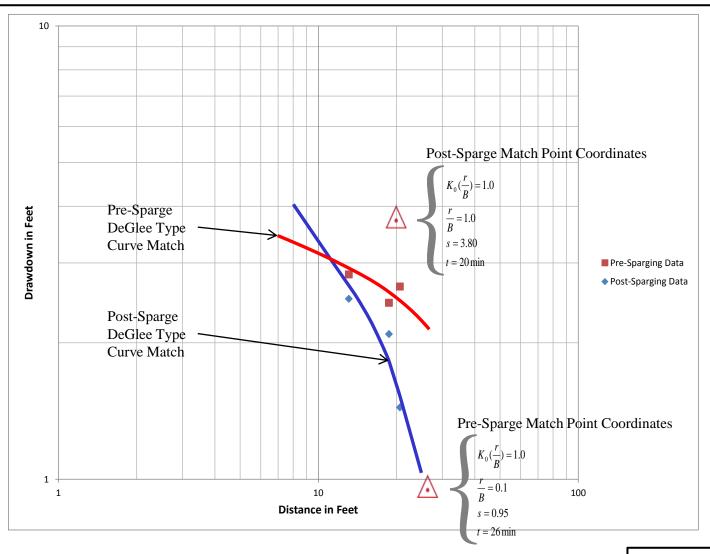


(Adapted from Pankow and Cherry, 1995)

Figure 4-26

Typical Reflective Permeability Curves





**Pre-Sparge Transmissivity** 

$$T = \frac{229QK_0(\frac{r}{B})}{s} = \frac{229(7.5 \text{ gpm})1.0}{0.95 \text{ feet}}$$
$$T = 1,800 \text{ gpd/ft}$$

Post-Sparge Transmissivity

$$T = \frac{229QK_0(\frac{r}{B})}{s} = \frac{229(7.5 \text{ gpm})1.0}{3.80 \text{ feet}}$$
$$T = 450 \text{ gpd/ft}$$

Figure 4-27
DeGlee Method
Distance-Drawdown Analysis
of Wells in Principal
Hydrostratigraphic Zone
LCP Chemical Site, Brunswick, GA



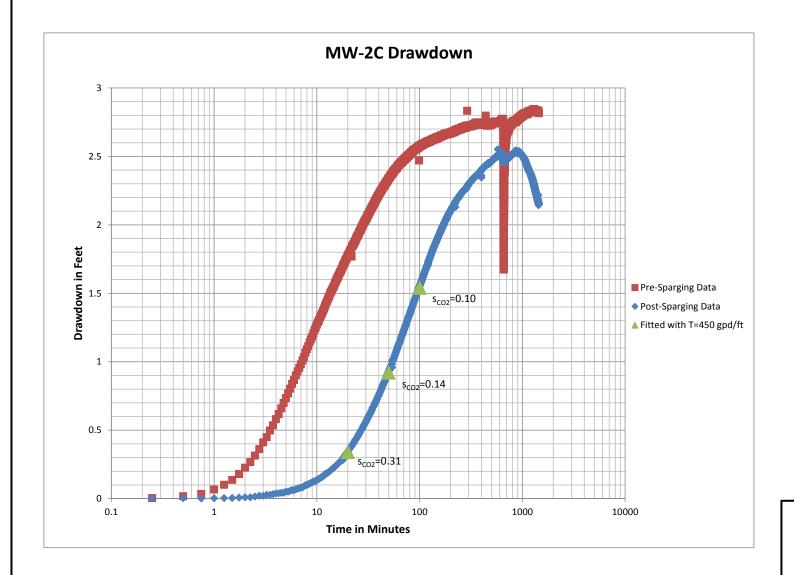


Figure 4-28
Predicted CO<sub>2</sub> Residual
Saturations by Matching
Drawdown in MW-2C using the
Modified Storativity Equation
LCP Chemical Site, Brunswick, GA



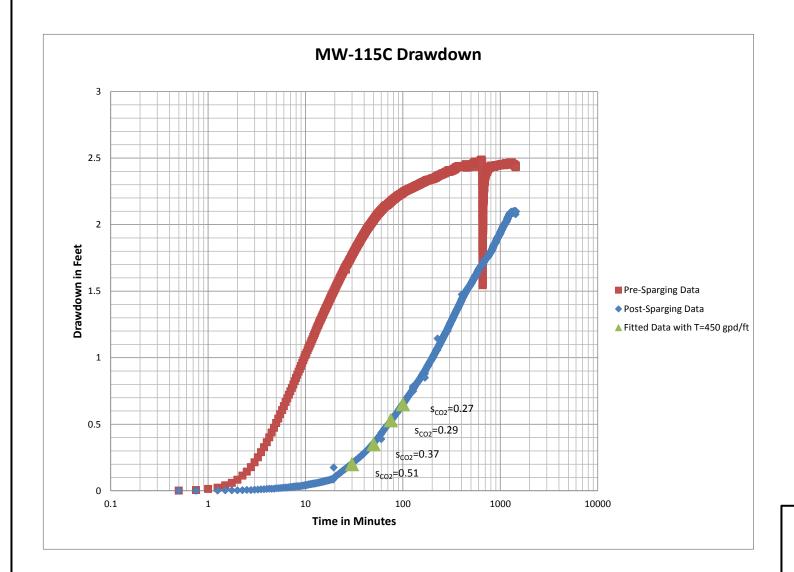


Figure 4-29
Predicted CO<sub>2</sub> Residual
Saturations by Matching
Drawdown in MW-115C using
the Modified Storativity Equation
LCP Chemical Site, Brunswick, GA



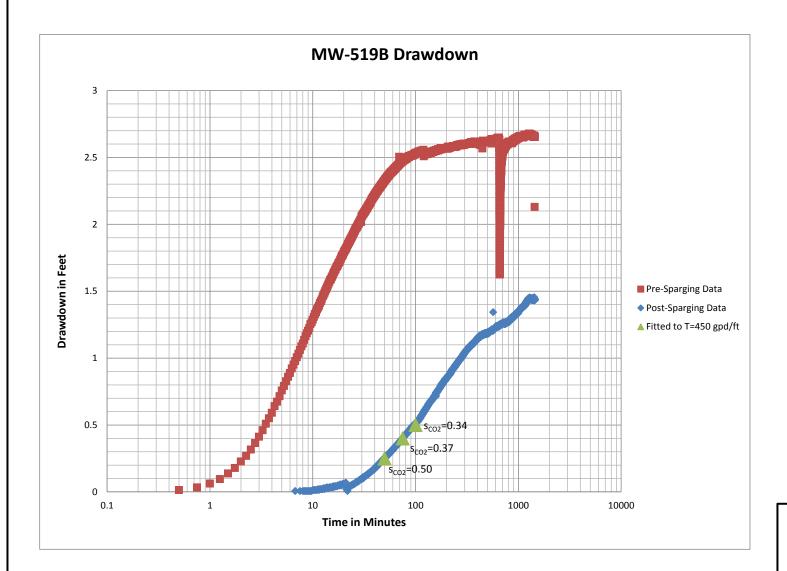


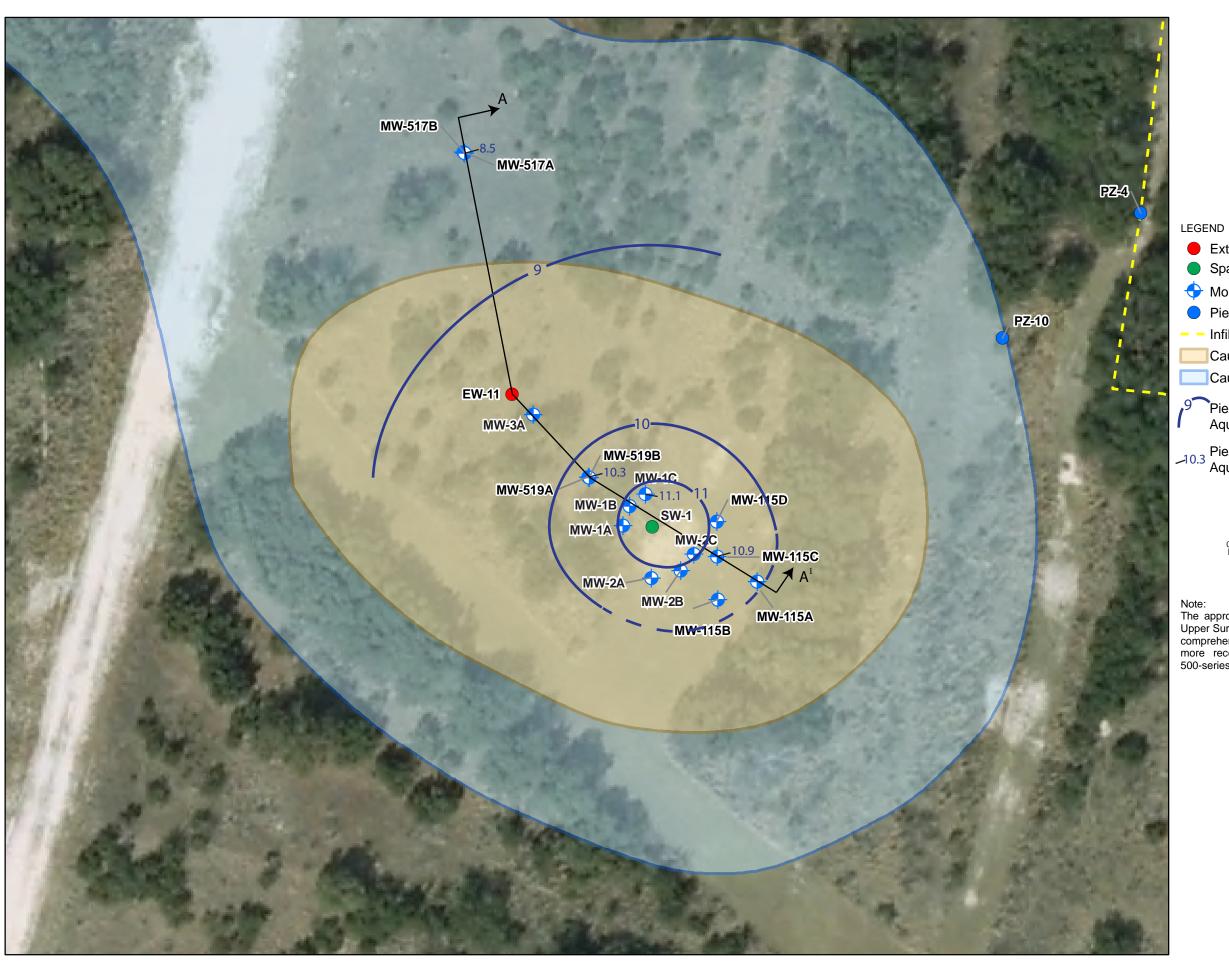
Figure 4-30
Predicted CO<sub>2</sub> Residual
Saturations by Matching
Drawdown in MW-519B using the
Modified Storativity Equation
LCP Chemical Site, Brunswick, GA



#### 2 Well Series Water Level Mounding MW2C ▲ MW2B MW2A 10 Decline in Piezometric Surface Peak Rise in Once CO<sub>2</sub> Channels are Fully Established Piezometric Surface in Basal 8 Satilla Aquifer Rapid Decline in Piezometric Surface Upon Cessation of Sparging Water Elevation (ft) Start of Sparging Transducer removed during pH Rebound in Piezometric Surface Electrode Recalibration Post-Sparging Collapse of Piezometric Surface 10/29/12 0:00 10/29/12 1:00 10/29/12 2:00 10/29/12 3:00 10/29/12 4:00 10/29/12 5:00 10/29/12 6:00 10/29/12 7:00 10/29/12 8:00 10/29/12 9:00 10/29/12 10:00 10/29/12 11:00 10/29/12 13:00 10/29/12 14:00 10/29/12 15:00 10/29/12 16:00 10/29/12 17:00 10/29/12 19:00 10/29/12 20:00 10/29/12 21:00 10/29/12 22:00 10/29/12 23:00 10/30/12 0:00 10/29/12 12:00 10/29/12 18:00 Figure 4-31

Mounding Water Level Behavior in the 2 Series Wells on the 10/29/12 Day 1 of Sparging LCP Chemical Site, Brunswick, GA





Extraction Well

Sparging Well

Monitoring Well

Piezometer

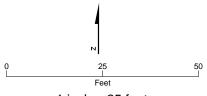
Infiltration Galleries

Caustic Brine Pool (pH > 11.5)

Caustic Brine Pool (pH > 10.5)

Piezometric Contour of Basal Satilla Aguifer Zone

10.3 Piezometric Surface of Basal Satilla Aquifer Zone



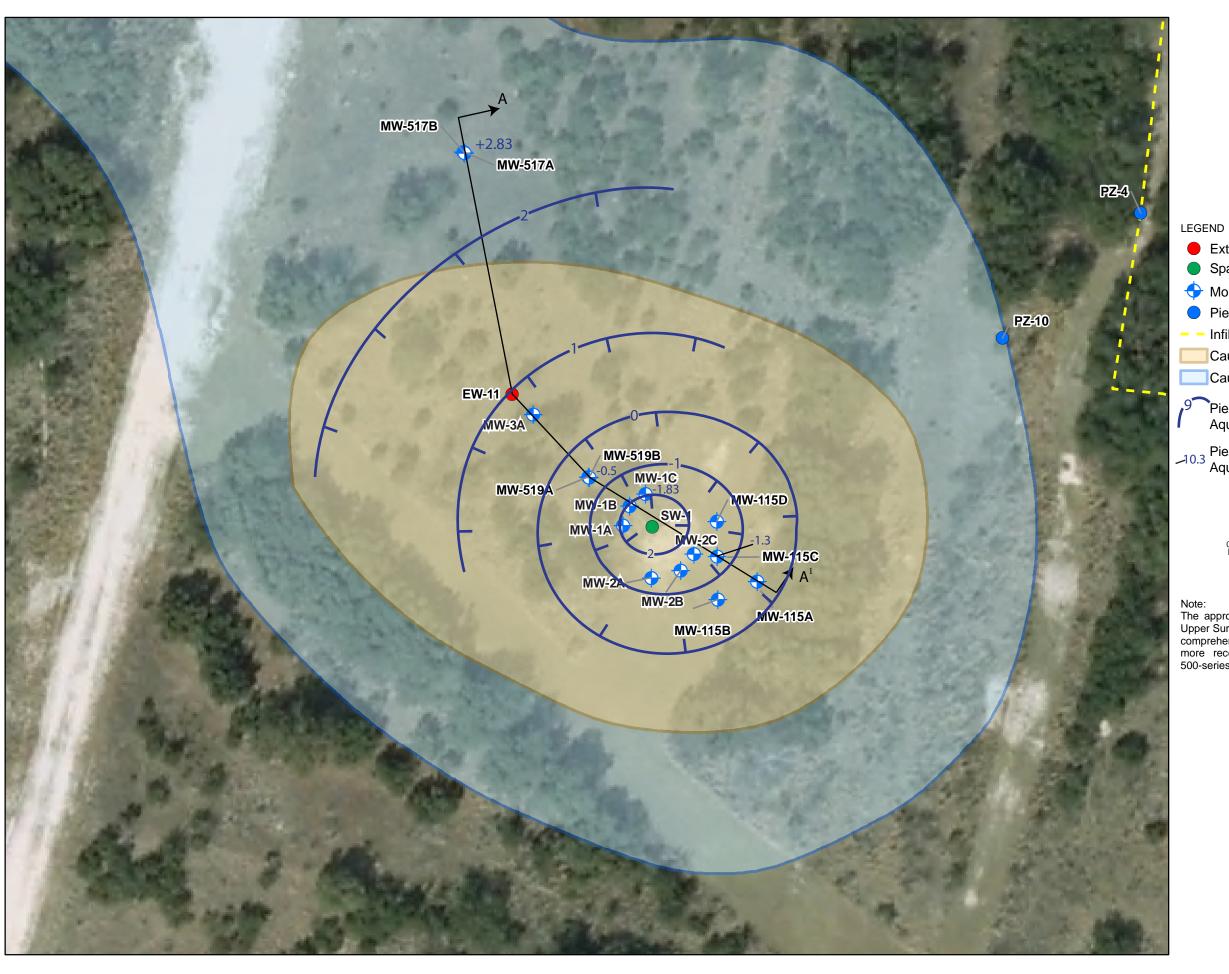
1 inch = 25 feet

The approximate current lateral extent of the CBP in the Upper Surficial Aquifer is based primarily on the most recent comprehensive data set from 2007 and supplemented with more recent data collected from extraction wells and 500-series monitoring wells between 2009 and April 2010.

Figure 4-32

Maximum Level of Piezometric Surface During Sparging on 10/29/12





Extraction Well

Sparging Well

Monitoring Well

Piezometer

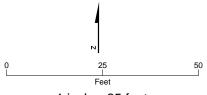
Infiltration Galleries

Caustic Brine Pool (pH > 11.5)

Caustic Brine Pool (pH > 10.5)

Piezometric Contour of Basal Satilla Aquifer Zone

10.3 Piezometric Surface of Basal Satilla Aquifer Zone



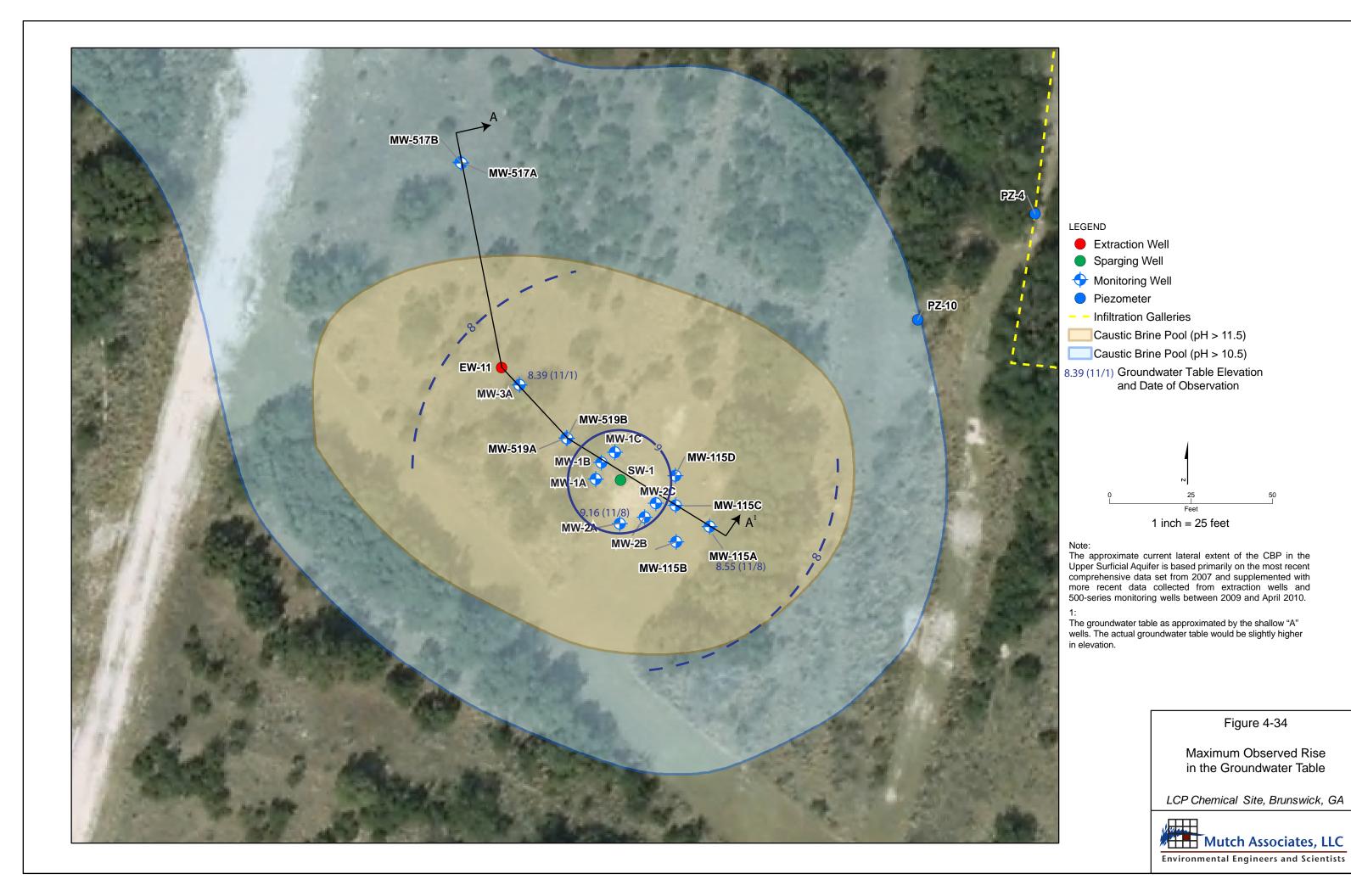
1 inch = 25 feet

The approximate current lateral extent of the CBP in the Upper Surficial Aquifer is based primarily on the most recent comprehensive data set from 2007 and supplemented with more recent data collected from extraction wells and 500-series monitoring wells between 2009 and April 2010.

Figure 4-33

Peak Decline in Piezometric Surface Following Sparging on 10/29/12





#### APPENDIX A. BORING LOGS/ WELL CONSTRUCTION DIAGRAMS

Page 1 of 1

#### Honeywell

Site: LCP Brunswick Boring No: MW-1A Diameter: 6 in

Date: 09/19/2012

Northing: 431518.42 Easting: 861711.77

Driller: Billy Moss (Groundwater Protection Inc)

Method: Sonic

Consultant: Christine Jaynes (PARSONS)

Total Depth: 20.0 Ft GW Depth: 4.0 Ft

Elevation: 12.80 Datum: NAVD88 Field Book No: Parsons #1 Depth | Soil Pattern Soil Description MW-1A Diagram Code Ft V SM Dry, loose, brown, fine to medium SAND, some silt, with odor. Moist, loose, light gray/white, fine to medium SAND, some silt, odor. SM 10 Wet, soft, CLAY and SILT, some wood/tree root material, odor. CL Wet, medium stiff, dark gray/black SILT, and very fine-fine sand, odor. SM Wet, loose, tan very fine to coarse SAND, odor. SW 15 -Wet, loose, tan, very fine to coarse SAND, odor. SW Wet, loose, gray, very fine to medium SAND, trace silt. SM Wet, loose, gray, very fine to coarse SAND, slight odor. SW 20.0 Boring GW Depth

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Site: LCP Brunswick Boring No: MW-1B

Diameter: 6 in Date: 09/19/2012

Northing: 431523.74 Easting: 861713.44

Elevation: 12.90

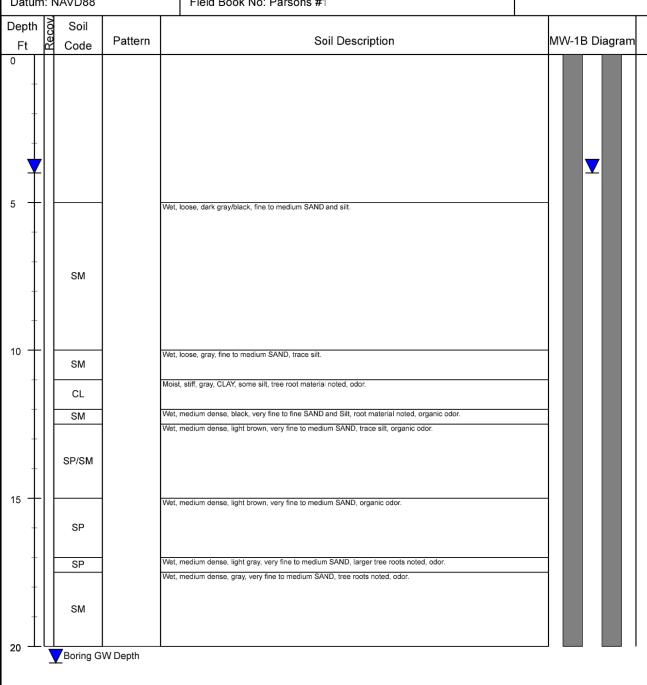
Driller: Billy Moss (Groundwater Protection Inc)

Method: Sonic

Consultant: Christine Jaynes (PARSONS)

Datum: NAVD88 Field Book No: Parsons #1 Total Depth: 35.0 Ft

GW Depth: 4.0 Ft



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## Honeywell

Site: LCP Brunswick Boring No: MW-1B Diameter: 6 in Date: 09/19/2012

Northing: 431523.74 Easting: 861713.44

Elevation: 12.90

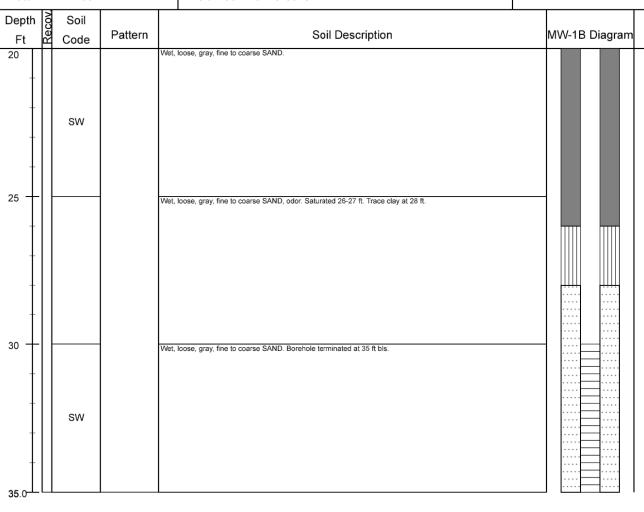
Driller: Billy Moss (Groundwater Protection Inc)

Method: Sonic

Consultant: Christine Jaynes (PARSONS)

Datum: NAVD88 Field Book No: Parsons #1

Total Depth: 35.0 Ft GW Depth: 4.0 Ft



Page 1 of 2

#### Honeywell

Site: LCP Brunswick Boring No: MW-1C Diameter: 2 in

Date: 09/17/2012

Northing: 431526.41 Easting: 861717.45

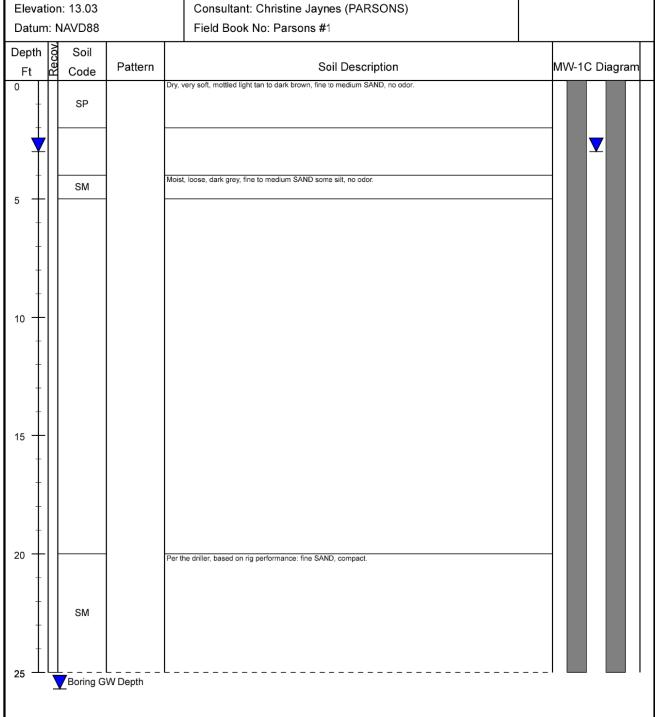
Driller: Billy Moss (Groundwater Protection Inc)

Method: Sonic

Consultant: Christine Jaynes (PARSONS)

Total Depth: 50.0 Ft

GW Depth: 3.0 Ft



Page 2 of 2



Site: LCP Brunswick Boring No: MW-1C Diameter: 2 in

Date: 09/17/2012

Northing: 431526.41

Driller: Billy Moss (Groundwater Protection Inc)

Easting: 861717.45

Method: Sonic

Total Depth: 50.0 Ft GW Depth: 3.0 Ft

Elevation: 13.03

Consultant: Christine Jaynes (PARSONS)

Datum: NAVD88			Project No:	Field Book No: Parsons #1		
Depth Ft	Soil Code	Pattern	•	Soil Description	MW-1C	Diagram
25	SM	P	er the driller, based on rig performance	: fine SAND, compact.		
35 +						
40 +	SW SC CL	   N	aturated, loose, dark grey/black, fine to loist, firm, dark grey/black, CLAY, and s loist, firm, dark grey/black, CLAY, slight aturated, loose, grey, course SAND, sli	sand. odor.		
45 —	SP SC CL SC	s N	aturated, loose, grey, very fine to fine S aturated, firm, grey, very fine SAND wit loist, firm, grey, CLAY (CL), slight odor. aturated, medium dense, grey, very fine	th clay stringers, slight odor.		
50.0	SC	N	loist, medium dense, grey, very fine to i	medium SAND with clay, slight odor.		
50.0						

Page 1 of 1

## Honeywell

Site: LCP Brunswick Boring No: MW-2A Diameter: 2 in Date: 09/20/2012

Northing: 431505.14 Easting: 861721.72

Boring GW Depth

Elevation: 12.68

Driller: Billy Moss (Groundwater Protection Inc)

Method: Sonic

Consultant: Christine Jaynes (PARSONS)

Total Depth: 20.0 Ft GW Depth: 3.0 Ft

Datum: NAVD88 Field Book No: Parsons #1 Depth 3 Soil Pattern Soil Description MW-2A Diagram Ft Code 10 Saturated, very soft, tan, very fine to medium SAND, odor. SP Saturated, very soft, tan, fine to course SAND, slight odor. SW 15 Saturated, soft, grey, very fine to course SAND, odor. SW

Page 1 of 2 **BORING LOG** 



Site: LCP Brunswick Boring No: MW-2B

Diameter: 2 in

Date: 09/18/2012 - 09/19/2012

Northing: 431507.07 Easting: 861726.66

Elevation: 12.77

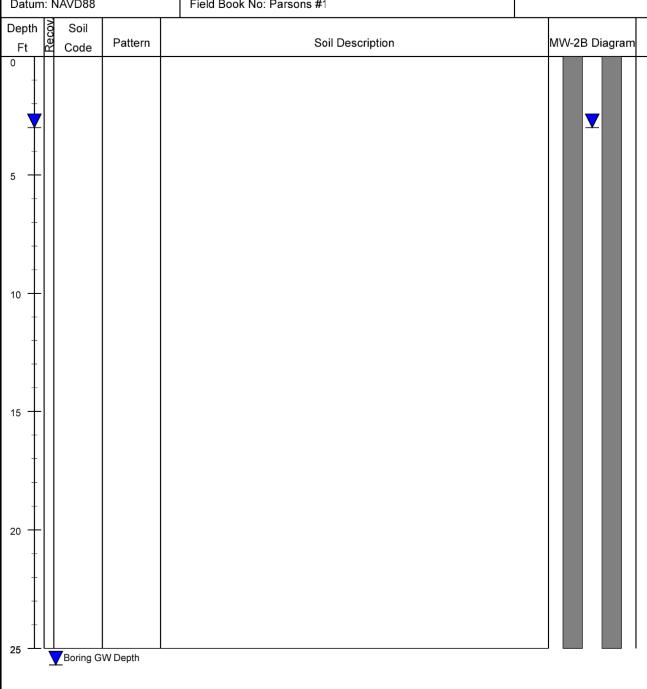
Driller: Billy Moss (Groundwater Protection Inc)

Method: Sonic

Consultant: Christine Jaynes (PARSONS)

Datum: NAVD88 Field Book No: Parsons #1 Total Depth: 35.0 Ft

GW Depth: 3.0 Ft



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#### Honeywell

Site: LCP Brunswick Boring No: MW-2B

Diameter: 2 in

Date: 09/18/2012 - 09/19/2012

Total Depth: 35.0 Ft

GW Depth: 3.0 Ft

Northing: 431507.07 Easting: 861726.66

Elevation: 12.77

Driller: Billy Moss (Groundwater Protection Inc)

Method: Sonic

Consultant: Christine Jaynes (PARSONS)

Datum: NAVD88 Project No: Field Book No: Parsons #1

Depth S	Soil			
Ft 8	Code	Pattern	Soil Description	MW-2B Diagram
30	SC CL SC		Saturated, soft, grey, fine to medium SAND trace day, odor.  CLAY lense Saturated, firm, grey, fine to course SAND some clay, odor.	



Site: LCP Brunswick

Boring No: MW-2C Diameter: 6 in

Date: 09/18/2012

Northing: 431511.18 Easting: 861730.19

Elevation: 12.67

Driller: Billy Moss (Groundwater Protection Inc)

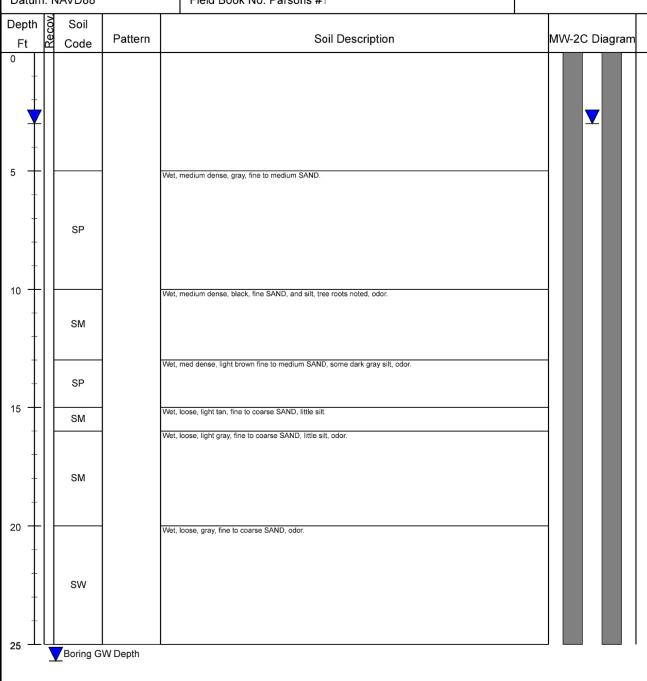
Method: Sonic

Page 1 of 2

Consultant: Christine Jaynes (PARSONS)

Datum: NAVD88 Field Book No: Parsons #1

Total Depth: 50.0 Ft GW Depth: 3.0 Ft



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# Honeywell

Site: LCP Brunswick Boring No: MW-2C Diameter: 6 in Date: 09/18/2012

Northing: 431511.18 Easting: 861730.19

Driller: Billy Moss (Groundwater Protection Inc)

Method: Sonic

Consultant: Christine Jaynes (PARSONS)

Total Depth: 50.0 Ft GW Depth: 3.0 Ft

Elevation: 12.67 Datum: NAVD88 Field Book No: Parsons #1 Depth Soil Pattern Soil Description MW-2C Diagram Ft Code Wet, loose, gray, fine to coarse SAND, odor. 25 SW 30 Wet, loose, gray, fine to coarse SAND. SW 35 Wet, loose, gray, fine to coarse SAND. SW Wet, loose, gray, fine to medium SAND, slight odor. SP 40 Wet, medium dense, dark gray, fine to coarse SAND, some stiff clay lenses, odor. SC Wet, medium dense, very fine to medium SAND, some stiff clay and silt lenses, odor. SC/SM 45 Wet, medium dense, gray, very fine to coarse SAND, odor. SW Wet, stiff, gray CLAY, odor. CL Wet, medium dense, gray, fine to coarse SAND, little clay, odor. SW/SC 50.0

Page 1 of 1



Site: LCP Brunswick Boring No: MW-3A Diameter: 2 in Date: 09/19/2012

Northing: 431547.14

Driller: Billy Moss (Groundwater Protection Inc)

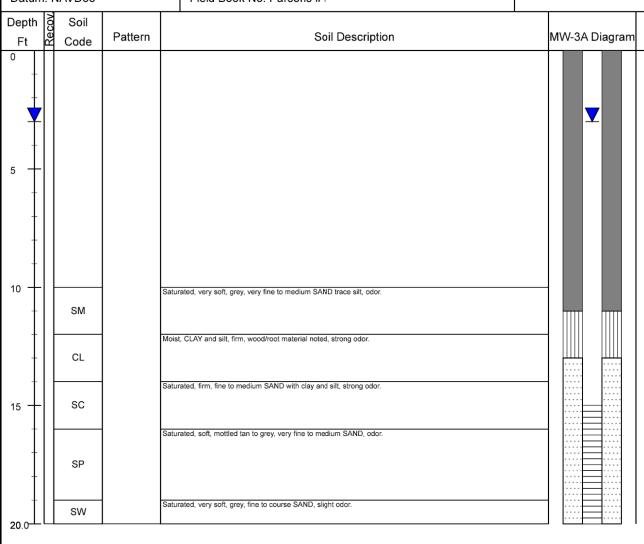
Easting: 861687.76 Elevation: 13.19 Method: Sonic

Consultant: Christine Jaynes (PARSONS)

Datum: NAVD88

Field Book No: Parsons #1

Total Depth: 20.0 Ft GW Depth: 3.0 Ft





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Site: LCP Brunswick

Boring No: SW-1 Diameter: 6 in

Date: 09/18/2012

Northing: 431518.21 Easting: 861719.08

Elevation: 13.03

Driller: Billy Moss (Groundwater Protection Inc)

Method: Sonic

Consultant: Christine Jaynes (PARSONS)

Total Depth: 50.0 Ft

GW Depth: 4.0 Ft

Datum: NAVD88			Field Book No: Parsons #1	
Depth S	Soil	Pattern	Soil Description	SW-1 Diagram
Ft r	Code	1 attern	Our Description	3VV-1 Diagram
			ry, loose, white, very fine to medium SAND.	_
	SP		,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,	
5	SM		oist, loose, brown/tan, fine to medium SAND, trace silt.	
	SM		let, loose, dark gray, very fine to medium SAND, some silt.	
+	SM		oist, loose, gray/brown mottled with dark gray, very fine to medium SAND, some silt, trace see roots.	
10 +	CL		et, medium stiff, dark gray/black, CLAY, some silt, trace root material, odor.	
	SM	7	let, loose, light brown/tan mottled with dark gray lenses, fine to medium SAND, some silt, odor.	
15 +	SP	7	let, medium dense, light tan, very fine to medium SAND, odor.	
+	sw		let, medium dense, light gray, fine to coarse SAND, odor.	
20 -	sw		let, loose, gray, fine to coarse SAND, odor.	
25	Boring G	W Depth		

Page 2 of 2



Site: LCP Brunswick

Boring No: SW-1 Diameter: 6 in

Date: 09/18/2012

Northing: 431518.21 Easting: 861719.08

Driller: Billy Moss (Groundwater Protection Inc)

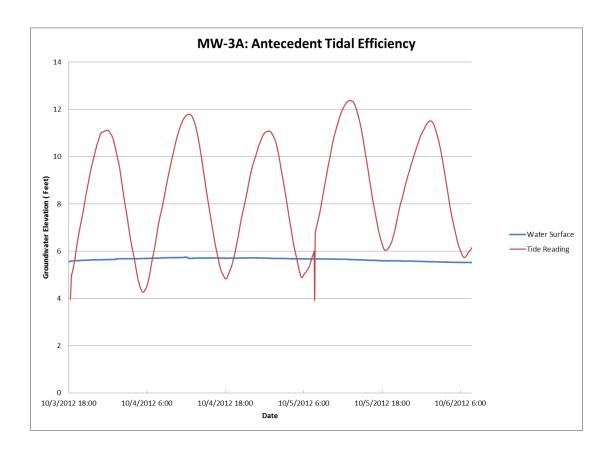
Method: Sonic

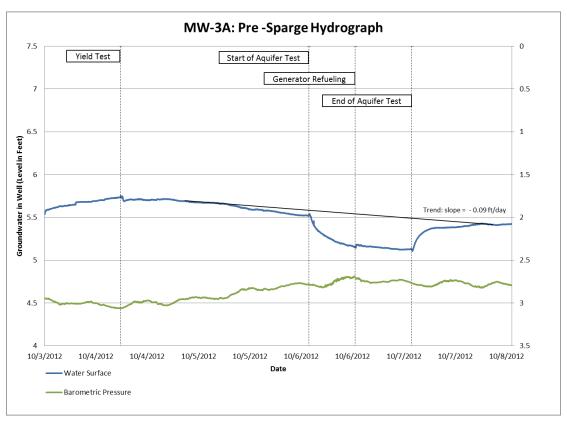
Consultant: Christine Jaynes (PARSONS)

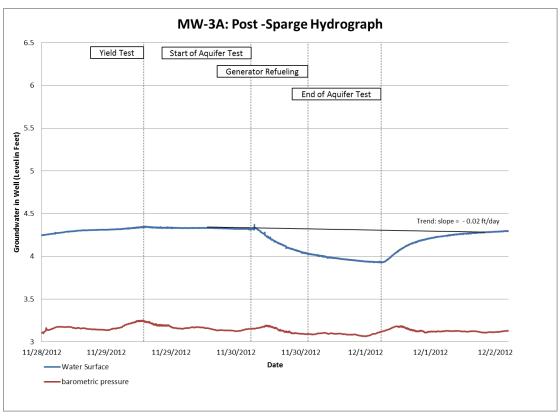
Total Depth: 50.0 Ft GW Depth: 4.0 Ft

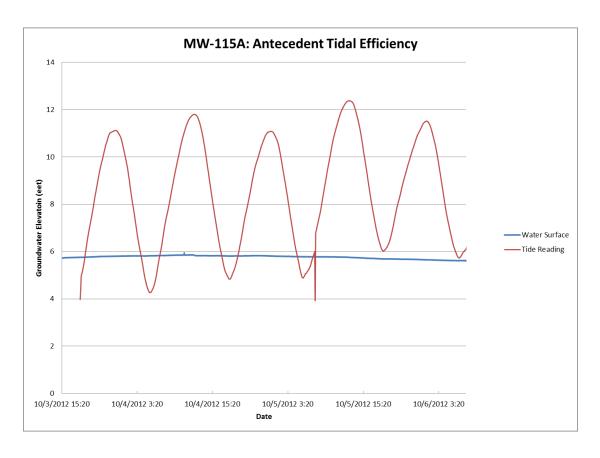
Elevation: 13.03 Datum: NAVD88 Field Book No: Parsons #1 Depth Soil Pattern Soil Description SW-1 Diagram Code Ft Wet, loose, gray, fine to coarse SAND, odor. 25 SW 30 35 Wet, medium dense, gray, fine to coarse SAND. SW Wet, loose, very fine to medium SAND, some clay stringers, odor. SC 40 Wet, loose, gray, fine to coarse SAND, little clay stringers at 42.5 ft, odor. SW/SC 45 Wet, medium dense, gray, fine to coarse SAND, and clay, odor. SC 50.0

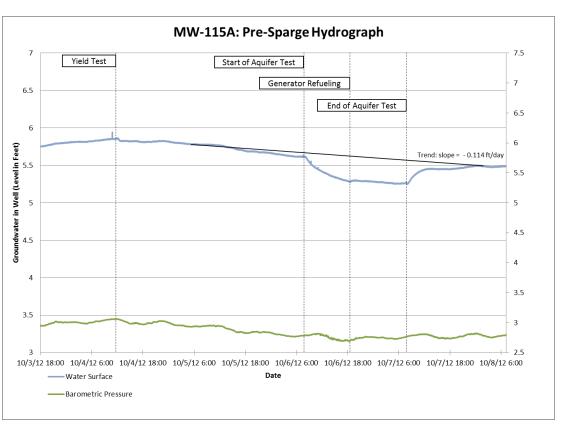
#### APPENDIX B. HYDROGRAPHS FOR OBSERVATION WELLS DURING AQUIFER TESTING

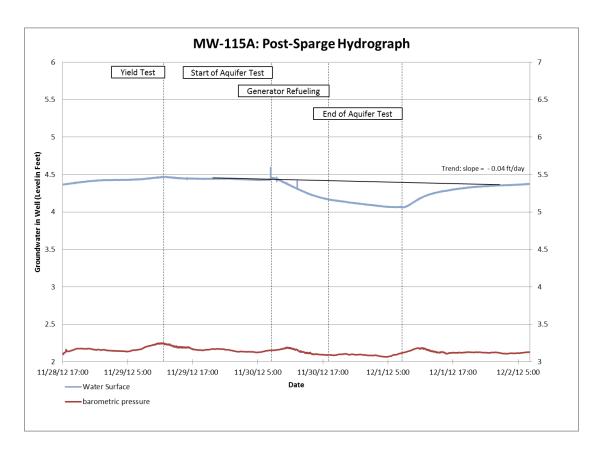


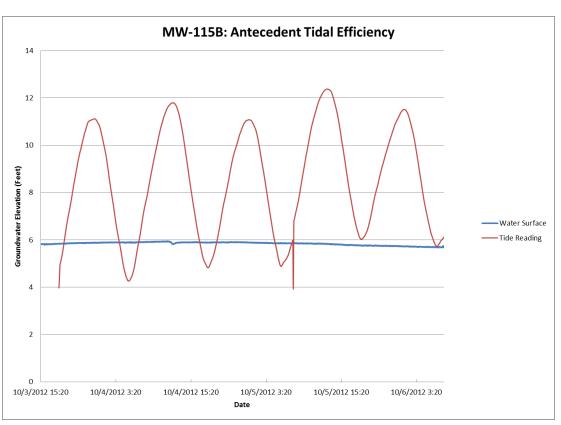


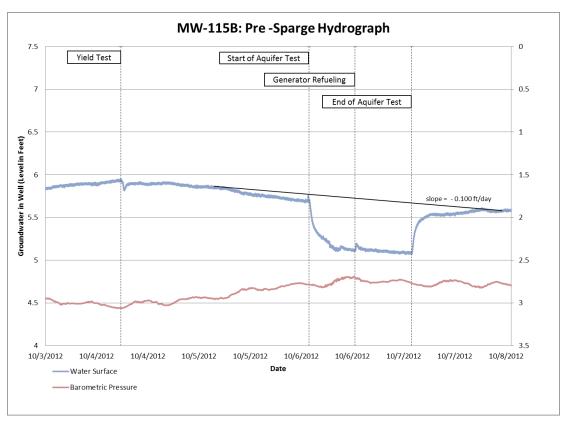


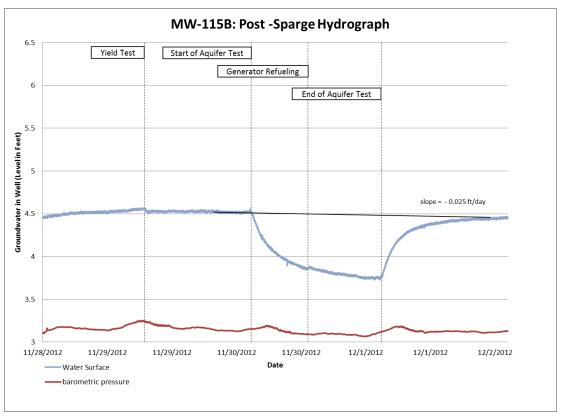


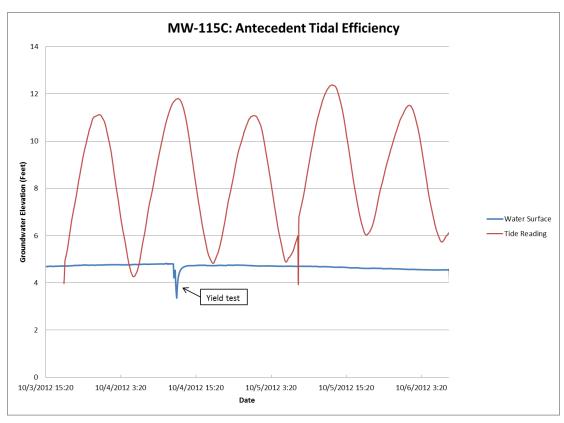


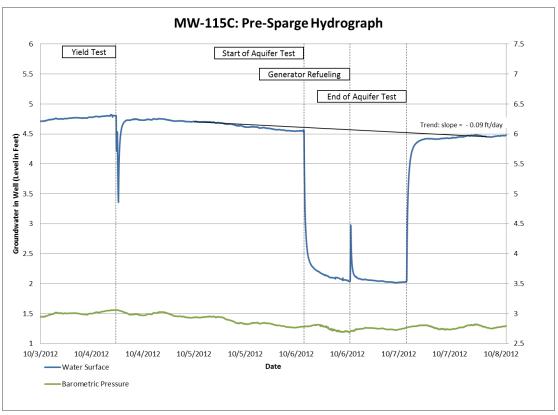


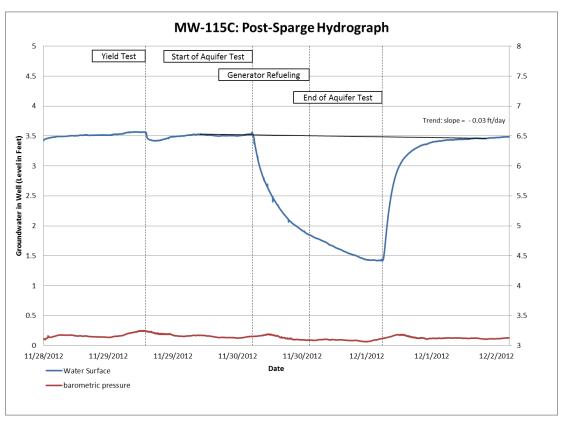


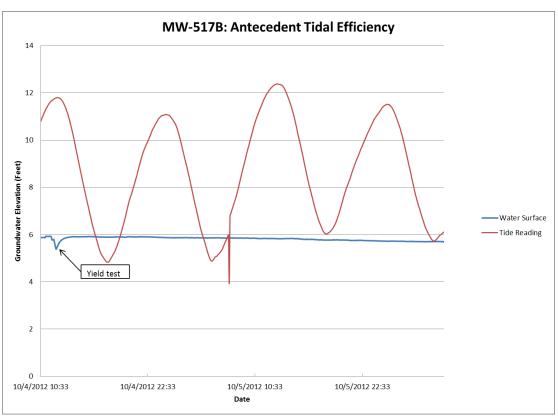


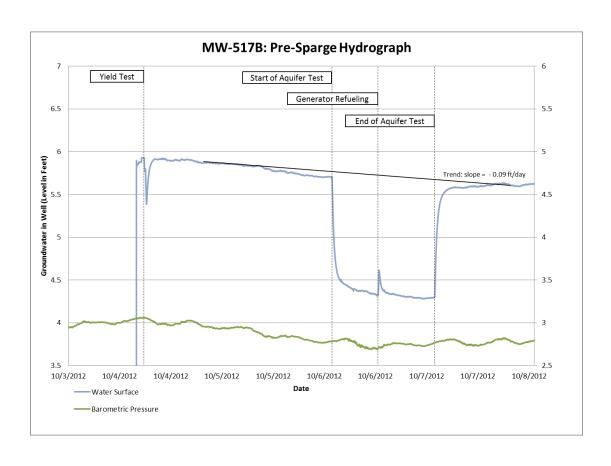


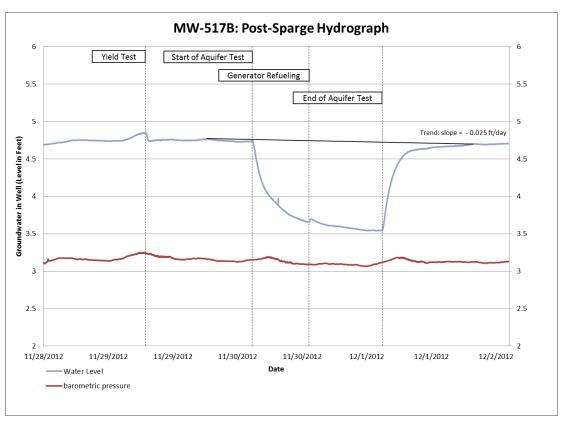


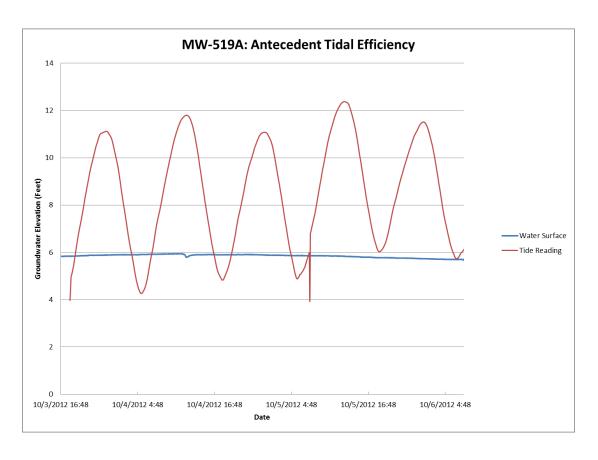


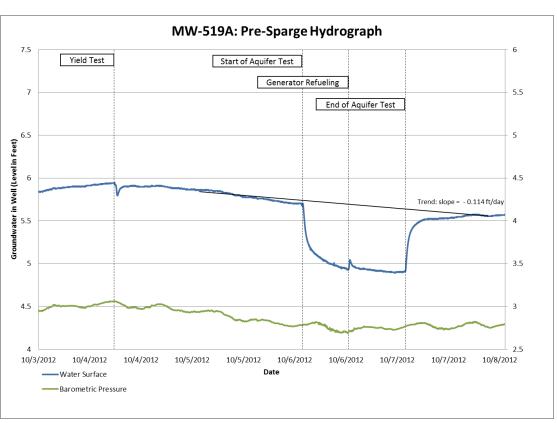


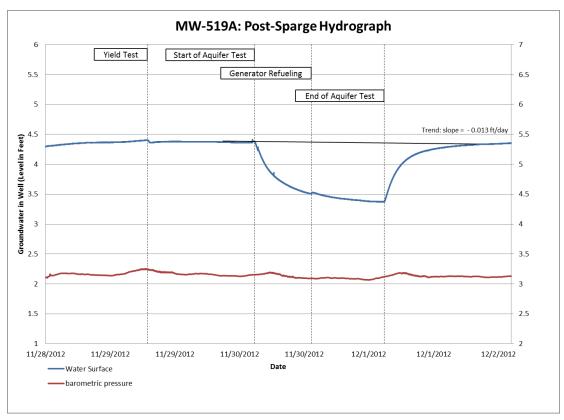


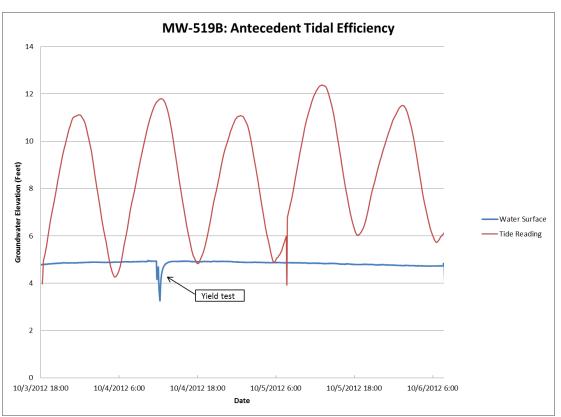


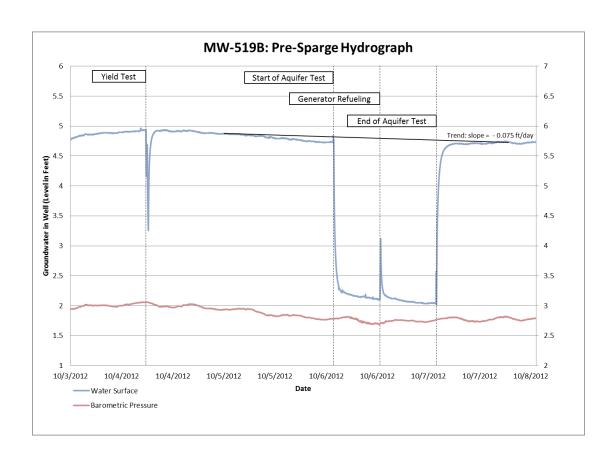


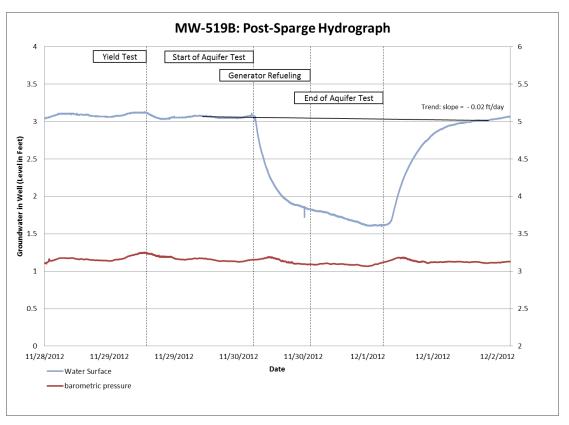


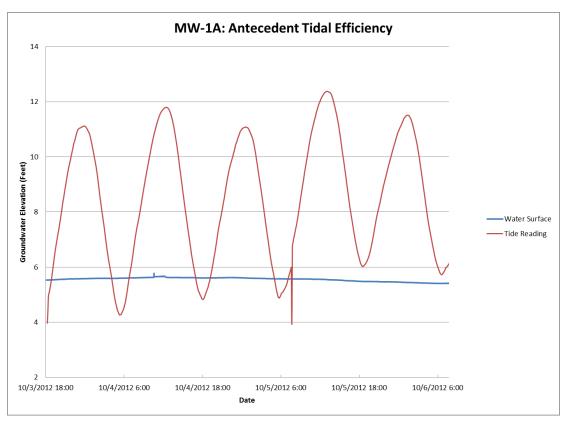


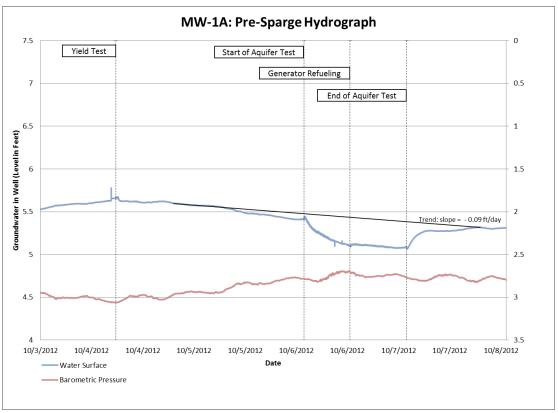


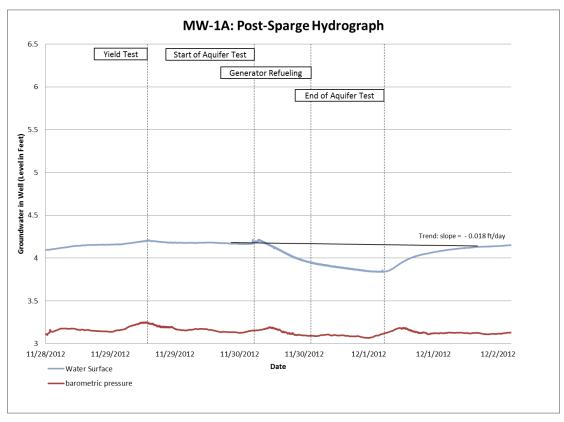


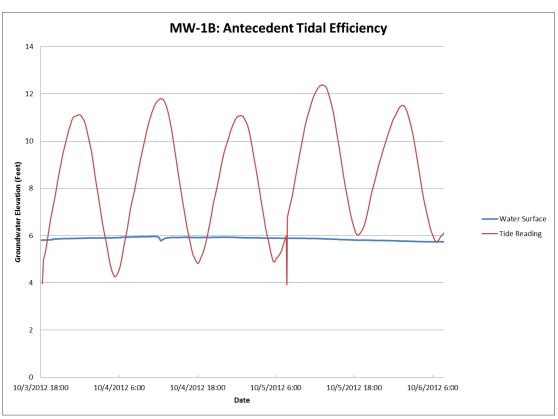


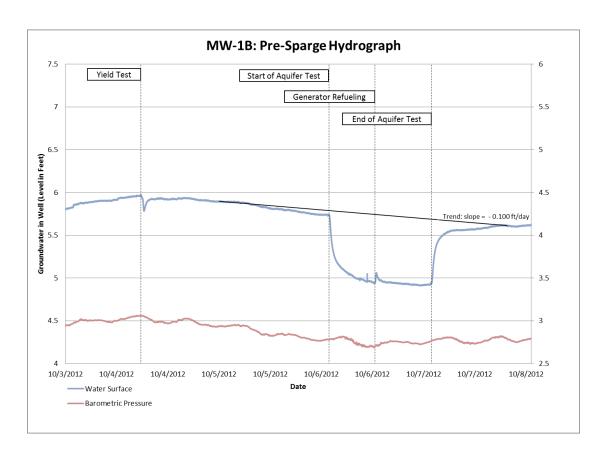


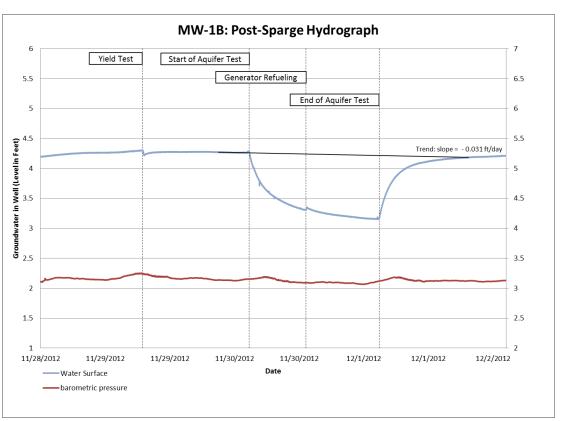


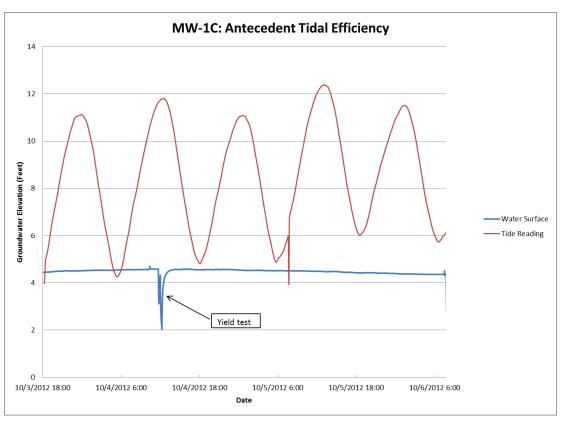


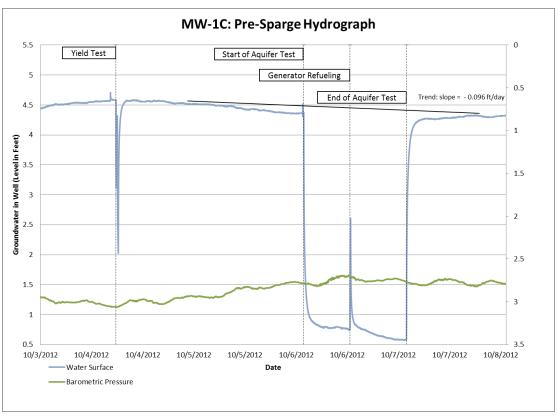


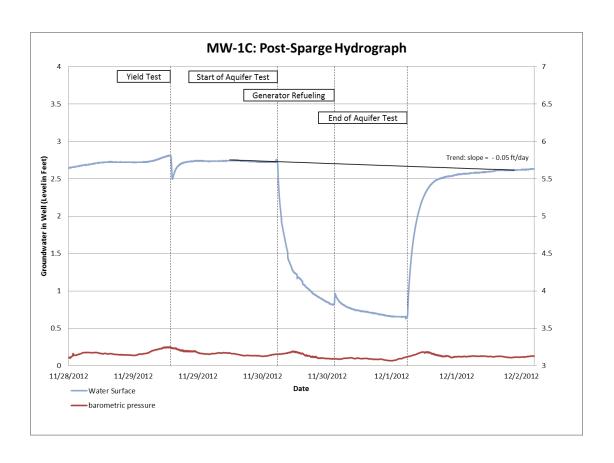


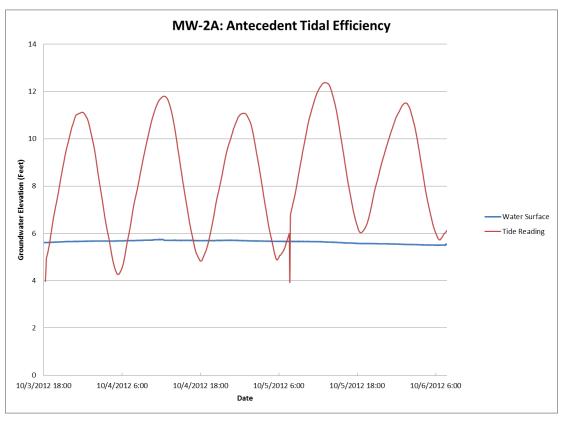


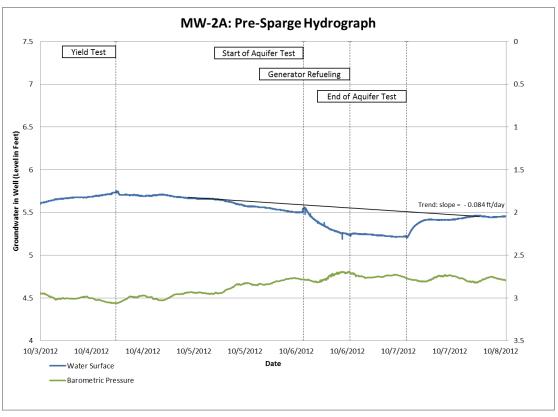


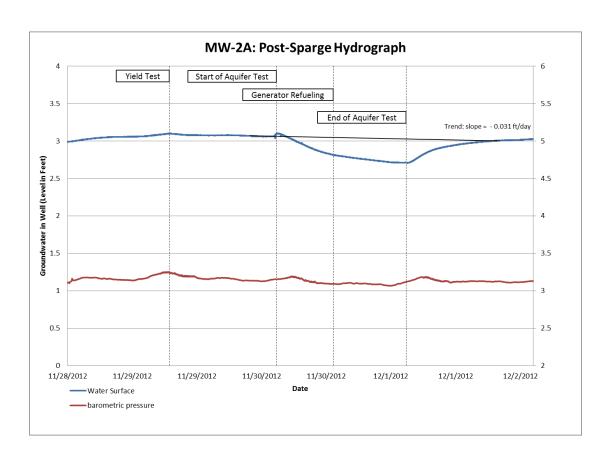


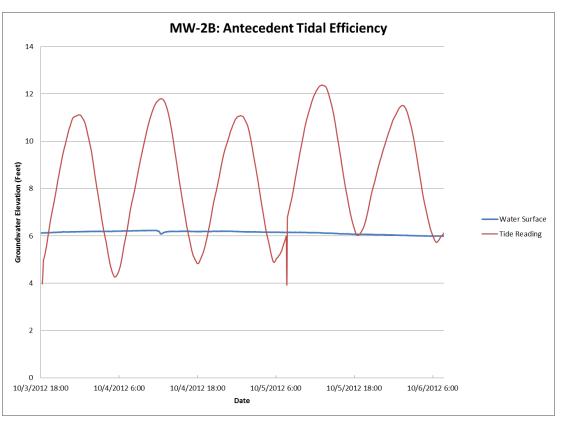


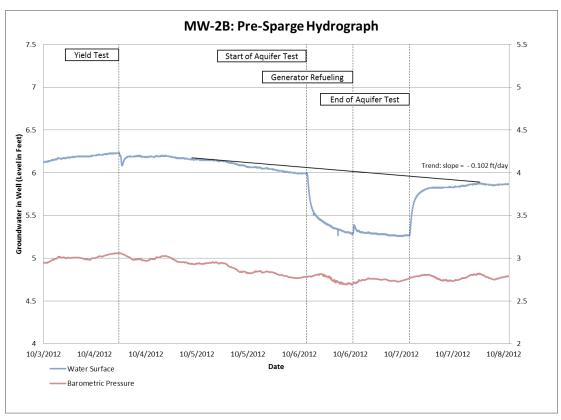


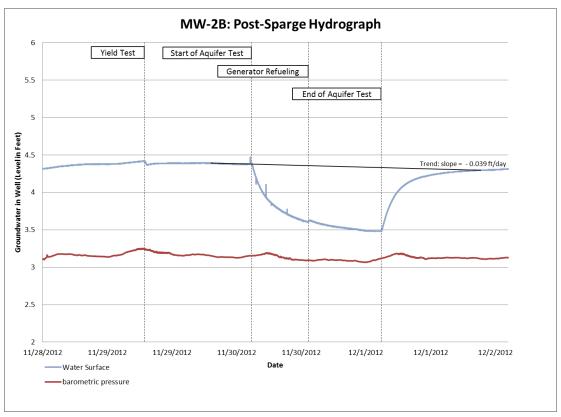


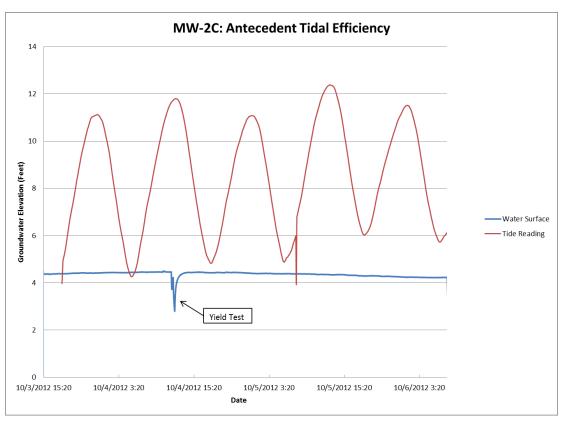


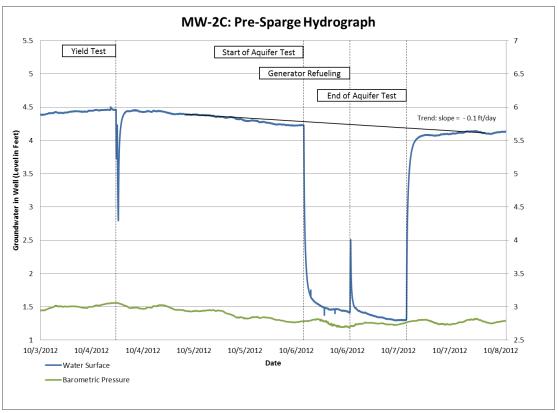


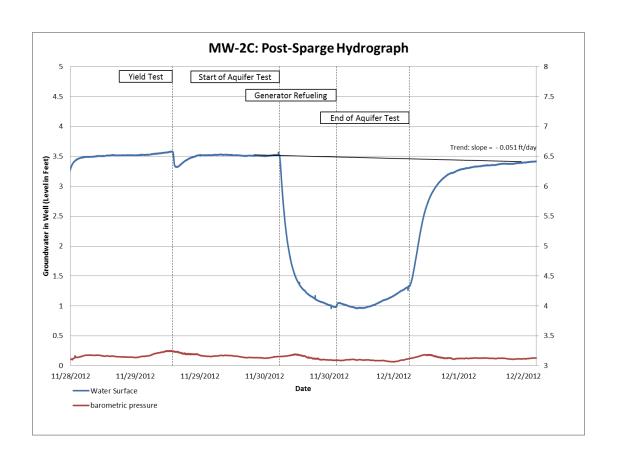












# APPENDIX C. PURGE LOGS

					- 1-									
SITE NAME: LC	P Chemical Site	:			_	ITE OCATION: Br	unswick, G	iA						
WELL NO:	: MW-1A			SAMPL	E ID: MW-1A	1				DATE: 1	0/2/12			
					PUR	GING DA	TA							
WELL		TUB			LL SCREEN	INTERVAL	STA	ATIC D				E PUMP T	YPE	
DIAMETEI	R (inches): 2	DIAM	METER (inches):	1/4 DE fee	, ,	8 feet to 23	3 TO	WATE	R (feet btoc): 7.	19	OR BA	ILER: PP		
	LUME PURGE: it if applicable)	1 WELL \	OLUME = (TO			ATIC DEPTH	TO WATER	R) X	WELL CAPACI	TY				
	,		= (		feet -			et) X		ons/foot			gallons	
	NT VOLUME PU it if applicable)	JRGE: 1 E	QUIPMENT VOI	L. = PUMP VO	LUME + (TUI	BING CAPAC	ITY X	TU	IBING LENGTH)	+ FLOW	/ CELL	VOLUME		
	11.15.05.TUDIN		= +.10 gallons					ns =	1		- 1 -			
	JMP OR TUBING WELL (feet btoo	-	_	MP OR TUBIN   WELL (feet b	-	PURGIN INITIAT	NG ED AT: 13	847	PURGING ENDED AT:	1556		TOTAL VOL PURGED (g	_UME gallons): 1.95	
TIME	VOLUME PURGED (gallons)	CUMUL VOLUM PURGE	E PURGE D RATE	DEPTH TO WATER (feet	pH (standard units)	TEMP.	SP CO		DISSOLVED OXYGEN (% saturation)	TURB (NT		ORP (mV)	,	
1548	1.55	(gallons	0.05	5toc) 7.14	8.48	25.52	6.85	4	1.2	65	5.7	-257.3	3	
1550	0.10	1.65	0.05	7.14	8.48	25.31	6.84		1.2	65		-274.		
	1552     0.10     1.75     0.05     7.14     8.47     25.08     6.839     1.2     66.4     -273.7       1554     0.10     1.85     0.05     7.14     8.48     24.92     6.831     1.2     70.1     -276.6       1556     0.10     1.95     0.05     7.14     8.48     24.88     6.842     1.2     69.6     -277.8     1.001													
1000														
WELL CA	ELL CAPACITY (Gallons Per Foot): <b>0.75</b> " = 0.02; <b>1</b> " = 0.04; <b>1.25</b> " = 0.06; <b>2</b> " = 0.16; <b>3</b> " = 0.37; <b>4</b> " = 0.65; <b>5</b> " = 1.02; <b>6</b> " = 1.47; <b>12</b> " = 5.88 BING INSIDE DIA. CAPACITY (Gal./Ft.): <b>1/8</b> " = 0.0006; <b>3/16</b> " = 0.0014; <b>1/4</b> " = 0.0026; <b>5/16</b> " = 0.004; <b>3/8</b> " = 0.006; <b>1/2</b> " = 0.010; <b>5/8</b> " = 0.016													
			al./Ft.): <b>1/8</b> " = 0 includes above g		5" = 0.0014;	1/4" = 0.002	26; <b>5/1</b> 0	<b>6</b> " = 0.0	004; <b>3/8</b> " = 0.	.006;	1/2" =	0.010;	<b>5/8"</b> = 0.016	
PURGING	EQUIPMENT C	ODES:	<b>B</b> = Bailer;	<b>BP</b> = Bladder		ESP = Electric		ble Pur	np; <b>PP</b> = Pe	ristaltic F	Pump;	<b>O</b> = O	ther (Specify)	
CAMPI ED	BY (PRINT) / A	EEU IATIO	<u> </u>	CAMDI ED/C	SAMF SIGNATUR	PLING DA	ATA		1		ı			
	ohnson/Pai		<b>v.</b>	2	ia.	almae	i		SAMPLING INITIATED AT	: 1559		SAMPLIN ENDED A		
PUMP OR	TUBING WELL (feet): 20	) 5		TUBING MATERIAL (	CODE: Teflon	lined PF			FILTERED: Yes/ on Equipment Typ			de FILTE	ER SIZE: <u>0.45</u> μm	
	CONTAMINATION		UMP Y N	No	TUBING		replaced		DUPLICATE:	oc. Cyll	N <sub>0</sub>	0		
SAM	PLE CONTAINE	R SPECIF	ICATION		SAMPLE P	RESERVATIO	N		INTENDE	:D	SAN	MPLING	SAMPLE PUMP	
SAMPLE ID CODE	# CONTAINERS	MATERIAL CODE	VOLUME	PRESERVATUSED		TOTAL VOL ED IN FIELD (		INAL pH	ANALYSIS AN METHOL	)		IIPMENT CODE	FLOW RATE (mL per minute)	
MW-1A	1	PE	250mL	HNO3					6010B T/ Metals/7470		A	APP	125	
MW-1A	1	PE	125mL						3500 FE/ 90 pH		A	APP	125	
MW-1A	1	PE	250mL						6010B Diss Silica	olved	-	APP	250	
MW-1A									9056A_2					
MW-1A	1	PE AG	125mL 125mL						Chloride SM 5310 E			APP APP	125 125	
MW-1A	2	PE	250mL	NaOH Zinc Aceta	ate				SM4500 St			APP	Field-Filtered	
MW-1A	1	PE	500mL						2540C TI			APP	125	
MW-1A	1	PE	250mL						2320B Alka			APP	250	
MW-1A	1	AG	125mL	HCI					SM5310 T			APP	125	
was use									ing-In-Scree ater than 10					
MATERIA		AG = Amb	er Glass; CG	= Clear Glass;	PE = Pol	yethylene;	<b>PP</b> = Poly	propyle	ene; <b>S</b> = Silico	ne; <b>T</b>	= Teflo	n; <b>O</b> = C	Other (Specify)	
SAMPLIN	G EQUIPMENT	CODES:	APP = After Pe				Bladder F		ESP = Electri Gravity Drain):		ersible I			

SITE NAME: I C	P Chemical Site				SIT	E CATION: Bru	ınswick GA							
WELL NO:		<u>;                                    </u>		SAMPLE	ID: MW-1B	0711101111211			DATE:	10/2/12	!			
					PURG	ING DA	ΤΔ							
WELL DIAMETEI	R (inches): 2	TUBING	G TER (inches):		L SCREEN I	NTERVAL	STATIO	C DEPTH (btoc)			E PUMP T	/PE		
	LUME PURGE: it if applicable)	1 WELL VO		TAL WELL DEP		ΓΙC DEPTH T	,	X WELL CAP						
	NT VOLUME PU	URGE: 1 EQI	= ( JIPMENT VOI	= PUMP VOL	feet – .UME + (TUB	ING CAPACI		X 0.16 g	gallons/foot ΓΗ) + FLOV		VOLUME	gallons		
(only fill ou	it if applicable)	=	+.10 gallons	(0.0026 gall	ons/foot X 3	8 feet) + .1	0 gallons :	= 0.3 galloi	ns					
	JMP OR TUBIN	G	FINAL PU	MP OR TUBINO	<del></del>	PURGIN	G	PURGINO	3		TOTAL VOL			
DEPTH IN	WELL (feet bto	r e	DEPTH IN	WELL (feet bto	oc): 35	INITIATE	D AT: 1046	ENDED A	T: 1138	F	PURGED (g	gallons): 1.6		
TIME	VOLUME PURGED (gallons)	CUMUL. VOLUME PURGED (gallons)	PURGE RATE (gpm)	TO WATER (feet btoc)	pH (standard units)	TEMP. (°C)	SP COND. ( mS/cm)	DISSOLVE OXYGEN (% saturatio	TURE (NIT	BIDITY ΓUs)	ORP (mV)			
1111	0.75	0.75	0.03	7.00	8.91	25.06	6.366	1.8	55	5.9	-278.0	)		
1114	0.10	0.85	0.03	7.00	8.94	25.02	6.382	1.7	52	2.7	-289.	5		
1118	0.15	1.00	0.04	7.11	8.96	25.18	6.397	1.7	52	2.6	-284.4	4		
1122	1122         0.15         1.15         0.04         7.11         8.98         25.45         6.408         1.6         52.4         -293.0           1132         0.35         1.50         0.04         7.11         9.05         25.47         6.400         1.5         56.4         -347.1           1136         0.10         1.60         0.03         7.11         9.04         25.43         6.398         1.3         56.4         -359.8         0.999													
1132	1132     0.35     1.50     0.04     7.11     9.05     25.47     6.400     1.5     56.4     -347.1       1136     0.10     1.60     0.03     7.11     9.04     25.43     6.398     1.3     56.4     -359.8     0.999													
1136	1136 0.10 1.60 0.03 7.11 9.04 25.43 6.398 1.3 56.4 -359.8 0.999  /ELL CAPACITY (Gallons Per Foot): 0.75" = 0.02; 1" = 0.04; 1.25" = 0.06; 2" = 0.16; 3" = 0.37; 4" = 0.65; 5" = 1.02; 6" = 1.47; 12" = 5.88													
	ELL CAPACITY (Gallons Per Foot): <b>0.75</b> " = 0.02; <b>1</b> " = 0.04; <b>1.25</b> " = 0.06; <b>2</b> " = 0.16; <b>3</b> " = 0.37; <b>4</b> " = 0.65; <b>5</b> " = 1.02; <b>6</b> " = 1.47; <b>12</b> " = 5.88													
TUBING II	ELL CAPACITY (Gallons Per Foot): 0.75" = 0.02; 1" = 0.04; 1.25" = 0.06; 2" = 0.16; 3" = 0.37; 4" = 0.65; 5" = 1.02; 6" = 1.47; 12" = 5.88  JBING INSIDE DIA. CAPACITY (Gal./Ft.): 1/8" = 0.0006; 3/16" = 0.0014; 1/4" = 0.0026; 5/16" = 0.004; 3/8" = 0.006; 1/2" = 0.010; 5/8" = 0.016													
								Pump; <b>PP</b> =	Peristaltic	Pump;	<b>O</b> = O	ther (Specify)		
			,		SAMP	LING DA	ATA							
PUMP OR DEPTH IN	TUBING WELL (feet): 3	.5		TUBING MATERIAL C	ODE: Teflon I	ined PE		LD-FILTERED: ation Equipment			ide FILTE	R SIZE: <u>0.45</u> μm		
	CONTAMINATIO		IP Y	lo	TUBING		(replaced)	DUPLICAT		go N	lo			
SAM	PLE CONTAINE	ER SPECIFICA	ATION		SAMPLE PR	ESERVATIO	N	INTEN	IDED		MPLING	SAMPLE PUMP		
SAMPLE ID CODE	# CONTAINERS	MATERIAL CODE	VOLUME	PRESERVAT USED		OTAL VOL D IN FIELD (I	mL) FINA	MET	HOD		IIPMENT CODE	FLOW RATE (mL per minute)		
MW-1B	1	PE	250mL	HNO3				6010E Metals/7		,	APP	125		
MW-1B	1	PE	125mL					3500 FE		,	APP	63		
MW-1B	1	PE	250mL					6010B D Sili		١,	APP	125		
			2002					9056A	_28D			0		
MW-1B	1	PE	125mL					Chlor Sulf		,	APP	63		
MW-1B	1	AG	125mL					SM 531	0 DOC	,	APP	125		
MW-1B	2	PE	250mL	NaOH Zinc Aceta	te			SM4500	Sulfide	,	APP	Field-Filtered		
MW-1B	1	PE	500mL					25400		,	APP	83		
MW-1B	1	PE	250mL					2320B A	lkalinity	/	APP	83		
MW-1B	1	AG	125mL	HCI				SM531			APP	125		
								ubing-In Sci	eened-l	nterv	al purge	method		
used. T	urbidity gre	ater than  AG = Amber		ut within 1( = Clear Glass;	)%. Purge PE = Poly		ear browr PP = Polypro		licone; T	= Teflo	n: <b>0</b> = 0	Other (Specify)		
	L GODES:										,, <b>U</b> = C	riner (opecity)		
SAMPI IN	G EQUIPMENT	CODES: 4	APP = After P	eristaltic Pump;	<b>B</b> = Bail	er: <b>RP</b> –	Bladder Pum	D: ESP = Fla	ctric Subm	ersible	Pump.			

**NOTES:** Stabilization Criteria for Range of Variation of Last Three Consecutive Readings: **pH:**  $\pm$  0.1 unit **Specific Conductance:**  $\pm$  5% **Dissolved Oxygen:** all readings  $\leq$  10% saturation; optionally,  $\pm$  0.2 mg/L **Turbidity:** all readings  $\leq$  10 NTU; or  $\pm$  10%

SITE						SITE								
WELL NO:	P Chemical MW-1C			SAMP	LE ID: MW	LOCATION:	Brunswi	ick, GA		DATE: 1	10/2/12			
WELE NO.	. WIVV-10			O/AIVII		RGING [	λΤΛ			DAIL.	10/2/12			
WELL DIAMETER	R (inches): 2	TUBING DIAME	FER (inches): 1/		ELL SCRE	EN INTERVA 45 feet to 5	L	STATIC I	DEPTH ER (feet btoc ): 8			E PUMP T'	YPE	
	LUME PURGE: it if applicable)	1 WELL VOL	_UME = (TOTA = (	L WELL DI	EPTH - S	STATIC DEPT	H TO W	ATER) X	WELL CAPACI	TY ons/foot	=		gallons	
	NT VOLUME PU it if applicable)				OLUME + (		ACITY + .10		UBING LENGTH)	+ FLOW		VOLUME	gamente	
	JMP OR TUBIN WELL (feet bto	G	FINAL PUMF DEPTH IN W	OR TUBI	NG	PUR	GING ATED A		PURGING ENDED AT:			TOTAL VOI PURGED (g	_UME gallons): 1.2	
TIME	VOLUME PURGED (gallons)	CUMUL. VOLUME PURGED (gallons)	PURGE RATE (gpm)	DEPTH TO WATER (feet btoc)	pН			P COND. mS/cm)	DISSOLVED OXYGEN (% saturation)	_	BIDITY 'Us)	ORP (mV)	,	
1107	1.0	1.0	0.05	8.5	12.20			58.48	1.5	5.	70	-347.	7	
1109	0.1	1.1	0.05	8.5	12.22			58.50	1.5		88	-351.	-	
1111	0.1	1.2	0.05	8.5	12.2	4 24.14	·	58.52	1.6	7.	12	-354.	4 1.023	
	WELL CAPACITY (Gallons Per Foot): 0.75" = 0.02; 1" = 0.04; 1.25" = 0.06; 2" = 0.16; 3" = 0.37; 4" = 0.65; 5" = 1.02; 6" = 1.47; 12" = 5.88  TUBING INSIDE DIA. CAPACITY (Gal./Ft.): 1/8" = 0.0006; 3/16" = 0.0014; 1/4" = 0.0026; 5/16" = 0.004; 3/8" = 0.006; 1/2" = 0.010; 5/8" = 0.016													
TUBING IN		PACITY (Gal./F	Ft.): <b>1/8"</b> = 0.0	006; <b>3/1</b>				<b>3</b> " = 0.37; <b>5/16</b> " = 0					<b>12"</b> = 5.88 <b>5/8"</b> = 0.016	
PURGING	EQUIPMENT C	ODES: B	= Bailer; B	P = Bladde		ESP = Elec			mp; <b>PP</b> = Pe	eristaltic l	Pump;	<b>O</b> = O	ther (Specify)	
SAMPLED	BY (PRINT) / A	FEILIATION:		SAMPLER	SAN S) SIGNAT	IPLING	DATA	4	1		I			
	ohnson/Pa			2	ria	) colon	Zell		SAMPLING INITIATED A	T: 1117		SAMPLIN ENDED A		
PUMP OR DEPTH IN	TUBING WELL (feet): 4	7.5		UBING MATERIAL	CODE: Te	flon-lined PE			on Equipment Ty			de FILTE	R SIZE: 0 <u>.45</u> μm	
	CONTAMINATION		l l		TUBI		No (rep	•	DUPLICATE:		N <sub>0</sub>	0		
	PLE CONTAINE					PRESERVA			INTENDE		_	MPLING IIPMENT	SAMPLE PUMP FLOW RATE	
SAMPLE ID CODE	# CONTAINERS	MATERIAL CODE	VOLUME F	RESERVA USED		TOTAL VC DDED IN FIEL		FINAL pH	ANALYSIS AI METHO			CODE	(mL per minute)	
MW- 1C	1	PE	250mL	HNO	3				6010B T Metals/7470			APP	125	
MW- 1C	1	PE	125mL						3500 FE/ 9 pH	040B	A	APP	125	
MW- 1C	1	PE	250mL						6010B Diss Silica		A	APP	125	
MW- 1C	1	PE	125mL						9056A_2 Chloride	28D	A	APP	125	
MW- 1C	1	AG	125mL						SM 5310 I		A	APP	125	
MW- 1C	2	PE	250mL	NaOH Zinc Ace					SM4500 S	ulfide	A	APP	Field-Filtered	
MW- 1C	1	PE	500mL						2540C T	DS	A	APP	167	
MW- 1C	1	PE	250mL						2320B Alka	alinity		APP	125	
MW- 1C	1	AG	125mL	HCI					SM5310 T			APP	125	
REMARKS	e: Per SOP, Purge water			r three	reading	s prior to s	sampli	ing. Tuk	oing-in-Scree	en- Inte	erval	Purge r	method	
MATERIAI		AG = Amber		Clear Glass	s; PE =	Polyethylene;	PP =	= Polypropy	lene; <b>S</b> = Silico	one; <b>T</b>	= Teflo	n; <b>O</b> = 0	Other (Specify)	
SAMPLING	G EQUIPMENT		APP = After Peri					lder Pump;	ESP = Electr					

SITE NAME: LC	P Chemical Site	<u> </u>			SIT	E CATION: Bru	unswick	k. GA						
WELL NO:				SAMPLE	ID: MW-2A			.,		DATE:	10/3/12			
				I	PURG	ING DA	TA							
	R (inches): 2		TER (inches):	1/4 (btoo	L SCREEN IN c) DEPTH: 18.	.5 feet to 23	3.5	TO WATE	EPTH (btoc) R (feet): 7.15		-	E PUMP TY AILER: PP	PE .	
(only fill ou	t if applicable)		= (		feet –			feet) X		lons/foot			gallons	
	NT VOLUME PO t if applicable)				`				JBING LENGTH = 0.26 gallor		V CELL	. VOLUME		
	JMP OR TUBIN WELL (feet bto			MP OR TUBING WELL (feet bto		PURGIN INITIATE	-	1439	PURGING ENDED AT:	1501		TOTAL VOL PURGED (g	UME allons): 1.2	
TIME	VOLUME PURGED (gallons)	CUMUL. VOLUME PURGED (gallons)	PURGE RATE (gpm)	DEPTH TO WATER (feet btoc)	pH (standard units)	TEMP. (°C)		COND. nS/cm)	DISSOLVED OXYGEN (% saturation)		BIDITY 'Us)	ORP (mV)	SP Gravity (sg)	
1456	1.0	1.0	0.06	7.1	8.77	24.77	6.	.802	1.6	96	6.8	-188.7	7	
1458	0.1	1.1	0.05	7.1	8.76	24.74		.809	1.5		7.7	-191.6		
1500	1500 0.1 1.2 0.05 7.1 8.74 24.69 6.810 1.5 99.7 -193.7 1.001													
	WELL CAPACITY (Gallons Per Foot): 0.75" = 0.02; 1" = 0.04; 1.25" = 0.06; 2" = 0.16; 3" = 0.37; 4" = 0.65; 5" = 1.02; 6" = 1.47; 12" = 5.88													
WELL CA	UBING INSIDE DIA. CAPACITY (Gal./Ft.): 1/8" = 0.0006; 3/16" = 0.0014; 1/4" = 0.0026; 5/16" = 0.004; 3/8" = 0.006; 1/2" = 0.010; 5/8" = 0.016													
TUBING II	BING INSIDE DÍA. CAPACITY (Gal./Ft.): 1/8" = 0.0006; 3/16" = 0.0014; 1/4" = 0.0026; 5/16" = 0.004; 3/8" = 0.006; 1/2" = 0.010; 5/8" = 0.016													
					Pump; ES	<b>SP</b> = Electric	Subme	ersible Pu	mp; <b>PP</b> = P	eristaltic	Pump;	<b>O</b> = Ot	her (Specify)	
							ATA		_					
	TUBING INSIDE DIA. CAPACITY (Gal./Ft.): 1/8" = 0.0006; 3/16" = 0.0014; 1/4" = 0.0026; 5/16" = 0.004; 3/8" = 0.006; 1/2" = 0.010; 5/8" = 0.016  BTOC = Below top of casing —which includes above grade riser  PURGING EQUIPMENT CODES: B = Bailer; BP = Bladder Pump; ESP = Electric Submersible Pump; PP = Peristaltic Pump; O = Other (Specify)  SAMPLING DATA  SAMPLED BY (PRINT) / AFFILIATION:  Maria Johnson/Parsons  SAMPLING SAMPLING INITIATED AT: 1506  SAMPLING ENDED AT: 1524													
PUMP OR	TUBING WELL (feet): 21	1.5		TUBING MATERIAL CO					-FILTERED: Yes			de FILTER	R SIZE: <u>0.45</u> μm	
	CONTAMINATION TO THE CONTAMINA		P Y N	lo	TUBING		(repla		DUPLICATE:		nige N	lo		
SAM	PLE CONTAINE	R SPECIFICA	TION		SAMPLE PRE	ESERVATIO	N		INTEND	ED	SAN	MPLING	SAMPLE PUMP	
SAMPLE ID CODE	# CONTAINERS	MATERIAL CODE	VOLUME	PRESERVATI USED		OTAL VOL ) IN FIELD (	mL)	FINAL pH	ANALYSIS A METHO	D		JIPMENT CODE	FLOW RATE (mL per minute)	
MW-2A	1	PE	250mL	HNO3					6010B T Metals/747		,	APP	250	
MW-2A	1	PE	125mL						3500 FE/ 9 pH		A	APP	125	
MW-2A	1	PE	250mL						6010B Diss Silica		,	APP	250	
									9056A_2 Chloride					
MW-2A	1	PE	125mL						Sulfate		,	APP	125	
MW-2A	1	AG	125mL	 NaOH					SM 5310	DOC	A	APP	125	
MW-2A	2	PE	250mL	Zinc Aceta	te				SM4500 S	ulfide	,	APP	Field-Filtered	
MW-2A	1	PE	500mL						2540C T	DS	1	APP	250	
MW-2A	1	PE	250mL						2320B Alka		1	APP	250	
MW-2A	1 Dor SOD	AG	125mL	HCI for three re	adings or	ior to col	loctio	 na com:	SM5310 <sup>-</sup> ole. Tubing-			APP d- Inton	125	
									er dark brow		CC110	u- mierv	ai puige	
MATERIA		AG = Amber (		= Clear Glass;	<b>PE</b> = Polye	ethylene;			ene; <b>S</b> = Silico		= Teflo	n; <b>O</b> = C	ther (Specify)	
SAMPLIN	G EQUIPMENT			eristaltic Pump;				er Pump;	ESP = Electric Gravity Drain):					

NOTES: Stabilization Criteria for Range of Variation of Last Three Consecutive Readings: -pH:  $\pm$  0.1 unit Specific Conductance:  $\pm$  5% Dissolved Oxygen: all readings  $\leq$  10% saturation; optionally,  $\pm$  0.2 mg/L Turbidity: all readings  $\leq$  10 NTU; or  $\pm$  10%

SITE NAME: LC	P Chemical Site					SIT	TE CATION: Bru	ınswi	ck GA					
WELL NO:				SA	MPLE ID:		<u> </u>	<u> </u>	on, or t		DATE:	10/3/12		
				<u> </u>	F	PURG	ING DA	TA						
WELL DIAMETEI	R (inches): 2	TUE	ING METER (inches):	1/4			NTERVAL 4 feet to 38 f	feet		DEPTH (btoc) ER (feet): 6.82			E PUMP T'	YPE
	LUME PURGE: it if applicable)	1 WELL	/OLUME = (TO	TAL WEL	L DEPTH	- STAT	TIC DEPTH 1	TO W	ATER) X	WELL CAPAC	CITY			
FOLIPME	NT VOLUME PL	IRGF: 1 F	= ( QUIPMENT VOI	= PUM	feet		ING CAPACI	ITY	feet) X	0.16 ga UBING LENGTH	llons/foo		VOLUME	gallons
	it if applicable)	J	= +.10 gallons			,					,	0222	VOLONIE	
	JMP OR TUBIN		FINAL PUI DEPTH IN		UBING eet btoc): 3	36	PURGIN INITIATE	-	Γ: 1348	PURGING ENDED AT	: 1430		FOTAL VOI PURGED (g	LUME gallons): 3.1
		CUMU	1	DEF						D100011/5D		1		
TIME	VOLUME PURGED (gallons)	VOLUM PURGE (gallon:	D RATE	T( WAT (fe	ΓER (sta	pH andard units)	TEMP. (°C)		P COND. mS/cm)	DISSOLVED OXYGEN (% saturation)	(N	BIDITY TUs)	ORP (mV)	
1412	1.90	1.90	0.08	6.8	39 9	9.37	23.86		5.762	2.3	1	9.1	-276.	6
1417	0.60	2.50	0.12	6.8		9.37	23.69		5.787	2.3		4.6	-294.	4
1422	0.25	2.75	0.05	6.8		9.36	23.65		5.740	2.2		5.6	-308.	
1426	0.35	3.10	0.09	6.8	39 9	9.36	23.77	;	5.736	2.1	1	5.9	-315.	6 1.000
	WELL CAPACITY (Gallons Per Foot): 0.75" = 0.02: 1" = 0.04: 1.25" = 0.06: 2" = 0.16: 3" = 0.37: 4" = 0.65: 5" = 1.02: 6" = 1.47: 12" = 5.88													
	ELL CAPACITY (Gallons Per Foot): 0.75" = 0.02; 1" = 0.04; 1.25" = 0.06; 2" = 0.16; 3" = 0.37; 4" = 0.65; 5" = 1.02; 6" = 1.47; 12" = 5.88													
TUBING II	JBING INSIDE DIA. CAPACITY (Gal./Ft.): 1/8" = 0.0006; 3/16" = 0.0014; 1/4" = 0.0026; 5/16" = 0.004; 3/8" = 0.006; 1/2" = 0.010; 5/8" = 0.016  FOC = Below top of casing —which includes above grade riser													
PURGING	EQUIPMENT C	ODES:	<b>B</b> = Bailer;	<b>BP</b> = Bla	dder Pump	); <b>E</b> \$	SP = Electric	Subn	nersible Pu	mp; <b>PP</b> = F	Peristaltic	Pump;	<b>0</b> = 0	ther (Specify)
							LING DA	<b>ATA</b>	١	1		ı		
	BY (PRINT) / A ne Jaynes/P		N:		ER(S) SIG					SAMPLING			SAMPLIN	
	-				- a	ejv	100)			INITIATED A	AT: 1441		ENDED A	T: 1459
PUMP OR	TUBING WELL (feet): 36			TUBING	AL CODE	· Teflon-l	ined PF			-FILTERED: Ye on Equipment T			de FILTE	R SIZE: <u>0.45</u> μm
	CONTAMINATION		UMP Y N	lo		TUBING		(repl	laced)	DUPLICATE		niigea N	lo	
SAM	PLE CONTAINE	R SPECIF	ICATION		SAM	IPLE PR	ESERVATIO	N .	<u> </u>	INTEND	DED	SAI	MPLING	SAMPLE PUMP
SAMPLE ID CODE	# CONTAINERS	MATERIAL CODE	VOLUME	_	RVATIVE SED		OTAL VOL D IN FIELD (	mL)	FINAL pH	ANALYSIS A	AND/OR	EQU	JIPMENT CODE	FLOW RATE (mL per minute)
MW-2B	1	PE	250mL	Н	NO3					6010B Metals/747		,	APP	250
MW-2B	1	PE	125mL							3500 FE/ pH	9040B	,	APP	125
MW-2B	1	PE	250mL							6010B Dis	solved	,	APP	250
MW-2B	1	PE	125mL							9056A_ Chlorid Sulfa	28D e &	,	APP	125
MW-2B	1	AG	125mL							SM 5310		,	APP	125
MW-2B	2	PE	250mL		aOH Acetate					SM4500 S		,	APP	Field-Filtered
MW-2B	1	PE	500mL							2540C	TDS	,	APP	250
MW-2B	1	PE	250mL							2320B Alk	alinity	,	APP	250
MW-2B	1	AG	125mL	F	ICI					SM5310	TOC	,	APP	125
			eters stable r brown. Tu								in-Scr	eenec	d- Interv	al purge
MATERIA		AG = Amb		= Clear G			ethylene;		Polypropy		one; 1	Γ = Teflo	n; <b>O</b> = 0	Other (Specify)
SAMPLIN	G EQUIPMENT	CODES:	APP = After Po			<b>B</b> = Bail ump;			der Pump; od (Tubing	ESP = Elec Gravity Drain);		nersible Other (S		

NOTES: Stabilization Criteria for Range of Variation of Last Three Consecutive Readings: -pH:  $\pm 0.1$  unit Specific Conductance:  $\pm 5\%$  Dissolved Oxygen: all readings  $\leq 10\%$  saturation; optionally,  $\pm 0.2$  mg/L Turbidity: all readings  $\leq 10$  NTU; or  $\pm 10\%$ 

SITE					SIT								
WELL NO:	P Chemical Site			SAMPLE	ID: MW-2C	CATION: Bru	ınswick, G	A		DATE:	10/3/12	······································	
WELL NO.	10100 20			O/ WIT EE		ING DA	ТΛ			DATE.	10/0/12		
WELL		TUBIN			L SCREEN I	NTERVAL	STA		EPTH (btoc)			SE PUMP T	YPE
	(inches): 2		TER (inches): 1		:) DEPTH: 48 TH – STAT				R (feet): 8.15 WELL CAPACI	TY	OR B/	AILER: PP	
(only fill out	t if applicable)		= (		feet –		fee	et) X	0.16 gall	ons/foot	=		gallons
	NT VOLUME PU	JRGE: 1 EQU	JIPMENT VOL.	= PUMP VOL	UME + (TUBI	ING CAPACI	TY X	TU	BING LENGTH)	+ FLOV	V CELL	_ VOLUME	
			+.10 gallons	` •				s = (			1.	TOTAL 1/0	
	IMP OR TUBING WELL (feet btoo	-	_	IP OR TUBING WELL (feet bto		PURGIN INITIATE	IG ED AT: 13	45	PURGING ENDED AT:	1408		TOTAL VOI PURGED (	gallons): 1.15
TIME	VOLUME PURGED (gallons)	CUMUL. VOLUME PURGED (gallons)	PURGE RATE (gpm)	DEPTH TO WATER (feet btoc)	pH (standard units)	TEMP. (°C)	SP COI ( mS/c		DISSOLVED OXYGEN (% saturation)	_	BIDITY TUs)	ORP (mV)	
1403	1.00	1.00	0.06	8.7	11.10	23.90	52.3	9	1.3	9.	.15	-363.	7
1405	0.05	1.05	0.03	8.7	11.10	23.92	52.4	7	1.3	4.	.60	-367.	4
1407	0.10	1.15	0.05	8.7	11.10	23.93	52.5	2	1.3	3.	.35	-371.	5 1.022
TUBING IN	PACITY (Gallons	PACITY (Gal./	Ft.): <b>1/8"</b> = 0.0	0006; 3/16"				0.37; <b>6"</b> = 0.0		<b>5</b> " = 1.0 .006;		" = 1.47; = 0.010;	<b>12</b> " = 5.88 <b>5/8</b> " = 0.016
	elow top of cas		•	grade riser <b>3P</b> = Bladder P	ump; E	SP = Electric	Submersi	ble Pun	np; <b>PP</b> = Pe	eristaltic	Pump;	<b>0</b> = 0	ther (Specify)
						LING DA	ATA						
	BY (PRINT) / A ohnson/Par			SAMPLER(S)	_	chnse			SAMPLING INITIATED AT	Γ: 1413		SAMPLIN ENDED A	
PUMP OR DEPTH IN	TUBING WELL (feet): 47	7.5		TUBING MATERIAL CO					L FILTERED: Yes, n Equipment Ty			ide FILTER	SIZE: <u>0.45 μm</u>
	CONTAMINATIO				TUBING		(replaced		DUPLICATE:			No	
	PLE CONTAINE		-		SAMPLE PR				INTENDE ANALYSIS AI			MPLING JIPMENT	SAMPLE PUMP FLOW RATE
SAMPLE ID CODE	# CONTAINERS	MATERIAL CODE	VOLUME	PRESERVATI USED		OTAL VOL D IN FIELD (		NAL pH	METHO	D	(	CODE	(mL per minute)
MW- 2C	1	PE	250mL	HNO3					6010B T. Metals/7470			APP	250
MW- 2C	1	PE	125mL						3500 FE/ 9			APP	125
MW-	1	PE	250mL						pH 6010B Diss	olved		APP	250
2C MW- 2C	1	PE	125mL						Silica 9056A_2 Chloride	&		APP	125
MW-	1	AG	125mL						Sulfate SM 5310 [			APP	125
2C MW-	2	PE	250mL	NaOH					SM4500 St			APP	Field-Filtered
2C MW-	1	PE	500mL	Zinc Acetat	<del>U</del>				2540C T	DS	1	APP	250
2C MW-	1	PE	250mL						2320B Alka	alinity	1	APP	250
2C MW- 2C	1	AG	125mL	HCI					SM5310 T	ОС		APP	125
REMARKS	: Per SOP, used. Purg				adings pr	ior to sar	nple co	llection	on. Tubing	-in-Sc	reen	ed-Inter	/al purge
MATERIAL		AG = Amber		Clear Glass;	PE = Polye	ethylene:	<b>PP</b> = Poly	nronyle	ene; <b>S</b> = Silico	ne· T	= Teflo	on: <b>0</b> – 0	Other (Specify)
	EQUIPMENT	CODES:	APP = After Pe	ristaltic Pump;	<b>B</b> = Baile	er; <b>BP</b> =	Bladder F	ump;	ESP = Electr				Salor (Opeolly)
		F	RFPP = Revers	e Flow Peristal	tic Pump;				Gravity Drain);	<b>O</b> = 0	Other (	Specify)	

SITE NAME: LO	CP Chemical Site	<u> </u>			SIT	E CATION: Bru	ınswick. GA							
WELL NO:		-		SAMPLE	ID: MW-3A		,			DATE: 10	/3/10			
					PURG	ING DA	TA							
	R (inches): 2		ER (inches): 1	/4 DEP	L SCREEN IN TH: 18 feet	to 23 feet	TO W		R (feet btoc): 7.	45 O	-	PUMP TYI .ER: PP	PE	
(only fill ou	LUME PURGE: it if applicable)		= (		feet –		feet)	X	0.16 gallo	ons/foot			gallons	
	NT VOLUME Pout if applicable)			= PUMP VOLI	- ( -				BING LENGTH) .27 gallons	+ FLOW (	CELL V	OLUME	•	
	JMP OR TUBIN WELL (feet bto	-	_	P OR TUBING VELL (feet btoo		PURGIN INITIATE	G ED AT: 0740	)	PURGING ENDED AT:	0822		TAL VOLU IRGED (ga	JME illons): 2.0	
TIME	VOLUME PURGED (gallons)	CUMUL. VOLUME PURGED (gallons)	PURGE RATE (gpm)	DEPTH TO WATER (feet btoc)	pH (standard units)	TEMP. (°C)	SP CONI ( mS/cm	.)	DISSOLVED OXYGEN (% saturation)	TURBIE (NTU		ORP (mV)	SP Gravity (sg)	
0816	1.75	1.75	0.05	7.55	8.01	24.71	46.86		3.0	37.4	1	-298.6		
0818	0.15	1.90	0.08	7.55	8.02	24.75	46.61		2.8	37.7		-308.6		
0820	0.10	2.00	0.05	7.55	8.02	24.77	45.97		2.6	37.9	9	-288.9	1.023	
	0020 0.10 2.00 0.05 7.55 6.02 24.77 45.97 2.0 37.9 -200.9 1.025													
	FIL CAPACITY (Callage Per Foot), 9.75", 9.00; 4", 9.04; 4.25", 9.05; 2", 9.45; 2", 9.37; 4", 9.05; 5", 4.47; 4.27; 5.99													
WELL CAL	ELL CAPACITY (Gallons Per Foot): 0.75" = 0.02; 1" = 0.04; 1.25" = 0.06; 2" = 0.16; 3" = 0.37; 4" = 0.65; 5" = 1.02; 6" = 1.47; 12" = 5.88													
TUBING IN	BING INSIDE DIA. CAPACITY (Gal./Ft.): 1/8" = 0.0006; 3/16" = 0.0014; 1/4" = 0.0026; 5/16" = 0.004; 3/8" = 0.006; 1/2" = 0.010; 5/8" = 0.016													
					ump. ES	SP = Flectric	Submersible	e Pum	n: <b>PP</b> = Pe	ristaltic Pu	ımb.	<b>O</b> = Oth	ner (Specify)	
					• •				<u>r,</u>				(0)	
PUMP OR		4		TUBING			FI		ILTERED: Yes			FILTER S	IZE: <u>0.45 μm</u>	
	WELL (feet): 2 CONTAMINATION			MATERIAL CO	TUBING		(replaced)		DUPLICATE:	oe: Syring	ge No			
	PLE CONTAINE				SAMPLE PRI		<u> </u>		INTENDE	:D	SAMP	PLING	SAMPLE PUMP	
SAMPLE ID CODE	# CONTAINERS	MATERIAL CODE		PRESERVATI USED	VE TO	OTAL VOL D IN FIELD (I	FIN		ANALYSIS AN	ND/OR	EQUIP CO	PMENT DE	FLOW RATE (mL per minute)	
MW-3A	1	PE	250mL	HNO3				-	6010B T		AF	PP	250	
MW-3A	1	PE	125mL						3500 FE/ 90 pH		AF	PP	125	
MW-3A	1	PE	250mL					-	6010B Diss Silica	olved	AF	PP	250	
MW-3A	1	PE	125mL					-	9056A_2 Chloride		AF	PP	125	
MW-3A	1	AG	125mL					-	SM 5310 E		AF	PP	125	
MW-3A	2	PE	250mL	NaOH Zinc Acetat	е			-	SM4500 St	ulfide	AF		Field-Filtered	
MW-3A	1	PE	500mL					-	2540C TI	os	AF		250	
MW-3A	1	PE	250mL					-	2320B Alka		AF		250	
MW-3A	1	AG	125mL	HCI				-	SM5310 T		AF		125	
	s: Per SOP, used. Spe													
MATERIA		<b>AG</b> = Amber 0	•	Clear Glass;	<b>PE</b> = Polye		<b>PP</b> = Polyp		-		Teflon;		her (Specify)	
SAMPLING	G EQUIPMENT		PP = After Per		<b>B</b> = Baile	,	Bladder Pur		ESP = Electri Gravity Drain):					

NOTES: Stabilization Criteria for Range of Variation of Last Three Consecutive Readings: -pH:  $\pm 0.1$  unit Specific Conductance:  $\pm 5\%$  Dissolved Oxygen: all readings  $\leq 10\%$  saturation; optionally,  $\pm 0.2$  mg/L Turbidity: all readings  $\leq 10$  NTU; or  $\pm 10\%$ 

SITE NAME: I C	P Chemical Site	<u> </u>			SIT	E CATION: Bru	nswick GA						
	: MW-115A			SAMPLE II	D: MW-115/				DATE:	10/3/12	2		
					PURG	ING DA	TA	Į.					
	R (inches): 2		TER (inches):	1/4 (btoc) feet		5 feet to 17	7.5 TO WATE	DEPTH (btoc) ER (feet): 6.0			E PUMP TY AILER: PP	PE .	
(only fill ou	t if applicable)		= (		eet –		feet) X		ITY lons/foot	: =		gallons	
	NT VOLUME PU it if applicable)			= PUMP VOLU ( 0.0026 gallor	( -			JBING LENGTH 0.25 gallons	) + FLOV	W CELL	VOLUME		
	JMP OR TUBIN			MP OR TUBING WELL (feet btoc)	): 15.5	PURGING INITIATE	G D AT: 1033	PURGING ENDED AT:	1114		TOTAL VOL PURGED (g	UME allons): 1.25	
TIME	VOLUME PURGED (gallons)	CUMUL. VOLUME PURGED (gallons)	PURGE RATE (gpm)	DEPTH TO WATER (feet btoc)	pH (standard units)	TEMP. (°C)	SP COND. ( mS/cm)	DISSOLVED OXYGEN (% saturation)		BIDITY TUs)	ORP (mV)	SP Gravity (sg)	
1107	1.00	1.00	0.03	6.11	7.44	23.37	5.261	2.5		.03	-214.2		
1111	0.20	1.20	0.05	6.11	7.44	23.36	5.238	2.3		.47	-216.2		
1113	0.05	1.25	0.03	6.11	7.45	23.35	5.232	2.3	9.	.88	-219.5	1.000	
TUBING IN	• •												
PURGING	EQUIPMENT C	ODES: B	= Bailer; I	<b>BP</b> = Bladder Pu	mp; ES	<b>P</b> = Electric	Submersible Pu	mp; <b>PP</b> = P	eristaltic	Pump;	<b>O</b> = Ot	her (Specify)	
0.11151.55	D) ( (   D       T ) (   A			0.11101 50(0) 0			TA	T					
	TOC = Below top of casing —which includes above grade riser  URGING EQUIPMENT CODES: B = Bailer; BP = Bladder Pump; ESP = Electric Submersible Pump; PP = Peristaltic Pump; O = Other (Specify)  SAMPLING DATA  AMPLED BY (PRINT) / AFFILIATION: // Agria Johnson/Parsons  SAMPLER(S) SIGNATURE(S): SAMPLING INITIATED AT: 1126  SAMPLING ENDED AT: 1206												
PUMP OR DEPTH IN	TUBING WELL (feet): 15	5.5		TUBING MATERIAL COI			FIELD	-FILTERED: Yes			de FILTER	SIZE: <u>0.45</u> μm	
FIELD DE	CONTAMINATIO	ON: PUM	P Y <b>N</b>	lo	TUBING	Y No	(replaced)	DUPLICATE:		Yes			
SAM	PLE CONTAINE	R SPECIFICA	TION	S	AMPLE PRE	ESERVATIO	N	INTEND			MPLING	SAMPLE PUMP	
SAMPLE ID CODE	# CONTAINERS	MATERIAL CODE	VOLUME	PRESERVATIV USED		OTAL VOL ) IN FIELD (n	FINAL nL) pH	ANALYSIS A METHO			JIPMENT CODE	FLOW RATE (mL per minute)	
MW- 115A	2	PE	250mL	HNO3				6010B T Metals/747		4	APP	125	
MW- 115A	2	PE	125mL					3500 FE/ 9 pH		1	APP	125	
MW- 115A	2	PE	250mL					6010B Diss		,	APP	167	
MW- 115A	2	PE	125mL					9056A_2 Chloride Sulfat	28D e &	,	APP	125	
MW- 115A	2	AG	125mL					SM 5310		,	APP	125	
MW- 115A	4	PE	250mL	NaOH Zinc Acetate				SM4500 S	ulfide	<u> </u>	APP	Field-Filtered	
MW- 115A	2	PE	500mL		,			2540C T	DS	<u> </u>	APP	167	
MW- 115A	2	PE	250mL					2320B Alk	alinity	,	APP	125	
MW- 115A	2	AG	125mL	HCI				SM5310			APP	125	
REMARKS	s: Per SOP, used. Purg			for three rea	ıdings pri	ior to san	nple collecti	ion. Tubing-	in-Scr	reene	d- Interv	al purge	
MATERIA	•	AG = Amber (		= Clear Glass;	<b>PE</b> = Polye	ethylene;	<b>PP</b> = Polypropyl	lene; <b>S</b> = Silico	one; <b>T</b>	= Teflo	on; <b>O</b> = C	ther (Specify)	
SAMPLING	G EQUIPMENT			eristaltic Pump; se Flow Peristalti	<b>B</b> = Baile c Pump;		Bladder Pump; Method (Tubing	<b>ESP</b> = Elect Gravity Drain);			Pump; Specify)		

**NOTES:** Stabilization Criteria for Range of Variation of Last Three Consecutive Readings: **pH**:  $\pm$  0.1 unit **Specific Conductance**:  $\pm$  5% **Dissolved Oxygen**: all readings  $\leq$  10% saturation; optionally,  $\pm$  0.2 mg/L **Turbidity**: all readings  $\leq$  10 NTU; or  $\pm$  10%

SITE NAME: LC	P Chemical Site	<u> </u>			SIT	E CATION: Bru	ınewick	GΔ						
	: MW-115B	<del>-</del>		SAMPLE	ID: MW-115		JI ISWICK,	, OA		DATE:	10/3/12			
					PURG	ING DA	TA							
	R (inches): 2		TER (inches):	1/4 (btoo	L SCREEN IN DEPTH: 29	NTERVAL 9 feet to 33	3 7		ER (feet btoc):			E PUMP T'	/PE	
(only fill ou	it if applicable)		= (		feet –		1	feet) X		lons/foot			gallons	
	NT VOLUME Pout if applicable)			= PUMP VOLI ( 0.0026 gallo	,				JBING LENGTH  0.29 gall	,	W CELL	VOLUME		
	JMP OR TUBIN WELL (feet bto	-	_	MP OR TUBING WELL (feet bto		PURGIN INITIATE		0903	PURGING ENDED AT:	0929		OTAL VOL PURGED (g	UME pallons): 1.1	
TIME	VOLUME PURGED (gallons)	CUMUL. VOLUME PURGED (gallons)	PURGE RATE (gpm)	DEPTH TO WATER (feet btoc)	pH (standard units)	TEMP. (°C)		COND. S/cm)	DISSOLVED OXYGEN (% saturation)		BIDITY TUs)	ORP (mV)	(sg)	
0925	1.00	1.00	0.05	5.65	9.48	22.80		914	3.1		.24	-200.0		
0927	0.05	1.05	0.03	5.65	9.48	22.77		915	2.9		.04	-197.		
0929														
	WELL CAPACITY (Gallons Per Foot): 0.75" = 0.02; 1" = 0.04; 1.25" = 0.06; 2" = 0.16; 3" = 0.37; 4" = 0.65; 5" = 1.02; 6" = 1.47; 12" = 5.88													
WELL CAI	ELL CAPACITY (Gallons Per Foot): 0.75" = 0.02; 1" = 0.04; 1.25" = 0.06; 2" = 0.16; 3" = 0.37; 4" = 0.65; 5" = 1.02; 6" = 1.47; 12" = 5.88  BING INSIDE DIA. CAPACITY (Gal./Ft.): 1/8" = 0.0006; 3/16" = 0.0014; 1/4" = 0.0026; 5/16" = 0.004; 3/8" = 0.006; 1/2" = 0.010; 5/8" = 0.016													
PURGING	EQUIPMENT C	ODES: I	<b>B</b> = Bailer;	<b>BP</b> = Bladder P	•	SP = Electric		rsible Pu	mp; <b>PP</b> = P	eristaltic	Pump;	<b>O</b> = O	ther (Specify)	
SAMPLED	BY (PRINT) / A	FEII IATION:	1	SAMPLER(S)		LING DA	AIA							
	ohnson/Pai			Mari	_	zhnze			SAMPLING INITIATED A	T: 0935		SAMPLIN ENDED A		
PUMP OR DEPTH IN	TUBING WELL (feet): 30	0.5		TUBING MATERIAL CO	DDE: Teflon-li	ned PE			-FILTERED: Ye on Equipment Ty			de FILTE	R SIZE: <u>0.45 μm</u>	
FIELD DE	CONTAMINATIO	ON: PUI	MP Y N	lo	TUBING	Y No	(replac	ced)	DUPLICATE		No	ı		
SAM	PLE CONTAINE	ER SPECIFIC	ATION		SAMPLE PRI	ESERVATIO	N		INTEND			MPLING	SAMPLE PUMP	
SAMPLE ID CODE	# CONTAINERS	MATERIAL CODE	VOLUME	PRESERVATI USED		OTAL VOL ) IN FIELD (	mL)	FINAL pH	ANALYSIS A	DD		ODE	FLOW RATE (mL per minute)	
MW- 115B	1	PE	250mL	HNO3					6010B 7 Metals/747		,	APP	250	
MW-	4	DE	10Fml						3500 FE/ 9	9040B		<b>A D D</b>	105	
115B MW-	1	PE	125mL						6010B Dis			APP	125	
115B MW-	1	PE	250mL						9056A_2		-	APP	250	
115B MW-	1	PE	125mL						Chloride		1	APP	125	
115B	1	AG	125mL						SM 5310	DOC	,	APP	125	
MW- 115B	2	PE	250mL	NaOH Zinc Acetat	е				SM4500 S	Sulfide	,	APP	Field Filtered	
MW- 115B	1	PE	500mL						2540C T	DS	,	APP	250	
MW- 115B	1	PE	250mL						2320B Alk	alinity		APP	125	
MW- 115B	1	AG	125mL	HCI					SM5310	TOC		APP	125	
REMARKS	e: Per SOP,	paramet	ers stable		adings pr	ior to sar	nple (	collect	ion. Tubing					
	l used. Purg			<u> </u>										
MATERIAL		AG = Amber		= Clear Glass;	PE = Polye			olypropy	•				Other (Specify)	
SAMPLING	G EQUIPMENT			eristaltic Pump; se Flow Peristal	<b>B</b> = Baile tic Pump;			r Pump; d (Tubing	<b>ESP</b> = Elect Gravity Drain);		iersible Other (S			

NOTES: Stabilization Criteria for Range of Variation of Last Three Consecutive Readings:  $pH: \pm 0.1$  unit Specific Conductance:  $\pm 5\%$  Dissolved Oxygen: all readings  $\leq 10\%$  saturation; optionally,  $\pm 0.2$  mg/L Turbidity: all readings  $\leq 10$  NTU; or  $\pm 10\%$ 

SITE	1D Ob - mi 1 Oit-					SIT			-l- OA					
	P Chemical Site MW-115C	1		SA	MPLE ID:		CATION: Bru 5C	inswic	K, GA		DATE:	10/3/12	<u> </u>	
							ING DA	ТΔ						
WELL		TUBIN	-		WELL S	CREEN I	NTERVAL			DEPTH (btoc)			E PUMP T	YPE
	R (inches): 2  LUME PURGE:		TER (inches): LUME = (TOT		. ,		feet to 45 f			R (feet): 6.65 WELL CAPAC	ITY	OR BA	AILER: PP	
(only fill ou	it if applicable)		,						,		lons/foot	: =		gallons
	NT VOLUME PU	JRGE: 1 EQ	UIPMENT VOL	= PUMI	P VOLUMI	E + (TUB	ING CAPACI	TY	X TI	JBING LENGTH			VOLUME	gament
` ,			+.10 gallons			foot X 4			gallons =		llons			
	JMP OR TUBING WELL (feet bto		FINAL PUI DEPTH IN			12.5	PURGIN INITIATE	-	: 0811	PURGING ENDED AT:	0934		ΓΟΤΑL VOL PURGED (g	LUME gallons): 2.6
		CUMUL.		DEP		pН	I			DISSOLVED				
TIME	VOLUME PURGED	VOLUME PURGED	PURGE RATE	WAT	ER (st	tandard	TEMP. (°C)		COND. nS/cm)	OXYGEN		BIDITY TUs)	ORP (mV)	
	(gallons)	(gallons)	(gpm)	(fe bto	c)	units)	. ,	,	,	(% saturation)	<u> </u>	,		
0922	2.2	2.2	0.03	7.0	00 1	11.26	23.32	4	19.70	2.0	4	.06	-371.0	0
0926	0.1	2.3	0.03	7.0		11.29	23.32		19.67	1.7		.15	-355.	
0930	0.2	2.5	0.05	7.1		11.31	23.21		19.65	1.6		.06	-382.4	
0933	0.1	2.6	0.03	7.1	1 1	11.32	23.27	4	19.56	1.4	3	.77	-379.	4 1.021
	WELL CAPACITY (Gallons Per Foot): 0.75" = 0.02; 1" = 0.04; 1.25" = 0.06; 2" = 0.16; 3" = 0.37; 4" = 0.65; 5" = 1.02; 6" = 1.47; 12" = 5.88  **TUBING INSIDE DIA. CAPACITY (Gal./Ft.): 1/8" = 0.0006; 3/16" = 0.0014; 1/4" = 0.0026; 5/16" = 0.004; 3/8" = 0.006; 1/2" = 0.010; 5/8" = 0.016													
WELL CAI	IBING INSIDE DIA. CAPACITY (Gal./Ft.): 1/8" = 0.0006; 3/16" = 0.0014; 1/4" = 0.0026; 5/16" = 0.004; 3/8" = 0.006; 1/2" = 0.010; 5/8" = 0.016													
TUBING IN	JBING INSIDE DIA. CAPACITY (Gal./Ft.): 1/8" = 0.0006; 3/16" = 0.0014; 1/4" = 0.0026; 5/16" = 0.004; 3/8" = 0.006; 1/2" = 0.010; 5/8" = 0.016  TOC = Below top of casing —which includes above grade riser													
PURGING	TOC = Below top of casing –which includes above grade riser  URGING EQUIPMENT CODES: B = Bailer; BP = Bladder Pump; ESP = Electric Submersible Pump; PP = Peristaltic Pump; O = Other (Specify)													
SAMPLED	SAMPLING DATA													
	SAMPLED BY (PRINT) / AFFILIATION: SAMPLER(S) SIGNATURE(S):													
	PUMP OR TUBING DEPTH IN WELL (feet): 42.5  TUBING MATERIAL CODE: Teflon-lined PE  SAMFLING ENDED AT: 1004  FIELD-FILTERED: Yes/SM 4500 Sulfide FILTER SIZE: 0.45 µm Filtration Equipment Type: Syringe													
	CONTAMINATIO		MP Y N	lo		TUBING		(repla	aced)	DUPLICATE:			lo	
SAM	PLE CONTAINE	R SPECIFIC	ATION		SAI	MPLE PR	ESERVATIO	N		INTEND			MPLING	SAMPLE PUMP
SAMPLE ID CODE	# CONTAINERS	MATERIAL CODE	VOLUME		RVATIVE SED		OTAL VOL D IN FIELD (	mL)	FINAL pH	ANALYSIS A METHO			JIPMENT CODE	FLOW RATE (mL per minute)
MW-		PE	250ml	LIN	103		,			6010B T Metals/747			A D D	125
115C MW-	1	PE	250mL	<u> </u>	NO3					3500 FE/ 9		<del>  '</del>	APP	125
115C MW-	1	PE	125mL							pH 6010B Diss		ļ ,	APP	125
115C	1	PE	250mL							Silica		,	APP	250
MW-										9056A_2 Chloride				
115C MW-	1	PE	125mL			1				Sulfate		1	APP	125
115C	1	AG	125mL							SM 5310	DOC	,	APP	125
MW- 115C	2	PE	250mL		OH Acetate					SM4500 S	ulfide	,	APP	Field-Filtered
MW- 115C	1	PE	500mL							2540C T	DS		APP	167
MW- 115C	1	PE	250mL							2320B Alka			APP	125
MW-	4													
115C REMARKS	: Per SOP	AG paramete	125mL ers stable		ICI ee read	ings ni	rior to sar	nple	collect	SM5310 - ion. Tubing-			APP d- Interv	63 /al purge
method	l used. Purg													30
MATERIA		AG = Amber		= Clear G			ethylene;		Polypropy	•		= Teflo		Other (Specify)
SAMPLING	G EQUIPMENT	CODES:	<b>APP</b> = After Pe <b>RFPP</b> = Revers	eristaltic F se Flow F	Pump; Peristaltic F	<b>B</b> = Bail Pump;	er; BP = SM = Straw	Bladd Metho	der Pump; od (Tubing	<b>ESP</b> = Electric Gravity Drain);		nersible Other (S		

SITE	CP Chemical Site	Δ				SITE LOCATION	l· Brunew	ick GA							
	: MW-519A	<u> </u>		SAM	IPLE ID: MV		i. Diulisw	ick, OA		DATE:	10/2/12				
					PU	RGING	DATA								
WELL DIAMETEI	R (inches): 2	TUBI	NG IETER (inches):		WELL SCRE	EEN INTERV 34.3 feet	AL.	STATIC D	EPTH R (feet btoc): 5	.72		E PUMP T' ILER: PP	YPE		
	LUME PURGE: it if applicable)	1 WELL V	<b>OLUME</b> = (TO) = (	ΓAL WELL	DEPTH - feet -	STATIC DEP	TH TO W	ATER) X feet) X	WELL CAPAC	ITY lons/foot	=		gallons		
	NT VOLUME PO	URGE: 1 E		= PUMP		(TUBING CA	PACITY		JBING LENGTH			VOLUME	ganerio		
` ,			= +.10 gallons	•			t) + .10	gallons =	0.3 gallons						
	JMP OR TUBIN WELL (feet bto	-	FINAL PUI DEPTH IN	WELL (fee	et btoc): 35	_	RGING TATED A	T: 0828	PURGING ENDED AT:	0904		OTAL VOL PURGED (g	LUME gallons): 1.4		
TIME	VOLUME PURGED (gallons)	CUMUL VOLUMI PURGEI (gallons	PURGE RATE	DEPT TO WATE (fee	pH ER (stand t units	ard   C		P COND. mS/cm)	DISSOLVED OXYGEN (% saturation)		BIDITY TUs)	ORP (mV)	,		
0858	1.25	1.25	0.04	5.80				7.714	9.8		.52	-75.3			
0900	0.05	1.30	0.03	5.80				7.735	9.9		.57	-75.2			
0902	0.10	1.40	0.05	5.80	) 10.4	2 25.5	U	7.748	9.6	9	.04	-77.6	1.024		
	VELL CAPACITY (Gallons Per Foot): 0.75" = 0.02; 1" = 0.04; 1.25" = 0.06; 2" = 0.16; 3" = 0.37; 4" = 0.65; 5" = 1.02; 6" = 1.47; 12" = 5.88  UBING INSIDE DIA. CAPACITY (Gall/Ft.): 1/8" = 0.0006: 3/16" = 0.0014: 1/4" = 0.0026: 5/16" = 0.004: 3/8" = 0.006: 1/2" = 0.010: 5/8" = 0.016														
	ELL CAPACITY (Gallons Per Foot): 0.75" = 0.02; 1" = 0.04; 1.25" = 0.06; 2" = 0.16; 3" = 0.37; 4" = 0.65; 5" = 1.02; 6" = 1.47; 12" = 5.88  ### JBING INSIDE DIA. CAPACITY (Gal./Ft.): 1/8" = 0.0006; 3/16" = 0.0014; 1/4" = 0.0026; 5/16" = 0.004; 3/8" = 0.006; 1/2" = 0.010; 5/8" = 0.016  **TOC= Below top of casing- which includes above grade riser.														
BTOC= B	elow top of cas	sing- which	ncludes above o	grade riser.											
PURGING	EQUIPMENT C	ODES:	<b>B</b> = Bailer;	<b>BP</b> = Blad	der Pump;	ESP = Ele MPLING		mersible Pui	mp; <b>PP</b> = P	eristaltic	Pump;	<b>0</b> = 0	ther (Specify)		
	BY (PRINT) / A		l:	100	R(S) SIGNA	ΓURE(S):		<u> </u>							
Maria J	ohnson/Pa	rsons		41)	Oniae	) ahn	241		SAMPLING INITIATED A	T: 0916		SAMPLIN ENDED A			
PUMP OR	TUBING WELL (feet): 3	5		TUBING		flon-lined PE			-FILTERED: Yes on Equipment Ty			de FILTE	R SIZE: <u>0.45 μm</u>		
	CONTAMINATION		JMP Y N	No	TUB		No (rep		DUPLICATE:		N <sub>1</sub>	0			
SAM	PLE CONTAINE	ER SPECIFI	CATION		SAMPL	E PRESERV	ATION		INTEND			//PLING	SAMPLE PUMP		
SAMPLE ID CODE	# CONTAINERS	MATERIAL CODE	VOLUME	PRESER USI		TOTAL V DDED IN FIE		FINAL pH	ANALYSIS A METHO			IPMENT ODE	FLOW RATE (mL per minute)		
MW- 519A	1	PE	250mL	HN			()		6010B T Metals/747		A	\PP	125		
MW- 519A	1	PE	125mL		_				3500 FE/ 9 pH	040B	4	APP	125		
MW-		PE							6010B Diss			NPP			
519A MW-	1		250mL						9056A_2	28D			125		
519A MW-	1	PE	125mL		-				Chloride			APP	125		
519A MW-	1	AG	125mL	Na(	DH				SM 5310	DOC	F	APP	125		
519A MW-	2	PE	250mL	Zinc A					SM4500 S	ulfide	P	APP	Field-Filtered		
519A	1	PE	500mL	-	-				2540C T	DS	P	APP	167		
MW- 519A	1	PE	250mL		-				2320B Alk	alinity	A	\PP	250		
MW- 519A	1	AG	125mL	Н	CI				SM5310	тос		APP	125		
REMARKS		•			e reading	s prior to	sampl	e collecti	on. Tubing	-in-Sc	reene	d-Interv	al purge		
method	was used.	Purge w		rown. = Clear Gla	ass: PF -	Polyethylene	: PP -	= Polypropyl	ene; <b>S</b> = Silico	one· T	= Tefloi	n: <b>O</b> = C	Other (Specify)		
	G EQUIPMENT		APP = After P	eristaltic Pu	ımp; <b>B</b> :	= Bailer;	<b>BP</b> = Blac	lder Pump;	ESP = Elect	ric Subm	nersible l	Pump;	Januar (Opoony)		
			RFPP = Rever	se Flow Pe	eristaltic Pum	p; $SM = S$	traw Met	nod (Tubing	Gravity Drain);	<b>O</b> = 0	Other (S	specify)			

0.75			G	ROUNL			MPL	LING	LOG					
SITE NAME: LC	P Chemical Site	9			SI LC	TE OCATION: Bru	unswick	, GA						
WELL NO	: MW-519B			SAMPLE	ID: MW-519	9B				DATE: 1	0/2/12			
				•	PURG	SING DA	ΤA							
WELL DIAMETE	R (inches): 2	TUBIN DIAME	G TER (inches):	1/4 (bto	L SCREEN c) DEPTH: 4				EPTH (btoc) R (feet): 5.95		-	E PUMP T\ ILER: PP	/PE	
	LUME PURGE:	1 WELL VO	LUME = (TOT		<u>5 feet</u> TH – STA	TIC DEPTH 1	TAW OT	ΓER) X	WELL CAPACI	TY				
, ,	NT VOLUME P	UBCE: 1 FOI	= (	- DUMB VOL	feet –	PINC CARAC		feet) X	0.16 gallo	ons/foot		VOLUME	ga	llons
	it if applicable)			. = FOWF VOL	•				,	+ FLOW	CELL	VOLUME		
	JMP OR TUBIN WELL (feet bto	-		MP OR TUBING WELL (feet bto		PURGIN INITIATI	-	0829	PURGING ENDED AT:	1352		OTAL VOL		): 10.8
		CUMUL.		DEPTH	-11	1			DICCOLVED					
TIME	VOLUME PURGED (gallons)	VOLUME PURGED (gallons)	PURGE RATE (gpm)	TO WATER (feet btoc)	pH (standard units)	TEMP. (°C)		COND. S/cm)	DISSOLVED OXYGEN (% saturation)	TURBI (NTL		ORP (mV)		SP Gravity (sg)
0903	0.75	0.75	0.02	7.08	11.67	25.46	41	1.33	2.8	42	4	-383.	5	
0922	0.50	1.25	0.03	7.10	11.78	25.13	53	3.14	2.5	11	6	-3812		
0931	0.25	1.50	0.03	7.10 7.08	11.78 11.76	25.41 26.19		3.04	2.4	57.		-430.5		
0940 1021	0.25 0.85	1.75 2.60	0.03	7.58 5.26	1.6	43		-434.0 -418.0						
1345	7.90	10.5	0.08	7.04 7.20	11.75 12.20	26.28 24.98		7.63	8.5	Over R		-340.0		
1348	0.20	10.7	0.06	7.15	12.22	25.08		7.63	6.5	5.2		-351.4		
1351	0.10	10.8	0.03	7.15	12.25	25.63	57	7.76	4.7	8.6	88	-347.3	3	1.000
	1351 0.10 10.8 0.03 7.15 12.25 25.63 57.76 4.7 8.68 -347.3 1.000  WELL CAPACITY (Gallons Per Foot): 0.75" = 0.02; 1" = 0.04; 1.25" = 0.06; 2" = 0.16; 3" = 0.37; 4" = 0.65; 5" = 1.02; 6" = 1.47; 12" = 5.88  TUBING INSIDE DIA. CAPACITY (Gall/Ft.): 1/8" = 0.0006; 3/16" = 0.0014; 1/4" = 0.0026; 5/16" = 0.004; 3/8" = 0.006; 1/2" = 0.010; 5/8" = 0.016													
	NSIDE DIA. CAI Below top of ca				= 0.0014;	1/4" = 0.002	26; \$	<b>5/16</b> " = 0.	004; 3/8" = 0.	.006;	1/2" =	0.010;	5/8" =	0.016
PURGING	EQUIPMENT C	CODES: E	B = Bailer;	<b>BP</b> = Bladder F	•	SP = Electric		ersible Pu	mp; <b>PP</b> = Pe	eristaltic P	ump;	<b>O</b> = O	ther (S	pecify)
SAMPLED	BY (PRINT) / A	AFFILIATION:		SAMPLER(S)		LING DA	AIA							
	ne Jaynes/F				0	200			SAMPLING INITIATED AT	T: 1358		SAMPLIN ENDED A		13
PUMP OR		_		TUBING					_  -FILTERED: Yes/			le FILTER	R SIZE:	<u>0.45</u> μm
	WELL (feet): 4   CONTAMINATIO		MP Y N	MATERIAL CO	DDE: Tetlon- TUBING		(repla	•	on Equipment Type DUPLICATE:	oe: Syrir	nge No	n		
	PLE CONTAINE			-		RESERVATIO			INTENDE	D		1PLING	SAM	PLE PUMP
SAMPLE	#	MATERIAL	VOLUME	PRESERVAT	IVE 7	TOTAL VOL		FINAL	ANALYSIS AN	ND/OR	EQU	IPMENT ODE	FLC	DW RATE per minute)
ID CODE MW-	CONTAINERS	CODE		USED	ADDE	D IN FIELD (	mL)	pН	6010B T	AL			(	· ,
519B MW-	1	PE	250mL	HNO3					Metals/7470 3500 FE/ 90		Α	\PP		250
519B	1	PE	125mL						pН		P	\PP		125
MW- 519B	1	PE	250mL						6010B Diss Silica		P	\PP		125
MW-									9056A_2 Chloride					
519B MW-	1	PE	125mL						Sulfate		P	\PP		125
519B	1	AG	125mL						SM 5310 E	оос	P	\PP		125
MW- 519B	2	PE	250mL	NaOH Zinc Aceta	te				SM4500 St	ulfide	P	\PP	Field	d-Filtered
MW- 519B	1	PE	500mL						2540C TI	DS	A	\PP		100
MW- 519B	1	PE	250mL						2320B Alka	llinity	Α	\PP		125
MW- 519B	1	AG	125mL	HCI					SM5310 T			\PP		125
REMARKS		, paramete	ers stable	for three re					on. Tubing-i				al pu	
	l used. Pur										T : C	•	ML (	D='( )
WAIERIA	L CODES:	AG = Amber	Glass; CG:	= Clear Glass;	PE = Poly	retnylene;	<b>PP</b> = P	∙oıypropyl	ene; S = Silico	ne; <b>I</b> =	= ı etlor	n; <b>U</b> = C	νιner (S	Specify)

SAMPLING EQUIPMENT CODES:

SITE SITE																	
NAME: LCP Chemical Site LOCATION: Brunswick, GA																	
WELL NO: EW-11 SAMPLE ID: EW-11 DATE: 10/												10/3/12	0/3/12				
	PURGING DATA																
WELL DIAMETER	R (inches): 4	TUBIN DIAME	IG ETER (inches):		REEN INTERVAL STATIC DEPTH (btoc) PTH: 45 feet to 50 feet TO WATER (feet): 3.5					PURGE PUMP TYPE  OR BAILER: PP							
		1 WELL VO	DLUME = (TOT	AL WELL	DEPTH	- STA	TIC DEPTH 1	TO WA	TER) X	WELL CAPAC	ITY						
, ,	t if applicable)		= (		feet				feet) X		lons/foot			gallons			
	NT VOLUME PU t if applicable)					•				JBING LENGTH	,	W CELL	. VOLUME				
			+.10 gallons	,		oot X 5	<del></del>		gallons =								
	JMP OR TUBING WELL (feet btoo	-	FINAL PUI DEPTH IN			17.5	PURGING INITIATED AT:			PURGING ENDED AT:	0823	TOTAL VOI PURGED (g		gallons): 1.45			
		CUMUL.		DEP		рН				DISSOLVED							
TIME	VOLUME PURGED	VOLUME PURGED		WAT	ER (sta	andard	TEMP. ( <sup>O</sup> C)		COND. nS/cm)	OXYGEN		BIDITY TUs)	ORP (mV)				
	(gallons)	(gallons)	(gpm)	(fee		ınits)		,	ŕ	(% saturation)	,	•	, ,				
0804	0.80	0.80	0.04			0.50	24.06		9.78	4.7		.86	-2614	-			
0809	0.20	1.00	0.04			0.66	24.09		9.85	3.4		.79	-307.				
0813	0.15	1.15	0.04			0.74	24.11		9.86	2.9		.77	-299.				
0816	0.10	1.25	0.03			0.78	24.12		9.86	2.6		.87	-298.				
0821	0.20	1.45	0.04		1	0.84	24.13	2	9.88	2.2	7	.08	-300.	5 1.016			
											<u> </u>						
<b>WELL CAPACITY</b> (Gallons Per Foot): $0.75" = 0.02$ ; $1" = 0.04$ ; $1.25" = 0.06$ ; $2" = 0.16$ ; $3" = 0.37$ ; $4" = 0.65$ ; $5" = 1.02$ ; $6" = 1.47$ ; $12" = 5.88$ <b>TUBING INSIDE DIA. CAPACITY</b> (Gal./Ft.): $1/8" = 0.0006$ ; $3/16" = 0.0014$ ; $1/4" = 0.0026$ ; $5/16" = 0.004$ ; $3/8" = 0.006$ ; $1/2" = 0.010$ ; $5/8" = 0.016$ <b>BTOC = Below top of casing</b> –includes above grade riser																	
PURGING EQUIPMENT CODES: B = Bailer; BP = Bladder Pump; ESP = Electric Submersible Pump; PP = Peristaltic Pump; O = Other (Specify)																	
SAMPLING DATA																	
SAMPLED BY (PRINT) / AFFILIATION: Christine Jaynes/Parsons  SAMPLER(S) SIGNATURE(S): SAMPLING INITIATED AT: 0831  SAMPLING ENDED AT: 0907																	
PUMP OR DEPTH IN	TUBING WELL (feet): 47	7.5		TUBING MATERI	IAL CODE:	: Teflon I	ined PE			-FILTERED: Yes on Equipment Ty			de FILTE	R SIZE: <u>0.45</u> μm			
FIELD DE	CONTAMINATIO	ON: PUI	MP Y N	lo	Т	UBING	Y <b>N</b> o	(repla	aced)	DUPLICATE:		N	lo				
SAM	PLE CONTAINE	R SPECIFIC	ATION		SAM	IPLE PR	ESERVATIO	N		INTEND			MPLING	SAMPLE PUMP			
SAMPLE ID CODE	# CONTAINERS	MATERIAL CODE	VOLUME		RVATIVE SED	TOTAL VOL ADDED IN FIELD (mL)			FINAL pH	ANALYSIS A METHC	IOD		JIPMENT CODE	FLOW RATE (mL per minute)			
EW-11	1	PE	250mL	HN	103					6010B T Metals/747	APP		125				
EW-11	1	PE	125mL	-						3500 FE/ 9 pH	0040B	,	APP	125			
EW-11	1	PE	250mL	-						6010B Diss Silica		,	APP	83			
EW-11	1	PE	125mL	-						9056A_2 Chloride Sulfate	28D e &	,	APP	125			
EW-11	1	AG	125mL	-	==					SM 5310		,	APP	125			
EW-11	2	PE	250mL		OH Acetate					SM4500 S	ulfide	,	APP	Field-Filtered			
EW-11	1	PE	500mL	-						2540C T	DS	,	APP	125			
EW-11	1	PE	250mL	-						2320B Alk	alinity	,	APP	83			
EW-11	1	AG	125mL		ICI					SM5310			APP	125			
method	used. Due	to small	diameter a	access	plug, u	nable	to collect	wate	er level	ion. Tubing s throughou purple/gree	ıt purg	je, pu					
MATERIAI		AG = Amber		= Clear GI			ethylene;		Polypropyl			= Teflo	on; <b>O</b> = 0	Other (Specify)			
SAMPLING	G EQUIPMENT		APP = After Pe			<b>B</b> = Bail			er Pump;	ESP = Elect Gravity Drain):							

SITE NAME: LCP Chemical Site  SITE LOCATION: Brunswick, GA																
WELL NO:		•		SAI	MPLE ID:											
PURGING DATA																
WELL		TUBING					NTERVAL		STATIC [	DEPTH (btoc)		PURG	E PUMP T	YPE		
	R (inches): 2		TER (inches):				8 feet to 23 f	feet	TO WATE	ER (feet): 8.61		OR BA	ALER: PP			
	WELL VOLUME PURGE: 1 WELL VOLUME = (TOTAL WELL DEPTH - STATIC DEPTH TO WATER) X WELL CAPACITY (only fill out if applicable)															
FOLIPME	NT VOLUME PL	IRGE: 1 FOI	= (	= (TUBI	feet	CITY	X TUB	ING L	feet) X	0.16 ga	Ilons/foo	t =		gallons		
	t if applicable)								,		OLOWIL					
INITIAI PI	JMP OR TUBIN		(0.0026 ga	ieet)	+ 0.13 g		= 0.19	PURGING		LUME						
DEPTH IN WELL (feet btoc ): 20.5 DEPTH IN WELL (feet btoc): 20.5														gallons): 1.5		
TIME	VOLUME PURGED (gallons)	CUMUL. VOLUME PURGED (gallons)	PURGE RATE (gpm)	DEP TC WAT (fee	ER (sta	pH andard inits)	TEMP. (°C)	_	COND. mS/cm)	DISSOLVED OXYGEN (% saturation)	TUR (N	BIDITY TUs)	ORP (mV)			
0923	0.50	0.50	0.05	8.7		6.6	20.88	1	13.36	11.4	9	.70	-193.	7		
0928	0.25	0.75	0.05	8.7	5	6.7	20.96	1	13.41	7.3	8	3.61	-199.	7		
0933	0.25	1.00	0.05	8.7	5	6.7	20.90	1	13.42	6.8	7	7.79	-204.	1		
0938	0.25	1.25	0.05	8.7	5	6.8	20.98	1	13.45	6.5	7	.05	-205.0	6		
0943	0.25	1.50	0.05	8.7	5	6.8	21.00	1	13.46	5.9	6	5.10	-216.	1 1.006		
WELL CAPACITY (Gallons Per Foot): $0.75" = 0.02$ ; $1" = 0.04$ ; $1.25" = 0.06$ ; $2" = 0.16$ ; $3" = 0.37$ ; $4" = 0.65$ ; $5" = 1.02$ ; $6" = 1.47$ ; $12" = 5.88$ TUBING INSIDE DIA. CAPACITY (Gal./Ft.): $1/8" = 0.0006$ ; $3/16" = 0.0014$ ; $1/4" = 0.0026$ ; $5/16" = 0.004$ ; $3/8" = 0.006$ ; $1/2" = 0.010$ ; $5/8" = 0.016$ BTOC = Below top of casing — feet below top of casing which includes above grade riser																
PURGING EQUIPMENT CODES: B = Bailer; BP = Bladder Pump; ESP = Electric Submersible Pump; PP = Peristaltic Pump; O = Other (Specify)																
SAMPLED BY (PRINT) / AFFILIATION: SAMPLER(S) SIGNATURE(S):																
SAMPLED BY (PRINT) / AFFILIATION: Maria Johnson/Parsons  SAMPLER(S) SIGNATURE(S): SAMPLING INITIATED AT: 0949  SAMPLING ENDED AT: 1017																
PUMP OR DEPTH IN	TUBING WELL (feet): 2	0.5		TUBING	AL CODE:					-FILTERED: Ye on Equipment T			de FILTER	SIZE: <u>0.45</u> μm		
	CONTAMINATIO		IP Y I	No		UBING		repla		DUPLICATE		No	0			
SAM	PLE CONTAINE	R SPECIFICA	ATION		SAM	IPLE PR	ESERVATIO	N		INTEND	DED	SAI	MPLING	SAMPLE PUMP		
SAMPLE ID CODE	# CONTAINERS	MATERIAL CODE	VOLUME		RVATIVE SED		TOTAL VOL ADDED IN FIELD (mL)			ANALYSIS AND/OR METHOD		EQUIPMENT CODE		FLOW RATE (mL per minute)		
MW-1A	1	PE	250mL	НМ	IO3					6010B Metals/747			APP	250		
MW-1A	1	PE	125mL	-	-					3500 FE/ pH	9040B		APP	125		
MW-1A	1	PE	250mL	-	·-					6010B Dis	solved		APP	125		
MW-1A	1	PE	125mL	-						9056A_ Chlorid Sulfa	28D e &	,	APP	125		
MW-1A	1	AG	125mL							SM 5310			APP	125		
MW-1A	2	PE	250mL		OH cetate					SM4500 S	Sulfide	,	APP	Field-Filtered		
MW-1A	1	PE	500mL							2540C	TDS		APP	167		
MW-1A	1	PE	250mL		==					2320B All	alinity		APP	125		
MW-1A	1	AG	125mL		Cl					SM5310			APP	125		
Purge v	vater "tea" (	colored.												nethod used.		
MATERIA		AG = Amber		= Clear G	-		ethylene;		Polypropy		one; 1		-	Other (Specify)		
SAMPLING	SAMPLING EQUIPMENT CODES:  APP = After Peristaltic Pump; B = Bailer; BP = Bladder Pump; ESP = Electric Submersible Pump; RFPP = Reverse Flow Peristaltic Pump; SM = Straw Method (Tubing Gravity Drain); O = Other (Specify)															

**NOTES:** Stabilization Criteria for Range of Variation of Last Three Consecutive Readings:  $-pH: \pm 0.1$  unit **Specific Conductance**:  $\pm 5\%$  **Dissolved Oxygen**: all readings  $\leq 10\%$  saturation; optionally,  $\pm 0.2$  mg/L **Turbidity**: all readings  $\leq 10$  NTU; or  $\pm 10\%$ 

SITE  NAME: LCP Chemical Site  SITE  LOCATION: Brunswick, GA														
WELL NO: MW-1B         SAMPLE ID: MW-1B         DATE: 11/27/12														
PURGING DATA														
WELL DIAMETER (inches): 2  TUBING DIAMETER (inches): 1/4  WELL SCREEN INTERVAL (btoc) DEPTH: 33 feet to 38 feet feet): 8.85										PΕ				
WELL VOLUME PURGE: 1 WELL VOLUME = (TOTAL WELL DEPTH - STATIC DEPTH TO WATER) X WELL CAPACITY (only fill out if applicable)														
	= ( feet - feet) X 0.16 gallons/foot = gallons  EQUIPMENT VOLUME PURGE: 1 EQUIPMENT VOL. = (TUBING CAPACITY X TUBING LENGTH) + FLOW CELL VOLUME													
	t if applicable)			ons/foot X 39.				•		LOIVIE				
	JMP OR TUBING		_	MP OR TUBING WELL (feet btoo		PURGIN INITIATE	URGING IITIATED AT: 1355		PURGING ENDED AT: 1552		TOTAL VOI PURGED (		LUME gallons): 1.75	
TIME	TIME VOLUME PURGED PURGED (gallons) (gallons) (gpm)			DEPTH TO WATER (feet btoc)	TEMP. (°C)		COND. S/cm)	DISSOLVED OXYGEN (% saturation)	TURB (NT		ORP (mV)	SP Gravity (sg)		
1456	0.75	0.75	0.012	8.85	6.5	22.67	6.3	309	4.7	1.5	55	-117.0	)	
1508	0.25	1.00	0.02	8.89	6.5	22.27	6.3	288	2.8	1.1	15	-137.8	3	
1527	0.25	1.25	0.03	8.89	6.5	22.52	6.2	2666	2.8	1.0	03	-140.0	)	
1536	0.25	1.50	0.03	8.89	6.5	22.34	6.:	261	3.3	0.9	95	-143.6	6	
1550										-144.7				
WELL CAPACITY (Gallons Per Foot): 0.75" = 0.02; 1" = 0.04; 1.25" = 0.06; 2" = 0.16; 3" = 0.37; 4" = 0.65; 5" = 1.02; 6" = 1.47; 12" = 5.88  TUBING INSIDE DIA. CAPACITY (Gal./Ft.): 1/8" = 0.0006; 3/16" = 0.0014; 1/4" = 0.0026; 5/16" = 0.004; 3/8" = 0.006; 1/2" = 0.010; 5/8" = 0.016  BTOC = Below top of casing – feet below top of casing which includes above grade riser														
PURGING EQUIPMENT CODES: B = Bailer; BP = Bladder Pump; ESP = Electric Submersible Pump; PP = Peristaltic Pump; O = Other (Specify)														
SAMPLING DATA														
SAMPLED BY (PRINT) / AFFILIATION:  Maria Johnson/Parsons  SAMPLER(S) SIGNATURE(S):  SAMPLING INITIATED AT: 1559  SAMPLING ENDED AT: 1643											-			
PUMP OR DEPTH IN	TUBING WELL (feet): 3	5.5		TUBING MATERIAL CC					-FILTERED: Yes/ on Equipment Typ			de FILTER :	SIZE: <u>0.45</u> μm	
FIELD DEC	CONTAMINATIO	ON: PUM	P Y N	0	TUBING	Y No	(replac	ced)	DUPLICATE:		No	0		
SAMI	PLE CONTAINE	R SPECIFICA	TION	;	SAMPLE PR	ESERVATIO	N		INTENDE			MPLING	SAMPLE PUMP	
SAMPLE ID CODE	# CONTAINERS	MATERIAL CODE	VOLUME	PRESERVATIV USED		OTAL VOL D IN FIELD (I	ml )	FINAL pH	ANALYSIS AN METHOL			IIPMENT CODE	FLOW RATE (mL per minute)	
MW-1B	1	PE	250mL	HNO3	7,0021		,,,,		6010B T		APP		125	
MW-1B	1	PE	125mL						3500 FE/ 90 pH	040B	A	APP	63	
MW-1B	1	PE	250mL						6010B Diss Silica	olved	A	APP	83	
MW-1B	1	PE	125mL						9056A_2 Chloride Sulfate	&	A	APP	125	
MW-1B	1	AG	125mL						SM 5310 E		A	APP	125	
MW-1B	2	PE	250mL	NaOH Zinc Acetate	e				SM4500 St	ulfide		APP	Field-Filtered	
MW-1B	1	PE	500mL						2540C TI	os		APP	83	
MW-1B	1	PE	250mL						2320B Alka	linity		APP	125	
MW-1B	1	AG	125mL	HCI					SM5310 T			APP	63	
	s: Per SOP, vater "tea" o								ing–in-Scre	en-Inte	erval	purge m	ethod used.	
MATERIAI		AG = Amber (		: Clear Glass;	PE = Poly		_	Polypropyl	ene; <b>S</b> = Silico	ne; T	= Teflo	n; <b>O</b> = O	ther (Specify)	
SAMPLING	G EQUIPMENT	CODES: A	PP = After Pe	ristaltic Pump;	B = Bail	er; BP =	Bladde	er Pump;	ESP = Electri	c Subme	ersible I	Pump;		

RFPP = Reverse Flow Peristaltic Pump; SM = Straw Method (Tubing Gravity Drain); O = Other (Specify)

NOTES: Stabilization Criteria for Range of Variation of Last Three Consecutive Readings:-pH: ± 0.1 unit Specific Conductance: ± 5% Dissolved Oxygen: all readings ≤ 10% saturation; optionally, ± 0.2 mg/L Turbidity: all readings ≤ 10 NTU; or ± 10%

OUTE	OUT.												
SITE NAME: LCP Chemical Site SITE LOCATION: Brunswick, GA													
WELL NO:	MW-1C			SAMPLE II	D: MW-1C			DATE: 11/26/12					
PURGING DATA													
WELL TUBING DIAMETER (inches): 1/4 WELL SCREEN INTERVAL STATIC DEPTH (btoc) DIAMETER (inches): 1/4 (btoc) DEPTH:48.5 feet to 53.5 feet											/PE		
	WELL VOLUME PURGE: 1 WELL VOLUME = (TOTAL WELL DEPTH - STATIC DEPTH TO WATER) X WELL CAPACITY  (only fill out if applicable) = ( feet - feet) X 0.16 gallons/foot = gallons												
	EQUIPMENT VOLUME PURGE: 1 EQUIPMENT VOL. = (TUBING CAPACITY X TUBING LENGTH) + FLOW CELL VOLUME  (only fill out if applicable) = s ( 0.0026 gallons/foot X 55 feet) + 0.13 gallons = 0.27 gallons												
-	JMP OR TUBIN	-	FINAL PUMP DEPTH IN W	OR TUBING ELL (feet btoc)	): 51.0	PURGIN INITIATI		1414	PURGING ENDED AT:	1524		TOTAL VOL PURGED (g	.UME pallons): 1.95
TIME VOLUME VOLUME PURGE PURGED (gallons) (gallons) (gpm)			DEPTH TO WATER (feet btoc)	pH (standard units)	TEMP.		P COND. DISSOI OXYC (% satu		TURBIDITY (NTUs)		ORP (mV)	SP Gravity (sg)	
1439	0.75	0.75	0.03	10.5	6.75	22.98	69	.34	4.3	-	-	-156.	1
1453	0.35	1.10	0.025	10.5	6.74	22.24	69	.00	3.2	0.3	35	-162.9	9
1506	0.30	1.40	0.027	10.5	6.74	22.39		.04	2.8	1.3		-170.9	
1516	0.25	1.65	0.025	10.5 10.5	6.74	22.40		.00	2.3	1.2		-177.4 -179.0	
1524	1524 0.30 1.95 0.038			10.5	22.31	69	.02	2.3	1.90		-179.0	1.040	
TUBING IN													
PURGING	PURGING EQUIPMENT CODES: B = Bailer; BP = Bladder Pump; ESP = Electric Submersible Pump; PP = Peristaltic Pump; O = Other (Specify)												
SAMPLING DATA  SAMPLED BY (PRINT) / AFFILIATION: SAMPLER(S) SIGNATURE(S):													
	SAMPLED BY (PRINT) / AFFILIATION: Maria Johnson/Parsons  SAMPLER(S) SIGNATURE(S): SAMPLING INITIATED AT: 1534  SAMPLING ENDED AT: 1614												
PUMP OR DEPTH IN	TUBING WELL (feet): 5	1.0		UBING IATERIAL COI					-FILTERED: Ye on Equipment Ty		nge	FILTER S	IZE: <u>0.45</u> μm
FIELD DEC	CONTAMINATIO	ON: PUN	MP Y N		TUBING	Y N (r	eplaced)		DUPLICATE:		N	o	
	PLE CONTAINE		_			RESERVATIO	N .		INTENDE		_	MPLING	SAMPLE PUMP FLOW RATE
SAMPLE ID CODE	# CONTAINERS	MATERIAL CODE	VOLUME F	RESERVATIV USED		TOTAL VOL D IN FIELD (	mL)	FINAL pH	ANALYSIS AND/OR METHOD		EQUIPMENT CODE		(mL per minute)
MW- 1C	1	PE	250mL	HNO3					6010B T Metals/ 747	0A Hg	APP		83
MW- 1C	1	PE	125mL						3500 FE/ 9 pH	040B	A	APP	63
MW- 1C	1	PE	250mL						6010B Diss Silica		APP		250
MW- 1C	1	PE	125mL						9056A_2 Chloride Sulfate	&	A	APP	63
MW- 1C	1	AG	125mL						SM 5310 [	оос	A	APP	125
MW- 1C	2	PE	250mL	NaOH Zinc Acetate	,				SM4500 S	ulfide	A	APP	Field-Filtered
MW- 1C	1	PE	500mL						2540C T	DS	A	APP	63
MW.										63			
MW- 1C	1	AG	125mL	HCI					SM5310 T	ОС	A	APP	63
REMARKS									ing–in-Scre				
used. Initial purge water was very dark brown with sandy slugs, and the turbidity was too high for the meter to read.  Water cleared throughout purge.													
	MATERIAL CODES: AG = Amber Glass; CG = Clear Glass; PE = Polyethylene; PP = Polypropylene; S = Silicone; T = Teflon; O = Other (Specify)  SAMPLING FOLIPMENT CODES: APP = After Peristaltic Pump: B = Bailer: BP = Bladder Pump: ESP = Electric Submersible Pump:												other (Specify)

SITE NAME: LC	SITE  NAME: LCP Chemical Site  SITE  LOCATION: Brunswick, GA													
WELL NO:	: MW-2A			SA	MPLE ID:						DATE:	11/28/12	2	
	PURGING DATA													
WELL	D (in the table 0	TUBIN		4/4			NTERVAL	<b>.</b>		DEPTH (btoc)			E PUMP TY	PE
	R (inches): 2  LUME PURGE:		TER (inches): LUME = (TOT				feet to 23 f			ER (feet): 8.41 WELL CAPAC	ITY	OR BA	ILER: PP	
(only fill ou	(only fill out if applicable)  = ( feet - feet) X 0.16 gallons/foot = gallons  EQUIPMENT VOLUME PURGE: 1 EQUIPMENT VOL. = (TUBING CAPACITY X TUBING LENGTH) + FLOW CELL VOLUME													
	NT VOLUME PU it if applicable)		JIPMENT VOL	`					,		DLUME			_
INITIAI PI	JMP OR TUBIN		FINAL PUI			ieet) + t	PURGIN		0.19 ga	PURGING		Т	OTAL VOL	UME
DEPTH IN WELL (feet btoc): 20.5  DEPTH IN WELL (feet btoc): 20.5  DEPTH IN WELL (feet btoc): 20.5							INITIATI		: 1028	ENDED AT:	1101			allons): 1.25
TIME	VOLUME PURGED (gallons)	CUMUL. VOLUME PURGED (gallons)	PURGE RATE (gpm)	T( WAT (fe	ER (st	pH andard units)	TEMP. (°C)	_	COND. mS/cm)	DISSOLVED OXYGEN (% saturation)	_	BIDITY TUs)	ORP (mV)	SP Gravity (sg)
1040	0.25	0.25	0.02	8.5		7.7	19.99	7	7.172	8.3	4	.83	-166.2	2
1045	0.25	0.50	0.05	8.5		7.0	20.07	7	7.185	6.8	4	.57	-167.9	)
1050	0.25	0.75	0.05	8.5		7.0	20.22		7.192	5.4		.00	-171.1	
1055	0.25	1.00	0.05	8.5		6.9	20.30		7.194	4.8		.82	-183.3	
1100	0.25	1.25	0.05	8.5	55	7.0	20.40	7	7.193	4.1	3	.72	-183.2	1.003
WELLCA	WELL CAPACITY (Gallons Per Foot): 0.75" = 0.02; 1" = 0.04; 1.25" = 0.06; 2" = 0.16; 3" = 0.37; 4" = 0.65; 5" = 1.02; 6" = 1.47; 12" = 5.88													
<b>TUBING INSIDE DIA. CAPACITY</b> (Gal./Ft.): $1/8$ " = 0.0006; $3/16$ " = 0.0014; $1/4$ " = 0.0026; $5/16$ " = 0.004; $3/8$ " = 0.006; $1/2$ " = 0.010; $5/8$ " = 0.016														
BTOC = Below top of casing – feet below top of casing which includes above grade riser  PURGING EQUIPMENT CODES: B = Bailer; BP = Bladder Pump; ESP = Electric Submersible Pump; PP = Peristaltic Pump; O = Other (Specify)														
SAMPLING DATA														
SAMPLED BY (PRINT) / AFFILIATION: Maria Johnson/Parsons  SAMPLER(S) SIGNATURE(S): SAMPLING INITIATED AT: 1106 SAMPLING ENDED AT: 1130														
PUMP OR DEPTH IN	TUBING WELL (feet): 2	0.5		TUBING	IAL CODE					-FILTERED: Yes on Equipment Ty			le FILTER	SIZE: <u>0.45</u> μm
FIELD DE	CONTAMINATIO	ON: PUN	1P Y N	lo		TUBING	Y No	(repl	aced)		DUPLIC	CATE:		No
SAM	PLE CONTAINE	R SPECIFICA	ATION		SAM	MPLE PR	ESERVATIO	N		INTEND			1PLING	SAMPLE PUMP
SAMPLE ID CODE	# CONTAINERS	MATERIAL CODE	VOLUME		RVATIVE SED		TOTAL VOL ADDED IN FIELD (mL)			FINAL ANALYSIS METH			IPMENT ODE	FLOW RATE (mL per minute)
MW-2A	1	PE	250mL	Н	1O3					6010B 7 Metals/747			\PP	125
MW-2A	1	PE	125mL							3500 FE/ 9 pH	3500 FE/ 9040B		\PP	125
MW-2A	1	PE	250mL							6010B Disa Silica	1	A	\PP	250
MW-2A	1	PE	125mL							9056A_2 Chloride Sulfat	- &	Δ	\PP	125
MW-2A	1	AG	125mL		-					SM 5310		Δ	\PP	125
MW-2A	2	PE	250mL		OH Acetate					SM4500 S	ulfide	Α	\PP	Field-Filtered
MW-2A	1	PE	500mL							2540C T	DS	Α	\PP	125
MW-2A	1	PE	250mL							2320B Alk	alinity	A	\PP	250
MW-2A	1	AG	125mL		ICI					SM5310			\PP	125
	s: Per SOP, vater "tea" o	•				ings be	efore san	nplin	g. Tubi	ng –in-Scre	en-Int	erval	purge m	nethod used.
MATERIA		AG = Amber		= Clear G		PE = Poly	ethylene;	PP =	Polypropyl	lene; <b>S</b> = Silic	one; <b>T</b>	= Teflor	n; <b>O</b> = C	ther (Specify)
SAMPLIN	G EQUIPMENT		APP = After Pe			<b>B</b> = Bail			der Pump;	ESP = Elect		nersible F Other (S		

SITE NAME: I C	SITE NAME: LCP Chemical Site  SITE LOCATION: Brunswick, GA												
WELL NO:		•		SAMPLE	ID: MW-2B		answick	., 0/1		DATE:	11/28/1	2	
					PURG	ING DA	TA						
WELL DIAMETER	R (inches): 2	TUBING	G TER (inches):		LL SCREEN (c) DEPTH: 3	INTERVAL			DEPTH (btoc) ER (feet): 8.31			E PUMP TY	PE
	LUME PURGE: t if applicable)	1 WELL VO	LUME = (TOT = (	AL WELL DEF	PTH - STA	TIC DEPTH 1		ΓER) X feet) X	WELL CAPAC	ITY ons/foot	_		gallons
	NT VOLUME PU	JRGE: 1 EQL		= (TUBING C		X TUB			FLOW CELL VC				ganoris
(Offig fill Ou	п п аррпсавіе)	=	(0.0026 gall	ons/foot X 39.	5 feet) + 0.1	13 gallons	= 0.2	23 gallo	ns				
	JMP OR TUBIN WELL (feet bto		_	MP OR TUBING WELL (feet bto		PURGIN INITIATI		0752	PURGING ENDED AT:	0828		FOTAL VOL PURGED (g	UME allons): 1.50
TIME	VOLUME PURGED (gallons)	CUMUL. VOLUME PURGED (gallons)	PURGE RATE (gpm)	DEPTH TO WATER (feet btoc)	pH (standard units)	TEMP. (°C)		COND. S/cm)	DISSOLVED OXYGEN (% saturation)	_	BIDITY (TUs)	ORP (mV)	SP Gravity (sg)
0806	0.50	0.50	0.036	8.4	6.26	19.84	5.	917	16.8	3.	.26	-121.8	3
0812	0.25	0.75	0.04	8.4	6.24	19.95	5.	955	12.0	3.	.14	-131.2	2
0817	0.25	1.00	0.05	8.4	6.2	19.98	5.	962	9.9	2.	.88	-132.1	l
0822	0.25	1.25	0.05	8.4	6.2	20.07	5.	972	8.2	2.	.39	-140.1	ı
0828	0.25	1.50	0.04	8.4	6.2	20.09	5.	976	8.0	1.	.53	-142.1	1.002
							L			<u> </u>			
TUBING IN	WELL CAPACITY (Gallons Per Foot): 0.75" = 0.02; 1" = 0.04; 1.25" = 0.06; 2" = 0.16; 3" = 0.37; 4" = 0.65; 5" = 1.02; 6" = 1.47; 12" = 5.88  TUBING INSIDE DIA. CAPACITY (Gal./Ft.): 1/8" = 0.0006; 3/16" = 0.0014; 1/4" = 0.0026; 5/16" = 0.004; 3/8" = 0.006; 1/2" = 0.010; 5/8" = 0.016  BTOC = Below top of casing – feet below top of casing which includes above grade riser												
PURGING EQUIPMENT CODES: B = Bailer; BP = Bladder Pump; ESP = Electric Submersible Pump; PP = Peristaltic Pump; O = Other (Specify)  SAMPLING DATA													
CAMDLED	BY (PRINT) / A	EEII IATIONI:		SAMPLER(S)			ATA						
	ohnson/Pai			-Man		almse			SAMPLING INITIATED A	T: 0835		SAMPLIN ENDED A	
PUMP OR DEPTH IN	TUBING WELL (feet): 3	5.5		TUBING MATERIAL C					-FILTERED: Yes on Equipment Ty			de FILTER	SIZE: <u>0.45</u> μm
FIELD DE	CONTAMINATIO	ON: PUM	IP Y N	lo	TUBING	Y No	(repla	ced)	DUPLICATE:		N	lo	
	PLE CONTAINE		ATION			RESERVATIO	N _		INTEND ANALYSIS A		_	MPLING JIPMENT	SAMPLE PUMP FLOW RATE
SAMPLE ID CODE	# CONTAINERS	MATERIAL CODE	VOLUME	PRESERVAT USED		FOTAL VOL ED IN FIELD (	mL)	FINAL pH	METHO	D		ODE	(mL per minute)
MW-2B	1	PE	250mL	HNO3					6010B T Metals/747		/	APP	250
MW-2B	1	PE	125mL						3500 FE/ 9 pH		,	APP	125
MW-2B	1	PE	250mL						6010B Diss Silica		,	APP	250
MW-2B	1	PE	125mL						9056A_2 Chloride	28D e &	,	APP	125
MW-2B	1	AG	125mL						Sulfate SM 5310		,	APP	125
MW-2B	2	PE	250mL	NaOH Zinc Aceta	ite				SM4500 S		,	APP	Field-Filtered
MW-2B	1	PE	500mL						2540C T	DS	,	APP	167
	MW-2B 1 PE 250mL 2320B Alkalinity APP 250												
MW-2B 1 AG 125mL HCI SM5310 TOC APP 125  REMARKS: Per SOP Parameters stable for three readings before sampling. Tubing—in-Screen-Interval purge method used.													
						efore sam	pling	. Tubi	ng–in-Scree	n-Inte	rval p	ourge me	ethod used.
Purge water very brown, indistinguishable sulfur-like odor  MATERIAL CODES: AG = Amber Glass; CG = Clear Glass; PE = Polyethylene; PP = Polypropylene; S = Silicone; T = Teflon; O = Other (Specify)													
	G EQUIPMENT	CODES: A	APP = After Pe	eristaltic Pump; se Flow Perista	<b>B</b> = Bai	ler; BP =	Bladde	er Pump;	ESP = Electric Gravity Drain);	ric Subm		Pump;	and (Opeony)
			110101			J Ollaw		- (. abing	a, Diamij,	<b>J</b> = (	, (	· · · · · /	

**NOTES:** Stabilization Criteria for Range of Variation of Last Three Consecutive Readings: **pH**:  $\pm$  0.1 unit **Specific Conductance**:  $\pm$  5% **Dissolved Oxygen**: all readings  $\leq$  10% saturation; optionally,  $\pm$  0.2 mg/L **Turbidity**: all readings  $\leq$  10 NTU; or  $\pm$  10%

SITE	SITE									
NAME: LCP Chemical Site	LOCATION: Brunswick, GA									
WELL NO: MW-2C	SAMPLE ID: MW-2C- <b>MID</b>	DATE: 11/27/12								
DUDANIA DATA										

#### PURGING DATA

					ING DA								
WELL	TUBING			LL SCREEN I			DEPTH (btoc)	_	RGE PUMP TYPE				
DIAMETER (inches): 2		ER (inches): 1/	,	oc) DEPTH: 48			ER (feet): 9.22		BAILER: PP				
WELL VOLUME PURGE: (only fill out if applicable)	1 WELL VOL	UME = (TOTA	L WELL DEF	PTH - STAT	TIC DEPTH T	O WATER) X		ΓY ons/foot =		gallons			
EQUIPMENT VOLUME P	IRGE: 1 FOUI	= ( PMENT VOL :	- (TUBING (		X TUBI		FLOW CELL VOI			yanons			
(only fill out if applicable) = ( 0.0026 gallons/foot X 55 feet) + 0.13 gallons = 0.27 gallons													
INITIAL PUMP OR TUBIN		FINAL PUMF			PURGIN		PURGING		TOTAL VOLUM	 E			
DEPTH IN WELL (feet bto	c): 53.5	DEPTH IN W	/ELL (feet bt	oc): 53.5	INITIATE	D AT: 1103	ENDED AT:	1351	PURGED (gallor	ns): 2.35			
TIME VOLUME PURGED (gallons) CUMUL. VOLUME PURGED (gallons) (gallo													
1242 0.55	0.55	0.019	11.97	8.54	23.56	52.40	1.4		-353.8				
1250 0.25	0.80	0.03	11.67	7.89	23.20	51.19	1.4		-335.4				
1300 0.25	1.05	0.03	12.15	7.48	22.89	50.47	0.9		-312.5				
1309 0.25	1.30	0.03	12.49	7.41	22.21	50.29	0.5		-320.5				
1319 0.25	1.55	0.03	12.75	7.60	22.36	50.33	0.6		-346.6				
1328 0.25	1.80	0.03	12.90	7.74	22.65	50.27	0.1		-371.9				
1341 0.30	2.10	0.02	13.06	7.75	22.83	50.29	0.4		-381.2				
1349 0.25	2.35	0.03	13.06	7.74	22.27	50.29	0.4		-387.4	1.024			
WELL CAPACITY (Gallons Per Foot): 0.75" = 0.02; 1" = 0.04; 1.25" = 0.06; 2" = 0.16; 3" = 0.37; 4" = 0.65; 5" = 1.02; 6" = 1.47; 12" = 5.88  TUBING INSIDE DIA. CAPACITY (Gal./Ft.): 1/8" = 0.0006; 3/16" = 0.0014; 1/4" = 0.0026; 5/16" = 0.004; 3/8" = 0.006; 1/2" = 0.010; 5/8" = 0.016  BTOC = Below top of casing – feet below top of casing which includes above grade riser													
PURGING EQUIPMENT	ODES: B =	Bailer; B	P = Bladder	Pump; E	SP = Electric	Submersible Pu	ımp; PP = Pe	ristaltic Pum	p; <b>O</b> = Other	(Specify)			

#### **SAMPLING DATA**

	BY (PRINT) / A		:	SAMPLER(S) SIGN	NATURE(S):				
Christine	e Jaynes/P	arsons		Cla	ynos)		SAMPLING INITIATED AT: 1358	SAMPLIN ENDED A	
PUMP OR T DEPTH IN V	UBING VELL (feet): 53	3.5		TUBING MATERIAL CODE:	Teflon-lined PE		FILTERED: Yes/ <b>SM 450</b> 0 n Equipment Type: Syri		SIZE: <u>0.45</u> μm
FIELD DEC	ONTAMINATIO	ON: PU	MP Y	No T	UBING Y <b>No (rep</b>	laced)	DUPLICATE:	Yes	
SAMP	LE CONTAINE	R SPECIFIC	CATION	SAM	PLE PRESERVATION		INTENDED	SAMPLING	SAMPLE PUMP
SAMPLE ID CODE	# CONTAINE RS	MATERIAL CODE	VOLUME	PRESERVATIVE USED	TOTAL VOL ADDED IN FIELD (mL)	FINAL pH	ANALYSIS AND/OR METHOD	EQUIPMENT CODE	FLOW RATE (mL per minute)
MW-2C- MID	2	PE	250mL	HNO3			6010B TAL Metals/7470A Hg	APP	83
MW-2C- MID	2	PE	125mL				3500 FE/ 9040B pH	APP	63
MW-2C- MID	2	PE	250mL				6010B Dissolved Silica	APP	71
MW-2C- MID	2	PE	125mL				9056A_28D Chloride & Sulfate	APP	83
MW-2C- MID	2	AG	125mL				SM 5310 DOC	APP	63
MW-2C- MID	4	PE	250mL	NaOH Zinc Acetate			SM4500 Sulfide	APP	Field-Filtered
MW-2C- MID	2	PE	500mL				2540C TDS	APP	71
MW-2C- MID	2	PE	250mL				2320B Alkalinity	APP	71
MW-2C- MID	2	2 AG 125mL HCl					SM5310 TOC	APP	83

REMARKS: Per SOP Parameters stable for three readings before sampling. Tubing –in-Screen-Interval purge method used. Turbidity too low for the meter to read; meter calibration was verified between readings. Purge paused from 1120-1230 water level recovered to 9.74ft during that time. Purge water clear, brown. Black "resign" noted on tubing interior wall and in filters.

MATERIAL CODES: AG = Amber Glass; CG = Clear Glass; **PE** = Polyethylene; **PP** = Polypropylene; **S** = Silicone; **T** = Teflon;

SAMPLING EQUIPMENT CODES: **B** = Bailer; **BP** = Bladder Pump; **ESP** = Electric Submersible Pump; APP = After Peristaltic Pump;

**RFPP** = Reverse Flow Peristaltic Pump; **SM** = Straw Method (Tubing Gravity Drain);

GROUNDWATER SAMPLING LOG														
SITE NAME: I CE	Chemical Site	<u> </u>			_	TE DCATION: Bru	nswic	k GA						
WELL NO:				SAMPLE ID				, 0		DATE: 1	11/27/1	2		
					PURG	SING DA	TA							
WELL	(inches), 2	TUBIN	-			INTERVAL			EPTH (btoc)			E PUMP T	YPE	
WELL VOL	, ,	l l	TER (inches):	TAL WELL DEPTH		8 feet to 53 fe TIC DEPTH T			R (feet): 12.0 WELL CAPAC		OR BA	AILER: PP		
(only fill out	if applicable)		= (	fe	et –			feet) X	0.16 gal	llons/foot	=		gallons	
	IT VOLUME PO if applicable)		UIPMENT VOI	= (TUBING CAP	ACITY				FLOW CELL VO					
INITIAL PUI	MP OR TUBIN		ì	MP OR TUBING		PURGIN		<b>J</b>	PURGING		Т	TOTAL VOI	LUME	
DEPTH IN \	NELL (feet bto	c): 51	DEPTH IN	WELL (feet btoc):	51	INITIATE	D AT	: 1527	ENDED AT:	1622	F	PURGED (g	gallons): 1.15	
TIME	VOLUME PURGED (gallons)	CUMUL. VOLUME PURGED (gallons)	PURGE RATE (gpm)	DEPTH TO WATER (s (feet btoc)	pH standard units)	TEMP. (°C)		COND. nS/cm)	DISSOLVED OXYGEN (% saturation)	(NIT	BIDITY 'Us)	ORP (mV)		
1535	0.27 in tubing &flow-thru	0.27	0.03	12.32	7.14	22.70	4	19.73	5.8	-	-181.	4		
1544 0.25 in 0.25in 0.03 12.54 6.96 22.41 bucket									2.2	-	-	-183.	0	
1554	0.25	0.50 in bucket	0.025	12.69	6.83	22.08	4	17.98	1.8	-	-	-191.	1	
1609	0.35	0.85 in bucket	0.027	12.77	6.80	21.92 47.90 2.4		-	-	-206.	3			
1620														
TUBING IN:	WELL CAPACITY (Gallons Per Foot): 0.75" = 0.02; 1" = 0.04; 1.25" = 0.06; 2" = 0.16; 3" = 0.37; 4" = 0.65; 5" = 1.02; 6" = 1.47; 12" = 5.88  TUBING INSIDE DIA. CAPACITY (Gall./Ft.): 1/8" = 0.0006; 3/16" = 0.0014; 1/4" = 0.0026; 5/16" = 0.004; 3/8" = 0.006; 1/2" = 0.010; 5/8" = 0.016  BTOC = Below top of casing – feet below top of casing which includes above grade riser													
PURGING I	EQUIPMENT C	ODES: E	B = Bailer;	BP = Bladder Pun	• • • • • • • • • • • • • • • • • • • •	SP = Electric			np; <b>PP</b> = P	eristaltic	Pump;	<b>O</b> = O	ther (Specify)	
SAMPLED	BY (PRINT) / A	FEILIATION:	<u> </u>	SAMPLER(S) SIG		LING DA	TA		1		1			
	e Jaynes/P			- 1 0		100).			SAMPLING INITIATED A	T: 1627		SAMPLIN ENDED A	-	
PUMP OR 1 DEPTH IN \	ΓUBING NELL (feet): 51	I		TUBING MATERIAL COD	E: Teflon	-lined PE			FILTERED: Yes n Equipment Ty			de FILTER	SIZE: <u>0.45</u> μm	
FIELD DEC	ONTAMINATIO	ON: PU	MP Y N	No	TUBING	Y <b>No</b>	(repla	aced)	DUPLICATE	:	No			
SAMP	LE CONTAINE	R SPECIFIC	ATION	SA	MPLE PR	RESERVATIO	N		INTEND	ED	SAN	MPLING	SAMPLE PUMP	
SAMPLE ID CODE	# CONTAINE RS	MATERIAL CODE	VOLUME	PRESERVATIVE USED		TOTAL VOL ED IN FIELD (r	nL)	FINAL pH	ANALYSIS A METHO	_		JIPMENT CODE	FLOW RATE (mL per minute)	
MW-2C- TOP	1	PE	250mL	HNO3					6010B 7 Metals/747		,	APP	63	
MW-2C- TOP	1	PE	125mL						3500 FE/ 9 pH		,	APP	63	
MW-2C- TOP	1	PE	250mL						6010B Dis		,	APP	63	
MW-2C- TOP	1	PE	125mL						9056A_2 Chloride Sulfat	28D e &	,	APP	63	
MW-2C- TOP	1	AG	125mL						SM 5310		,	APP	63	
NaOH   NaOH   NaOH   Zinc Acetate								SM4500 S	Sulfide	,	APP	Field-Filtered		
MW-2C- TOP	1	PE	500mL						2540C T	TDS	1	APP	71	
MW-2C-	1	PE	250mL						2220B VIP	alinity	-	APP	63	

REMARKS: Per SOP, parameters stable for three readings prior to sampling. Turbidity was too low for the meter to read; meter calibration was verified between readings. Purge water clear, brown. Black "resign" not noted in the filters.

APP

2320B Alkalinity

**SM5310 TOC** 

63

MATERIAL CODES: **AG** = Amber Glass; O = Other (Specify) CG = Clear Glass; PE = Polyethylene; **PP** = Polypropylene; S = Silicone; T = Teflon;

**APP** = After Peristaltic Pump; **B** = B **RFPP** = Reverse Flow Peristaltic Pump; B = Bailer; BP = Bladder Pump; Let - Let ump; SM = Straw Method (Tubing Gravity Drain); **SAMPLING EQUIPMENT CODES: ESP** = Electric Submersible Pump; O = Other (Specify)

HCI

AG

TOP

MW-2C-

125mL

	SITE  NAME: LCP Chemical Site  SITE  LOCATION: Brunswick, GA												
SITE NAME: LC	P Chemical Site				_		nswick, GA						
WELL NO:	MW-3A			SAMPLE ID	): MW-3A					DATE:	11/28/12	2	
					PURG	ING DA	TA		L				
WELL	R (inches): 2	TUBIN	IG ETER (inches):			INTERVAL 3 feet to 23 fe			EPTH (btoc) R (feet): 8.9			E PUMP TY	/PE
	, ,		, ,	AL WELL DEPTH					, ,	TY	OK BA	ILLIX. I I	
` •	t if applicable)		= (	fe	et –		feet)	Х	0.16 gall	ons/foot	=		gallons
	NT VOLUME PU t if applicable)			. = (TUBING CAF	PACITY		NG LENGTI	H) + F	LOW CELL VO	LUME			
INITIAL PU	JMP OR TUBING			MP OR TUBING	1001) 1	PURGIN		gain	PURGING		Т	OTAL VOL	UME
DEPTH IN	WELL (feet btoo	c): 20.5	DEPTH IN	WELL (feet btoc)	: 20.5	INITIATE	D AT: 1418	8	ENDED AT:	1457	P	URGED (g	allons): 1.2
TIME	VOLUME PURGED (gallons)	CUMUL. VOLUME PURGED (gallons)		ТО	pH (standard units)	TEMP. (°C)	SP CONE ( mS/cm)		DISSOLVED OXYGEN (% saturation)	_	BIDITY TUs)	ORP (mV)	
1430	0.25	0.25	0.02	9.4	6.8	21.14	47.42		5.5	-1	.43	-217.4	1
1435	0.25	0.50	0.05	9.4	6.8	21.03	47.44		4.7	-1	.36	-254.	5
1440	0.20	0.70	0.04	9.4	6.8	20.55	47.44		3.1	-1	.21	-256.0	)
1450	0.30	1.00	0.03	9.4	6.9	20.80	47.25		2.7	-0	.87	-194.8	
1456	0.20	1.20	0.03	9.35	6.9	20.92	47.11		3.2	-0	).72	-240.9	9 1.022
	WELL CAPACITY (Gallons Per Foot): 0.75" = 0.02: 1" = 0.04: 1.25" = 0.06: 2" = 0.16: 3" = 0.37: 4" = 0.65: 5" = 1.02: 6" = 1.47: 12" = 5.88												
WELL CAPACITY (Gallons Per Foot): 0.75" = 0.02; 1" = 0.04; 1.25" = 0.06; 2" = 0.16; 3" = 0.37; 4" = 0.65; 5" = 1.02; 6" = 1.47; 12" = 5.88  TUBING INSIDE DIA. CAPACITY (Gal./Ft.): 1/8" = 0.0006; 3/16" = 0.0014; 1/4" = 0.0026; 5/16" = 0.004; 3/8" = 0.006; 1/2" = 0.010; 5/8" = 0.016  BTOC = Below top of casing – feet below top of casing which includes above grade riser													
PURGING EQUIPMENT CODES: B = Bailer; BP = Bladder Pump; ESP = Electric Submersible Pump; PP = Peristaltic Pump; O = Other (Specify)													
CAMPI ED	SAMPLING DATA  SAMPLED BY (PRINT) / AFFILIATION: SAMPLER(S) SIGNATURE(S):												
	ohnson/Pai			The second second		chnsel			SAMPLING INITIATED AT	Γ: 1503		SAMPLIN ENDED A	-
PUMP OR DEPTH IN	TUBING WELL (feet): 20	0.5		TUBING MATERIAL COL	DE: Teflon	-lined PE			FILTERED: Yes			le FILTER	SIZE: <u>0.45</u> μm
FIELD DEC	CONTAMINATIO	ON: PU	MP Y N	О	TUBING	Y <b>No</b>	(replaced)		DUPLICATE:		N	0	
SAMI	PLE CONTAINE	R SPECIFIC	ATION	S	AMPLE PR	RESERVATIO	N		INTENDE		_	/PLING	SAMPLE PUMP
SAMPLE ID CODE	# CONTAINERS	MATERIAL CODE	VOLUME	PRESERVATIVI USED		TOTAL VOL D IN FIELD (n	nL) FIN		ANALYSIS AI METHO			IPMENT ODE	FLOW RATE (mL per minute)
MW-3A	1	PE	250mL	HNO3				-	6010B T Metals/7470		P	\PP	125
MW-3A	1	PE	125mL						3500 FE/ 9 pH		P	\PP	125
MW-3A	1	PE	250mL					-	6010B Diss Silica		P	\PP	250
MW-3A	1	PE	125mL					=	9056A_2 Chloride Sulfate	8D &	A	\PP	125
MW-3A	1	AG	125mL					_	SM 5310 [		P	\PP	125
MW-3A	2	PE	250mL	NaOH Zinc Acetate				-	SM4500 S	ulfide	P	\PP	Field-Filtered
	MW-3A 1 PE 500mL 2540C TDS APP 250												
MW-3A	2020 7 mainty												
MW-3A	1	AG	125mL	HCI				-	SM5310 T			\PP	125
Turbidit	REMARKS: Per SOP, parameters stable for three readings prior to sampling. Tubing—in-Screen-Interval purge method used. Turbidity was too low for the meter to read and negative values were recorded; meter calibration was verified between readings.												
MATERIAL	CODES:	AG = Ambe	Glass; CG =	: Clear Glass;	<b>PE</b> = Poly	vethylene;	<b>PP</b> = Polypi	ropyle	ne; <b>S</b> = Silico	ne; T	= Teflo	n; <b>O</b> = C	Other (Specify)
SAMPLING	3 EQUIPMENT		APP = After Pe	ristaltic Pump; se Flow Peristaltic	<b>B</b> = Bai : Pump:		Bladder Pur Method (Tu		ESP = Electr Gravity Drain):		ersible f Other (S		

			G	ROUND	NATE	ER SAI	MPL	.ING	LOG					
SITE NAME: LC	CP Chemical Site	<u> </u>			SI	TE OCATION: Bru	ınewick	GA						
	: MW-115A	<u>,                                      </u>		SAMPLE ID			an iowicit,	O/ C		DATE: 11	/28/12	2		
					PURG	ING DA	ΤΔ							
WELL DIAMETE	R (inches): 2	TUBIN	IG ETER (inches):		SCREEN DEPTH: 1	INTERVAL 5.25 feet to	5	STATIC D feet btoc)	EPTH TO WATI : 7.36			E PUMP TY ILER: PP	/PE	
		1 WELL VC	DLUME = (TO	TAL WELL DEPTI	H – STA	TIC DEPTH T	TO WAT	ER) X	WELL CAPACI	TY				
. ,	ut if applicable)		= (		eet –		f	eet) X	0.16 gall	ons/foot	=		gallo	ns
	INT VOLUME PU ut if applicable)	JRGE: 1 EQ	UIPMENT VOI	L. = (TUBING CAF	PACITY	X TUB	ING LEN	NGTH) +	FLOW CELL VO	LUME				
(, ,		=	= ( 0.0026 ga	allons/foot X 20.	5 feet) +			0.18	gallons					
	UMP OR TUBIN			MP OR TUBING I WELL (feet btoc)	20.5	PURGIN INITIATE		1255	PURGING ENDED AT:	1323		OTAL VOL		19
TIME	VOLUME PURGED (gallons)	CUMUL. VOLUME PURGED (gallons)	PURGE	DEPTH TO	pH (standard units)	TEMP.	SP C	OND.	DISSOLVED OXYGEN (% saturation)	TURBIE (NTU	OITY	ORP (mV)	S	P Gravity (sg)
1303	0.50	0.50	0.06	7.60	7.4	20.95	5.0	)27	11.7	-1.4	2	-154.6	3	
1308	0.35	0.85	0.07	7.60	7.4	21.24	4.9	927	9.0	-1.6	2	-162.8	3	
1312	0.35	1.20	0.09	7.60	7.4	21.41	4.9	919	6.5	-1.2	8	-162.0	)	
1317         0.30         1.50         0.06         7.60         7.4         21.54         4.834         5.4         -1.41         -166.3														
1322         0.40         1.90         0.08         7.60         7.4         21.57         4.793         4.3         -1.52         -171.5         1.000														
TUBING II BTOC = I	WELL CAPACITY (Gallons Per Foot): 0.75" = 0.02; 1" = 0.04; 1.25" = 0.06; 2" = 0.16; 3" = 0.37; 4" = 0.65; 5" = 1.02; 6" = 1.47; 12" = 5.88  TUBING INSIDE DIA. CAPACITY (Gal./Ft.): 1/8" = 0.0006; 3/16" = 0.0014; 1/4" = 0.0026; 5/16" = 0.004; 3/8" = 0.006; 1/2" = 0.010; 5/8" = 0.016  BTOC = Below top of casing - feet below top of casing which includes above grade riser  PURGING EQUIPMENT CODES: B = Bailer; BP = Bladder Pump; ESP = Electric Submersible Pump; PP = Peristaltic Pump; O = Other (Specify)													
						LING DA	ATA		1					
	BY (PRINT) / A Iohnson/Pai			SAMPLER(S) S	_	chnoe			SAMPLING INITIATED AT	Г: 1330		SAMPLIN ENDED A	-	
PUMP OR DEPTH IN	TUBING WELL (feet): 2	0.5		TUBING MATERIAL COI					FILTERED: Yes/ on Equipment Typ			de FILTER	SIZE: 0	<u>.45</u> μm
FIELD DE	CONTAMINATIO	ON: PUI	MP Y	No	TUBING		(replac		DUPLICATE:	, ,	No	0		
SAM	IPLE CONTAINE	R SPECIFIC	ATION	S	AMPLE PF	RESERVATIO	N		INTENDE			/PLING		E PUMP
SAMPLE ID CODE	# CONTAINERS	MATERIAL CODE	VOLUME	PRESERVATIV USED		OTAL VOL D IN FIELD (	mL)	FINAL pH	ANALYSIS AN METHO			IPMENT ODE		V RATE er minute)
MW- 115A	1	PE	250mL	HNO3	1.232		.=,		6010B T		P	APP	2	250
MW- 115A	1	PE	125mL						3500 FE/ 9		P	APP	1	25
MW- 1 PE 250mL									6010B Diss		P	APP	2	250
115A MW- 115A	1	125mL					Silica 9056A_2 Chloride Sulfate	8D &	P	APP	1	25		
MW- 115A	1	AG	125mL						SM 5310 [		P	APP	1	25
MW- 115A	2	PE	250mL	NaOH Zinc Acetate					SM4500 St	ulfide	P	\PP	Field-	Filtered
MW- 115A	1	PE	500mL						2540C T	DS	P	\PP	1	67
MW- 115A	1	PE	250mL						2320B Alka	alinity	P	\PP	2	250
MW-	1	AG	125mL	HCI					SM5310 T	ос	P	APP		42

REMARKS: Per SOP, parameters stable for three readings before sampling. Tubing–in-Screen-Interval purge method used. Turbidity was too low for the meter to read and negative values were recorded; meter calibration was verified between readings. Purge water dark brown.

MATERIAL CODES: AG = Amber Glass; CG = Clear Glass; PE = Polyethylene; PP = Polypropylene; S = Silicone; T = Teflon; O = Other (Specify)

SAMPLING EQUIPMENT CODES:APP = After Peristaltic Pump;B = Bailer;BP = Bladder Pump;ESP = Electric Submersible Pump;RFPP = Reverse Flow Peristaltic Pump;SM = Straw Method (Tubing Gravity Drain);O = Other (Specify)

SITE	Chemical Site				SIT	E CATION: Bru	unswick GA				
WELL NO:				SAMPLE	ID: MW-115		IIISWICK, GA		DATE: 11/2	8/12	
WELE NO.	11100			O/ (IVII EE			ΤΛ		DATE: 11/2	0/12	
WELL		TUBING		1 14/51	LL SCREEN I	ING DA		OFFIL (btoo)	I DUI	RGE PUMP TYPE	
DIAMETER	(inches): 2		ER (inches): 1/4		c) DEPTH: 31			DEPTH (btoc) ER (feet): 7.00		BAILER: PP	
	UME PURGE: if applicable)	1 WELL VOLU	JME = (TOTAL			TIC DEPTH T	O WATER) X	WELL CAPAC	CITY		
` ,	, ,		= (		feet -		feet) X		llons/foot =	,	gallons
	IT VOLUME PU if applicable)	RGE: 1 EQUII	PMENT VOL. =	(TUBING C	APACITY	X TUBI	NG LENGTH) +	FLOW CELL V	OLUME		
		ì	0.0026 gallor					gallons		1	
	MP OR TUBING WELL (feet btoc		FINAL PUMP DEPTH IN W			PURGIN INITIATE	G ED AT: 0755	PURGING ENDED AT	: 1312	TOTAL VOLUMI PURGED (gallor	
		CUMUL.		DEPTH TO	pH			DISSOLVED			•
TIME	VOLUME PURGED (gallons)	VOLUME PURGED (gallons)	PURGE RATE (gpm)	WATER (feet btoc)	(standard units)	TEMP. ( <sup>°</sup> C)	SP COND. ( mS/cm)	OXYGEN (% saturation)	TURBIDI <sup>*</sup> (NTUs)		SP Gravity (sg)
0807	0.25	0.25	0.02	7.05	7.49	19.64	5.873	7.7	0.67	-116.9	
0811	0.25	0.50	0.06	7.07	7.86	19.89	5.907	5.6	0.67	-164.2	
0816	0.25	0.75	0.05	7.07	7.10	19.92	5.925	4.8	1.09	-136.4	
0822	0.25	1.00	0.04	7.06	6.94	20.13	5.919	3.7	1.64	-133.4	
0828	0.25	1.25	0.04	7.07	6.40	20.06	5.967	3.5	0.73	-118.9	
0836	0.25	1.60	0.03	7.07	9.58	20.06	5.978	3.1	1.63	-236.0	
0845	0.40	2.00	0.04	7.11	10.59	19.97	5.980	2.9	1.70	-234.7	
0853	0.28	2.28	0.04	7.06	11.20	19.99	5.994	2.9	0.65	-251.4	
0859	0.22	2.50	0.04	7.08	10.41	20.08	5.995	2.9	0.99	-220.9	
0906	0.25	2.75	0.04	7.06	10.46	20.04	5.991	3.0	0.85	-229.6	
0912	0.25	3.00	0.04	7.06	10.69	20.04	5.989	3.3	0.66	-228.5	
0925 0933	0.25 0.50	3.25	0.02	7.08	9.10 9.43	20.06 19.95	6.009	3.0	0.86	-169.9 -199.7	
0933	0.30	4.05	0.05	7.07	9.43	19.93	5.985	3.0	0.56	-199.7	
0945	0.20	4.25	0.03	7.07	9.16	19.92	5.980	3.2	0.64	-189.3	
0952	0.25	4.50	0.04	7.07	8.58	19.97	5.990	3.2	0.58	-188.8	
1002	0.50	5.00	0.08	7.08	8.00	20.09	5.996	3.2	0.68	-175.4	
1008	0.20	5.20	0.03	7.08	7.86	20.16	6.016	3.1	0.57	-172.4	
1018	0.30	5.50	0.03	7.08	7.74	20.28	6.017	3.1	0.57	-176.4	
1025	0.25	5.75	0.04	7.08	10.38	20.30	6.018	2.9	0.57	-308.3	
1032	0.25	6.00	0.04	7.08	10.44	20.35	6.010	2.9	0.59	-297.3	
1040	0.25	6.25	0.04	7.08	10.76	20.28	6.021	2.9	0.69	-273.4	
1058	0.75	7.00	0.04	7.08	11.57	20.12	6.010	2.8	0.62	-272.8	
1109	0.50	7.50	0.05	7.10	11.07	20.31	6.006	2.9	0.76	-255.4	
1125	0.75	8.25	0.05	7.09	10.70	20.45	6.018	2.8	0.57	-265.7	
1137	0.50	8.75	0.04	7.11	11.43	20.63	6.028	2.9	0.57	-269.0	
1258	0.25	9.00	0.04	7.04	9.88	19.89	5.971	5.1	0.59	-306.7	
1305	0.25	9.25	0.04	7.05	9.02	20.51	6.029	2.6	0.57	-274.4	
1311	0.25	9.11	0.04	7.06	8.97	20.48	6.042	2.4	0.59	-269.4	1.004
WELL CAPACITY (Gallons Per Foot): 0.75" = 0.02; 1" = 0.04; 1.25" = 0.06; 2" = 0.16; 3" = 0.37; 4" = 0.65; 5" = 1.02; 6" = 1.47; 12" = 5.88  TUBING INSIDE DIA. CAPACITY (Gal./Ft.): 1/8" = 0.0006; 3/16" = 0.0014; 1/4" = 0.0026; 5/16" = 0.004; 3/8" = 0.006; 1/2" = 0.010; 5/8" = 0.016  BTOC = Below top of casing – feet below top of casing which includes above grade riser											
	EQUIPMENT CO			P = Bladder F			Submersible Pu	mp; <b>PP</b> = F	Peristaltic Pum	np; <b>O</b> = Other	(Specify)

	SAMPLING DATA  SAMPLED BY (PRINT) / AFFILIATION: SAMPLER(S) SIGNATURE(S):												
	BY (PRINT) / A ne Jaynes/P				NATURE(S):		SAMPLING INITIATED AT: 1321	SAMPLIN ENDED	NG AT: 1346				
PUMP OR DEPTH IN	TUBING WELL (feet): 3	2.25		TUBING MATERIAL CODE:	Teflon-lined PE		FILTERED: Yes/ <b>SM 450</b> 0 n Equipment Type: Syri		SIZE: <u>0.45</u> μm				
FIELD DE	CONTAMINATIO	ON: PU	MP Y	No T	UBING Y <b>No (rep</b>	laced)	DUPLICATE:	No					
SAM	IPLE CONTAINE	R SPECIFIC	ATION	SAM	IPLE PRESERVATION		INTENDED	SAMPLING	SAMPLE PUMP				
SAMPLE ID CODE	# CONTAINERS	MATERIAL CODE	VOLUME	PRESERVATIVE USED	TOTAL VOL ADDED IN FIELD (mL)	FINAL pH	ANALYSIS AND/OR METHOD	EQUIPMENT CODE	FLOW RATE (mL per minute)				
MW- 115B	1	PE	250mL	HNO3		6010B TAL Metals/7470A Hg	APP	125					
MW- 115B	1	PE	125mL				3500 FE/ 9040B pH	APP	125				
MW- 115B	1	PE	250mL			6010B Dissolved Silica	APP						
MW- 115B	1	PE	125mL				9056A_28D Chloride & Sulfate	APP	63				
MW- 115B	1	AG	125mL				SM 5310 DOC	APP	125				
MW- 115B	2	PE	250mL	NaOH Zinc Acetate		1	SM4500 Sulfide	APP	Field-Filtered				
MW- 115B	1	PE	500mL				2540C TDS	APP					
MW- 115B	1	PE	250mL				2320B Alkalinity	APP	83				
MW- 115B	1	AG	125mL	HCI			SM5310 TOC	APP					
REMARKS: Tubing—in-Screen-Interval purge method used. Unable to stabilize pH, Per Jim, ok to collect sample. Purge water clear brown. Sample collection times recorded incorrectly and therefore unable to calculate mL/min for some of the samples.													
	MATERIAL CODES: AG = Amber Glass; CG = Clear Glass; PE = Polyethylene; PP = Polypropylene; S = Silicone; T = Teflon; O = Other (Specify)  SAMPLING EQUIPMENT CODES: APP = After Peristaltic Pump; B = Bailer; BP = Bladder Pump; ESP = Electric Submersible Pump; RFPP = Reverse Flow Peristaltic Pump; SM = Straw Method (Tubing Gravity Drain); O = Other (Specify)												

NOTES: Stabilization Criteria for Range of Variation of Last Three Consecutive Readings:-pH: ± 0.1 unit Specific Conductance: ± 5% Dissolved Oxygen: all readings ≤ 10% saturation; optionally, ± 0.2 mg/L Turbidity: all readings ≤ 10 NTU; or ± 10%

			GR	OUND	WATE	ER SAN	ИPLIN	IG I	LOG				
SITE NAME: LC	P Chemical Site	•			SI <sup>-</sup>	TE OCATION: Bru	nswick, GA						
	: MW-115C			SAMPLE	ID: MW-115		,			DATE:	11/27/1	2	
					PURG	SING DA	TA						
WELL	D (inches), 2	TUBING			L SCREEN	INTERVAL			PTH (btoc) (feet): 9.4			E PUMP TY	/PE
	R (inches): 2		TER (inches): 1/-	feet	,				,		OR BA	AILER: PP	
	LUME PURGE: it if applicable)	1 WELL VO	LUME = (TOTAI	- WELL DEP	TH – STA	TIC DEPTH T	O WATER)	X \	WELL CAPACI	ITY			
	,	IIDGE: 1 EOI	= ( JIPMENT VOL. =	/TURING C	feet –	X TUBI		) X (	0.16 gall LOW CELL VC	lons/foot	=		gallons
	it if applicable)			,				,		COIVIE			
INITIAI DI	JMP OR TUBIN		( 0.0026 gallo			+ 0.13 gal		25 g:	allons PURGING		1-	TOTAL VOL	LIME
	WELL (feet bto		DEPTH IN W	ELL (feet bto			D AT: 104	3	ENDED AT:	1254			allons): 1.75
PURGED (gallons) PURGED (gallons) RATE (feet btoc) PURGED (standard units) (standard units) (oC) (mS/cm) (mS/cm) (oC) (mS/cm) (NTUs) (mV) (standard (mV) (standard units) (standard units) (oC) (mS/cm) (mS/cm) (mV) (standard (mV) (standard units) (mV) (standard unit													
1058	0.45	0.45	0.03	10.05	10.3	21.88	52.29		4.1	-2.	.24	-206.0	)
1103	0.13	0.58	0.03	10.10	10.3	21.91	52.35		3.9	-2.	.44	-207.2	2
1108	0.17	0.75	0.03	10.10	10.4	21.78	52.39		3.6	-2.	.50	-214.6	6
1116	0.25	1.00	0.03	10.10	10.5	21.88	52.33		4.0	-2.	.52	-215.9	9
1237	0.25	1.25	0.03	9.25	10.5	22.52	52.50		2.9	-2.	.53	-273.6	6
1244	0.25	1.50	0.04	9.95	10.5	22.64	52.51		3.1			-231.0	
1252	0.25	1.75	0.03	10.05	10.4	22.59	52.46		2.5		.47	-284.4	
TUBING IN		PACITY (Gal./	<b>0.75"</b> = 0.02; Ft.): <b>1/8"</b> = 0.00 low top of casing	06; <b>3/16</b> "	<b>1.25</b> " = 0.06 = 0.0014; es above gra	<b>1/4"</b> = 0.002		).37; ' = 0.00		<b>5"</b> = 1.02 0.006;		" = 1.47; = 0.010;	<b>12</b> " = 5.88 <b>5/8</b> " = 0.016
PURGING	EQUIPMENT C	ODES: B	= Bailer; BF	P = Bladder P	- 17	SP = Electric		e Pump	p; <b>PP</b> = Pe	eristaltic	Pump;	<b>O</b> = O	ther (Specify)
SAMPLED	BY (PRINT) / A	AFFILIATION:	I s	AMPLER(S)		LING DA	IA						
	ohnson/Pa			Mari	_	alman			SAMPLING INITIATED A	T: 1301		SAMPLIN ENDED A	
PUMP OR DEPTH IN	TUBING WELL (feet): 4	4.25		UBING IATERIAL CO			FI		ILTERED: Yes Equipment Ty			de FILTER	SIZE: <u>0.45</u> μm
FIELD DE	CONTAMINATION	ON: PUM	IP Y <b>No</b>	TUBING	Y No	(replaced)		DUPLICATE:		N	0		
						RESERVATIO			INTENDE			MPLING JIPMENT	SAMPLE PUMP FLOW RATE
SAMPLE ID CODE	# CONTAINERS	MATERIAL CODE	VOLUME P	RESERVATI USED		TOTAL VOL D IN FIELD (r	nL) FIN		ANALYSIS AI METHO			CODE	(mL per minute)
MW- 115C	1	PE	250mL	HNO3				i	6010B T Metals/7470		,	APP	125
MW- 115C	1	PE	125mL						3500 FE/ 9 pH		,	APP	125
MW-	1	PE	250mL				<u> </u>	_	6010B Diss	solved		APP	125

				rance	- Comsein				
	R TUBING N WELL (feet): 4	4.25		TUBING MATERIAL CODE:	Teflon-lined PE		FILTERED: Yes/ <b>SM 450</b> in Equipment Type: Syri		SIZE: <u>0.45</u> μm
FIELD DE	CONTAMINATIO	ON: PU	MP Y	No T	UBING Y No (rep	placed)	DUPLICATE:	No	
SAM	IPLE CONTAINE	R SPECIFIC	CATION	SAM	IPLE PRESERVATION		INTENDED	SAMPLING	SAMPLE PUMP
SAMPLE ID CODE	# CONTAINERS	MATERIAL CODE	VOLUME	PRESERVATIVE USED	TOTAL VOL ADDED IN FIELD (mL)	FINAL pH	ANALYSIS AND/OR METHOD	EQUIPMENT CODE	FLOW RATE (mL per minute)
MW- 115C	1	PE	250mL	HNO3			6010B TAL Metals/7470A Hg	APP	125
MW- 115C	1	PE	125mL				3500 FE/ 9040B pH	APP	125
MW- 115C	1	PE	250mL				6010B Dissolved Silica	APP	125
MW- 115C	1	PE	125mL				9056A_28D Chloride & Sulfate	APP	125
MW- 115C	1	AG	125mL				SM 5310 DOC	APP	63
MW- 115C	2	PE	250mL	NaOH Zinc Acetate			SM4500 Sulfide	APP	Field-Filtered
MW- 115C	1	PE	500mL				2540C TDS	APP	125
MW- 115C	1	PE	250mL				2320B Alkalinity	APP	83
MW-	1	AG	125mL	HCI			SM5310 TOC	APP	125

REMARKS: Per SOP, parameters stable for three readings before sampling. Tubing-in-Screen-Interval purge method used. Turbidity was too low for the meter to read and negative values were recorded; meter calibration was verified between readings. Pump shut off several times during purge due to trying to achieve low flow rate and reduce drawdown.

MATERIAL CODES: **AG** = Amber Glass; **CG** = Clear Glass; PE = Polyethylene; **PP** = Polypropylene; **S** = Silicone; **T** = Teflon; **O** = Other (Specify)

SAMPLING EQUIPMENT CODES: **BP** = Bladder Pump; **ESP** = Electric Submersible Pump; **APP** = After Peristaltic Pump; B = Bailer; **RFPP** = Reverse Flow Peristaltic Pump; **SM** = Straw Method (Tubing Gravity Drain); O = Other (Specify)

SITE	NAME: LCP Chemical Site LOCATION: Brunswick, GA												
	: MW-519A			SAMPLE ID:			HSWICK, GA		DATE:	11/28/1	12		
					PURGI	NG DA	TA						
	R (inches): 2		ER (inches): 1	/4 (btoc) D feet	CREEN IN EPTH: 32.	TERVAL 3 feet to 37	STATIC TO WAT	DEPTH (btoc) TER (feet): 7.35			E PUMP TY AILER: PP	/PE	
	LUME PURGE: it if applicable)	1 WELL VOL	UME = (TOTA = (	AL WELL DEPTH		C DEPTH T	,		CITY allons/foot	: =		gallons	
	NT VOLUME PU it if applicable)			= (TUBING CAPA ons/foot X 38.8			NG LENGTH)	+ FLOW CELL V					
	JMP OR TUBING WELL (feet btoo		_	P OR TUBING VELL (feet btoc):	34.8	PURGIN INITIATE	G ED AT: 1418	PURGING ENDED AT	: 1515		TOTAL VOL PURGED (g	LUME gallons): 1.5	
TIME	VOLUME PURGED (gallons)	CUMUL. VOLUME PURGED (gallons)	PURGE RATE (gpm)		pH tandard units)	TEMP. (°C)	SP COND. ( mS/cm)	DISSOLVED OXYGEN (% saturation	TURI	BIDITY TUs)	ORP (mV)	,	
1443	0.50	0.50	0.02		5.89	20.08	7.800	8.2		.44	-20.9		
1450 1458	0.25 0.25	0.75 1.00	0.04		5.78 5.73	20.08	7.834 7.871	6.6 5.6		.05	25.5 24.9		
1505	0.25	1.00	0.03		5.73	20.49	7.901	5.6		.43	27.3		
1513	0.25	1.50	0.03		5.72	20.65	7.925	5.2		.88	26.4		
TUBING IN BTOC = E	WELL CAPACITY (Gallons Per Foot): 0.75" = 0.02; 1" = 0.04; 1.25" = 0.06; 2" = 0.16; 3" = 0.37; 4" = 0.65; 5" = 1.02; 6" = 1.47; 12" = 5.88  TUBING INSIDE DIA. CAPACITY (Gal./Ft.): 1/8" = 0.0006; 3/16" = 0.0014; 1/4" = 0.0026; 5/16" = 0.004; 3/8" = 0.006; 1/2" = 0.010; 5/8" = 0.016  BTOC = Below top of casing – feet below top of casing which includes above grade riser												
PURGING	EQUIPMENT C	ODES: B	= Bailer; B	SP = Bladder Pum	•			ump; PP =	Peristaltic	Pump;	<b>O</b> = O	ther (Specify)	
SAMPLING DATA  SAMPLED BY (PRINT) / AFFILIATION: SAMPLER(S) SIGNATURE(S):													
Christin	ie Jaynes/P	arsons		Cla	rejen	(دو		SAMPLING INITIATED	AT: 1520		SAMPLIN ENDED A		
	TUBING WELL (feet): 34			TUBING MATERIAL CODE	E: Teflon-lii			D-FILTERED: Yetion Equipment ToUPLICATE	ype: Sy	ringe	de FILTER	SIZE: <u>0.45</u> μm	
	PLE CONTAINE					SERVATIO	,	INTEN			MPLING	SAMPLE PUMP	
SAMPLE	#	MATERIAL		PRESERVATIVE	TO	TAL VOL	FINAL	ANALVOIC	AND/OR	EQU	JIPMENT CODE	FLOW RATE (mL per minute)	
MW-	CONTAINERS 1	PE CODE	250mL	USED HNO3	ADDED	IN FIELD (r	nL) pH 	6010B	TAL		APP	83	
519A MW- 519A	1	PE	125mL					Metals/74 3500 FE/ pH	9040B		APP	125	
MW- 519A	1	PE	250mL					6010B Dis			APP	125	
MW- 519A	1	PE	125mL					9056A_ Chlorid Sulfa	_28D le &		APP	125	
MW- 519A	1	AG	125mL					SM 5310			APP	63	
MW- 519A	2	PE	250mL	NaOH Zinc Acetate				SM4500	Sulfide		APP	Field-Filtered	
MW- 519A	1	PE	500mL					2540C	TDS		APP	71	
MW- 519A	1	PE	250mL					2320B AI	kalinity		APP	250	
MW- 519A	MW- 1 AG 125mL HCI SM5310 TOC APP 63												
REMARKS: Per SOP, parameters stable for three readings before sampling. Tubing–in-Screen-Interval purge method used. Purge water clear brown, air/CO2 bubbles in tubing, slight odor noted.													
	MATERIAL CODES: AG = Amber Glass; CG = Clear Glass; PE = Polyethylene; PP = Polypropylene; S = Silicone; T = Teflon; O = Other (Specify)												
SAMPLIN	G EQUIPMENT		<b>PP</b> = After Per <b>FPP</b> = Reverse	istaltic Pump; e Flow Peristaltic I	<b>B</b> = Bailer Pump;		Bladder Pump Method (Tubin	; <b>ESP</b> = Elect g Gravity Drain);			Pump; Specify)		

			GF	ROUND	WATE	ER SAN	/IPLIN	١G	LOG				
SITE NAME: LC	P Chemical Site	)				TE DCATION: Bru	nswick. GA						
	MW-519B			SAMPLE I	D: MW-519		,			DATE:	11/27/1	2	
					PURC	SING DA	TA						
WELL		TUBIN	IG		SCREEN	INTERVAL	STA		EPTH (btoc)			E PUMP T	YPE
DIAMETER	R (inches): 2	DIAME	ETER (inches): 1	/4 (btoc) 47.55		12.55 feet to	TO V	VATE	R (feet): 9.4		OR BA	ILER: PP	
	LUME PURGE: t if applicable)	1 WELL VO	DLUME = (TOT)	AL WELL DEPT	H – STA	TIC DEPTH T	•		WELL CAPACI				
	NT VOLUME Po	URGE: 1 EQ	= ( UIPMENT VOL.	= (TUBING CA	eet – PACITY	X TUBII	NG LENGT	) X ГН) + F	FLOW CELL VO	ons/foot LUME	=		gallons
(0) 00	т п арриоавто)	=	= ( 0.0026 gal	ons/foot X 49.	5 feet) + (	0.13 gallons	= 0.26	gallo	ns				
	JMP OR TUBIN WELL (feet bto	-		P OR TUBING VELL (feet btoo	): 45.05	PURGING INITIATE	3 D AT: 075	55	PURGING ENDED AT:	0851		OTAL VOI PURGED (	LUME gallons): 2.26
TIME	VOLUME PURGED (gallons)	CUMUL. VOLUME PURGED (gallons)	PURGE RATE (gpm)	DEPTH TO WATER (feet btoc)	pH (standard units)	TEMP. (°C)	SP CON ( mS/cm		DISSOLVED OXYGEN (% saturation)		BIDITY (Us)	ORP (mV)	
0812	0.75	0.75	0.04	11.2	8.96	21.12	63.67		9.2	-2	.19	-220.	8
0821	0.35	1.10	0.04	11.8	8.92	21.32	63.55		9.5	-2	.20	-238.	4
0829	0.30	1.40	0.04	11.9	8.98	21.57	63.78		9.2	-2	.35	-304.	9
0835	0.30	1.70	0.05	12.05	9.11	21.75	64.50		7.4	-2	.38	-298.	6
0842	0.30	2.00	0.04	12.05	9.19	21.78	65.01		8.8	-2	.49	-287.	5
0850	0.26	2.26	0.03	12.13	9.22	21.85	65.42		8.1		.37	-327.	
TUBING IN		PACITY (Gal.	<b>0.75</b> " = 0.02; /Ft.): <b>1/8</b> " = 0.0 elow top of casin	0006; <b>3/16</b> " =	= 0.0014;	6; <b>2</b> " = 0.16 <b>1/4</b> " = 0.0026 ade riser		0.37; " = 0.0		<b>5"</b> = 1.0 .006;		' = 1.47; 0.010;	<b>12"</b> = 5.88 <b>5/8"</b> = 0.016
PURGING	EQUIPMENT (	ODES: I	<b>B</b> = Bailer; <b>E</b>	BP = Bladder Pι		SP = Electric		le Pun	np; <b>PP =</b> Pe	eristaltic	Pump;	<b>O</b> = 0	ther (Specify)
CAMPLED	BY (PRINT) / A	EEU IATION		SAMPLER(S) S		LING DA	TA		1		1		
	ohnson/Pa			2		celmou	~		SAMPLING INITIATED AT			SAMPLIN ENDED A	AT: 0927
PUMP OR DEPTH IN	TUBING WELL (feet): 4	5.05		TUBING MATERIAL CO			F		FILTERED: Yes/ n Equipment Tyl			de FILTER	SIZE: <u>0.45</u> μm
FIELD DEC	CONTAMINATIO	ON: PUI	MP Y No		TUBING	Y <b>No</b>	(replaced)	)	DUPLICATE:		N	0	
SAMPLE	PLE CONTAINE	R SPECIFIC	-	PRESERVATIV		RESERVATION		JAL .	INTENDE ANALYSIS AN	ND/OR	EQU	MPLING IPMENT	SAMPLE PUMP FLOW RATE
ID CODE	CONTAINERS	CODE	VOLUME	USED		D IN FIELD (n		H	METHO	D		ODE	(mL per minute)
MW- 519B	1	PE	250mL	HNO3			-		6010B T			APP	125
MW-	1	PE	125mL						3500 FE/ 9	040B	A	APP	125

	PUMP OR TUBING DEPTH IN WELL (feet): 45.05				Comsein				
		5.05		TUBING MATERIAL CODE:	: Teflon-lined PE		FILTERED: Yes/ <b>SM 450</b> 0 n Equipment Type: Syri		SIZE: <u>0.45</u> μm
FIELD DE	CONTAMINATIO	ON: PU	MP Y	No T	UBING Y <b>No (rep</b> l	laced)	DUPLICATE:	No	
SAN	MPLE CONTAINE	ER SPECIFIC	CATION	SAM	IPLE PRESERVATION		INTENDED	SAMPLING	SAMPLE PUMP
SAMPLE ID CODE	# CONTAINERS	MATERIAL CODE	VOLUME	PRESERVATIVE USED	TOTAL VOL ADDED IN FIELD (mL)	FINAL pH	ANALYSIS AND/OR METHOD	EQUIPMENT CODE	FLOW RATE (mL per minute)
MW- 519B	1	PE	250mL	HNO3			6010B TAL Metals/7470A Hg	APP	125
MW- 519B	1	PE	125mL				3500 FE/ 9040B pH	APP	125
MW- 519B	1	PE	250mL				6010B Dissolved Silica	APP	125
MW- 519B	1	PE	125mL				9056A_28D Chloride & Sulfate	APP	63
MW- 519B	1	AG	125mL				SM 5310 DOC	APP	125
MW- 519B	2	PE	250mL	NaOH Zinc Acetate			SM4500 Sulfide	APP	Field-Filtered
MW- 519B	1	PE	500mL				2540C TDS	APP	83
MW- 519B	1	PE	250mL				2320B Alkalinity	APP	83
MW- 519B	1	AG	125mL	HCI			SM5310 TOC	APP	125

Temarks: Per SOP, parameters stable for three readings before sampling. Tubing—in-Screen Interval purge method was used. Pump was set to lowest setting possible however, water levels continued to drop but less than 100mL/ min. Turbidity was too low for the meter to read and negative values were recorded; meter calibration was verified between readings.

MATERIAL CODES: **AG** = Amber Glass; **CG** = Clear Glass; **PE** = Polyethylene; **PP** = Polypropylene; **S** = Silicone; T = Teflon; O = Other (Specify) 

 APP = After Peristaltic Pump;
 B = Bailer;
 BP = Bladder Pump;
 ESP = Elect

 RFPP = Reverse Flow Peristaltic Pump;
 SM = Straw Method (Tubing Gravity Drain);

 **B** = Bailer; SAMPLING EQUIPMENT CODES: **ESP** = Electric Submersible Pump;

O = Other (Specify)

SITE NAME: LCP	Chemical Site				SIT	E CATION: Bru	ınswic	rk GA					
WELL NO:				SAMPLE ID:			anowic	ж, ол		DATE:	11/27/12		
						ING DA	TA						
WELL DIAMETER	(inches): 2	TUBIN	IG ETER (inches):	WELL S	CREEN II EPTH: 42	NTERVAL .55 feet to			DEPTH (btoc) ER (feet): 11.7			PUMP TY LER: PP	/PE
	UME PURGE: if applicable)	1 WELL VO		AL WELL DEPTH	- STAT	TIC DEPTH 1	TO WA	,					
EQUIPMEN	T VOLUME PL	JRGE: 1 EQ	= ( UIPMENT VOL	fee TUBING CAPA:=		X TUB	ING L	feet) X ENGTH) +	0.16 gal	llons/foot DLUME	=		gallons
(only fill out	if applicable)	=	= ( 0.0026 ga	lons/foot X 49.5	feet) +	0.13 gall		•	gallons				
_	MP OR TUBING VELL (feet btoo		_	MP OR TUBING WELL (feet btoc):	42.55	PURGIN INITIATI	_	: 0939	PURGING ENDED AT:	1014		OTAL VOL JRGED (g	UME allons): 1.1
TIME	VOLUME PURGED (gallons)	CUMUL. VOLUME PURGED (gallons)			pH tandard units)	TEMP. (°C)		COND. mS/cm)	DISSOLVED OXYGEN (% saturation)	(NIT	BIDITY 'Us)	ORP (mV)	SP Gravity (sg)
0951	0.45	0.45	0.04	11.70	9.0	22.10	6	55.13	6.3	-2	.44	-323.6	6
1000	0.30	0.75	0.03	11.95	8.9	22.19	6	65.11	5.6	-2	.54	-299.2	2
1011	0.35	1.10	0.03		8.87	22.67		65.12	5.5		.53	-271.0	Not Recorded
<b>TUBING INS</b>		PACITY (Gal.	/Ft.): <b>1/8"</b> = 0	1" = 0.04; 1.2 .0006; 3/16" = 0 ng which includes	.0014;	; <b>2</b> " = 0.1 <b>1/4</b> " = 0.002 de riser		<b>3</b> " = 0.37; <b>5/16</b> " = 0.		<b>5</b> " = 1.02 0.006;	2; <b>6"</b> : <b>1/2"</b> = (	= 1.47; ).010;	<b>12</b> " = 5.88 <b>5/8</b> " = 0.016
	QUIPMENT C		-	<b>BP</b> = Bladder Pum		SP = Electric	Subm	nersible Pu	mp; <b>PP</b> = P	eristaltic	Pump;	<b>O</b> = O	ther (Specify)
						ING DA	<b>ATA</b>	ı					
	Y (PRINT) / A Mutch and			SAMPLER(S) SIG	NATURE	(S):			SAMPLING INITIATED A	T: 1033		SAMPLIN ENDED A	
PUMP OR T DEPTH IN V	UBING VELL (feet): 47	7.55		TUBING MATERIAL CODE	: Teflon-l	lined PE			-FILTERED: Yes			FILTER	SIZE: <u>0.45</u> μm
FIELD DEC	ONTAMINATIO	N: PUI	MP Y N	lo	TUBING	Y No	(repl	aced)	DUPLICATE	:	Y N	l	
SAMP	LE CONTAINE	R SPECIFIC	ATION	SAI	MPLE PR	ESERVATIO	N		INTEND			PLING	SAMPLE PUMP
	# CONTAINERS	MATERIAL CODE	VOLUME	PRESERVATIVE USED		OTAL VOL ) IN FIELD (	mL)	FINAL pH	ANALYSIS A METHO		CC	PMENT DDE	FLOW RATE (mL per minute)
MW- 519B TOP	1	PE	250mL	HNO3					6010B 7 Metals/747		A	PP	
MW- 519B TOP	1	PE	125mL						3500 FE/ 9 pH		A	PP	
MW- 519B TOP	1	PE	250mL						6010B Disa Silica		A	PP	
MW- 519B TOP	1	PE	125mL						9056A_2 Chloride Sulfat	e &	А	PP	
MW- 519B TOP	1	AG	125mL						SM 5310		А	PP	
MW- 519B TOP	2	PE	250mL	NaOH Zinc Acetate					SM4500 S	Sulfide	A	PP	Field-Filtered
MW- 519B TOP	1	PE	500mL						2540C T	rds	A	PP	
MW- 519B TOP	1	PE	250mL						2320B Alk	alinity	А	PP	
MW- 519B TOP	1	AG	125mL	HCI					SM5310	тос	A	PP	
REMARKS:				for three read David with N									ed and
MATERIAL		AG = Amber			PE = Polye				lene; $\mathbf{S} = \text{Silic}$				ther (Specify)
				•	<b>B</b> = Baile			,	ESP = Elect				

SITE NAME: LC	P Chemical Site						SIT	E CATION: Bru	ınswic	ck. GA					
WELL NO:					SA	MPLE ID:		071110111101111		on, <b>o</b> , .		DATE	: 11/27/	12	
							PURG	ING DA	TA						
WELL DIAMETER	R (inches): 4		UBING NAMETE	ER (inches): 1	/4			NTERVAL feet to 47 f	eet		DEPTH (btd ER (feet): 9	,		GE PUMP T	YPE
	LUME PURGE: it if applicable)	1 WEL	L VOLU	JME = (TOTA	AL WEL	L DEPTH	- STAT	TIC DEPTH 1	TO W	ATER) X	WELL CA	PACITY			
EQUIPME	NT VOLUME PU	JRGE: 1	1 EQUIF	= ( PMENT VOL.	= (TUB	feet		X TUB	ING I	feet) X FNGTH) +	0.16 FLOW CE	gallons/fo			gallons
	it if applicable)			0.0026 gallo	`					,	gallons		_		
	JMP OR TUBIN		5	FINAL PUM DEPTH IN V			45.5	PURGIN		T: 0810	PURGI ENDEI	NG D AT: 0937		TOTAL VOI	UME gallons): 1.25
		CUM	ЛUI		DEF	TH		I			1		l .		, ,
TIME	VOLUME PURGED (gallons)	VOLI PUR (galle	UME GED	PURGE RATE (gpm)	WAT (fe	TER (st et ι	pH andard units)	TEMP. (°C)	_	COND. mS/cm)	DISSOLY OXYGE (% satura	N I	IRBIDITY (NTUs)	ORP (mV)	
0837	0.25	0.2	25	0.01	9.5		6.65	18.79	4	43.14	3.7			-87.4	ļ
0852	0.25	0.5	50	0.02	9.5		6.65	19.18	4	43.05	3.0			-104.	1
0906	0.25	0.7		0.02	9.5		6.65	19.36		43.05	2.6			-112.	
0922         0.25         1.00         0.02         9.49         6.66         19.76         43.03         2.3          -119.5           0936         0.25         1.25         0.02         9.52         6.66         20.23         43.01         2.4          -123.5         1.022															
0936 0.25 1.25 0.02 9.52 6.66 20.23 43.01 2.4123.5 1.022															
WELL CAPACITY (Callogs Por East): 0.75" = 0.02: 1" = 0.04: 1.25" = 0.06: 2" = 0.16: 2" = 0.27: 4" = 0.65: 5" = 1.02: 6" = 1.47: 1.2" = 5.99															
TUBING IN	WELL CAPACITY (Gallons Per Foot): 0.75" = 0.02; 1" = 0.04; 1.25" = 0.06; 2" = 0.16; 3" = 0.37; 4" = 0.65; 5" = 1.02; 6" = 1.47; 12" = 5.88  TUBING INSIDE DIA. CAPACITY (Gall/Ft.): 1/8" = 0.0006; 3/16" = 0.0014; 1/4" = 0.0026; 5/16" = 0.004; 3/8" = 0.006; 1/2" = 0.010; 5/8" = 0.016  BTOC = Below top of casing – feet below top of casing which includes above grade riser														
PURGING	EQUIPMENT C	ODES:	B =	Bailer; E	BP = Bla	dder Pump		SP = Electric			ımp; P	P = Peristal	tic Pump	; <b>O</b> = O	ther (Specify)
CAMPLED	BY (PRINT) / A		ION.		CAMDI	ER(S) SIG		LING DA	ATA	<u> </u>	1			1	
	ie Jaynes/P					200		100)			SAMPL INITIAT	NG ED AT: 09	50	SAMPLIN ENDED A	
PUMP OR					TUBING		. T-0	line of DE						ide FILTER	SIZE: <u>0.45</u> μm
	WELL (feet): 4: CONTAMINATION		PUMP			IAL CODE	: retion-		(repl	laced)	ion Equipme DUPLIC			No .	
	PLE CONTAINE							ESERVATIO			1	ENDED	1	AMPLING	SAMPLE PUMP
SAMPLE ID CODE	# CONTAINERS	MATER CODE	RIAL			RVATIVE SED	Т	OTAL VOL D IN FIELD (		FINAL pH	ANALY	SIS AND/O ETHOD	R EQ	UIPMENT CODE	FLOW RATE (mL per minute)
SW-1	1	PE		250mL	Н	VO3						0B TAL /7470A H	g	APP	83
SW-1	1	PE		125mL							3500	FE/ 9040E pH	3	APP	42
SW-1	1	PE		250mL							I	Dissolve Silica	d	APP	50
SW-1	1	PE		125mL							905 Ch	6A_28D oride & ulfate		APP	63
SW-1	1	AG	ì	125mL							1	310 DOC		APP	63
SW-1	2	PE		250mL		aOH Acetate					SM45	00 Sulfide	•	APP	Field-Filtered
SW-1	1	PE		500mL							254	OC TDS		APP	55
SW-1	1	PE		250mL							_	8 Alkalinity	,	APP	42
SW-1	SW-1 1 AG 125mL HCI SM5310 TOC APP 63  REMARKS: Per SOP, parameters stable for three readings before sampling. Tubing—in-Screen-Interval purge method used.														
	s: Per SOP, sy was too lo														
MATERIA			mber Gl		Clear G			ethylene;		Polypropy		Silicone;	T = Tefl		Other (Specify)
SAMPLIN	G EQUIPMENT	CODES		<b>P</b> = After Per <b>PP</b> = Reverse			<b>B</b> = Bail Pump;	er; BP = SM = Straw		der Pump; od (Tubing		Electric Sulain); <b>O</b>	omersible = Other (		

NOTES: Stabilization Criteria for Range of Variation of Last Three Consecutive Readings:-pH:  $\pm$  0.1 unit Specific Conductance:  $\pm$  5% Dissolved Oxygen: all readings  $\leq$  10% saturation; optionally,  $\pm$  0.2 mg/L Turbidity: all readings  $\leq$  10 NTU; or  $\pm$  10%

# APPENDIX D. SPARGING FLOW RATES

		Pressure		Pressure		Temp		Corrected CO2	
Date	Time	(psi)	Flow (CFM)	Factor	CO2 Temp (F)	Factor	Air SCFM	SCFM	Log
10/29/2012	9:37	10	6	0.60	62.00	1.00	10.0	8.1	Start
10/29/2012	9:43	8	6	0.65	62.00	1.00	9.2	7.5	
10/29/2012	9:45	12.5	6	0.54	62.00	1.00	11.1	9.0	
10/29/2012	9:50	17.5	5.5	0.46	62.00	1.00	12.0	9.7	
10/29/2012	10:03	17	5.5	0.46	61.80	1.00	11.8	9.6	Ramping Up
10/29/2012	10:27	18	8	0.45	61.80	1.00	17.7	14.4	Period
10/29/2012	10:30	18.5	9	0.44	61.80	1.00	20.3	16.4	
10/29/2012	10:32	18.8	11	0.44	61.80	1.00	25.0	20.2	
10/29/2012	10:35	19	11	0.44	61.80	1.00	25.1	20.4	
10/29/2012	10:36	19	11	0.44	61.80	1.00	25.1	20.4	Steady
10/29/2012	10:55	19	11	0.44	61.80	1.00	25.1	20.4	state run
10/29/2012	10:56	20	16	0.42	61.20	1.00	37.7	30.5	
10/29/2012	10:59	21	19	0.41	61.20	1.00	46.0	37.3	Ramping Up
10/29/2012	11:02	21.5	20	0.41	61.20	1.00	49.1	39.8	Period
10/29/2012	11:05	22	21	0.40	61.20	1.00	52.3	42.4	
10/29/2012	13:05	21.8	21.8	0.40	49.20	0.98	55.3	44.8	
10/29/2012	15:14	21.8	21.8	0.40	49.20	0.98	55.3	44.8	Shut down
10/30/2012	10:45	22.5	10.5	0.40	58.80	1.00	26.6	21.6	Start
10/30/2012	10:56	24.5	15	0.38	58.80	1.00	40.1	32.5	
10/30/2012	11:18	23.5	13	0.38	60.00	1.00	33.8	27.4	
10/30/2012	11:35	22.5	13	0.40	58.80	1.00	33.0	26.7	
10/30/2012	12:02	22	13.2	0.40	58.40	1.00	33.1	26.8	
10/30/2012	12:50	21.5	13.4	0.41	59.40	1.00	33.0	26.8	
10/30/2012	14:00	20.6	13.5	0.42	59.30	1.00	32.5	26.3	]
10/30/2012	15:18	21.5	20	0.41	60.00	1.00	49.3	39.9	ramp up
10/30/2012	15:31	22	19.8	0.40	60.00	1.00	49.4	40.0	·
10/30/2012	16:16	22	19.5	0.40	55.00	0.99	49.2	39.8	
10/30/2012	17:02	21.5	19.5	0.41	53.90	0.99	48.6	39.4	
10/30/2012	18:28	21.5	20	0.41	39.70	0.96	51.3	41.5	
10/30/2012	18:31	21.5	20	0.41	39.70	0.96	51.3	41.5	shutdown

		Pressure		Pressure		Temp		Corrected CO2	
Date	Time	(psi)	Flow (CFM)	Factor	CO2 Temp (F)	Factor	Air SCFM	SCFM	Log
10/31/2012	11:05	22	7.5	0.40	71.70	1.02	18.3	14.8	Start
10/31/2012	11:07	23.8	10	0.38	70.80	1.02	25.7	20.8	
10/31/2012	11:09	24.2	12	0.38	69.00	1.02	31.2	25.3	
10/31/2012	11:12	24	12.5	0.38	67.80	1.02	32.4	26.3	-
10/31/2012	11:18	23.5	13	0.38	66.00	1.01	33.4	27.1	Period
10/31/2012	11:20	23.8	13.8	0.38	65.60	1.01	35.8	29.0	Pe
10/31/2012	11:29	23.5	13.5	0.38	63.80	1.01	34.8	28.2	å
10/31/2012	11:31	24	14.2	0.38	63.80	1.01	37.1	30.1	
10/31/2012	11:39	24	14.5	0.38	63.60	1.01	37.9	30.7	ř
10/31/2012	11:41	24.4	15	0.38	63.50	1.01	39.6	32.1	Ramping
10/31/2012	11:48	24.4	15.2	0.38	62.70	1.01	40.2	32.6	<b>62</b>
10/31/2012	11:50	24.6	16	0.37	62.60	1.01	42.6	34.5	
10/31/2012	12:01	24.6	16	0.37	62.00	1.00	42.6	34.5	
10/31/2012	12:36	24.2	16	0.38	62.90	1.01	42.1	34.1	
10/31/2012	12:43	24.2	16.2	0.38	62.90	1.01	42.6	34.5	
10/31/2012	12:46	24.25	16.5	0.38	63.10	1.01	43.5	35.2	
10/31/2012	12:48	24.4	17	0.38	63.10	1.01	44.9	36.4	
10/31/2012	12:55	24.5	17.8	0.38	62.90	1.01	47.2	38.2	
10/31/2012	14:00	23.5	17.8	0.38	64.20	1.01	45.9	37.2	
10/31/2012	14:18	23.5	18.4	0.38	65.60	1.01	47.3	38.3	
10/31/2012	14:21	23.7	19	0.38	65.50	1.01	49.1	39.8	
10/31/2012	14:23	23.7	19.4	0.38	65.40	1.01	50.2	40.6	
10/31/2012	14:25	24	20	0.38	65.30	1.01	52.1	42.2	Ramping Up
10/31/2012	14:33	24.5	21.6	0.38	62.20	1.00	57.4	46.5	
10/31/2012	14:48	24.5	22.1	0.38	57.20	0.99	59.3	48.0	
10/31/2012	15:30	24.2	22.5	0.38	50.30	0.98	60.7	49.1	
10/31/2012	15:45	24	22.5	0.38	50.90	0.98	60.3	48.8	Ramping
10/31/2012	15:47	24	22	0.38	50.90	0.98	58.9	47.7	Down
10/31/2012	15:53	23.6	22.6	0.38	51.00	0.98	59.9	48.5	
10/31/2012	15:57	23.2	22	0.39	54.60	0.99	57.3	46.4	
10/31/2012	17:15	22.2	22.5	0.40	55.00	0.99	57.0	46.2	
10/31/2012	18:20	21.9	22.6	0.40	44.20	0.97	58.0	47.0	
10/31/2012	18:30	21.9	22.6	0.40	41.50	0.96	58.3	47.3	Shutdown

		Pressure		Pressure		Temp		Corrected CO2	
Date	Time	(psi)	Flow (CFM)	Factor	CO2 Temp (F)	Factor	Air SCFM	SCFM	Log
11/1/2012	8:33	21	10.8	0.41	47.40	0.98	26.9	21.8	Start
11/1/2012	8:35	21.3	13	0.41	46.50	0.97	32.7	26.5	- 75
11/1/2012	8:37	21.6	14.3	0.40	45.60	0.97	36.3	29.4	Period
11/1/2012	8:39	22.8	15	0.39	44.90	0.97	39.4	31.9	g.
11/1/2012	8:52	21.5	15	0.41	44.60	0.97	38.1	30.8	υp
11/1/2012	8:53	22.6	17.2	0.39	44.70	0.97	45.0	36.4	
11/1/2012	8:57	23.2	19.6	0.39	45.10	0.97	52.0	42.1	Ramping
11/1/2012	9:00	23.9	21	0.38	45.50	0.97	56.7	45.9	l am
11/1/2012	9:02	24.1	21.9	0.38	45.50	0.97	59.5	48.2	E
11/1/2012	9:13	24.5	21.8	0.38	42.00	0.97	60.2	48.8	
11/1/2012	9:15	24.8	21.7	0.38	41.30	0.96	59.1	47.9	
11/1/2012	9:40	25	20.9	0.38	46.00	0.97	56.7	45.9	air=49F
11/1/2012	10:00	24.9	20.8	0.37	49.20	0.98	57.2	46.3	
11/1/2012	10:37	24.5	20.6	0.38	47.60	0.98	56.3	45.6	
11/1/2012	10:39	24.6	21	0.37	47.60	0.98	57.5	46.6	
11/1/2012	11:02	24.5	20.9	0.38	49.20	0.98	56.9	46.1	
11/1/2012	11:40	24.4	20.9	0.38	51.00	0.98	56.6	45.8	
11/1/2012	12:20	24	21	0.38	52.80	0.99	56.1	45.4	
11/1/2012	12:21	24.2	22	0.38	52.80	0.99	59.0	47.8	
11/1/2012	13:00	24	22	0.38	48.70	0.98	59.2	48.0	
11/1/2012	13:04	24.1	23	0.38	48.70	0.98	62.1	50.3	
11/1/2012	13:25	23.6	23	0.38	45.30	0.97	61.7	50.0	
11/1/2012	14:30	23	23	0.39	55.40	0.99	59.5	48.2	
11/1/2012	15:15	22.7	23.1	0.39	55.20	0.99	59.3	48.0	
11/1/2012	15:25	23.5	27	0.38	54.50	0.99	70.9	57.4	
11/1/2012	15:30	24	29.5	0.38	51.20	0.98	79.0	64.0	
11/1/2012	16:00	24.5	29.6	0.38	22.60	0.93	85.1	68.9	Adjusted
11/1/2012	16:05	24.3	28.8	0.38	23.10	0.93	82.2	66.6	main PrReg
11/1/2012	17:50	24	28.8	0.38	1.70	0.89	85.4	69.2	
11/1/2012	18:00	23.5	27.5	0.38	-5.70	0.87	81.8	66.3	
11/1/2012	18:10	24.8	28.5	0.37	-10.20	0.87	88.5	71.7	
11/1/2012	18:15	24.8	28.5	0.37	-10.00	0.87	88.5	71.7	shutdown

		Pressure		Pressure		Temp		Corrected CO2	
Date	Time	(psi)	Flow (CFM)	Factor	CO2 Temp (F)	Factor	Air SCFM	SCFM	Log
11/2/2012	8:45	23	5.5	0.39	38.40	0.96	14.7	11.9	Start
11/2/2012	8:48	22	8.5	0.40	37.90	0.96	22.2	18.0	Up
11/2/2012	8:52	23	12.5	0.39	37.70	0.96	33.5	27.1	
11/2/2012	8:54	24	15.9	0.38	37.50	0.96	43.8	35.4	Ramping Period
11/2/2012	8:57	24.4	17	0.38	38.40	0.96	47.2	38.2	aml
11/2/2012	8:59	24.75	18.5	0.37	38.80	0.96	51.8	41.9	ě.
11/2/2012	9:14	24.9	18.5	0.37	38.60	0.96	52.0	42.1	
11/2/2012	9:28	25.1	18.5	0.37	53.00	0.99	50.8	41.1	
11/2/2012	9:35	25.25	18.5	0.37	50.90	0.98	51.2	41.4	
11/2/2012	9:42	25	18.1	0.37	51.40	0.98	49.7	40.3	
11/2/2012	10:06	25.25	18	0.37	56.40	0.99	49.3	39.9	
11/2/2012	10:07	25	17.5	0.37	56.10	0.99	47.6	38.6	
11/2/2012	10:46	25.1	17.4	0.37	63.10	1.01	46.8	37.9	
11/2/2012	11:38	25.25	17.4	0.37	68.50	1.02	46.5	37.7	
11/2/2012	11:39	25	16.4	0.37	68.50	1.02	43.6	35.3	
11/2/2012	12:50	24.5	16.5	0.38	71.20	1.02	43.1	34.9	
11/2/2012	13:48	24.5	16.5	0.38	71.00	1.02	43.1	34.9	
11/2/2012	13:50	24.5	16.9	0.38	71.00	1.02	44.1	35.7	
11/2/2012	15:00	24.5	18	0.38	70.70	1.02	47.0	38.1	
11/2/2012	15:15	24.5	17.5	0.38	72.30	1.02	45.6	36.9	
11/2/2012	16:05	24.5	18.6	0.38	71.90	1.02	48.5	39.3	
11/2/2012	16:55	24.5	18.6	0.38	69.90	1.02	48.7	39.4	
11/2/2012	16:57	24.6	19	0.37	69.60	1.02	49.9	40.4	
11/2/2012	17:40	24.6	19	0.37	64.90	1.01	50.3	40.8	
11/2/2012	17:46	24.6	20	0.37	64.90	1.01	53.0	42.9	
11/2/2012	17:52	24.7	20	0.37	63.60	1.01	53.2	43.1	
11/2/2012	18:00	24.7	20	0.37	63.30	1.01	53.3	43.1	
11/2/2012	18:01	24.7	20	0.37	63.30	1.01	53.3	43.1	Shut down

		Pressure		Pressure		Temp		Corrected CO2	
Date	Time	(psi)	Flow (CFM)	Factor	CO2 Temp (F)	Factor	Air SCFM	SCFM	Log
11/5/2012	11:22	24	5.5	0.38	78.40	1.04	14.0	11.3	Start
11/5/2012	11:24	21	5.5	0.41	78.40	1.04	12.9	10.4	70
11/5/2012	11:25	20	5.5	0.42	78.40	1.04	12.5	10.2	Period
11/5/2012	11:26	19.5	7	0.43	78.00	1.03	15.7	12.8	Pe
11/5/2012	11:29	20.6	10	0.42	76.40	1.03	23.3	18.9	٩
11/5/2012	11:31	21.2	13	0.41	76.00	1.03	30.8	24.9	
11/5/2012	11:34	22.4	15.4	0.40	75.70	1.03	37.7	30.6	pin
11/5/2012	11:36	23	17	0.39	75.50	1.03	42.3	34.3	Ramping
11/5/2012	11:38	23.5	18	0.38	75.30	1.03	45.4	36.8	<u> </u>
11/5/2012	11:41	23.9	19.5	0.38	75.00	1.03	49.8	40.3	
11/5/2012	12:15	23.9	19.8	0.39	61.50	1.00	50.6	41.0	air=59F
11/5/2012	12:40	23.9	19.9	0.38	59.70	1.00	51.7	41.9	
11/5/2012	13:15	23.4	20	0.39	57.30	0.99	52.1	42.2	
11/5/2012	14:00	23.2	20.5	0.39	55.00	0.99	53.4	43.2	
11/5/2012	14:45	22.4	20.2	0.40	69.20	1.02	50.1	40.6	
11/5/2012	14:49	22.6	21.3	0.39	69.20	1.02	53.1	43.0	ramp up
11/5/2012	14:52	22.8	22.5	0.39	54.80	0.99	58.0	47.0	ramp up
11/5/2012	14:54	23	23.75	0.39	54.10	0.99	61.6	49.9	ramp up
11/5/2012	15:03	23.4	24.75	0.39	46.50	0.97	65.9	53.3	air=66F
11/5/2012	15:07	23.5	25	0.38	44.70	0.97	66.9	54.2	ramp up
11/5/2012	15:15	23.5	25	0.38	37.50	0.96	67.9	55.0	see note
11/5/2012	15:28	23.8	25.1	0.38	36.60	0.96	68.8	55.8	
11/5/2012	16:05	23.6	25.5	0.38	24.40	0.93	71.3	57.8	
11/5/2012	16:06	23.2	24.3	0.39	24.80	0.93	67.2	54.4	ramp down
11/5/2012	16:46	23.2	24.5	0.39	22.60	0.93	68.1	55.1	]
11/5/2012	16:48	23.2	24.5	0.39	23.10	0.93	68.0	55.1	ramp down
11/5/2012	17:30	23.2	24.5	0.39	9.10	0.90	70.0	56.7	
11/5/2012	17:45	23.2	24.5	0.39	1.70	0.89	71.1	57.6	Shut down

		Pressure		Pressure		Temp		Corrected CO2	
Date	Time	(psi)	Flow (CFM)	Factor	CO2 Temp (F)	Factor	Air SCFM	SCFM	Log
11/6/2012	8:00			1.00		0.88	0.0	0.0	Start
11/6/2012	8:02	20	11	0.42	50.90	0.98	26.4	21.4	ramp up
11/6/2012	8:06	19.4	15	0.43	49.60	0.98	35.5	28.8	air temp
11/6/2012	8:10	20	16.5	0.42	48.70	0.98	39.8	32.2	55F Frost
11/6/2012	8:15	20.6	19	0.42	48.30	0.98	46.7	37.8	on CO2 GP
11/6/2012	8:24	20.8	21	0.41	47.40	0.98	52.0	42.1	line at
11/6/2012	8:28	21.2	21.4	0.41	45.30	0.97	53.8	43.6	0835hrs
11/6/2012	8:35	21.4	23	0.41	44.90	0.97	58.2	47.1	00331113
11/6/2012	8:50	22	23.3	0.40	39.20	0.96	60.6	49.1	stdy state
11/6/2012	8:55	22.4	25	0.40	36.60	0.96	66.1	53.5	ramp up
11/6/2012	9:01	22.4	25	0.41	33.00	0.95	64.8	52.5	]
11/6/2012	9:30	23	25	0.40	22.40	0.93	67.3	54.5	steady state
11/6/2012	10:06	23	25	0.39	29.30	0.94	68.1	55.2	air temp
11/6/2012	10:55	22.7	24.75	0.39	35.90	0.95	66.0	53.5	57 F
11/6/2012	11:41	22.7	24.75	0.39	47.10	0.98	64.6	52.3	] 3,.
11/6/2012	12:00	22.4	24.5	0.40	49.60	0.98	63.1	51.1	
11/6/2012	12:03	22.6	26	0.39	50.50	0.98	67.2	54.4	ramp up
11/6/2012	12:29	22.6	26	0.39	47.60	0.98	67.6	54.7	
11/6/2012	12:30	22.8	28	0.39	47.30	0.98	73.2	59.3	ramp up
11/6/2012	12:40	23	28	0.39	43.30	0.97	74.2	60.1	
11/6/2012	13:30	23.2	28.5	0.39	33.20	0.95	77.5	62.8	
11/6/2012	14:15	23.2	29	0.39	12.00	0.91	82.4	66.7	steady state
11/6/2012	15:00	22.9	29	0.39	6.90	0.90	82.6	66.9	air temp
11/6/2012	16:19	22.8	29	0.39	2.80	0.89	83.1	67.3	65-50 F
11/6/2012	17:00	22.8	29	0.39	-5.30	0.87	84.6	68.5	03-301
11/6/2012	17:17	22.8	29	0.39	-8.90	0.87	85.3	69.1	
11/6/2012	17:30	22.8	28.5	0.39	-13.80	0.86	84.7	68.6	
11/6/2012	17:32	20.8	0	0.41		0.88			shut down

		Pressure		Pressure		Temp		Corrected CO2	
Date	Time	(psi)	Flow (CFM)	Factor	CO2 Temp (F)		Air SCFM	SCFM	Log
11/7/2012	7:30	19.4		0.43	40.10	0.96		15.6	Start
11/7/2012	7:33	19.4		0.43	39.30			28.4	
11/7/2012	7:35	19.8		0.43	38.40			33.7	ramp up
11/7/2012	7:37	19.2	20	0.43	37.70	0.96	48.2	39.0	air = 42 F
11/7/2012	7:40	20.2	22.6	0.42	36.60	0.96	56.2	45.5	Ice on CO2
11/7/2012	7:42	21	25	0.41	35.90	0.95	63.7	51.6	all lines at
11/7/2012	7:44	21.6	28.3	0.40	35.00	0.95	73.4	59.5	0744 hrs
11/7/2012	8:00	22.6	29	0.39	-17.00	0.85	86.4	70.0	
11/7/2012	8:15	22.6	29	0.39	-23.50	0.84	87.7	71.0	stdy state
11/7/2012	8:16	21.6	21.5	0.40	-26.00	0.83	63.6	51.5	1
									shutdown-
									ice on
	8:22			0.39		0.88	0.0	0.0	rubber CO2
11/7/2012									deliv hose
11/7/2012	8:49	16	0	0.39		0.88	0.0	0.0	restart
11/7/2012	8:53	18	18	0.45	37.40	0.96	41.9	33.9	ramp up
11/7/2012	8:55	19.4	21	0.43	37.20	0.96	50.9	41.3	ramp up
11/7/2012	9:28	20.8	22	0.41	35.60		55.7	45.2	-44
11/7/2012	9:30	21.2	25	0.41	35.60	0.95	64.1	51.9	steady
11/7/2012	9:50	21.6	25	0.40	26.90	0.94	65.9	53.4	state
									shutdown -
	9:57		0	1.00		0.88	0.0	0.0	install new
11/7/2012									hose
11/7/2012	10:06	20.9	25	0.41	43.80	0.97	62.5	50.6	startup
11/7/2012	10:10	21.4	27.5	0.41	43.50	0.97	69.7	56.5	ramp up
11/7/2012	10:25	22	28	0.40	33.90	0.95	73.6	59.6	
11/7/2012	10:27	22.2	28.5	0.40	32.50	0.95	75.5	61.2	ramp up
11/7/2012	10:57	22.7	28.7	0.39	12.50	0.91	80.4	65.1	
11/7/2012	11:34	22.8	29	0.39	10.70	0.91	81.7	66.2	
11/7/2012	12:15	22.8	29	0.39	12.20	0.91	81.5	66.0	
11/7/2012	12:45	22.9	29	0.39	10.70	0.91	81.9	66.4	
11/7/2012	13:30	22.8	29	0.39	2.40	0.89	83.2	67.4	steady state
11/7/2012	14:00	22.6	28.5	0.39	8.00	0.90	80.4	65.1	
11/7/2012	14:30	22.6	29	0.39	1.70		82.9	67.1	
11/7/2012	15:00	22.6	28.3	0.39	-5.50	0.87	82.2	66.5	
11/7/2012	15:33	22.5	28.2	0.40	-3.70	0.88	81.3	65.9	]
11/7/2012	15:35	22.5	28.2	0.40	-4.60	0.88	81.5	66.0	ramp up
11/7/2012	15:39	22.6	28.6	0.39	-12.00	0.86	84.2	68.2	ramp up
11/7/2012	16:10	22.6	29	0.39	-19.70	0.85	86.9	70.4	
11/7/2012	16:35	22.1	28	0.40	-16.80	0.85	82.2	66.6	steady state
11/7/2012	17:08	22.4	28	0.40	-19.70	0.85	83.5	67.6	]
11/7/2012	17:30	22	28	0.40	-33.60	0.82	85.2	69.1	]
11/7/2012	17:45	22	28	0.40	-36.60	0.81	85.9	69.5	shutdown
11/7/2012	17:47	19	0	0.44		0.88			

		Pressure		Pressure		Temp		Corrected CO2	
Date	Time	(psi)	Flow (CFM)	Factor	CO2 Temp (F)	Factor	Air SCFM	SCFM	Log
11/8/2012	8:32	18.4	12.5	0.44	53.20	0.99	28.5	23.1	Start
11/8/2012	8:39	18.8	16.75	0.44	52.80	0.99	38.7	31.4	rampun
11/8/2012	8:41	19.6	20	0.43	53.30	0.99	47.3	38.3	ramp up air = 42 F
11/8/2012	8:44	20	23	0.42	51.40	0.98	55.2	44.7	ice forming
11/8/2012	8:57	20.8	26	0.41	51.40	0.98	63.8	51.7	@0913hrs
11/8/2012	9:12	21	26.4	0.41	40.60	0.96	66.6	53.9	CO2 temp
11/8/2012	9:14	21	26.4	0.41	36.80	0.96	67.1	54.4	=36.8F
11/8/2012	9:15	21.6	28.2	0.40	36.30	0.95	73.0	59.1	-30.86
11/8/2012	9:16	21.6	28.2	0.40	36.30	0.95	73.0	59.1	steady state
11/8/2012	9:45	21.8	28.2	0.40	16.80	0.92	76.4	61.9	ice on1/2
11/8/2012	10:20	22	28.5	0.40	13.60	0.91	77.3	62.6	inch line
									ramp up 100
	10:22	22.2	29	0.40	14.30	0.91	78.5	63.6	psi
11/8/2012									@GasPnl
11/8/2012	11:11	22.2	29.5	0.40	5.70	0.90	82.7	67.0	
11/8/2012	12:01	22.2	29	0.40	9.60	0.90	80.6	65.3	steady state
11/8/2012	12:30	22.1	29	0.40	11.40	0.91	80.1	64.9	
11/8/2012	12:33	22.1	29	0.40	12.00	0.91	80.0	64.8	RAMP UP
11/8/2012	13:07	22	29	0.40	15.90	0.92	79.1	64.1	
11/8/2012	13:33	22	29	0.40	15.90	0.92	79.1	64.1	steady state
11/8/2012	14:00	22	29	0.40	16.00	0.92	79.1	64.1	
11/8/2012	14:39	21.9	29	0.40	11.60	0.91	79.6	64.5	RAMP UP
11/8/2012	15:37	21.8	29.5	0.40	3.30	0.89	82.2	66.6	steady state
11/8/2012	16:06	21.6	29.6	0.40	-3.70	0.88	83.3	67.5	1700 hrs ice
11/8/2012	16:36	21.8	29	0.40	-8.70	0.87	83.0	67.2	on chicago
11/8/2012	17:00	21.9	28.8	0.40	-10.20	0.87	82.9	67.1	ftgs at well
11/8/2012	17:30	21.9	28.4	0.40	-28.20	0.83	85.2	69.0	itgs at well
11/8/2012	17:33	18.4	0	0.44		0.88			shutdown
11/9/2012	9:07	22	10	0.40	53.20	0.99	25.3	20.5	Start
11/9/2012	9:09	18.1	13	0.45	678.00	2.19	13.3	10.7	
11/9/2012	9:11	18.9	17.8	0.44	676.10		18.6	15.1	ramp up
11/9/2012	9:13	19.8	21.2	0.43	66.20	1.01	49.2	39.8	air = 42 F
11/9/2012	9:15	20.5	24.2	0.42	65.10		57.4	46.5	Gas panel
11/9/2012	9:18	20.9	26	0.41	62.70	1.01	62.6	50.7	=100 psig @
11/9/2012	9:31	20.9			52.10	0.98		52.8	0933 hrs

Start	20.5	25.3	0.99	53.20	0.40	10	22	9:07	11/9/2012
	10.7	13.3	2.19	678.00	0.45	13	18.1	9:09	11/9/2012
ramp up	15.1	18.6	2.18	676.10	0.44	17.8	18.9	9:11	11/9/2012
air = 42 F	39.8	49.2	1.01	66.20	0.43	21.2	19.8	9:13	11/9/2012
Gas panel	46.5	57.4	1.01	65.10	0.42	24.2	20.5	9:15	11/9/2012
=100 psig @	50.7	62.6	1.01	62.70	0.41	26	20.9	9:18	11/9/2012
0933 hrs	52.8	65.2	0.98	52.10	0.41	26.5	20.9	9:31	11/9/2012
	58.7	72.5	0.98	50.30	0.40	28.8	21.6	9:33	11/9/2012
	63.5	78.3	0.93	23.50	0.40	29.5	21.6	9:45	11/9/2012
]	64.8	80.0	0.91	15.00	0.40	29.5	21.7	10:18	11/9/2012
]	64.4	79.5	0.92	16.50	0.40	29.5	21.7	10:48	11/9/2012
]	64.1	79.1	0.91	15.60	0.40	29.3	21.6	11:45	11/9/2012
]	62.0	76.6	0.93	25.10	0.41	29	21.5	12:35	11/9/2012
steady state	64.0	79.0	0.92	18.10	0.41	29.5	21.5	13:12	11/9/2012
]	63.8	78.7	0.91	13.10	0.40	29	21.6	14:00	11/9/2012
]	64.2	79.2	0.91	12.20	0.41	29.3	21.4	14:55	11/9/2012
]	65.3	80.6	0.89	4.10	0.41	29.3	21.4	16:04	11/9/2012
	66.7	82.4	0.86	-13.60	0.41	28.8	21.4	16:38	11/9/2012
]	66.8	82.5	0.84	-22.60	0.40	28.1	21.6	17:04	11/9/2012
	68.1	84.1	0.84	-25.50	0.40	28.3	21.8	17:32	11/9/2012
shutdown			0.88		0.45	0	18	17:33	11/9/2012

		Pressure		Pressure		Temp		Corrected CO2	
Date	Time	(psi)	Flow (CFM)	Factor	CO2 Temp (F)	Factor	Air SCFM	SCFM	Log
11/12/2012	15:33	21.8	7	0.40	68.50	1.02	17.1	13.9	Start
11/12/2012	15:38	22.6	9.5	0.39	68.50	1.02	23.7	19.2	
11/12/2012	15:40	23.2	11	0.39	66.90	1.01	28.0	22.7	
11/12/2012	15:41	24	12.75	0.38	65.80	1.01	33.2	26.9	
11/12/2012	16:02	23	12.5	0.39	60.80	1.00	32.0	25.9	ramp up
11/12/2012	16:04	23.4	14	0.39	60.80	1.00	36.2	29.3	air = 66 F
11/12/2012	16:07	23.6	14.5	0.38	60.80	1.00	37.7	30.6	
11/12/2012	16:08	24	16	0.38	60.80	1.00	42.1	34.1	
11/12/2012	16:18	24	16	0.38	59.30	1.00	42.2	34.2	
11/12/2012	17:14	24	16	0.38	51.90	0.98	42.8	34.7	
11/12/2012	17:35	24	16	0.38	49.10	0.98	43.0	34.8	steady state
11/12/2012	18:20	23.2	16	0.38	48.20	0.98	43.1	34.9	
11/12/2012	18:23	23.3	17	0.39	48.20	0.98	45.0	36.4	
11/12/2012	18:25	23.4	19	0.39	48.50	0.98	50.4	40.8	ramp up
11/12/2012	18:28	24	20	0.38	48.50	0.98	53.8	43.6	
11/12/2012	18:45	23.9	20	0.38	41.70	0.96	54.4	44.1	Steady
11/12/2012	19:33	23.9	20	0.38	34.80	0.95	55.2	44.7	state;
11/12/2012	19:58	23.9	20	0.38	34.80	0.95	55.2	44.7	shutdown

		Pressure		Pressure		Temp		Corrected CO2	
Date	Time	(psi)	Flow (CFM)	Factor	CO2 Temp (F)	Factor	Air SCFM	SCFM	Log
11/13/2012	11:40	20	4	0.42	83.40	1.05	9.0	7.3	Start
11/13/2012	11:41	18.6	4	0.44	83.40	1.05	8.7	7.0	
11/13/2012	11:42	19.9	9	0.42	84.20	1.05	20.2	16.4	
11/13/2012	11:45	21	13	0.41	82.90	1.04	30.2	24.5	1
11/13/2012	11:47	21.6		0.40	81.30	1.04	35.6	28.8	1
11/13/2012	11:49	22.8	18	0.39	80.20	1.04	44.2	35.8	1
11/13/2012	11:51	23.2	19	0.39	79.30	1.04	47.2	38.3	1
11/13/2012	11:54	23.9	20.2	0.38	78.90	1.04	51.2	41.5	1
11/13/2012	11:58	23.9	20.2	0.38	77.90	1.03	51.3	41.5	1
11/13/2012	12:03	23.9	20.2	0.38	77.10	1.03	51.4	41.6	
11/13/2012	12:24	23.9	20.2	0.38	77.10	1.03	51.4	41.6	shutdown- foaming @ SW-1
11/13/2012	15:30	18.8	5.5	0.44	80.40	1.04	12.1	9.8	re-start
11/13/2012	15:31	18.8	5.5	0.44	80.40	1.04	12.1	9.8	
11/13/2012	15:35	19.2	10	0.43	80.20	1.04	22.2	18.0	
11/13/2012	15:37	19.9	13	0.42	79.00	1.04	29.5	23.9	1
11/13/2012	15:39	20.8	15.3	0.41	78.60	1.04	35.7	28.9	ramp up
11/13/2012	15:41	21.6	18	0.40	77.70	1.03	43.0	34.8	ramp up
11/13/2012	15:44	22.8	20.2	0.39	76.80	1.03	49.9	40.4	
11/13/2012	15:46	23.4	21.5	0.39	75.50	1.03	54.1	43.8	
11/13/2012	15:48	24	23	0.38	74.30	1.03	58.9	47.7	
11/13/2012	16:08	24.6	22.8	0.37	59.90	1.00	61.0	49.4	_
11/13/2012	16:48	24.6	23	0.37	46.20	0.97	63.2	51.2	
11/13/2012	17:00	24.7	23	0.37	41.50	0.96	63.9	51.8	steady state
11/13/2012	17:41	24.7	23	0.37	30.30	0.94	65.4	53.0	
11/13/2012	18:00	24.7	23	0.37	-33.70	0.82	75.2	60.9	
11/13/2012	18:30	24.8	24	0.37	-33.70	0.82	78.7	63.7	temp
11/13/2012	19:30	24.8	24	0.37	-33.70	0.82	78.7	63.7	sensor
11/13/2012	20:15	24.4	24	0.38	32.00	0.95	67.5	54.7	failed
11/13/2012	21:00	24	23.5	0.38	50.00	0.98	63.1	51.1	temps
11/13/2012	21:08	23	18.5	0.39	50.00	0.98	48.4	39.2	estimated
11/13/2012	21:30	22.6	18.5	0.39	50.00	0.98		38.8	_
11/13/2012	22:00	22.4	18.5	0.40	50.00	0.98	47.6	38.6	
11/13/2012	22:02	22.4	18.5	0.40	50.00	0.98	47.6	38.6	shutdown

		Pressure		Pressure		Temp		Corrected CO2	
Date	Time	(psi)	Flow (CFM)	Factor	CO2 Temp (F)	Factor	Air SCFM	SCFM	Log
11/14/2012	10:45	24	5	0.38	57.30	0.99	13.2	10.7	Start
11/14/2012	10:46	18.6	13	0.44	57.30	0.99	29.6	24.0	
11/14/2012	10:47	19.8	16	0.43	57.30	0.99	37.7	30.6	
11/14/2012	10:49	20.2	18.8	0.42	55.90	0.99	45.0	36.4	
11/14/2012	10:51	21	20	0.41	54.30	0.99	49.1	39.8	
11/14/2012	10:54	21.4	20.8	0.41	53.60	0.99	51.7	41.9	ramp up;
11/14/2012	10:56	22	22	0.40	53.20	0.99	55.7	45.1	
11/14/2012	10:58	22.6	24	0.39	52.50	0.99	61.8	50.0	
11/14/2012	11:00	23.2	25	0.39	51.80	0.98	65.5	53.0	
11/14/2012	11:02	23.6	26	0.38	51.40	0.98	68.9	55.8	
11/14/2012	11:04	24	26	0.38	51.00	0.98	69.7	56.4	
11/14/2012	11:34	24.6	26	0.37	15.60	0.91	76.0	61.6	
11/14/2012	12:22	25	26	0.37	0.10	0.88	79.4	64.3	steady state
11/14/2012	13:00	25	26	0.37	-8.70	0.87	80.9	65.5	steady state
11/14/2012	13:27	25.2	26	0.37	-33.00	0.82	85.9	69.6	
11/14/2012	13:28	25	25.5	0.37	-13.90	0.86	80.3	65.0	ramp down
11/14/2012	14:03	25.2	25.5	0.37	-11.60	0.86	80.3	65.0	
11/14/2012	14:30	25	25.5	0.37	-12.30	0.86	80.0	64.8	
11/14/2012	15:00	24.8	25	0.37	-18.60	0.85	79.1	64.1	
11/14/2012	15:30	24.8	25.5	0.37	-21.50	0.84	81.3	65.8	
11/14/2012	16:00	24.8	25.5	0.37	-31.40	0.82	83.1	67.3	steady state
11/14/2012	16:30	24.8	25.5	0.37	-35.50	0.82	83.9	68.0	
11/14/2012	17:00	24.6	25.5	0.37	-33.00	0.82	83.0	67.2	
11/14/2012	17:06		15.75	0.39	-28.75	0.83	48.4	39.2	ramp down
11/14/2012	17:16		15	0.40	3.00		42.1	34.1	· ·
11/14/2012	17:30	21.4	14.75	0.41	25.80	0.93	38.8	31.4	steady state
11/14/2012	17:41	21.4	15.5	0.41	25.30		40.8	33.0	ramp up;
11/14/2012	18:10	21.4	15.5	0.41	30.00	0.94	40.4	32.7	
11/14/2012	18:30		15.5	0.41	40.20			32.1	steady state
11/14/2012	19:00	21.4	15.5	0.41	41.70	0.96	39.5	32.0	1
11/14/2012	19:02	19.6		0.43		0.88		_	shutdown

		Pressure		Pressure		Temp		Corrected CO2	
Date	Time	(psi)	Flow (CFM)	Factor	CO2 Temp (F)	Factor	Air SCFM	SCFM	Log
									Residual
	10:50	16		0.48		0.88			Well
11/15/2012									Pressue
11/15/2012	10:51	19	5	0.44	56.30	0.99	11.5	9.4	Start
11/15/2012	10:53	21.8	12.5	0.40	56.30	0.99	31.3	25.3	ramp up
11/15/2012	10:55	22.6	16	0.39	54.50	0.99	41.0	33.2	ramp up
11/15/2012	11:15	22.2	16.75	0.40	48.90	0.98	43.0	34.8	steady
11/15/2012	11:45	21.8	16.75	0.40	57.20	0.99	41.8	33.9	statw
11/15/2012	11:28	21.5	16.5	0.41	61.70	1.00	40.5	32.8	Statev
11/15/2012	11:45	21.8	16.75	0.40	60.90	1.00	41.5	33.6	
11/15/2012	12:28	21.5	16.5	0.41	61.70	1.00	40.5	32.8	steady state
11/15/2012	12:33	21.4	17	0.41	60.90	1.00	41.7	33.8	ramp up
11/15/2012	13:24	21.6	17	0.40	58.80	1.00	42.1	34.1	
11/15/2012	14:00	21.8	17	0.40	56.10	0.99	42.5	34.4	
11/15/2012	15:00	22	17	0.40	51.60	0.98	43.1	34.9	steady state
11/15/2012	16:00	22	17	0.40	50.00	0.98	43.3	35.1	
11/15/2012	16:40	23.2	22	0.39	49.80	0.98	57.9	46.9	
11/15/2012	16:42	24.4	25.5	0.38	49.60	0.98	69.2	56.1	ramp up
11/15/2012	17:00	25	26	0.37	2.10	0.89	79.0	64.0	
11/15/2012	17:30	25.2	25	0.37	-36.30	0.81	83.3	67.5	ramp dwn
11/15/2012	17:32	25	25	0.37	-36.30	0.81	82.9	67.1	
11/15/2012	18:00	25	25	0.37	-36.30	0.81	82.9	67.1	
11/15/2012	19:00	24.8	24	0.37	-36.30	0.81	79.1	64.1	steady
									state
11/15/2012	19:30	24.6	24	0.37	-36.30	0.81	78.7	63.8	
11/15/2012	19:32	24.6	25	0.37	-36.30	0.81	82.0	66.4	ramp up
11/15/2012	20:00	24.6	24	0.37	-36.30	0.81	78.7	63.8	
11/15/2012	20:02	24.6	24.5	0.37	-36.30	0.81	80.4	65.1	ramp up
11/15/2012	20:30	24.6	24.5	0.37	-36.30	0.81	80.4	65.1	
11/15/2012	20:32	24.6	25	0.37	-36.30	0.81	82.0	66.4	ramp up
11/15/2012	21:00	24.6	25	0.37	-36.30	0.81	82.0	66.4	]
11/15/2012	21:30	24.2	24.5	0.38	-36.30	0.81	79.6	64.5	steady state
11/15/2012	22:00	GENERAT		-APPROX	25 GAL FUEL IN TAI	NK WILL		OR IN THE AM	
11/15/2012	22:02		0	1.00		0.88	0.0	0.0	shutdown

		Pressure		Pressure		Temp		Corrected CO2	
Date Ti	ime	(psi)	Flow (CFM)	Factor	CO2 Temp (F)	•	Air SCFM	SCFM	Log
Dute 11		(60.7	11000 (C1101)	1 40101	002 iciiip (i )	. ucto.	All SCI IVI	33.11.	Residual
	10:50	16		0.48		0.88			Well
11/16/2012	10.50	10		0.46		0.66			Pressue
11/16/2012	10:55	22	5	0.40	50.30	0.98	12.7	10.3	Start
11/10/2012	10.55	22	5	0.40	50.50	0.96	12.7	10.5	Start
11/16/2012	10:56	18	5	0.45	50.30	0.98	11.3	9.2	
11/16/2012	11:00	23	16	0.39	50.30	0.98	41.8	33.9	
11/16/2012	11:02	23.6	18	0.38	49.20	0.98	47.9	38.8	
11/16/2012	11:04	23.8	19.5	0.38	48.30	0.98	52.2	42.3	ramp up
11/16/2012	11:08	24.2	21.5	0.38	47.30	0.98	58.3	47.2	
11/16/2012	11:10	24.4	22.5	0.38	47.00	0.98	61.4	49.7	
11/16/2012	11:12	24.6	23	0.37	46.50	0.97	63.1	51.1	
11/16/2012	11:14	24.9	23.5	0.37	46.30	0.97	65.0	52.7	
11/16/2012	11:40	25	24.3	0.37	5.90	0.90	73.2	59.3	
11/16/2012	12:45	25	24.5	0.37	-6.90	0.87	75.9	61.5	steady state
11/16/2012	13:20	24.7	24.5	0.37	3.30	0.89	73.7	59.7	
11/16/2012	13:22	24.8	25	0.37	0.60	0.89	75.8	61.4	ramp up
11/16/2012	13:45	24.8	25	0.37	0.30	0.89	75.9	61.5	1 1
11/16/2012	14:05	24.8	25	0.37	-1.30	0.88	76.2	61.7	-
11/16/2012	14:30	24.8	25	0.37	-3.30	0.88	76.5	62.0	-
11/16/2012	15:05	24.8	25	0.37	-6.70	0.87	77.1	62.4	steady state
11/16/2012	15:32	24.6	25	0.37	-6.70	0.87	76.7	62.1	-
11/16/2012	16:00	24.6	25	0.37	-7.80	0.87	76.7	62.3	_
11/16/2012	16:30	24.6	25	0.37	-7.80	0.87	76.9	62.3	_
11/16/2012	16:32	24.8	26.5	0.37	-7.80	0.87	81.9	66.3	rampun
11/16/2012	17:00	24.8	20.3	0.37	-25.80	0.84	87.3	70.7	ramp up
	17:30	25	26.7	0.37	-32.50	0.84	87.7	71.0	steady state
11/16/2012	18:30	24.8	26.7	0.37		0.82	87.7 85.4	69.2	Steady State
11/16/2012	16.50	24.0	20	0.57	-34.80	0.62	65.4	09.2	
									shut down s
	10.05	24.0	20	0.27	24.00	0.00	05.4	60.3	due to
	19:05	24.8	26	0.37	-34.80	0.82	85.4	69.2	bubbling
11/15/2012									thru 519A
11/16/2012	40.07	24	20	0.44	20.00	0.04	72.0	F0.2	fitting
11/16/2012	19:27	21	28	0.41	30.90	0.94	72.0	58.3	restart
									Gas Panel
									pressure
									maxed out
11/16/2012	19:35	23	27	0.39	30.90		73.3	59.4	at 100 psig
11/16/2012	20:00	24	28	0.38	-25.80	0.84	88.3	71.5	_
11/16/2012	20:30	24	27.5	0.38	-36.60		88.9	72.0	_
11/16/2012	21:00	24	27	0.38	-36.60		87.3	70.7	
11/16/2012	21:01	24.4	27	0.38	-36.60		88.2	71.4	ramp up
11/16/2012	21:30	24.4	27	0.38	-36.60		88.2	71.4	
11/16/2012	21:32	24.6	28	0.37	-36.60		91.9	74.5	ramp up
11/16/2012	22:00	24.6	28	0.37	-36.60		91.9	74.5	
11/16/2012	22:30	24.6	28	0.37	-36.60		91.9	74.5	
11/16/2012	23:00	24.4	27.5	0.38	-36.60	0.81	89.8	72.8	
11/16/2012	23:30	24.3	27.5	0.38	-36.60	0.81	89.6	72.6	
11/16/2012 24	1:00:00	24.3	27.5	0.38	-36.60	0.81	89.6	72.6	
, -, -									

		Pressure		Pressure		Temp		Corrected CO2	
Date	Time	(psi)	Flow (CFM)	Factor	CO2 Temp (F)	Factor	Air SCFM	SCFM	Log
11/17/2012	9:30	15.4		0.49		0.88			Residual Well Pressue
11/17/2012	9:33	19	11	0.44	53.90	0.99	25.5	20.7	Start
11/17/2012	9:35	20.6	21.5	0.42	53.90	0.99	52.2	42.3	ramp up;
11/17/2012	9:38	22	27	0.40	53.70	0.99	68.2	55.3	gas panelat
11/17/2012	9:40	22	27.2	0.40	53.70	0.99	68.7	55.7	100 psi @
11/17/2012	9:43	22.4	28	0.40	52.80	0.99	71.7	58.0	0940 hrs
11/17/2012	10:00	23.2	29	0.39	2.30	0.89	84.1	68.1	
11/17/2012	10:30	23.6	28	0.38	-12.90	0.86	84.8	68.7	steady state
11/17/2012	11:00	24	28	0.38	-14.50	0.86	86.0	69.7	Steady State
11/17/2012	11:30	23.8	27.8	0.38	-9.40	0.87	84.0	68.1	
11/17/2012	11:32	23.8	28	0.38	-11.00	0.86	84.9	68.8	ramp up
11/17/2012	12:15	24	28	0.38	-12.90	0.86	85.7	69.4	
11/17/2012	13:00	24.1	27.9	0.38	-11.60	0.86	85.4	69.2	
11/17/2012	13:30	24	28	0.38	-2.70	0.88	83.8	67.9	steady state
11/17/2012	14:00	24.2	28	0.38	-6.90	0.87	85.0	68.9	steady state
11/17/2012	14:35	24	27.8	0.38	-3.70	0.88	83.4	67.6	
11/17/2012	15:08	24	27.8	0.38	-7.30	0.87	84.1	68.1	
11/17/2012	15:12	24	28	0.38	-8.00	0.87	84.8	68.7	ramp up
11/17/2012	15:30	24	28	0.38	9.40	0.90	81.7	66.1	
11/17/2012	16:05	24.4	27.5	0.38	-14.50	0.86	85.4	69.2	
11/17/2012	16:30	24.4	28	0.38	-12.30	0.86	86.5	70.1	
11/17/2012	16:45	24.4	28.5	0.38	-13.00	0.86	88.2	71.4	
11/17/2012	17:00	24.5	28.5	0.38	-14.80	0.86	88.8	71.9	
11/17/2012	17:45	24.4	28	0.38	-17.40	0.85	87.5	70.9	
11/17/2012	18:06	24.4	29	0.38	-19.30	0.85	91.0	73.7	
11/17/2012	18:35	24.4	29	0.38	-19.30	0.85	91.0	73.7	]
11/17/2012	19:00	24.4	28.5	0.38	-19.90	0.85	89.6	72.6	
11/17/2012	19:30	24.2	28	0.38	-19.00	0.85	87.4	70.8	
11/17/2012	20:00	24.2	28	0.38	-19.00	0.85	87.4	70.8	
11/17/2012	20:02			1.00		0.88		·	shutdown

# APPENDIX E. LABORATORY ANALYTICAL DATA

## **Pre-Sparge Analytical Data**

		Field Sample ID	EQB-100312		EW-11-100312		MW-115A- 100312		MW-115A2- 100312		MW-115B-100312		MW-115C- 100312		MW-1A-100212	N	4W-1B-100212	
		Location	Equipment Blank		EW-11-100312 EW-11		MW-115A		MW-115A		MW-115B-100512 MW-115B		MW-115C		MW-1A-100212 MW-1A		MW-1B-100212	
			10/3/2012		10/3/2012		10/3/2012		10/3/2012		10/3/2012		10/3/2012		10/2/2012		0/2/2012	
		Sample Date SDG	680-83469-1		680-83469-1		680-83469-1		680-83469-1		680-83469-1		680-83469-1		680-83469-1		80-83414-1	
		Matrix	WATER		WATER		WATER		WATER		WATER		WATER		WATER		VATER	_
																		_
		Sample Purpose	Equipment blank		Regular sample		Regular sample		Field duplicate		Regular sample		Regular sample		Regular sample		Regular sample	_
Method	Parameter Name	Sample Type Units	Blank water		Ground Water		Ground Water		Ground Water		Ground Water		Ground Water		Ground Water	U	Ground Water	_
Method		Ullits																
SM2320B	ALKALINITY, CARBONATE (AS CACO3)	mg/L	5	U	1800	Н	100	U,H	100	U,H	100	U,H	3500	Н	100 U,F	H 10	00	U,H
	BICARBONATE ALKALINITY AS																	
SM2320B	CACO3	mg/L	5	U	650	Н		Н	640	Н		H	700	Н	820 H		70	Н
SM2320B	TOTAL ALKALINITY	mg/L	5	U	2700	Н		Н	640	Н		H	4700	Н			80	Н
SM2540C	TOTAL DISSOLVED SOLIDS	mg/L	22		20000		3700		3700		3400		33000		5000		500	
SM3500-FeD	FERROUS IRON	μg/L	100	U	2300		190		170		960		1300		1200	54	400	
SM4500S2-F	SULFIDE	mg/L	1	U	17		4.5		5.8		6.3		35		7.3			
SM4500S2-F	SULFIDE, DISSOLVED	mg/L														1		U
SM5310B	DISSOLVED ORGANIC CARBON	mg/L	1		1700		240		230		230		1300		230	20	00	
SM5310B	TOTAL ORGANIC CARBON	mg/L			280		220		210		230		1500		350	19	90	
SW6010	ALUMINUM	mg/L	0.2	U	0.48		24		24		2.1		0.2	U	20	14		
SW6010	ANTIMONY	μg/L	20		20	U	20	U	20	U	20	U	20	U	20 U	20	0	U
SW6010	ARSENIC	mg/L	0.02	U	0.14		0.0095	J	0.0086	J	0.011	J	0.28		0.012 J	0.	.012	J
SW6010	BARIUM	mg/L	0.01	U	0.052		0.069		0.07		0.046		0.016		0.072	0.	.061	
SW6010	BERYLLIUM	mg/L	0.004	U	0.0043		0.0032	J	0.0032	J	0.011		0.0019	J	0.011	0.	.01	
SW6010	CADMIUM	mg/L	0.005	U	0.005	U	0.005	U	0.005	U	0.005	U	0.002	J	0.005 U	0.	.005	U
SW6010	CALCIUM	mg/L	0.5	U	17		17		17		12		0.56		10	14	4	
SW6010	CHROMIUM	mg/L	0.01	U	0.45		0.09		0.089		0.07		0.34		0.078	0.	.093	
SW6010	COBALT	mg/L	0.01	U	0.0035	J	0.0014	J	0.0017	J	0.01	U	0.0019	J	0.004 J	0.	.0011	J
SW6010	COPPER	mg/L	0.02	U	0.022		0.0065	J	0.0057	J	0.0023	J	0.022		0.0035 J	0.	.0041	J
SW6010	IRON	mg/L	0.1	U	2.6		1.1		1.1		0.65		1.5		2.9	8.	.5	
SW6010	LEAD	mg/L	0.01	U	0.01		0.019		0.019		0.013		0.01	U	0.024	0.	.016	
SW6010	MAGNESIUM	mg/L	0.5	U	0.1	J	3.1		3.1		0.98		0.019	J	2.5	4.	.2	
SW6010	MANGANESE	mg/L	0.01	U	0.044		0.35		0.35		0.0071	J	0.01	U	0.039	0.	.17	
SW6010	NICKEL	mg/L	0.04	U	0.06		0.012	J	0.012	J	0.008	J	0.069		0.01 J	0.	.0092	J
SW6010	POTASSIUM	mg/L	1	U	9.8		6.9		7		0.61	J	11		6.4	2.	.4	
SW6010	RESPIRABLE QUARTZ	μg/L	280	J	610000		19000		19000		18000		2000000		44000	5	7000	
SW6010	SELENIUM	mg/L	0.02	U	0.027		0.014	J	0.016	J	0.0083	J	0.025		0.012 J	0.	.0089	J
SW6010	SILVER	mg/L	0.01	U	0.01	U	0.01	U	0.01	U		U	0.01	U	0.01 U	_	.01	U
SW6010	SODIUM	mg/L	1	U	7900		1200		1200		1100		13000		1500		300	
SW6010	THALLIUM	mg/L	0.025	U	0.025	U	0.025	U	0.025	U		U	0.025	U	0.025 U		.025	U
SW6010	VANADIUM	μg/L	10	U	1400		150	1	150		110		1500		120	12	20	
SW6010	ZINC	μg/L	20				13	J	12	J		U	15	J	51	28		
SW7470	MERCURY	μg/L	0.2	U	64		7.2	1	7		5.5		120		8.1	5		
SW9040	pH	S.U.	6.14		11.1	Н		Н	7.69	Н		H	11.4	Н	8.42 H	8	.93	Н
SW9056	CHLORIDE	mg/L	5	U	9000		1300		1300		1200	-	15000		1800		600	
SW9056	SULFATE	mg/L	5		420		100	U	100	U		U	950		100 U		00	U

Analytical Lab was TestAmerica Savannah (5102 LaRoche Avenue, Savannah, GA 31404)

Qualifiers:

Indicates the analyte was analyzed for but not detected.

Result is less than the RL but greater than or equal to the MDL and the concentration is an approximate value. Sample was prepped or analyzed beyond the specified holding time

Field parameter with a holding time of 15 minutes

Duplicate RPD exceeds the control limit

Compound was found in the blank and sample

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		Eight Commission	MW 1C 100212		MW 24 100212		MW 2D 100212		MW 2C 100212		MW 24 100212		MW-519A-		MW-519B-	
		Field Sample ID	MW-1C-100212		MW-2A-100312		MW-2B-100312		MW-2C-100312		MW-3A-100312		100212	<u> </u>	100212	
		Location	MW-1C		MW-2A		MW-2B 10/3/2012		MW-2C 10/3/2012		MW-3A 10/3/2012		MW-519A 10/2/2012	<u> </u>	MW-519B 10/2/2012	
		Sample Date	10/2/2012 680-83414-1		10/3/2012									<del>                                     </del>	680-83414-1	
		SDG	WATER		680-83469-1 WATER		680-83469-1		680-83469-1		680-83469-1 WATER		680-83414-1 WATER	<u> </u>	WATER	
		Matrix					WATER		WATER					<u> </u>		
		Sample Purpose	Regular sample		Regular sample		Regular sample Ground Water		Regular sample		Regular sample		Regular sample	<u> </u>	Regular sample Ground Water	
M-41 J	Danier de Name	Sample Type	Ground Water		Ground Water		Ground water		Ground Water		Ground Water		Ground Water	<u> </u>	Ground water	
Method	Parameter Name ALKALINITY, CARBONATE (AS	Units												<del>                                     </del>		
SM2320B	CACO3)	ma/I	4300	Н	100	U,H	100	U,H	4000	Н	100	Н	160	Н	3900	Н
SW12320B	BICARBONATE ALKALINITY AS	mg/L	4300	п	100	О,П	100	О,П	4000	п	100	п	100	П	3900	П
SM2320B	CACO3	mg/L	790	Н	830	Н	770	Н	810	Н	4800	Н	820	Н	780	Н
SM2320B	TOTAL ALKALINITY	mg/L	5700	Н	840	H	780	H	5300	H	4900	H	1000	Н		H
SM2540C	TOTAL DISSOLVED SOLIDS		48000	11	5200	11	4300	11	38000	11	30000	11	5800	11	43000	11
SM3500-FeD	FERROUS IRON	mg/L	3300		2200		1800		1700		490		790	+	2200	
SM4500S2-F	SULFIDE	μg/L	3300		5.9				28		5.1		130	+	2200	
SM4500S2-F SM4500S2-F	SULFIDE SULFIDE, DISSOLVED	mg/L	52		J.7		14		40		J.1	-	8.3	+	61	
SM5310B		mg/L	2300		280		280		1600		530		230	<del>                                     </del>	2100	
	DISSOLVED ORGANIC CARBON	mg/L									440			<u> </u>		
SM5310B	TOTAL ORGANIC CARBON	mg/L	1900		250		280		1600				390	<del>                                     </del>	1900	
SW6010	ALUMINUM	mg/L	0.28	TT	47	TT	4.7	TT	0.47	U	16	IJ	1.3	TI	0.73	II
SW6010	ANTIMONY	μg/L	0.32	U	20	U	20	U	20	U	20	U	20 0.019	U	0.39	U
SW6010	ARSENIC	mg/L			0.021		0.012	J	0.26		0.02			J		
SW6010	BARIUM	mg/L	0.021	т т	0.2		0.068		0.022		0.066	-	0.057	<u> </u>	0.017	Ī
SW6010	BERYLLIUM	mg/L	0.0023	J	0.01	TT	0.011	TT	0.0022	J	0.003	J	0.0075	T.T.	0.0023	J
SW6010	CADMIUM	mg/L	0.0024	J	0.005	U	0.005	U	0.0024	J	0.005	U	0.005	U	0.0027	J
SW6010	CALCIUM	mg/L	1.4		20		14		2.5		31		11	<u> </u>	1.6	
SW6010	CHROMIUM	mg/L	0.5	т.	0.14		0.095	T.T.	0.37		0.092	-	0.084	T.T.	0.61	т
SW6010	COBALT	mg/L	0.0031	J	0.006	J	0.01	U	0.0019	J	0.0016	J	0.01	U	0.003	J
SW6010	COPPER	mg/L	0.031		0.0053	J	0.0031	J	0.022		0.0034	J	0.0042	J	0.037	
SW6010	IRON	mg/L	2.1		6.7		1.8		1.8	**	1.9	-	0.55	<u> </u>	2.6	_
SW6010	LEAD	mg/L	0.01	U	0.032		0.017		0.01	U	0.0078	J	0.014	+	0.0051	J
SW6010	MAGNESIUM	mg/L	0.13	J	3.4		0.81		0.12	J	24		0.22	J	0.15	J
SW6010	MANGANESE	mg/L	0.0021	J	0.3	-	0.027	_	0.0028	J	0.18	_	0.0064	J	0.0036	J
SW6010	NICKEL	mg/L	0.09		0.016	J	0.0097	J	0.069		0.026	J	0.0093	J	0.1	
SW6010	POTASSIUM	mg/L	14		7.8		1.3		14		100		0.95	J	25	
SW6010	RESPIRABLE QUARTZ	μg/L	2000000		80000	-	30000	_	1900000		13000		30000	<u> </u>	2000000	
SW6010	SELENIUM	mg/L	0.042		0.013	J	0.01	J	0.035		0.025		0.013	J	0.046	
SW6010	SILVER	mg/L	0.01	U	0.01	U	0.01	U	0.01	U	0.01	U	0.01	U	0.01	U
SW6010	SODIUM	mg/L	20000		1700		1400		13000		11000		1600	<u> </u> '	19000	
SW6010	THALLIUM	mg/L	0.025	U	0.025	U	0.025	U	0.025	U	0.025	U	0.025	U		U
SW6010	VANADIUM	μg/L	2200		170		150		1700		130		180	<b>↓</b> '	2300	_
SW6010	ZINC	μg/L	16	J	48		9.5	J	16	J	26		20	U	18	J
SW7470	MERCURY	μg/L	110		11		4.8		110		0.16	J	7.9	<u> </u>	120	
SW9040	pH	S.U.	11.2	Н	8.68	Н	9.16	Н	11.3	Н	8.14	Н	9.71	Н	11.2	Н
SW9056	CHLORIDE	mg/L	19000		1800		1400		17000		13000		2100	<u> </u>	19000	
SW9056	SULFATE	mg/L	1300		100	U	100	U	1000		100	U	100	U	1300	

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Field parameter with a holding time of 15 minutes
Duplicate RPD exceeds the control limit
Compound was found in the blank and sample

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# Post-Sparge Analytical Data (1 week after conclusion of sparging)

					MW-115A-		MW-115B-		MW-115C-		MW-1A-		MW-1B-				MW-2A-	$\top$
		Field Sample ID	EQB-112815		112812		112812		112712		112812		112712		MW-1C-112612		112812	
			Equipment															
		Location	Blank		MW-115A		MW-115B		MW-115C		MW-1A		MW-1B		MW-1C		MW-2A	
		Sample Date	11/28/2012		11/28/2012		11/28/2012		11/27/2012		11/28/2012		11/27/2012		11/26/2012		11/28/2012	
		SDG	680-85180-2		680-85180-2		680-85180-2		680-85137-2		680-85180-2		680-85180-2		680-85137-2		680-85180-2	
		Matrix	WATER		WATER		WATER		WATER		WATER		WATER		WATER		WATER	
													Regular					
		Sample Purpose	Equipment blank		Regular sample		Regular sample		Regular sample		Regular sample		sample		Regular sample		Regular sample	
		Sample Type	Blank water		Ground Water		Ground Water		Ground Water		Ground Water		Ground Water		Ground Water		Ground Water	
Method	Parameter Name	Units																
	ALKALINITY, CARBONATE (AS																	
SM2320B	CACO3)	mg/L	5	U	100	U,H	100	U,H	3200	Н	100	U,H	100	U,H	120	Н	100	U,H
	BICARBONATE ALKALINITY AS																	
SM2320B	CACO3	mg/L	5	U	800	Н	1400	Н	1700	Н	1500	Н	1400	Н	7800	Н	1700	Н
SM2320B	TOTAL ALKALINITY	mg/L	5	U	800	Н	1400	Н	5100	Н		Н	1400	Н	7900	Н	1700	Н
SM2540C	TOTAL DISSOLVED SOLIDS	mg/L	16		3800		4300		34000		8200		5600		48000		5100	
SM3500-FeD	FERROUS IRON	μg/L	100	U	210		5000		1500		370		7900		18000		1200	
SM4500S2-F	SULFIDE	mg/L	1	U	16		12		40		10	U	10	U	22		14	
SM5310B	DISSOLVED ORGANIC CARBON	mg/L	1.4		240		210		450	В	160		170		390	В	200	
SM5310B	TOTAL ORGANIC CARBON	mg/L	1	U	220		190		560		140		160		430		190	
SW6010	ALUMINUM	mg/L	100	U	27		5		0.2	U			4.6		0.2	U	23	
SW6010	ANTIMONY	μg/L	10000	U	20	U	20	U	14	J		U	20	U	20	U	20	U
SW6010	ARSENIC	mg/L	10	U	0.0083	J	0.016	J	0.098		0.02	U	0.012	J	0.12		0.0095	J
SW6010	BARIUM	mg/L	5	U	0.069		0.031		0.056		0.034		0.026		0.39		0.14	
SW6010	BERYLLIUM	mg/L	2	U	0.0036	J	0.013		0.0019	J	0.0018	J	0.015		0.0027	J	0.0062	
SW6010	CADMIUM	mg/L	2.5	U	0.005	U	0.005	U	0.0025	J	0.005	U	0.005	U	0.0037	J	0.005	U
SW6010	CALCIUM	mg/L	250	U	16		9		2.8		14		8.2		65		13	
SW6010	CHROMIUM	mg/L	5	U	0.087		0.096		0.34		0.03		0.13		0.32		0.089	
SW6010	COBALT	mg/L	5	U	0.0021	J	0.01	U	0.0018	J	0.0013	J	0.01	U	0.01	U	0.0022	J
SW6010	COPPER	mg/L	10	U	0.0064	J	0.0023	J	0.02		0.02	U	0.0022	J	0.0049	J	0.0033	J
SW6010	IRON	mg/L	50	U	1.3		3.8		1.1		0.69		7.5		17		1.9	
SW6010	LEAD	mg/L	5	U	0.025		0.015		0.01	U	0.01	U	0.012		0.063		0.017	
SW6010	MAGNESIUM	mg/L	250	U	2.9		7.5		0.38	J	12		4.9		19		1.4	
SW6010	MANGANESE	mg/L	5	U	0.34		0.063		0.0052	J	0.034		0.11		0.24		0.14	
SW6010	NICKEL	mg/L	20	U	0.013	J	0.0062	J	0.059		0.0054	J	0.0047	J	0.016	J	0.0079	J
SW6010	POTASSIUM	mg/L	500	U	7.6		1.1		19		25		2.1		48		8.4	
SW6010	RESPIRABLE QUARTZ	μg/L	500	U	28000		110000		470000		40000		91000		86000		50000	
SW6010	SELENIUM	mg/L	3.5	J	0.015	J	0.012	J	0.036		0.02		0.0099	J	0.032		0.017	J
SW6010	SILVER	mg/L	5	U	0.01	U	0.01	U	0.01	U	0.01	U	0.01	U	0.01	U	0.01	U
SW6010	SODIUM	mg/L	500	U	470	J	640		6600		1600		690		8700		650	
SW6010	THALLIUM	mg/L	13	U	0.025	U	0.025	U	0.025	U	0.025	U	0.025	U	0.025	U	0.025	U
SW6010	VANADIUM	μg/L	5000	U	140		130		1400		81		140		370		110	
SW6010	ZINC	μg/L	10000	U	33		11	J	18	J	15	J	49		9.5	J	18	J
SW7470	MERCURY	μg/L	0.20	U	7.6		3.9		110		1.1		3.5		21		4.5	
SW9040	рН	S.U.	5.74		7.7		6.41		9.94		6.76	Н	6.46	Н	6.97	Н	7.19	
SW9056	CHLORIDE	mg/L	5	U	1100		1200		18000		4000		1200		25000		1500	
SW9056	SULFATE	mg/L	5	U	100	U	100	U	1100		100	U	100	U	1400		100	U

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Field parameter with a holding time of 15 minutes
Duplicate RPD exceeds the control limit
Compound was found in the blank and sample

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					MW-2C-		MW-2C-		MW-2C-		MW-3A-		MW-519A-		MW-519B-		MW-519B-			
		Field Sample ID	MW-2B-112812		MID-112712		MID2-112712		TOP-112712		112812		112812		112712		TOP-112712		SW-1-112712	1
		Location	MW-2B		MW-2C		MW-2C		MW-2C		MW-3A		MW-519A		MW-519B		MW-519B		SW-1	
		Sample Date	11/28/2012		11/27/2012		11/27/2012		11/27/2012		11/28/2012		11/28/2012		11/27/2012		11/27/2012		11/27/2012	
		SDG	680-85180-2		680-85137-2		680-85137-2		680-85180-2		680-85180-2		680-85180-2		680-85137-2		680-85137-2		680-85137-2	
		Matrix	WATER		WATER		WATER		WATER		WATER		WATER		WATER		WATER		WATER	
					Regular		Field		Regular		Regular		Regular		Regular				Regular	
		Sample Purpose	Regular sample		sample		duplicate		sample		sample		sample		sample		Regular sample		sample	
		Sample Type	Ground Water		Ground Water		Ground Water		Ground Water		Ground Water		Ground Water		Ground Water		Ground Water		Ground Water	r
Method	Parameter Name	Units																		
	ALKALINITY, CARBONATE (AS																			
SM2320B	CaCO <sub>3</sub> )	mg/L	100	U,H	110	Н	100	U,H	100	U,H	100 L	J <b>,H</b>	100 U	J <b>,H</b>	1200	Н	400	Н	100	U,H
	BICARBONATE ALKALINITY AS																			
SM2320B	CaCO <sub>3</sub>	mg/L	1100	Н	5600	Н	5700	Н	6000	Н	7200 H		1500 H		6200	Н	7100	Н	5400	Н
SM2320B	TOTAL ALKALINITY	mg/L	1100	Н	5700	Н	5800	Н	6000	Н	7200 H	I	1600 H	I	7400	H	7500	Н	5400	Н
SM2540C	TOTAL DISSOLVED SOLIDS	mg/L	4800		35000		33000		32000		30000		5400		46000		45000		24000	
SM3500-FeD	FERROUS IRON	μg/L	6200		5200		6000		6900		1800		7600		2500		4000		9900	
SM4500S2-F	SULFIDE	mg/L	19		20		20		22		18		11		43		35		15	
SM5310B	DISSOLVED ORGANIC CARBON	mg/L	210		410	В	440	В	300		330		170		580	В	550	В	310	В
SM5310B	TOTAL ORGANIC CARBON	mg/L	200		480		470		270		830		150		670		630		310	
SW6010	ALUMINUM	mg/L	6		0.2	U	0.2	U	0.2	U	5.9		2.5		0.2	U	0.2	U	0.18	J
SW6010	ANTIMONY	μg/L	20	U	14	J	19	J	9.1	J	20 U	J	20 U	J	9.4	J	20	U	20	U
SW6010	ARSENIC	mg/L	0.015	J	0.039		0.044		0.026		0.013 J	•	0.011 J		0.17		0.13		0.045	
SW6010	BARIUM	mg/L	0.04		0.11		0.13		0.17		0.075		0.044		0.11		0.13		0.3	
SW6010	BERYLLIUM	mg/L	0.013		0.0021	J	0.0024	J	0.003	J	0.0016 J	•	0.011		0.0024	J	0.0025	J	0.0042	
SW6010	CADMIUM	mg/L	0.005	U	0.005	U	0.0021	J	0.0025	J	0.005 L	J	0.005 U	J	0.003	J	0.0026	J	0.0028	J
SW6010	CALCIUM	mg/L	10		12		14		19		40		9.1		13		13		21	
SW6010	CHROMIUM	mg/L	0.11		0.25		0.32		0.3		0.044		0.11		0.38		0.39		0.2	
SW6010	COBALT	mg/L	0.01	U	0.01	U	0.01	U	0.01	U	0.01 L	J	0.01 U	J	0.0012	J	0.0013	J	0.01	U
SW6010	COPPER	mg/L	0.0026	J	0.0089	J	0.011	J	0.0087	J	0.02 L	J	0.02 U	J	0.016	J	0.014	J	0.0043	J
SW6010	IRON	mg/L	6.2		6.1		7.2		8.4		1.3		6.7		2.3		3.2		14	
SW6010	LEAD	mg/L	0.013		0.01	U	0.01	U	0.01	U	0.01 L	J	0.0083 J		0.01	U	0.01	U	0.01	U
SW6010	MAGNESIUM	mg/L	3.1		7		8.3		12		28		4.5		3.9		4.2		14	
SW6010	MANGANESE	mg/L	0.081		0.18		0.21		0.24		0.33		0.078		0.054		0.074		0.14	
SW6010	NICKEL	mg/L	0.0077	J	0.027	J	0.033	J	0.027	J	0.019 J		0.0044 J		0.045		0.041		0.014	J
SW6010	POTASSIUM	mg/L	2		24		28		30		120		1.5		29		29		16	
SW6010	RESPIRABLE QUARTZ	μg/L	83000		180000		190000		110000		24000		84000		210000		180000		97000	
SW6010	SELENIUM	mg/L	0.013	J	0.023		0.031		0.032		0.017 J		0.014 J		0.032		0.031		0.025	
SW6010	SILVER	mg/L	0.01	U	0.01	U	0.01	U	0.01	U	0.01 U	J	0.01 U	J	0.01	U	0.01	U	0.01	U
SW6010	SODIUM	mg/L	660		5600		6200		6300		5500		830		7300		8300		6500	
SW6010	THALLIUM	mg/L	0.025	U	0.025	U	0.025	U	0.025	U	0.025 L	J	0.025 U	J	0.025	U	0.025	U	0.025	U
SW6010	VANADIUM	μg/L	160		630		760		620		97		160		1100		1100		340	
SW6010	ZINC	μg/L	14	J	11	J	11	J	12	J	12 J	2	20 U	J	14	J	14	J	16	J
SW7470	MERCURY	μg/L	4.5		55		74		33		0.52		3.1		99		89		11	
SW9040	pH	S.U.	6.58	Н	7.81		7.75		7.2	Н	7.08		6.49		8.78	Н	8.26	Н		Н
SW9056	CHLORIDE	mg/L	1400		18000		17000		16000		18000		1700		24000		25000		13000	+
SW9056	SULFATE	mg/L	100	U	930	1	940		920		100 L	T	100 U	T	1400		1300		670	+

Analytical Lab was TestAmerica Savannah (5102 LaRoche Avenue, Savannah, GA 31404)

Qualifiers: U Indicates the analyte was analyzed for but not detected.

Result is less than the RL but greater than or equal to the MDL and the concentration is an approximate value. Sample was prepped or analyzed beyond the specified holding time Field parameter with a holding time of 15 minutes

Duplicate RPD exceeds the old roll limit

Η

HF

Compound was found in the blank and sample

# APPENDIX F. DERIVATION OF STORATIVITY TERM TO INCLUDE CO<sub>2</sub> EXPANSION

The storativity of a confined, semi-confined, or an unconfined aquifer during early-time behavior (before the onset of delayed gravity drainage) is attributable to two mechanisms—aquifer compression and water expansion. The equation for conventional storativity attributable to these two mechanisms is given by Walton (1970):

```
water expansion term aquifer compression term S = \eta \gamma m \beta + \alpha \gamma m Where: S = storativity \eta = porosity \gamma = unit weight of water m = aquifer thickness \beta = water compressibility \alpha = aquifer compressibility
```

Storativity is defined as the volume of water that an aquifer releases from storage per unit area of aquifer per unit decline in hydraulic head (Freeze and Cherry, 1979; Fetter, 2001). The concept of storativity ism illustrated in Figure A-1. When the potentiometric surface or a unit area of aquifer is reduced by a unit amount, the water within that volume of the aquifer expands. The aquifer also undergoes compression, which also releases water from storage. This is best conceptualized by considering Terzaghi's Law, a fundamental equation of geotechnical engineering:

$$\partial_T = \partial_E + p$$
  
Where: $\partial_T = \text{Total stress}$   
 $\partial_E = \text{Effective stress}$   
 $p = \text{Pore pressure}$ 

Lowering the potentiometric surface on an aquifer reduces the pore pressure in Terzaghi's Law by a unit amount. The equation dictates that to maintain equality and support the total stress imposed by the weight of the overburden, the effective stress must be increased by a like amount. The effective stress is the stress borne by the aquifer skeleton. As this stress increases, the aquifer is subject to an elastic compression as the sand and other soil particles are packed together more tightly. As the aquifer compresses, water is released from storage.

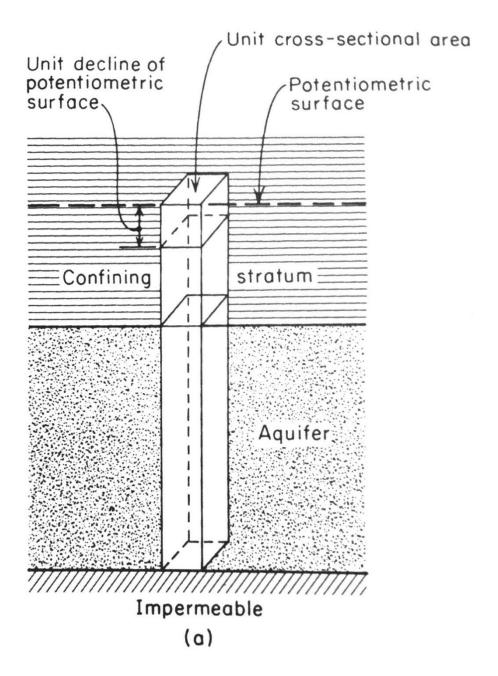


Figure A-1:

If the volume of aquifer affected by a change in potentiometric surface contains a residual saturation of a gas, like CO<sub>2</sub>, then the gaseous phase will also undergo expansion. The resultant gas expansion will increase the partial saturation of the gas at the expense of the water saturation. In other words, as the gas expands, it will decrease water saturation and release water from storage in the aquifer. We can derive an expanded storativity equation to take into account the presence of a residual saturation of a gas, such as CO<sub>2</sub>, in the aquifer. The derivation makes the following assumptions:

- 1. The gas acts an Ideal Gas
- 2. The temperature of the gas remains constant

3. Changes in aqueous-phase hydraulic head will produce identical changes in gaseous-phase pressure head as the capillary pressure between the aqueous-phase and the gaseous phase remains constant.

The Ideal Gas Law (Mortimer, 1967) states the following:

PV = nRT

Where: P = pressure

V = volume

n = number of moles of gas

R = constant

T = temperature

Solving for the volume, V, we see that if all other terms remain equal, the volume of gas is inversely proportional to the pressure.

$$V = \frac{nRT}{P}$$

Therefore, the change in the initial volume of a gas is proportional to the change in pressure and inversely proportional to the initial pressure, as follows:

$$\Delta V = \frac{\Delta P V_i}{P_i}$$

Where:  $\Delta V$  = change in volume

 $\Delta P$  = change in pressure

 $V_i$  = Initial volume

P<sub>i</sub> = Initial pressure

:

Since  $\Delta P$ , in this case, equals the drawdown in the aquifer(s), the equation can be re-written as:

$$\Delta V = \frac{sV_i}{P_i}$$

The initial volume of gas in the unit area of aquifer illustrated in Figure A-1 can be defined as follows:

$$V_i = s_{CO_2} nm$$

Where:  $s_{CO_2}$  = saturation of  $CO_2$  in the pore spaces

n = total porosity

m = aquifer thickness

Substituting, this term into the above equation for  $\Delta V$ , we derive the following term for storativity associated with residual gas expansion:

$$\Delta V = \frac{s_{CO_2} nms}{P_i}$$

The expanded storativity equation is given below:

$$S = \underbrace{(n - s_{CO_2})\eta\gamma m\beta}_{\text{aquifer compression term}} + \underbrace{\frac{cO_2 \text{ expansion term}}{s_{CO_2} nms}}_{\text{p,total}} + \underbrace{\frac{s_{CO_2} nms}{h_{p,total}}}$$

Where :  $s_{CO_2}$  = residual saturation of  $CO_2$ 

s = drawdown

 $h_{p,total} = total pressure head including atm p$ 

In the above equation, the water expansion term has been modified by changing the total porosity ( $\eta$ ) to the water-filled saturation (n – sco2) to properly reflect the fact that CO<sub>2</sub> occupies a portion of the total porosity. However, because the water expansion term is de minimis compared to the CO<sub>2</sub> expansion term, the equation can be simplified by using the total porosity in this term without sacrificing any significant accuracy, as shown below:

$$S = n\gamma m\beta + \alpha\gamma m + \frac{s_{CO_2}nms}{h_{p,total}}$$

# APPENDIX G. MONITORING RESULTS (3 MONTHS AFTER CONCLULSION OF SPARGING)

#### Introduction

Mutch Associates, LLC, in collaboration with Parsons Corporation (Parsons), have prepared this appendix describing the analytical results of the second post-sparge monitoring for the CO<sub>2</sub> sparging Proof of Concept test conducted at the LCP Chemical Site in Brunswick, Georgia. The Proof of Concept test was conducted in accordance with the "Final Work Plan for CO<sub>2</sub> Sparging Proof of Concept Test, LCP Chemical Site, Brunswick, GA" (Mutch Associates, 2012) dated September 11, 2012. The Proof of Concept test was designed to evaluate the feasibility of CO<sub>2</sub> sparging to remediate a sub-surface caustic brine pool (CBP) formed by historical production of industrial chemicals on the site. The purpose of the post-sparge sampling events are to assess any rebound in pH and other constituents of concern.

This appendix describes the results of the second of three post-sparge monitoring events that occurred on February  $4^{th}$  and  $5^{th}$  of 2013. The first post-sparge monitoring event occurred approximately one week after the end of the sparging on November  $26^{th} - 28^{th}$ , 2012. The third and final event is scheduled to take place 6 months after the end of sparging, in May 2013.

## **Groundwater Sampling**

In accordance with the workplan, five out of 13 monitoring wells were selected for rebound monitoring pending the outcome of pH and geochemistry results from the first post-sparging sampling round. The wells selected were SW-1, MW-1C, MW-2C, MW-519B and MW-115C. MW-1C was selected to serve as a field duplicate bringing the total number of samples to six.

The five monitoring wells were purged and sampled using the low flow "Tubing-in-Screened-Interval" method, pursuant to US EPA Region IV Environmental Investigations Standard Operating Procedure (SOP) – October 2011. The guidance document *Groundwater Sampling Guidelines for Superfund and RCRA Project Managers* was also referenced for additional technical support. Per the method, the tubing intake was lowered to the middle of the screened interval of the well, and a peristaltic pump was used to purge the groundwater at a very low flow rate. Throughout the purge process, depth to water measurements were collected to assess and maintain stable drawdown. A minimum one equipment volume was purged prior to stabilization parameters (pH, specific conductivity, dissolved oxygen, and turbidity) being collected. Although not considered stabilization parameters, temperature and oxidation reduction potential were also recorded. The field sampling logs are included as Appendix A to this report. Once the required parameters were stable for three consecutive readings, groundwater samples were collected for laboratory analysis as described in Table 3-2 of the Proof of Concept Report. The groundwater samples were preserved on ice and submitted to TestAmerica Laboratories in Savannah, GA for analysis. Once the groundwater samples had been collected, approximately 900 mL of groundwater were pumped into a graduated cylinder and the specific gravity was determined using a hydrometer.

### **Sampling Results**

A summary of the results from the groundwater analysis is presented in Table G-1. All of the analytical data from TestAmerica and the well purge logs are provided at the end of this Appendix.

Table G-1: Sun	Table G-1: Summary of field and lab results from 3 month post-sparge sampling													
	SW-1	MW-1C	MW-1C (duplicate)	MW-2C	MW- 519B	MW-115C								
pH (field)	6.72	6.88	-	8.93	8.67	11.73								
pH (lab)	6.86	7.19	7.19	8.58	8.22	10.7								
Hg (µg/L)	4.2	44	42	41	68	110								
As (μg/L)	9.5 J	23	19 J	34	120	180								
Cr (µg/L)	110	420	410	290	440	340								
V (µg/L)	150	680	670	730	1100	1500								
Si (mg/L)	83	78	78	130	82	2,000								
Specific gravity	1.015	1.034	-	1.026	1.037	1.028								

A comparison of these results to the pre-sparge and post-sparge monitoring events are shown in Table G-2 for pH, Hg, As and Cr and in Figure G-1 for pH and Hg. Note that all pH data presented in Figure G-1 is for water collected at the midpoint of the well screen.

## Changes in pH

The two sparge wells (MW-1C and SW-1) both held their pH values (pH < 7.0) from the November (post-sparge) sampling event. With respect to the two monitoring wells that are within the 20 ft ROI (MW-519B and MW-2C), one well (MW-2C) decreased from 10.08 to 8.93 (midpoint of screen); the other (MW-519B) stayed steady near pH 8.7 (midpoint of screen). Values for pH of both of these wells are well below the 10.5 threshold stated in the AOC. The decrease observed in MW-519B may be the result of the continual dissolution of residual saturation of CO<sub>2</sub> into the water. MW-115C returned to pre-sparge pH values based on the field pH value (the laboratory pH value was 10.7). This well is ~25 ft away from MW-1C. This pH rebound is not a complete surprise based on its distance from the sparge well, and our inability to move its pH downward below pH 10 during sparging.

#### **Changes in Mercury Concentrations**

Among the two sparge wells (MW-1C and SW-1), SW-1 saw a decrease in Hg from 11 to 4.4  $\mu$ g/L, while MW-1C saw an increase from 21 to 44  $\mu$ g/L. The average percent removal of Hg in these two wells (relative to pre-sparge concentrations) is 78%. This is down only slightly from the average 85% removal observed after the first post-sparge monitoring event. With respect to the two monitoring wells that are within the 20 ft ROI (MW-519B and MW-2C), both showed decreases in Hg relative to the first post-sparge event. MW-519B decreased from 99 to 68  $\mu$ g/L (midpoint of screen), while MW-2C decreased from 64.5 to 41  $\mu$ g/L (midpoint of screen). MW-115C which was relatively unaffected by sparging showed no change in Hg concentrations and has held steady at 110  $\mu$ g/L since before the Proof of Concept Test began.

Table G-2: St	ummary of field and	d lab results from 3 month p	ost-sparge sampling
рН	Pre-sparge (a)	Post-sparge (1 week after sparging) (b)	Post-sparge (3 mo. after sparging) (c)
SW-1	11.6 mid	6.66 mid	6.72 mid
MW-1C	11.61 mid	6.86 mid	6.88 mid
MW-2C	11.78 mid	7.96 top / 10.08 mid	8.93 mid
MW-519B	11.91 mid	8.68 top / 8.73 mid	8.67 mid
MW-115C	11.18 mid	9.97 mid	11.73 mid
Hg	Pre-sparge (d)	Post-sparge (1 week after sparging)	Post-sparge (3 mo. after sparging)
SW-1	110 mid	11 mid	4.4 mid
MW-1C	110 mid	21 mid	44 mid
MW-2C	110 mid	33 top / 64.5 mid	41 mid
MW-519B	120 mid	89 top / 99 mid	68 mid
MW-115C	120 mid	110 mid	110 mid
As	Pre-sparge (d)	Post-sparge (1 week after sparging)	Post-sparge (3 mo. after sparging)
SW-1	-	45 mid	9.5 mid
MW-1C	320 mid	120 mid	23 mid
MW-2C	260 mid	26 top / 44 mid	24 mid
MW-519B	390 mid	130 top / 170 mid	120 mid
MW-115C	280 mid	98 mid	180 mid
Cr	Pre-sparge (d)	Post-sparge (1 week after sparging)	Post-sparge (3 mo. after sparging)
SW-1	-	200 mid	110 mid
MW-1C	500 mid	320 mid	420 mid
MW-2C	370 mid	300 top / 320 mid	290 mid
MW-519B	610 mid	390 top / 380 mid	440 mid
WI W -3 1 9 D	340 mid	340 mid	340 mid

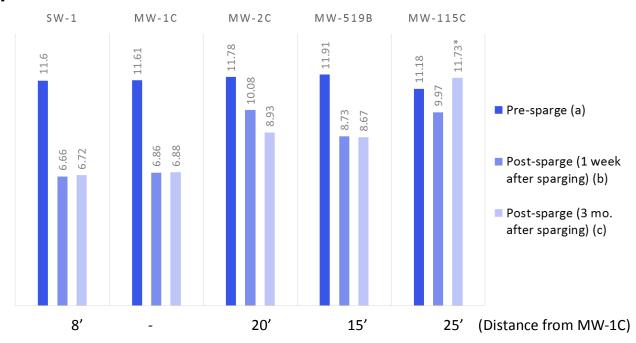
#### Notation:

mid – indicates sample was collected from midpoint of well screen

- (a) pH values are from field measurements made prior to the start of sparging on October 28, 2012.
- (b) Values from field measurements made at the end of the continuous monitoring period on November
- (c) Values are from Parsons field purge logs from February 4-5, 2012 (Appendix A). (d) Values are from laboratory; sampling event occurring on October 1<sup>st</sup> to 3<sup>rd</sup>, 2012.

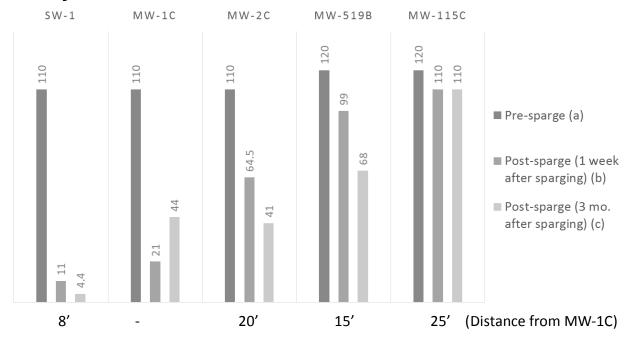
top – indicates sample was collected from top of well screen

# рΗ



\* MW-115C had a post-sparge (3 mo.) laboratory pH that was significantly lower than the field reading (10.7)

# Mercury



**Figure G-1:** Summary of pre and post sparge monitoring results for pH and Hg. All data is from the midpoint of the well screen.

## **Changes in Arsenic and Chromium Concentrations**

Arsenic concentrations in all of the deep Satilla wells within 20 feet of MW-1C decreased from the 1 month post-sparge sampling to the 3 month post-sparge sampling. As a result, the average percent removal of As increased from 65% to 83% for MW-1C, MW-2C and MW-519B. Average chromium concentrations were essentially unchanged in deep Satilla wells in going from the 1 month to the 3 month post-sparge sampling.

#### **Conclusions**

These results show that changes in aquifer geochemistry since the post-sparge monitoring event have been mostly small, with some evidence of lower pH, Hg and As concentrations in select wells within the 20 ft ROI of CO<sub>2</sub> sparging. Downward movement of pH during the last 3 months of sparging inactivity at the site may be the result of dissolution of residual CO<sub>2</sub> saturation into groundwater. The only well which saw significant rebound was MW-115C which was greater than 25 ft from MW-1C and is not inside the 20 ft ROI.

# **Analytical Data from 3-month Post Sparge Monitoring Event**

					MW-1C-		MW-1C#2-				MW-2C-MID-		MW-115C-		MW-519B-	
		Field Sample ID	EQB-020413		020413		020413		SW-1-020413		020413		020413		MID-020413	
			Equipment													
		Location	Blank		MW-1C		MW-1C#2		SW-1		MW-2C-MID		MW-115C		MW-519B-MID	
		Sample Date	2/4/2013		2/4/2013		2/4/2013		2/4/2013		2/4/2013		2/4/2013		2/4/2013	
		SDG	680-87157-1		680-87157-1		680-87157-1		680-87157-1		680-87157-1		680-87157-1		680-87157-1	
		Matrix	WATER		WATER		WATER		WATER		WATER		WATER		WATER	
		Sample Purpose	Equipment blank		Regular sample		Regular sample		Regular sample		Regular sample		Regular sample		Regular sample	
		Sample Type	Blank water		Ground Water		Ground Water		Ground Water		Ground Water		Ground Water		Ground Water	
Method	Parameter Name	Units														
	ALKALINITY, CARBONATE (AS															
SM2320B	CACO3)	mg/L	5	U	5	U	5	U	5	U	35		97		39	<u> </u>
	BICARBONATE ALKALINITY AS	_														
SM2320B	CACO3	mg/L	5	U	600		610		380		450		340		620	
SM2320B	TOTAL ALKALINITY	mg/L	5	U	600		610		380	1	490		450		660	
SM2540C	TOTAL DISSOLVED SOLIDS	mg/L	16	11.11	42,000	1.11	42,000	177	19,000		33,000	111	35,000	1117	41,000	
SM3500-FeD	FERROUS IRON	μg/L	100	U, HF	7,300	HF	7,600	HF	8,100		1,100	HF	1,600	HF	3,300	
SM4500S2-F	SULFIDE	mg/L	1.0	U	22		25		10	U	21		69		41	
SM5310B	DISSOLVED ORGANIC CARBON	mg/L	1.0	U	290		290		170		320		1,300		390	
SM5310B	TOTAL ORGANIC CARBON	mg/L	1.0	U	270	**	280	**	130		290		1,100		460	
SW6010	ALUMINUM	mg/L	0.2	U	0.2		0.2		0.2		0.2	U		U	0.2	
SW6010	ANTIMONY	μg/L	0.02	U	0.02	U	0.02	U	0.02	U	0.037		0.011	J	0.025	
SW6010	ARSENIC	mg/L	0.02	U	0.023		0.019	J	0.0095	J	0.034		0.18		0.12	
SW6010	BARIUM	mg/L	0.01	U	0.230	_	0.230	_	0.200		0.089		0.026		0.16	
SW6010	BERYLLIUM	mg/L	0.004	U	0.0033		0.0033	J	0.003	J	0.002	J	0.0015		0.0024	
SW6010	CADMIUM	mg/L	0.005	U	0.0025	J	0.0025	J	0.005	U	0.005	U	0.0021	J	0.0026	
SW6010	CALCIUM	mg/L	0.5	U	29		29		19		11		0.85		18	
SW6010	CHROMIUM	mg/L	0.01	U	0.42		0.41		0.11		0.29		0.34		0.44	
SW6010	COBALT	mg/L	0.01	U	0.01	U	0.01	U	0.01	U	0.01	U	0.0021		0.01	
SW6010	COPPER	mg/L	0.02	U	0.012	J	0.013	J	0.0021	J	0.01	U	0.0018	J	0.014	
SW6010	IRON	mg/L	0.1	U	6.8	**	7.0	**	8.4		0.92		1.2		2.2	
SW6010	LEAD	mg/L	0.01	U	0.01	U	0.01	U	0.01	U	0.01	U	0.01		0.01	
SW6010	MAGNESIUM	mg/L	0.5	U	11		11		14		5.6		0.097		7.7	
SW6010	MANGANESE	mg/L	0.01	U	0.094	-	0.095	_	0.072		0.067	_	0.01	U	0.11	
SW6010	NICKEL	mg/L	0.04	U	0.033	J	0.031	J	0.0078	J	0.033	J	0.067		0.045	
SW6010	POTASSIUM	mg/L	1	U	34		32		10		21		8		29	
SW6010	RESPIRABLE QUARTZ	μg/L	0.5	U	78,000		78,000		83,000		130,000		2,000,000		82,000	
SW6010	SELENIUM	mg/L	0.02	U	0.032		0.036		0.032		0.031		0.034		0.04	
SW6010	SILVER	mg/L	0.01	U	0.01	U	0.01	U	0.01	U	0.01	U	0.01	U	0.01	
SW6010	SODIUM	mg/L	0.76	J	14,000	**	14,000	**	6,800		13,000		12,000		16,000	
SW6010	THALLIUM	mg/L	0.025	U	0.025	U	0.025	U	0.025	U	0.025	U	0.025	U	0.025	U
SW6010	VANADIUM	μg/L	0.01	U	0.68	т.	0.67		0.15		0.73		1.5		1.1	
SW6010	ZINC	μg/L	0.02	U	0.015	J	0.016	J	0.0096	J	0.024		0.023		0.023	
SW7470	MERCURY	μg/L	0.20	U	44		42	17	42		41		0.11		68	
SW9040	pH	S.U.	6.26	H	7.19	Н	7.19	Н	6.86	Н	8.58		10.7		8.22	_
SW9056	CHLORIDE	mg/L	5.0	U	21,000		22,000		9,000	-	19,000		17,000		21,000	
SW9056	SULFATE	mg/L	5.0	U	1,400		1,400		330		920		1,000		1,400	

Analytical Lab was TestAmerica Savannah (5102 LaRoche Avenue, Savannah, GA 31404)

Qualifiers: Indicates the analyte was analyzed for but not detected.

Result is less than the RL but greater than or equal to the MDL and the concentration is an approximate value. Sample was prepped or analyzed beyond the specified holding time Field parameter with a holding time of 15 minutes Duplicate RPD exceeds the control limit

Н

HF

			GR	OUND	WATE	ER SAM	MPL	ING	LOG				
SITE NAME: <b>LC</b> I	P Chemical Sit	te			SI'	TE OCATION: <b>Bru</b>	ınswick	, GA					
WELL NO:	MW-1C			SAMPLE	ID: MW-1C					DATE: <b>2/4/2013</b>			
				II.	PURG	SING DA	TA						
WELL		TUBING	-		L SCREEN	INTERVAL	S	TATIC D			_	GE PUMP T	YPE
DIAMETER	R (inches): 2	DIAME	TER (inches): 1/	4 DEP	TH(ft btoc):	48.5 to 53.5	Т	O WATE	R (ft btoc): 10.5	5	OR B	AILER: PP	
EQUIPMEN	NT VOLUME P		s (0.0026 ga					NGTH) + 27 gallon	FLOW CELL VO	OLUME			
	MP OR TUBIN	-	FINAL PUMF			PURGIN	-		PURGING			TOTAL VOI	-
DEPTHIN	WELL (ft btoc)		DEPTH IN W	DEPTH	50.5	INITIATE	DAI:	1349	ENDED AT:	1540		PURGED (g	gallons): 3.0
TIME	VOLUME PURGED (gallons)	CUMUL. VOLUME PURGED (gallons)	PURGE RATE (gpm)	TO WATER (feet btoc)	pH (standard units)	TEMP. (°C)		OND. /cm)	DISSOLVED OXYGEN (% saturation)	(NI	BIDITY TUs)	ORP (mV)	
1405	0.3	0.3	0.05	10.79	6.89	20.43	59	.87	15.3	3	1.1	102.6	6
1414	0.3	0.6	0.03	10.72	6.90	20.24	59	.72	8.6	2	8.0	20.4	
1432	0.3	0.9	0.02	10.73	6.88	19.41	60	.03	6.1	1	8.4	-36.8	3
1439	0.3	1.2	0.04	10.74	6.87	19.63	60	.22	4.0	1	4.6	-37.8	3
1454	0.3	1.5	0.02	10.68	6.88	19.83	60	.60	4.4	1	1.9	-50.4	ļ.
1505	0.3	1.8	0.03	10.67	6.89	20.08	60	.62	3.4	1	3.2	-62.0	)
1521	0.6	2.4	0.04	10.79	6.88	20.15	60	.72	2.6	1	0.3	-71.5	5
1531	0.3	2.7	0.03	10.79	6.88	19.99	60	.61	2.4	9	.83	-73.1	
1539	0.3	3.0	0.04	10.79	6.88	20.13		.62	2.3		0.2	-71.1	1.034
TUBING IN		<b>PACITY</b> (Gal./F	<b>0.75"</b> = 0.02; Ft.): <b>1/8"</b> = 0.00 low top of casing			<b>1/4"</b> = 0.002		= 0.37; <b>/16"</b> = 0.0	<b>4"</b> = 0.65; 004; <b>3/8"</b> = 0	<b>5"</b> = 1.0		<b>6"</b> = 1.47; = 0.010;	<b>12</b> " = 5.88 <b>5/8</b> " = 0.016
PURGING	EQUIPMENT (	CODES: B	= Bailer; BI	P = Bladder P		SP = Electric		sible Pur	np; <b>PP</b> = P	eristaltic	Pump	; <b>O</b> = O	ther (Specify)
0.11451.55	D) ( (DDINET) ( A		1.0			LING DA	ATA		1			1	
	BY (PRINT) / A e Jaynes/F			SAMPLER(S)	yno				SAMPLING INITIATED A	T: <b>1548</b>		SAMPLIN ENDED A	
PUMP OR DEPTH IN	TUBING WELL (feet): <b>5</b>	60.5		UBING MATERIAL CO	DDE: <b>Teflon</b>	-lined PE			FILTERED: You Equipment Ty				R SIZE: <u>0.45</u> μm
FIELD DEC	CONTAMINATIO	ON: PUM	IP Y <b>No</b>		TUBING	Yes N	lo (repl	aced)	DUPLICATE	<u> </u>		Yes	
SAME	PLE CONTAINE	ER SPECIFICA	ATION		SAMPLE PF	RESERVATIO	N		INTEND			AMPLING	Additional
SAMPLE ID CODE	# CONTAINERS	MATERIAL CODE	VOLUME F	PRESERVATI USED		TOTAL VOL D IN FIELD (r	mL)	FINAL pH	ANALYSIS A METHO	DD		UIPMENT CODE	Comments
N/N/_		1					1		6010B T	ΓΔΙ	1		

	ne Jaynes/F			C/ay	`='		SAMPLING INITIATED AT: <b>1548</b>		SAMPLING ENDED AT: 1629	
PUMP OR DEPTH IN	R TUBING I WELL (feet): <b>5</b>	0.5		TUBING MATERIAL CODE:	Teflon-lined PE		FILTERED: Yes <b>SM 4500 Sulfide</b> FILTER SIZE: <u>0.45 </u> µm n Equipment Type: In-line filter			
FIELD DE	CONTAMINATIO	ON: PUI	MP Y	No T	UBING Yes <b>No (r</b> e	eplaced)	DUPLICATE:			
SAM	IPLE CONTAINE	ER SPECIFIC	ATION	SAM	IPLE PRESERVATION		INTENDED	SAMPLING	Additional	
SAMPLE ID CODE	# CONTAINERS	MATERIAL CODE	VOLUME	PRESERVATIVE USED	TOTAL VOL ADDED IN FIELD (mL)	FINAL pH	ANALYSIS AND/OR METHOD	EQUIPMENT CODE	Comments	
MW- 1C	1	PE	250mL	HNO3			6010B TAL Metals/ 7470A Hg	APP		
MW- 1C	1	PE	125mL				3500 FE/ 9040B pH	APP		
MW- 1C	1	PE	250mL				6010B Dissolved Silica	APP		
MW- 1C	1	PE	125mL				9056A_28D Chloride & Sulfate	APP		
MW- 1C	1	AG	125mL				SM 5310 DOC	APP		
MW- 1C	2	PE	250mL	NaOH Zinc Acetate			SM4500 Sulfide	APP	Field-Filtered	
MW- 1C	1	PE	500mL			-	2540C TDS	APP		
MW- 1C	1	PE	250mL				2320B Alkalinity	APP		
MW- 1C	1	AG	125mL	HCI			SM5310 TOC	APP		

REMARKS: Purge rate variability due to decreasing pump battery and the associated manual adjustments made to the pump RPM. Per SOP, parameters stable for three readings prior to sample collection; turbidity +/-10%. Tubing-in-Screen Interval purge method utilized. Purge water clear brown with very slight odor. The odor was stronger at the time of sample collection. Minimal air/CO2 bubbles noted in tubing.

MATERIAL CODES: AG = Amber Glass; CG = Clear Glass; PE = Polyethylene; PP = Polypropylene; S = Silicone; T = Teflon; O = Other (Specify)

SAMPLING EQUIPMENT CODES: APP = After Peristaltic Pump; B = Bailer; BP = Bladder Pump; ESP = Electric Submersible Pump; SM = Straw Method (Tubing Gravity Drain); O = Other (Specify)

NOTES: Stabilization Criteria for Range of Variation of Last Three Consecutive Readings:-pH:  $\pm$  0.1 unit Specific Conductance:  $\pm$  5% Dissolved Oxygen: all readings  $\leq$  10% saturation; optionally,  $\pm$  0.2 mg/L Turbidity: all readings  $\leq$  10 NTU; or  $\pm$  10%

SITE		SITE						
NAME: LCP Chemical Site		LOCATION: Brunswick, GA						
WELL NO: MW-2C	SAMPLE ID: MW	1-2C- <b>MID</b>	DATE: <b>2/5/2013</b>					

## PURGING DATA

					PURG	SING DA	IA					
WELL DIAMETER	(inches): 2	TUBING DIAMET	ER (inches): 1/		ELL SCREEN   PTH (ft btoc):		STATIC I TO WAT	DEPTH ER (ft btoc): <b>9.55</b>	_	PURGE PUMP TYPE OR BAILER: <b>PP</b>		
EQUIPMEN	IT VOLUME PU	JRGE: 1 EQUI = (	PMENT VOL. (0.0026 gallo				ING LENGTH) + = <b>0.27 gallo</b> n	FLOW CELL VO s	LUME			
INITIAL PUMP OR TUBING DEPTH IN WELL (feet btoc ): 50.5  FINAL PUMP OF DEPTH IN WELL								PURGING ENDED AT:	1140	TOTAL VOLUME PURGED (gallons): 1.55		
TIME	VOLUME PURGED (gallons)	CUMUL. VOLUME PURGED (gallons)	PURGE RATE (gpm)	DEPTH TO WATER (feet btoc)	pH (standard units)	TEMP. (°C)	SP COND. (mS/cm)	DISSOLVED OXYGEN (% saturation)	TURBIDIT (NTUs)	_	SP Gravity (sg)	
0941	0.5	0.5	0.01	11.21	8.38	14.79	47.95	2.0	20.7	-336.1		
1004	0.25	0.75	0.01	11.53	8.81	16.74	49.06	1.0	21.0	-331.6		
1038	0.25	1.0	0.007	11.70	8.73	17.29	48.58	0.7	18.4	-305.1		
1105	0.2	1.2	0.007	11.71	8.79	18.20	48.41	0.7	17.4	-327.8		
1110	0.03	1.23	0.006	11.71	8.78	18.27	48.32	0.5	17.8	-339.0		
1115	0.02	1.25	0.004	11.71	8.73	18.38	48.11	0.7	15.7	-298.3		
1126	0.15	1.4	0.01	11.98	8.70	18.80	47.73	0.7	15.2	-339.4		
1133	0.1	1.5	0.01	11.92	8.89	19.10	47.86	0.6	13.8	-370.6		
1138	0.05	1.55	0.01	11.88	8.93	19.04	48.27	0.6	13.5	-344.0	1.026	
<b>TUBING IN</b>	SIDE DÌA. CAF	s Per Foot): 0. PACITY (Gal./Fi sing – feet belo	t.): <b>1/8"</b> = 0.0	006; <b>3/16</b>	<b>"</b> = 0.0014;	<b>1/4"</b> = 0.002			5" = 1.02; .006; <b>1/2</b>		= 5.88 = 0.016	
PURGING I	EQUIPMENT C	ODES: B	Bailer; B	P = Bladder	Pump; <b>E</b>	SP = Electric	Submersible Pu	ımp; <b>PP</b> = Pe	eristaltic Pum	np; <b>O</b> = Other	(Specify)	

#### SAMPLING DATA

	BY (PRINT) / A B Jaynes/F			SAMPLER(S) SIGN	NATURE(S):	SAMPLING INITIATED AT: 1151		SAMPLING ENDED AT: Not Recorded			
PUMP OR T DEPTH IN V	UBING VELL (feet): <b>5</b> :	3.5		TUBING MATERIAL CODE:	Teflon-lined PE		FILTERED: Yes/ <b>SM 4500 Sulfide</b> FILTER SIZE: <u>0.45</u> µr n Equipment Type: <b>In-line filter</b>				
FIELD DEC	ONTAMINATIO	ON: PU	MP Y	No T	UBING Y <b>No (rep</b>	laced)	DUPLICATE:	No			
SAMP	LE CONTAINE	ER SPECIFIC	CATION	SAM	IPLE PRESERVATION		INTENDED	SAMPLING			
SAMPLE ID CODE	# CONTAINE RS	MATERIAL CODE	VOLUME	PRESERVATIVE TOTAL VOL ADDED IN FIELD (mL)		FINAL pH	ANALYSIS AND/OR METHOD	EQUIPMENT CODE	Additional Comments		
MW-2C- MID	2	PE	250mL	HNO3			6010B TAL Metals/7470A Hg	APP			
MW-2C- MID	2	PE	125mL				3500 FE/ 9040B pH	APP			
MW-2C- MID	2	PE	250mL				6010B Dissolved Silica	APP			
MW-2C- MID	2	PE	125mL				9056A_28D Chloride & Sulfate	APP			
MW-2C- MID	2	AG	125mL				SM 5310 DOC	APP			
MW-2C- MID	4	PE	250mL	NaOH Zinc Acetate			SM4500 Sulfide	APP	Field-Filtered		
MW-2C- MID	2	PE	500mL				2540C TDS	APP			
MW-2C- MID	2	PE	250mL	L			2320B Alkalinity	APP			
MW-2C- MID	2	AG	125mL	HCI			SM5310 TOC	APP			

REMARKS: Purge paused at 0823 and again at 0914. Parameters **not** stable prior to sample collection: pH >+/- 0.1 SU; turbidity >10 NTU. However, based on the water level, the sample was believed to be indicative of the water at the screen interval and not stagnant water in the well casing. Tubing–in-Screen-Interval purge method utilized. Purge water clear, brown odor noted.

MATERIAL CODES: AG = Amber Glass; CG = Clear Glass; PE = Polyethylene; PP = Polypropylene; S = Silicone; T = Teflon; O = Other (Specify)

SAMPLING EQUIPMENT CODES: APP = After Peristaltic Pump; B = Bailer; BP = Bladder Pump; ESP = Electric Submersible Pump; RFPP = Reverse Flow Peristaltic Pump; SM = Straw Method (Tubing Gravity Drain); O = Other (Specify)

SITE NAME: LCP Chemical Site		SITE LOCATION: <b>Brunswick</b> , <b>GA</b>	
WELL NO: MW-115C	SAMPLE ID: MW	/-115C	DATE: <b>2/5/2013</b>

## **PURGING DATA**

WELL	TUBING			LL SCREEN I		STATIC I		PURGE PUMP TYPE		
DIAMETER (inches): 2	DIAME	TER (inches): 1	<b>14</b> DEF	PTH (ft btoc):	43.5 to 45	TO WATE	ER (feet btoc): 8.40	OR E	BAILER: <b>PP</b>	
EQUIPMENT VOLUM						ING LENGTH) + llons = <b>0.26 g</b>	FLOW CELL VOL	UME		
INITIAL PUMP OR TU DEPTH IN WELL (feet		FINAL PUMI DEPTH IN V	/ELL (feet bto	-	PURGIN INITIATE	IG ED AT: <b>1012</b>	PURGING ENDED AT: 1	1326	TOTAL VOLUME PURGED (gallons): 2.5	
TIME VOLUM PURGE (gallons	PURGED	PURGE RATE (gpm)	DEPTH TO WATER (feet btoc)	pH (standard units)	TEMP. (°C)	SP COND. (mS/cm)	DISSOLVED OXYGEN (% saturation)	TURBIDIT (NTUs)	Y ORP (mV)	SP Gravity (sg)
1205 0.8	0.8	0.019	9.85	11.24	20.00	50.44	1.0	4.16	-378.3	
1210 0.2	1.0	0.04	10.15	11.11	20.19	50.41	0.8	4.71	-384.9	
1218 0.2	1.2	0.025	10.13	11.20	20.51	50.38	0.6	3.85	-390.4	
1228 0.1	1.3	0.01	10.10	11.42	20.93	50.53	0.8	4.16	-401.5	
1233 0.15	1.45	0.03	10.20	11.39	20.85	50.44	0.8	248	-396.3	
1244 0.2	1.65	0.018	10.33	11.41	20.69	50.46	0.7	16.5	-412.3	
1252 0.25	1.9	0.006	10.46	11.38	21.02	50.41	0.7	30.9	-409.2	
1305 0.25	2.15	0.019	10.10	11.47	21.07	50.41	0.6	7.90	-391.3	
1311 0.1	2.25	0.016	10.10	11.69	21.19	50.47	0.7	3.25	-400.7	
1317 0.15	2.4	0.025	10.10	11.77	21.04	50.51	0.6	2.95	-421.6	
1323 0.1	2.5	0.017	10.07	11.73	21.05	50.50	0.5	3.25	-413.9	1.028
WELL CAPACITY (Gallons Per Foot): 0.75" = 0.02; 1" = 0.04; 1.25" = 0.06; 2" = 0.16; 3" = 0.37; 4" = 0.65; 5" = 1.02; 6" = 1.47; 12" = 5.88  TUBING INSIDE DIA. CAPACITY (Gal./Ft.): 1/8" = 0.0006; 3/16" = 0.0014; 1/4" = 0.0026; 5/16" = 0.004; 3/8" = 0.006; 1/2" = 0.010; 5/8" = 0.016  BTOC = Below top of casing – feet below top of casing which includes above grade riser										
PURGING EQUIPMEN	IT CODES: B	= Bailer; B	P = Bladder I	Pump; E	SP = Electric	Submersible Pu	ımp; <b>PP</b> = Peı	ristaltic Pump	o; <b>O</b> = Other	(Specify)

#### **SAMPLING DATA**

	BY (PRINT) / A ne Jaynes/P			SAMPLER(S) SIGN	` '		SAMPLING INITIATED AT: 1330	SAMPLII <b>1405</b>		
PUMP OR DEPTH IN	TUBING WELL (feet): 4	4.25		TUBING MATERIAL CODE:	Teflon-lined PE		FILTERED: Yes/ <b>SM 4500 Sulfide</b> FILTER SIZE: <u>0.45 µm</u> n Equipment Type: <b>In-line filter</b>			
FIELD DE	CONTAMINATIO	ON: PU	MP Y	No T	UBING Y <b>No (rep</b>	laced)	DUPLICATE: No			
SAM	IPLE CONTAINE	R SPECIFIC	ATION	SAM	IPLE PRESERVATION		INTENDED	SAMPLING	Additional	
SAMPLE ID CODE	# CONTAINERS	MATERIAL CODE	VOLUME	PRESERVATIVE USED	TOTAL VOL ADDED IN FIELD (mL)	FINAL pH	ANALYSIS AND/OR METHOD	EQUIPMENT CODE	Comments	
MW- 115C	1	PE	250mL	HNO3			6010B TAL Metals/7470A Hg	APP		
MW- 115C	1	PE	125mL				3500 FE/ 9040B pH	APP		
MW- 115C	1	PE	250mL				6010B Dissolved Silica	APP		
MW- 115C	1	PE	125mL				9056A_28D Chloride & Sulfate	APP		
MW- 115C	1	AG	125mL				SM 5310 DOC	APP		
MW- 115C	2	PE	250mL	NaOH Zinc Acetate			SM4500 Sulfide	APP	Field-Filtered	
MW- 115C	1	PE	500mL				2540C TDS	APP		
MW- 115C	1	PE	250mL				2320B Alkalinity	APP		
MW- 115C	1	AG	125mL	HCI			SM5310 TOC	APP		

REMARKS: Purge paused with 0.5 gallons purged at 1034; purge continued at 1144. Difficulty stabilizing the water level due in part to the pump RPM slowing down. The pump was switched out after the 1252 reading. Per SOP, parameters stable for three readings prior to sample collection. Tubing—in-Screen-Interval purge method utilized. The turbidity reading of 248 NTU is believed to be the result of a precipitate noted in the sample cell.

 $\textbf{MATERIAL CODES}: \qquad \textbf{AG} = \textbf{Amber Glass}; \qquad \textbf{CG} = \textbf{Clear Glass}; \qquad \textbf{PE} = \textbf{Polyethylene}; \qquad \textbf{PP} = \textbf{Polypropylene}; \qquad \textbf{S} = \textbf{Silicone}; \qquad \textbf{T} = \textbf{Teflon}; \qquad \textbf{O} = \textbf{Other (Specify)}$ 

SAMPLING EQUIPMENT CODES:APP = After Peristaltic Pump;B = Bailer;BP = Bladder Pump;ESP = Electric Submersible Pump;RFPP = Reverse Flow Peristaltic Pump;SM = Straw Method (Tubing Gravity Drain);O = Other (Specify)

SITE NAME: LCP Chemical Site		SITE LOCATION: Brunswick, GA	
WELL NO: MW-519B	SAMPLE ID: MW		DATE: <b>2/5/2013</b>

#### PURGING DATA

					FUNG	IIING DA	17					
WELL DIAMETER	(inches): 2	TUBING	ER (inches): 1/		LL SCREEN I		7 55	-	DEPTH FER (feet btoc): 9	_	RGE PUMP TYPE BAILER: <b>PP</b>	
DIMINETER	(Inchico). Z	DITABLE	Lit (inches). I	7 00	111 (1001 0100	). <b>42.00</b> to 4	1.00	10 11/1	TETT (ICCT DIOC). 3	.10	D/ (ILLIV. I I	
EQUIPMEN	EQUIPMENT VOLUME PURGE: 1 EQUIPMENT VOL. = (TUBING CAPACITY X TUBING LENGTH) + FLOW CELL VOLUME = (0.0026 gallons/foot X 48.55 feet) + 0.13 gallons = 0.26 gallons											
INITIAL PUMP OR TUBING DEPTH IN WELL (feet btoc ): 45.05    DEPTH IN WELL (feet btoc ): 45.05    DEPTH IN WELL (feet btoc ): 45.05    DEPTH IN WELL (feet btoc): 45.05												
TIME	VOLUME PURGED (gallons)	CUMUL. VOLUME PURGED (gallons)	PURGE RATE (gpm)	DEPTH TO WATER (feet btoc)	pH (standard units)	TEMP. (°C)		COND. S/cm)	DISSOLVED OXYGEN (% saturation)	TURBIDIT (NTUs)	ORP (mV)	SP Gravity (sg)
1520	0.7	0.7	0.013	11.77	8.70	22.26	63	3.70	0.9	11.1	-385.4	
1528	0.1	0.8	0.125	11.85	8.73	21.87	63	3.17	0.8	10.4	-388.1	
1535	0.1	0.9	0.014	11.93	8.65	21.90	62	2.90	0.8	10.1	-379.1	
1542	0.1	1.0	0.014	11.95	8.69	21.38	62	2.73	0.6	9.26	-375.9	
1549	0.1	1.1	0.014	11.97	8.67	21.36	62	2.61	0.5	9.81	-378.3	
1555	0.1	1.2	0.016	11.99	8.67	21.38	62	2.53	0.5	8.41	-381.6	1.037
	WELL CAPACITY (Gallons Per Foot): 0.75" = 0.02; 1" = 0.04; 1.25" = 0.06; 2" = 0.16; 3" = 0.37; 4" = 0.65; 5" = 1.02; 6" = 1.47; 12" = 5.88  TUBING INSIDE DIA. CAPACITY (Gal./Ft.): 1/8" = 0.0006; 3/16" = 0.0014; 1/4" = 0.0026; 5/16" = 0.004; 3/8" = 0.006; 1/2" = 0.010; 5/8" = 0.016											

#### SAMPLING DATA

**ESP** = Electric Submersible Pump;

**PP =** Peristaltic Pump;

O = Other (Specify)

BTOC = Below top of casing – feet below top of casing which includes above grade riser

**B** = Bailer;

**BP** = Bladder Pump;

PURGING EQUIPMENT CODES:

					AMIF LING DATA					
SAMPLED BY (PRINT) / AFFILIATION: Christine Jaynes/Parsons				SAMPLER(S) SIGNATURE(S):			SAMPLING INITIATED AT: <b>1601</b>		SAMPLING ENDED AT: Not Recorded	
PUMP OR TUBING DEPTH IN WELL (feet): 45.05							FILTERED: <b>Yes/SM 4500 Sulfide</b> FILTER SIZE: <u>0.45                                    </u>			
FIELD DEC	ONTAMINATIO	ON: PU	MP Y	No T	UBING Y <b>No (repl</b> a	iced)	DUPLICATE:	No		
SAMPLE CONTAINER SPECIFICATION				SAM	PLE PRESERVATION		INTENDED	SAMPLING	Additional	
SAMPLE ID CODE	# CONTAINERS	MATERIAL CODE	VOLUME	PRESERVATIVE USED	TOTAL VOL ADDED IN FIELD (mL)	FINAL pH	ANALYSIS AND/OR METHOD	EQUIPMENT CODE	Comments	
MW- 519B- MID	1	PE	250mL	HNO3	-	-1	6010B TAL Metals/7470A Hg	APP		
MW- 519B- MID	1	PE	125mL				3500 FE/ 9040B pH	APP		
MW- 519B- MID	1	PE	250mL				6010B Dissolved Silica	APP		
MW- 519B- MID	1	PE	125mL				9056A_28D Chloride & Sulfate	APP		
MW- 519B- MID	1	AG	125mL			-	SM 5310 DOC	APP		
MW- 519B- MID	2	PE	250mL	NaOH Zinc Acetate		-	SM4500 Sulfide	APP	Field-Filtered	
MW- 519B- MID	1	PE	500mL		2540C TDS APP					
MW- 519B- MID	1	PE	250mL			1	2320B Alkalinity	APP		
MW- 519B- MID	1	AG	125mL	HCI		-	SM5310 TOC	APP		
REMARKS:	Per SOP,	parameter	s stable for	three readings p	prior to sample collect	ion. Tub	ing-in-Screen Interv	val purge met	hod utilized.	

REMARKS: Per SOP, parameters stable for three readings prior to sample collection. Tubing–in-Screen Interval purge method utilized. Water level stabilized prior to collecting parameters. Purge water clear brown, sulfur-like odor.

MATERIAL CODES: AG = Amber Glass; CG = Clear Glass; PE = Polyethylene; PP = Polypropylene; S = Silicone; T = Teflon; O = Other (Specify)

SAMPLING EQUIPMENT CODES:

APP = After Peristaltic Pump; B = Bailer; BP = Bladder Pump; ESP = Electric Submersible Pump; SM = Straw Method (Tubing Gravity Drain); O = Other (Specify)

SITE NAME: LCP Chemical Site						SITE LOCATION: Brunswick, GA							
WELL NO: SW-1				SAMPLE	SAMPLE ID: <b>SW-1</b>				DATE: <b>2/5/2013</b>				
					PUR	GING DA	TA	<u>'</u>					
	R (inches): 4	IRGE: 1 EQUI	ER (inches): <b>1/4 PMENT VOL.</b> = ( 0.0026 gallon	(TUBING (		<b>43 to 48</b> X TUB	ING LENGTH) -	ER (ft btoc): 9.5	2 OR	RGE PUMP TYPE BAILER: <b>PP</b>			
_	INITIAL PUMP OR TUBING DEPTH IN WELL (feet btoc ): 45.5  DEPTH IN W				-		PURGING PURGIN INITIATED AT: 0731 ENDED		0840		TOTAL VOLUME PURGED (gallons): 1.5		
TIME	VOLUME PURGED (gallons)	CUMUL. VOLUME PURGED (gallons)	PURGE RATE (gpm)	DEPTH TO WATER (feet btoc)	pH (standard units)	TEMP.	SP COND. (mS/cm)	DISSOLVED OXYGEN (% saturation)	TURBIDI (NTUs)	_	SP Gravity (sg)		
0758	0.5	0.5	0.02	9.58	6.71	16.42	28.45	20.1	5.36	-120.3			
0808	0.25	0.75	0.03	9.59	6.73	17.22	28.62	8.1	2.96	-150.5			
0817	0.25	1.0	0.03	9.60	6.72	17.74	28.48	6.1	2.36	-167.8			

**1**" = 0.04; **2**" = 0.16; WELL CAPACITY (Gallons Per Foot): 0.75" = 0.02; **1.25**" = 0.06; **4**" = 0.65; **6**" = 1.47; **3**" = 0.37; **12**" = 5.88 **5**" = 1.02; TUBING INSIDE DIA. CAPACITY (Gal./Ft.): 1/8" = 0.0006; 3/16" = 0.0014; 1/4" = 0.0026; **5/16"** = 0.004; **1/2"** = 0.010; **3/8"** = 0.006; **5/8"** = 0.016 BTOC = Below top of casing - feet below top of casing which includes above grade riser PP = Peristaltic Pump;

6.72

6.72

**PURGING EQUIPMENT CODES: B** = Bailer; **BP** = Bladder Pump; **ESP** = Electric Submersible Pump;

0.03

0.03

9.60

9.60

1.25

1.5

0827

0836

0.25

0.25

#### **SAMPLING DATA**

18.14

18.15

28.35

28.35

5.1

4.4

4.02

1.40

-180.6

-185.8

O = Other (Specify)

1.015

SAMPLED B	V (DRINT) / A	FEILIATION:		SAMPLER(S) SIGN	MATURE(S):	`				
SAMPLED BY (PRINT) / AFFILIATION: Christine Jaynes/Parsons				BB 0 3 2	pros		SAMPLING INITIATED AT: <b>0851</b>	SAMPLIN ENDED A	NG AT: <b>0922</b>	
PUMP OR TU DEPTH IN W	UBING /ELL (feet): 4	5.5		TUBING MATERIAL CODE:	Teflon-lined PE		FILTERED: Yes/ <b>SM 4500 Sulfide</b> FILTER SIZE: <u>0.45                                    </u>			
FIELD DECC	ONTAMINATIO	ON: PU	MP Y	<b>No</b> T	UBING Y <b>No (rep</b>	laced)	DUPLICATE:	No		
SAMPL	E CONTAINE	R SPECIFIC	ATION	SAM	IPLE PRESERVATION		INTENDED	SAMPLING	Additional Comments	
SAMPLE ID CODE (	# CONTAINERS	MATERIAL CODE	VOLUME	PRESERVATIVE USED	TOTAL VOL ADDED IN FIELD (mL)	FINAL pH	ANALYSIS AND/OR METHOD	EQUIPMENT CODE		
SW-1	1	PE	250mL	HNO3			6010B TAL Metals/7470A Hg	APP		
SW-1	1	PE	125mL				3500 FE/ 9040B pH	APP		
SW-1	1	PE	250mL			-	6010B Dissolved Silica	APP		
SW-1	1	PE	125mL			-	9056A_28D Chloride & Sulfate	APP		
SW-1	1	AG	125mL				SM 5310 DOC	APP		
SW-1	2	PE	250mL	NaOH Zinc Acetate			SM4500 Sulfide	APP	Field-Filtered	
SW-1	1	PE	500mL				2540C TDS	APP		
SW-1	1	PE	250mL				2320B Alkalinity	APP		
SW-1	1	AG	125mL	HCI			SM5310 TOC	APP		
					pefore sampling. Tub continued, odor note		creen-Interval purge	e method utiliz	ed. Purge	
MATERIAL C	CODES:	AG = Ambe	r Glass; CG	= Clear Glass; PI	E = Polyethylene; PP =	- Polypropyle	ene; <b>S</b> = Silicone; <b>T</b>	= Teflon; <b>O</b> = 0	Other (Specify)	
SAMPLING E	EQUIPMENT	CODES:	APP = After P	eristaltic Pump;	<b>B</b> = Bailer; <b>BP</b> = Blad	der Pump;	ESP = Electric Subme	ersible Pump;		

NOTES: Stabilization Criteria for Range of Variation of Last Three Consecutive Readings: pH: ± 0.1 unit Specific Conductance: ± 5% Dissolved Oxygen: all readings ≤ 10% saturation; optionally, ± 0.2 mg/L Turbidity: all readings ≤ 10 NTU; or ± 10%

RFPP = Reverse Flow Peristaltic Pump; SM = Straw Method (Tubing Gravity Drain); O = Other (Specify)